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Role of Oxygen Vacancy Defects in the Electrocatalytic Activity of Substoichiometric Molybdenum Oxide

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Abstract

Mesoporous $\alpha$-MoO$_{3-x}$ combined with poly (diallyldimethylammonium chloride)-functionalized reduced graphene oxide (PDDA-rGO) are introduced as an inexpensive and efficient oxygen reduction reaction (ORR) catalyst. The mesoporous catalysts are wrapped by conductive rGO sheets via an electrostatic interaction induced by PDDA polyelectrolyte. Thermal interaction of PDDA with MoO$_3$ efficiently reduces the metal oxide to MoO$_{3-x}$ at 400-600°C creating surface oxygen vacancy. Through a combination of density functional theory (DFT) and experiments, the role of the surface oxygen vacancy sites in the ORR activity of MoO$_{3-x}$ is identified. For the first time, all the energy barriers opposing ORR are calculated at each step for MoO$_3$ with no oxygen vacancies and MoO$_{3-x}$ with surface oxygen vacancies. It is shown that presence of a $\text{Mo}^{4+}$-$\text{O}_\text{v}$ oxygen vacancy site on the surface significantly reduces the energy barriers against ORR in the reaction pathways. An overpotential of 0.86 V (vs. RHE) with excellent
electrochemical stability was obtained with the newly designed catalyst, with only a 9% decrease in activity after ~17 hours. These results offer a new paradigm in defect engineering of metal oxides with a potential for the synthesis of stable and active noble metal-free ORR electrocatalysts.
Introduction

The oxygen reduction reaction (ORR) is central to the development of various electrochemical systems for energy conversion applications. Developing highly efficient catalysts for ORR is of particular significance in the fabrication of commercial fuel cell devices and metal–air batteries. One of the main challenges in the development of such devices with acceptable cost-effective and energy-efficient characteristics is to find an ideal electrocatalyst for oxygen reduction at the cathode. Nevertheless, electrocatalytic control of the reduction process for gas-phase oxygen is still limited due to slow ORR kinetics which, in turn, is caused by difficult absorption, bond activation, bond cleavage, and removal of oxygen at the solid-gas interface. The slow kinetics of ORR can be overcome through the use of precious noble metal-based catalysts, particularly Pt, which increases the cost significantly. Numerous studies have been conducted on Pt-free catalysts such as transition metal oxides, chalcogenides, nitrides, and oxynitrides. However, the catalytic activity and durability of the existing ‘beyond platinum’ ORR catalysts are not adequate to an extent that would allow them to replace Pt-based catalysts.

The unique properties of molybdenum-based oxides such as relatively high electrical conductivity and mechanical and thermal durability make them ideal candidates for development of efficient electrochemical energy storage systems. Among different Mo-based electrocatalysts, layered orthorhombic MoO$_3$ and conductive monoclinic MoO$_2$ are the most promising. The majority of previous studies on these materials have been carried out in the fields of Li-ion batteries, supercapacitors, and the hydrogen evolution reaction. However, the main objective of current work is to expand the unique features of Mo-based metal oxides to ORR applications. To the best of our knowledge, only one study has discussed the ORR activity of a MoO$_3$ which has been conducted on a non-layered hexagonal structure.

ORR is a reaction that mainly occurs on the surface of the catalyst due to limited oxygen diffusion into the bulk material. As a result, any effort for an improvement should be achievable by modification of the surface chemistry. Liang and Müllen et al. reported a collection of mesoporous metal-based ORR catalysts including cobalt/iron–nitrogen-doped carbon by employing vitamin B$_{12}$ and polyaniline–Fe complexes as precursors. The high ORR activity of the mesoporous catalysts was attributed to their high surface area, and uniform distribution of
metal and nitrogen active spots. A high surface area ensures the maximum oxygen accessibility to the catalyst. The electrical conductivity is another factor that plays a crucial role in the ORR activity of catalysts. Graphene supported metal-based catalysts are one of the most effective means to significantly improve the mechanical and electrical properties as well as surface area\textsuperscript{7,10-12}. Recently, we reported that a thermochemical reaction between PDDA polyelectrolyte and MoO\textsubscript{3} can induce large quantities of oxygen vacancy sites in the metal oxide\textsuperscript{13}. It was observed that with a thermal annealing of α-MoO\textsubscript{3} at 600°C under Ar with no PDDA, only a small substoichiometry value of \(x \sim 0.03\) was obtained. In contrast, with the use of PDDA, \(x = 0.36\) and \(x = 0.98\) were obtained for the samples annealed at 600°C under Ar and H\textsubscript{2}-containing gas (5%H\textsubscript{2}/95%Ar), respectively. This emphasized the effectiveness of PDDA polyelectrolyte in creating high densities of oxygen vacancies in addition to inducing the electrostatic charges useful for wrapping of the active material with conductive supports such as rGO.

Here, reduced graphene oxide (rGO) was used as the conductive support and current collector for the mesoporous catalysts. To have the maximum effectiveness, the samples in our work were made mesoporous with surface areas greater than 50 m\textsuperscript{2}g\textsuperscript{-1}. We combine mesoporous MoO\textsubscript{3} with rGO into a single composite without spoiling the porous mesostructure. Poly(diallyldimethylammonium chloride) (PDDA) was used to create a strong interaction between the rGO support and mesoporous catalysts, as it induces positive charges on rGO\textsuperscript{12} causing a strong electrostatic attraction towards mesoporous MoO\textsubscript{3} samples with negative charges. Additionally, a comprehensive computational study was also performed to fully understand the effects of surface oxygen vacancy sites on the ORR activity of MoO\textsubscript{3-x}. The results of our DFT calculations supported by experimental observations indicated that the presence of a Mo\textsuperscript{4+}-v\textsubscript{O} oxygen vacancy site can greatly facilitate the reactions by lowering the corresponding energy barriers.

**Experimental section**

**Chemicals.** All chemicals were used as received. Pluronic P123 triblock poly(ethylene oxide)-b-poly(propylene oxide)-b-poly(ethylene oxide) copolymer (\(M_w = 5800, \text{EO}_{20}\text{PO}_{70}\text{EO}_{20}\)), 1-butanol (anhydrous, 99.8%), tetraethyl orthosilicate (TEOS), hydrochloric acid (HCl, 37% aqueous), ethyl alcohol (CH\textsubscript{3}CH\textsubscript{2}OH), phosphomolybdic acid (PMA, H\textsubscript{3}P\textsubscript{2}Mo\textsubscript{12}O\textsubscript{40-}\text{xH}\textsubscript{2}O),
poly(diallyldimethylammonium chloride) (PDDA), potassium permanganate (KMnO₄), hydrogen peroxide (H₂O₂, 30%), graphite flakes, and sodium nitrate (NaNO₃) were purchased from Sigma-Aldrich Co. LLC.

**Synthesis of mesoporous MoO₃ electrocatalysts.** In accordance with established procedures¹⁴,¹⁵, mesoporous silica SBA-15 and KIT-6 hard templates were prepared over the period of 24 hours under hydrothermal conditions at a temperature of 100°C. A solvent evaporation induced impregnation process¹⁶,¹⁷ was used to incorporate the PMA precursor into the channels of mesoporous silica similar to the common practice in nanocasting processes. 4.4 g of PMA powder were dispersed in 25 g of ethanol followed by the addition of 1 g of SBA-15 template to the solution. The mixture was then stirred intensively at room temperature (20–30°C) for 3 h, before transferring it to a petri dish to be dried at 60°C for 12 h until all of the ethanol evaporated. The obtained PMA/mesoporous silica powder (denoted as PMA@SBA-15) was then transferred into a crucible, heated to 550°C at the rate of 1°C/min, and kept in those conditions for 4 h, producing a MoO₃/mesoporous silica powder (denoted as MoO₃@SBA-15). The silica SBA-15 template in the MoO₃@SBA-15 composite was removed by etching in hydrofluoric acid (4%, aqueous solution). While it may be possible that a small quantity of molybdenum oxide is dissolved in HF, our observation was that MoO₃ was stable in 4% HF aqueous solutions for a period of more than 6 hours. A similar procedure was used to prepare ordered mesoporous MoO₃@KIT-6 samples, except that the SBA-15 template was replaced with an equal amount of KIT-6. The resultant silica template-free powders of MoO₃ nanocast from KIT-6 and SBA-15 are denoted as MoO₃–KIT-6 and MoO₃–SBA-15, respectively.

**Synthesis of graphene-wrapped MoO₃–SBA-15.** A modified Hummers’ method¹⁸,¹⁹ with a lower concentration of oxidizing agent was used to synthesize graphene oxide. The rGO/MoO₃–SBA-15 composite (denoted rGMS) was obtained via an electrostatic interaction between poly(diallyldimethylammonium chloride) (PDDA)-modified graphene oxide and metal oxides in aqueous solutions. In accordance with the procedure described by Chang et al.²⁰, 0.1 mL of a 20 wt% PDDA solution was first mixed into 40 mL of graphene oxide solution with concentration of 0.5 mL/mg and the mixture was sonicated for 1 h until a transparent solution was obtained. After diluting the solution to 100 mL, 200 mg of mesoporous MoO₃–SBA-15 was sonicated into 100 mL of ethanol. Then, the mesoporous MoO₃–SBA-15 solution (negatively charged) was
mixed with 100 mL of graphene oxide solution (positively charged) and stirred for 12 h. After filtering and drying, the as-prepared GO/MoO$_3$–SBA-15 composite was thermally reduced at 400°C and 600°C with a rate of 1 °C/min and kept for 2 h at these temperatures in an Ar. Finally, the black-colored products of the reduced samples were obtained. Because MoO$_3$ is partially reduced during the annealing process, the abbreviation MoO$_{3-x}$ is used to refer to the mixed-phase composites. The products rGO/MoO$_{3-x}$–SBA15-400°C and rGO/MoO$_{3-x}$–SBA15-600°C are subsequently denoted as rGMS-400 and rGMS-600.

**Characterization.** Powder X-ray diffraction (XRD) analysis was performed on a Rigaku Ultima IV diffractometer with Cu Kα radiation ($\lambda = 1.5406$ Å), with an operating current of 44 mA and voltage of 40 kV, and a Bruker D2 Phaser with Cu Kα radiation ($\lambda = 1.54184$ Å) with an operating voltage and current of 30 kV and 10 mA at room temperature. Nitrogen adsorption-desorption isotherms were obtained at -196°C on a Micrometrics ASAP 2010 instrument. Samples were first degassed at 150°C in a vacuum for 6 h. The specific surface areas were derived from adsorption data by the Brunauer–Emmett–Teller (BET) method. The pore-size distributions of the samples were retrieved from the adsorption curves of isotherms by using the Barrett–Joyner–Halenda (BJH) method. The total pore volumes were calculated using the adsorbed volumes at a pressure of $P/P_0 = 0.99$. Transmission electron microscopy (TEM) analysis was conducted using a FEI Talos F200X TEM/STEM and JEOL 2010 FasTEM both at an accelerating voltage of 200 kV, and chemical analysis was collected using energy dispersive X-ray spectroscopy (EDS). The TEM samples were sonicated in ethanol and collected using thin carbon films covered copper grids. Morphologies of the samples were investigated using field emission scanning electron microscopy (SEM) on a FEI Nova Nano SEM 450 with accelerating voltage of 2.0 kV.

**Electrochemical measurements.** The electrochemical measurements were carried out at room temperature in a three-electrode glass cell connected to a CH Instruments 760E electrochemistry workstation. A graphite rod was used as the counter electrode and a saturated calomel electrode (SCE) was used as the reference electrode. The potential was calibrated with respect to a reversible hydrogen electrode (RHE) by experimental measurements using two Pt electrodes and working and counter electrodes in a hydrogen-saturated solution. To prepare the working electrode, 4 mg catalyst, 1 mg carbon black, 200 uL ethanol, 800 uL DI-water and 50 uL nafion
solutions were mixed and ultrasonicated for at least 1 h to form a homogeneous catalyst ink. 
Afterward, 10 µL of this ink was drop-cast onto the 5 mm-diameter glassy carbon rotating disk 
electrode (RDE, Pine Instruments) and dried under an infrared lamp for 30 min, yielding a 
catalyst loading of ~0.255 mg/cm². Before the test measurements, O₂ was bubbled through the 
electrolyte solution to supply enough O₂ reactant. Cyclic voltammetry was firstly conducted for 
tens of scans with a scan rate of 50 mV/s to reach a stable state, and linear sweep voltammetry 
(polarization curve) with a scan rate of 5 mV/s was measured in 0.1 M KOH electrolyte. AC 
impedance measurements were carried out in the same configuration at the potential of 1.71 
versus RHE from 0.1–10⁵ Hz with an AC voltage of 5 mV.

**Density functional theory calculations.** The density functional theory (DFT) calculations were 
performed using Vienna Ab initio Simulation Package²¹, by employing a basis set of plane 
waves with kinetic energies up to 500 eV. For all calculations, the Perdew-Burke-Ernzerhof 
functional²² was adopted for exchange-correlation energies. Equilibrium structures were assumed 
when the atomic forces calculated during the optimization fall below 0.01 eV/Å. Following ref. 
23, Dudarev’s approach²⁴ was employed to describe the d and f electrons of Mo, using U = 6.0 
eV for the onsite Coulomb term. The dispersion van der Waals interaction was calculated using 
the optB88-vdW functional. For the polaron (Mo⁴⁺), we followed the procedure introduced in 
ref. 25 by intentionally localizing/delocalizing the electron density at the particular Mo sites of 
interest. For MoO₃ slabs, we appended a vacuum layer of 10 Å thickness to the bulk models, 
uncovering the O₁ atoms on the (010) surface, and suppressing the interaction along the y 
direction. Because of its layered structure, this is the most stable surface of MoO₃. Reaction with 
PDDA was assumed to occur on this surface.

**Results and Discussion**

**Chemical and structural analyses.** Possessing a high surface area can guarantee the access of 
oxygen to the catalyst while also favoring formation of more vacancy sites on the surface. 
Mesoporous molybdenum oxide-graphene composites were synthesized using the method 
described in the experimental section. In the first step, mesoporous MoO₃ was synthesized via a 
nanocasting technique where SBA-15 and KIT-6 mesoporous silica were used to template 
cylindrical and gyroidal structures, respectively. After synthesis of mesoporous SBA-15 and
KIT-6, phosphomolybdic acid (PMA, H$_3$PMo$_{12}$O$_{40}$) was used as the molybdenum precursor, and was impregnated inside the porous structure of mesoporous silica templates. The choice of precursor in this technique is of the utmost importance; PMA provides required hydrogen-bond interactions with silica templates and it has both a high molybdenum content and high solubility in ethanol, which was used as the solvent. After solvent evaporation, composites of PMA@SBA-15 and PMA@KIT-6 were calcined at 550°C to decompose the PMA into crystalline MoO$_3$ inside the channels of SBA-15 or KIT-6 templates. The silica templates were removed by etching in a 4% hydrogen fluoride (HF) aqueous solution. Figure 1 shows the low-angle X-ray diffraction (XRD) patterns the SBA-15 and KIT-6 derived mesoporous molybdenum oxide samples. For the SBA-15-based samples (Figure 1a), four distinct peaks are observed which can be assigned to the (100), (110), (200), and (210) Bragg reflections of the P6mm hexagonal structure as per ref. 9. The low-angle XRD of KIT-6 (Figure 1b) shows peaks attributed to the (211), (220), and (321) Bragg reflections of the bicontinuous cubic gyroidal Ia3d structure (Figure 1b), indicating highly ordered mesostructures as per ref. 26. The low-angle XRD patterns of the mesoporous MoO$_3$@KIT-6 and MoO$_3$@SBA-15 prepared at 550°C show one intense peak at $2\theta = 1.0^\circ$, corresponding to the poorly resolved (211) and (100) diffraction peaks of SBA-15 and KIT-6, respectively. After removing the template by HF, three well-resolved diffraction peaks were observed from the low-angle XRD pattern of MoO$_3$–SBA-15, which can be indexed to (100), (110), and (200) diffraction planes of a highly ordered 2D hexagonal structure. This, in turn, indicated that the MoO$_3$ crystal nanoarrays replicated the ordered mesostructure of their host silica template. In comparison, after removal of silica with HF, the MoO$_3$–KIT-6 sample only exhibited one intense peak at $2\theta = 0.9^\circ$ [assigned to (211)], indicating lower structural regularity (see Figure 1b). Further details on the low-angle diffraction patterns of the samples is discussed in the supporting information. As shown in Figure 2, peaks in the high-angle XRD patterns of the mesoporous sample after removing SBA-15 and KIT-6, denoted as MoO$_3$–SBA15 and MoO$_3$–KIT–6 respectively, were assigned to orthorhombic MoO$_3$ (powder diffraction file #05-0508).

In order to boost the electrical conductivity of the electrode, the mesoporous samples were wrapped by graphene oxide sheets. PDDA polyelectrolyte was added during the synthesis to provide strong electrostatic interaction between the GO support and mesoporous catalysts. In
order to reduce GO to reduced graphene oxide (rGO), the samples were annealed at temperatures of 400 and 600°C under an argon atmosphere. Figure 2 illustrates the XRD patterns of the MoO$_3$–SBA15 sample compositied with both polymer and rGO and annealed at 400 and 600°C, denoted as rGMS-400 and rGMS-600 respectively. Unexpectedly, the XRD patterns indicated that the annealed samples were a mixed phase of partially reduced MoO$_3$ and a monoclinic phase of MoO$_2$ (powder diffraction file #73-1807).

Transmission electron microscopy (TEM) analysis revealed that samples preserve the regularity of the template mesostructures (Figure 3). We observe the MoO$_3$ products have a highly ordered mesostructure throughout the whole domain consisting of hexagonally aligned nanowires and gyroid-porous structures for MoO$_3$–SBA-15 and MoO$_3$–KIT-6, respectively, reflecting true replication of the hard templates and a high yield of MoO$_3$ incorporation into the template channels. N$_2$ adsorption–desorption isotherms was obtained to examine the textural properties of the catalysts. The prominent hysteresis loops indicate the mesoporous nature of MoO$_3$–SBA-15 and MoO$_3$–KIT-6 samples (Figure 3d,e). The Brunauer–Emmett–Teller (BET) surface areas of these catalysts were 50 m$^2$/g for MoO$_3$–SBA-15 and 63 m$^2$/g for MoO$_3$–KIT-6, all of which were much lower than that for the SBA-15 (529 m$^2$/g) and KIT-6 (851 m$^2$/g) templates (see Figure S1 and Table S1, supporting information). The Barrett–Joyner–Halenda (BJH) pore size distributions of MoO$_3$–SBA-15 and MoO$_3$–KIT-6 catalysts were centered at 7.2 nm. In the case of MoO$_3$–SBA-15, the peak at 7.2 nm agrees with that of the original SBA-15 (5.4 nm) and is evidence of well controlled template replication.

Additionally, TEM analysis of rGMS-400 shown in Figure 3c confirmed that thin layers of graphene were attached to the MoO$_3$-x likely as a result of electrostatic interaction. This encapsulation of the mesoporous structure can significantly facilitate the transport of electrons through the highly conductive graphene-based scaffold. Moreover, the conventional (0002) peak expected for graphite at 2$\theta$ = 26.68° was not resolved in XRD, which suggests a homogeneous dispersion of the graphene sheets over the surface of the MoO$_x$ samples$^{27}$. The porosity of the rGMS-400 and rGMS-600 composites was quantified using nitrogen adsorption–desorption isotherm measurements (Figure 3f and Table S1, supporting information). According to the BJH equation, the centered pore diameter in rGMS-400 was 7.4 nm, which confirms a relatively uniform pore size distribution. The BET specific surface areas of rGMS-400 and rGMS-600
were 122 and 53 m²/g, respectively. The higher specific surface area of rGMS-400 compared to MoO₃–SBA-15 (50 m²/g) is due to the porosity of the replicate MoO₃ and the secondary pores between the MoO₃ and the graphene sheets. The lower surface area of rGMS-600, on the other hand, results from a partial collapse of the mesoporous structure after high temperature reduction at 600°C. TEM and HAADF-STEM images of rGMS-600 (Figure 4) and rGMS-400 (Figure S2, supporting information) catalysts confirm the attachment of mesoporous particles to the rGO. TEM also reveals partial collapse of the porous structures indicated by BET data.

Raman spectra of mesoporous MoO₃–SBA-15 powders and rGMS-400 and rGMS-600 composites is shown in Figure 5. Similar to MoO₃–SBA-15, Raman spectrum of the rGMS-400 composite displayed characteristic orthorhombic MoO₃ vibrational frequencies whereas rGMS-600 peaks are ascribed to Raman bands of monoclinic MoO₂ consistent with the XRD analysis. In the MoO₃ spectra, various bending modes were found responsible for the peaks below 400 cm⁻¹, while the three peaks at 663, 820, and 993 cm⁻¹ were traced to the various stretching frequencies of molybdenum and oxygen. Raman bands detected at 743, 571, 493, 364, 345 and 229 cm⁻¹ in the rGMS-600 sample are the evidence of reduction of MoO₃ to MoO₂. The Raman spectra of the rGMS-400 and rGMS-600 composites in the range of 1200 to 3000 cm⁻¹ exhibit the characteristic peaks of rGO. The D and G graphitic bands observed at 1360 and 1594 cm⁻¹ for rGMS-400, respectively, and at 1359 and 1583 cm⁻¹ for rGMS-600, respectively, confirm the existence of defects in the sp²-bonded carbon in the composite. The removal of oxygen-containing groups in rGMS-400 and rGMS-600 was monitored by Raman spectroscopy in the range of 1200 to 3000 cm⁻¹. The major oxygen functional groups in GO include epoxide (–O–) and hydroxyl (–OH) groups, which are located on the basal plane of GO, while minor functional groups include carbonyl (–C=O) and carboxyl (–COOH) groups located at the edges. GO by itself is known to be electrically insulating due to presence these oxygen groups. Thermal or chemical reduction can remove these groups and restore the electrical properties depending on the degree of reduction, layer disorder, and structural defects. The appearance of the defect-induced D-band in the Raman spectra of rGMS-400 at 1360 cm⁻¹ as well as a rather broad G-band at 1594 cm⁻¹ and unresolved second-order 2D peak (expected ~2700 cm⁻¹) indicated that a high degree of oxidation and disorder was still present in rGMS-400 even though it had been reduced at 400°C (Figure 5b). For rGMS-600, the D-peak shifted to 1359 cm⁻¹ and a narrower G-peak at 1583 cm⁻¹ was observed. The \( \frac{I_D}{I_G} \) ratio decreased from 0.86 for rGMS-400 to 0.19 for
rGMS-600 which indicated that reduction was improved as the annealing temperature was elevated to 600°C. Further reduction of oxygen functional groups in GO by raising the thermal reduction temperature from 400 to 600°C was verified by the high-resolution C 1s spectra acquired from X-ray photoelectron spectroscopy (XPS, shown in Figure 6a). The C 1s spectra of the GMS-400 and GMS-600 composites were deconvolved into four peaks corresponding to carbon atoms with different oxygen-containing functional groups: (1) non-oxygenated C sp² and sp³ at 284.6 and 285.8 eV, respectively, (2) carbon in C–O at 287.4 eV, (3) carbonyl carbon (C=O) at 287.9 eV, and (4) carboxylate carbon (O–C=O) at 289.0 eV. Increasing the intensity of the sp² carbon peak relative to the peaks of sp³ carbon and carbon binding to oxygen indicates a higher degree of reduction by increasing the annealing temperature.

Presence of oxygen vacancy sites (XPS analysis). The presence of oxygen vacancies in the samples was confirmed by XPS analysis (Figure 6b). For the MoO₃–SBA-15 sample, only peaks assigned to Mo⁶⁺ 3d₃/₂ and Mo⁶⁺ 3d₅/₂ at 236.34 and 233.20 eV were detected, respectively. This showed that there were no detectable near-surface oxygen vacancies in MoO₃–SBA-15 and this sample could be regarded as a stoichiometric reference. For rGMS-400 (sampled annealed at 400°C), peaks assigned to Mo⁵⁺ 3d₃/₂ (234.84 eV) and Mo⁵⁺ 3d₅/₂ (231.50 eV) valance states were detected which was an indication of the presence of vₒ⁻ vacancy sites (vₒ⁻ refers to an oxygen vacancy with a single positive charge according to Kröger-Vink notation). Peaks centered at 232.99 and 229.13 eV were attributed to Mo⁴⁺ 3d₃/₂ and Mo⁴⁺ 3d₅/₂ showing vₒ⁻ oxygen vacancy sites being present with two positive charges. For rGMS-600 (sampled annealed at 600°C), the majority of oxygen vacancy sites were vₒ⁻.

Role of defects in the electrocatalytic reduction of oxygen. The ORR electrocatalytic activity of mesoporous MoO₃–SBA-15, rGMS-400, and rGMS-600 composites were characterized by linear sweep voltammetric (LSV) measurements in 0.1 M KOH and are shown in Figure 7. The activity for MoO₃–KIT-6 is shown in Figure S3, supporting information. The ORR onset potentials of mesoporous MoO₃–SBA-15 and MoO₃–KIT-6 were 0.78 and 0.79 V versus reversible hydrogen electrode (RHE). The improved performance of MoO₃–KIT-6 compared to MoO₃–SBA-15 is assigned to the higher surface area and abundance of three-dimensional channels in the gyroidal structure improving oxygen diffusion on the catalyst surface. Compared with MoO₃–SBA-15,
the rGMS-400 and rGMS-600 electrodes showed an even greater positive shift in the onset potential, 0.82 and 0.86 V (vs. RHE), respectively, with a more notable increase in the current density as shown in Figure 7a. The improved ORR activity of rGMS-400 and rGMS-600 can be explained by following factors. PDDA can functionalize GO through the reduction process and a possible synergetic effect between rGO, PDDA, and catalyst plays an important role in high ORR activity of rGMS-400 and rGMS-600. This happens through the physical adsorption of polyelectrolyte chains that contain positively charged nitrogen moieties on rGO where intermolecular charges created a net positive charge on the carbon atoms. This can change the electronic properties of rGO causing the electrons to be attracted more from the anode to the cathode and facilitating oxygen desorption as well as the ORR process. The integration of MoO$_3$–SBA-15 with PDDA-rGO helps overcome the slow electron conduction in MoO$_3$–SBA-15 and the interface between them plays a key role in increasing the overall catalytic performance.

Moreover, although the surface area of rGMS-600 (53 m$^2$/g) was lower than that of rGMS-400 (122 m$^2$/g), its onset potential (vs. RHE) was 40 mV higher than rGMS-400 at the same mass loading. This higher ORR activity, in spite of having lower surface area, can be attributed to the higher degree of oxygen vacancies on the surface of the active material in the rGMS-600 catalyst due to reduction of orthorhombic MoO$_3$ to monoclinic MoO$_2$ by increasing the reduction temperature from 400 to 600 °C accompanied by a higher degree of reduction of GO as confirmed by XPS and Raman spectroscopy.

Electrochemical impedance spectroscopy (EIS) of the catalysts showed smaller diameter of the Nyquist plot curves for rGMS-400, and rGMS-600 compared to MoO$_3$–SBA-15 (Figure 7b). This is an indication of lower electrical resistance of rGMS-400, and rGMS-600 due to wrapping with more electrically conductive rGO sheets in these samples. The smaller diameter of the rGMS-600 curve compared to rGMS-400 is due to a combination of the higher oxygen vacancy concentration and a higher degree of reduction of rGO as well as the reduction of the bulk of rGMS-600 from orthorhombic $\alpha$-MoO$_3$ to nearly monoclinic MoO$_2$. Although outside the scope of the current work, the effects of oxygen vacancy concentrations on conductivity can be studied by a set of controlled experiments where the oxygen vacancy concentration is kept as the only
variable in the investigation, most appropriate for single crystalline samples so that the intrinsic contribution of oxygen vacancies to the conductivity can be determined.

Because of its strong orbital overlap\textsuperscript{41}, MoO\textsubscript{2} has a relatively low, metallic electrical resistivity (8.8×10\textsuperscript{-5} Ω-cm)\textsuperscript{16} which can significantly facilitate the electron transfer through the core of catalyst. Accordingly, a comparison between the RDE polarization curves of MoO\textsubscript{3}–SBA-15 and rGMS-600 indicates improved the ORR kinetic of rGMS-600 due to this promoted electron conduction the catalyst (Figure 7c,d). The integration of MoO\textsubscript{3} with PDDA-rGO also helps overcome the slow electron conduction in MoO\textsubscript{3}–SBA-15. Additionally, in order to reveal the role of the oxygen vacancies on the ORR activity, the LSV of MoO\textsubscript{3}–SBA-15 with a sub-stoichiometry degree of \( x = 0.024 \) was compared with that of as-purchased MoO\textsubscript{3} (Alfa Aesar No. 12930) as a reference sample (denoted as Ref. Alfa Aesar No. 12930) with a slightly higher sub-stoichiometry degree of \( x = 0.035 \)\textsuperscript{13} (Figure S4, supporting information). The results indicated that the Ref. Alfa Aesar No. 12930 sample was more active than the closer-to-stoichiometric MoO\textsubscript{3}–SBA-15 sample by a potential difference of 200 mV (vs. RHE). This was despite the fact that MoO\textsubscript{3}–SBA-15 was a mesoporous sample with a high surface area.

In order to model the ORR catalyzed by MoO\textsubscript{3–x}, the following reaction pathways employed for alkaline solutions:\textsuperscript{42}

\[
M^{m+} + O_2^- + H_2O + e^- \rightarrow M^{(m-1)+} - OH^- + OH^- \quad (1)
\]

\[
O_2 + e^- \rightarrow O_{2,ads}^- \quad (2)
\]

\[
M^{(m-1)+} - OH^- + O_{2,ads}^- \rightarrow M^{m+} - O - O^- + OH^- \quad (3)
\]

\[
M^{m+} - O - O^- + H_2O + e^- \rightarrow M^{(m-1)+} - O - OH^- + OH^- \quad (4)
\]

\[
M^{(m-1)+} - O - OH^- + e^- \rightarrow M^{m+} - O_2^- + OH^- \quad (5)
\]

where M represents the transition metal Mo, \( m \) denotes the oxidation state, and the subscript “ads” stands for adsorption. In order to identify the ORR active site, DFT calculations based on the above reaction pathways were performed. According to Kim and Dunn et al.\textsuperscript{43}, Mo\textsuperscript{5+} bipolarons and Mo\textsuperscript{4+} polarons at oxygen terminal sites (\( O_t \)) are the most favorable defect
configurations with formation enthalpies of 1.32 and 1.51 eV, respectively. The barrier energies against reactions (1), (3), (4), and (5) were calculated by DFT for MoO$_3$ without oxygen vacancies, and for MoO$_{3-x}$ with a Mo$^{4+}$-v$_O$ surface oxygen vacancy site (Figure 8, Table 1). For reaction (1), barrier energies of 1.54 and 3 eV were significantly reduced to -0.47 and -0.55 eV, respectively, by the presence of the adjacent Mo$^{4+}$-v$_O$ oxygen vacancy site (Figure 8a,b and Table 1). For reaction (3), a similar trend is observed by reducing the energy barriers of 0.471 and 2.053 eV to -1.689 and -1.692 eV, respectively (Figure 8c,d and Table 1). For Reaction (4), the formation of Mo$^{5+}$—O—OH is greatly facilitated by the presence of the surface oxygen vacancy site as the barrier was reduced from 2.158 to -1.410 eV (Figure 8e,f, and Table 1). For Reaction (5), however, the energy barrier against the release of OH$^-$ was slightly increased from 0.739 to 0.968 eV by the presence of the Mo$^{4+}$-v$_O$ vacancy (Figure 8g,h, and Table 1). All the calculated energies were based on the reference states identified in Figure 8. These results agreed with the experimental observations as the rGMS-600 catalyst with the highest degree of metal oxide reduction exhibited the highest ORR activity.

Since durability is a major concern of today’s fuel cell industry, the stability of MoO$_3$–SBA-15 and Pt/C catalysts during ORR were assessed through chronoamperometric measurements at -0.5 V. As shown in Figure S5, supporting information, a relative current of 91% still persisted after 16.7 h on the MoO$_3$–SBA-15 catalyst. In contrast, Pt/C showed a gradual decrease to 60.0% relative current after only 5.6 h. These results indicate the superior stability of the mesoporous MoO$_3$–SBA-15 catalyst compared to the Pt/C catalyst in an alkaline solution popular in the development of alkaline fuel cells. On the one hand, Pt-based catalysts gradually degrade over time (especially in alkaline electrolytes) because of surface oxidation, particle dissolution, and particle aggregation. On the other hand, existing ORR catalysts that show improved stability over Pt (such as Ag) still lack the needed activity and are not durable enough for practical purposes$^{9,44-46}$. The excellent stability and durability of the mesoporous molybdenum oxide even in the absence of rGO protection makes it a promising candidate as a catalyst for ORR.

Conclusion

Reduced graphene oxide-wrapped mesoporous molybdenum oxides were synthesized via a two-step procedure, utilizing nanocasting and a self-assembly/thermal reduction approach, then used
as an electrocatalyst in ORR. The obtained products replicated the mesostructure of both KIT-6 and SBA-15 silica templates and exhibited large surfaces areas (up to 80 m$^2$/g), and narrow pore size distributions (~3 nm full width at half maximum). The obtained mesoporous MoO$_3$ material exhibited improved ORR activity, which was associated with the well-defined mesoporous structure. Experimental results indicated that using PDDA for wrapping mesoporous $\alpha$-MoO$_{3-x}$ with rGO followed with thermal annealing created catalyst surfaces with qualitatively high degree of vacancy densities. Theoretical results have demonstrated that these surface vacancy sites are crucial in the electrochemical activity of catalysts by being the origin of ORR activity in $\alpha$-MoO$_{3-x}$ based materials for the first time. Finally, we emphasize that the synthesis approach presented here can be readily extended to the preparation of other mesoporous metal oxide–graphene composite materials, with broad applications in various critical energy conversion areas.$^{46}$ The calculated results indicated that the energy barriers against ORR were significantly reduced by the presence of Mo$^{4+}$-$\nu$O oxygen vacancy for reactions (1), (3) and (4). The barrier opposing the release of OH$^-$, given by reaction (5), slightly increased due to the presence of the surface O$\nu$ vacancy.

The obtained experimental and computational results demonstrate a pathway for improvement of ORR activity using MoO$_{3-x}$-based materials, which are known for high thermal stability$^{13}$ and electrical conductivity (such as MoO$_2$)$^{6}$. Future breakthroughs in improving the ORR activity of these materials will be highly impactful due to the rich electrochemical applications enabled by Mo-based metal oxides. For instance, $\alpha$-MoO$_3$ is a layered material providing a better access to the crystallographic planes where the reaction occurs. In addition, MoO$_3$ can be a corrosion-resistant metal oxide, as we have observed stability of the materials even in a strong acid solution such as HF for long periods of several hours. Such properties can have potential applications in chemically-harsh fuel cell environments. Moreover, the synthesis method used in this work for wrapping mesoporous molybdenum oxide with rGO through electrostatic interactions can be used for improving the electrical conductivity of other mesoporous materials when used in composite electrodes. As this study is a first step emphasizing the need for further investigations and advancements on the ORR activity of MoO$_3$ materials, we hope it will inspire future investigations and performance improvements, especially in the computational realm where understanding of descriptors needed for materials design is in a very early stage.
Acknowledgements

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Supporting Information Available: Additional details and discussion of x-ray diffraction (XRD) and specific surface area including table of structural data, transmission electron microscopy (TEM) images and specific surface area analysis of SBA-15 and KIT-6 hard templates, scanning transmission electron microscopy (STEM) analysis of sample rGMS-400, linear sweep voltammetric (LSV) measurements of mesoporous MoO$_3$–SBA-15 and MoO$_3$–KIT-6 catalysts, XRD and LSV measurements of MoO$_3$–SBA-15 and commercially obtained MoO$_3$ (sample Ref. Alfa Aesar No. 12930), and chronamperometric response at a potential of -0.5 V vs. SCE for mesoporous MoO$_3$–SBA-15 and Pt/C. This material is available free of charge via the Internet at http://pubs.acs.org.

References


Figures and Figure Captions

Figure 1. X-ray diffraction (XRD) analysis of the molybdenum oxide hard templating process. (a) Low-angle powder XRD of the mesoporous silica KIT-6 hard template, the mesostructured composite of phosphomolybdic acid (Mo precursor) impregnated into the SBA-15 mesochannels (PMA@SBA-15), the mesostructured MoO$_3$@SBA-15 composite prepared via high-temperature calcination of PMA@SBA-15 in air at 600°C, and the final product of mesoporous MoO$_3$ after removal of the SBA-15 hard template by hydrofluoric acid (MoO$_3$–SBA-15). (b) Low-angle powder XRD of KIT-6, PMA@KIT-6, MoO$_3$@KIT-6, and the mesoporous MoO$_3$–KIT-6 sample after removing the template.
Figure 2. High-angle powder XRD patterns of the mesoporous MoO$_3$–SBA-15 and MoO$_3$–KIT-6 samples. The patterns are assigned to an orthorhombic phase of MoO$_3$ (powder diffraction file #05-0508). High-angle powder XRD patterns of the composites with MoO$_3$–SBA-15, PDDA polyelectrolyte, and rGO annealed at 400 and 600°C under argon, denoted as rGMS-400 and rGMS-600 respectively. The patterns are assigned to the monoclinic phase of MoO$_2$ (powder diffraction file #73-1807).
Figure 3. Transmission electron microscopy (TEM) analysis of mesoporous MoO$_3$ and composite catalysts. TEM images of (a) MoO$_3$–SBA-15, (b) MoO$_3$–KIT-6, and (c) rGMS-400. (d–f) Corresponding N$_2$ adsorption isotherm curves for the three mesoporous MoO$_3$ catalysts shown in panels (a–c). Insets show the calculated Barrett–Joyner–Halenda pore size distributions.
Figure 4. Scanning transmission electron microscopy (STEM) confirms wrapping of MoO$_3$ x catalysts by rGO. (a) Bright field STEM and (b-e) scanning energy dispersive X-ray spectroscopy (EDS) and high angle annular dark field (HAADF) micrographs of rGMS-600.
Figure 5. (a) Raman spectra of rGMS-400 and rGMS-600 composites shown in comparison with that of mesoporous MoO$_3$-SBA-15. (b) Raman spectra of the rGO-related peaks of rGMS-400 and rGMS-600 samples.
Figure 6. (a) Deconvoluted XPS carbon 1s peak of MoO$_3$–SBA-15 and the rGMS-400 and rGMS-600 composites. (b) XPS analysis illustrating the presence of Mo$^{5+}$ and Mo$^{4+}$ valance states corresponding to $\nu_0^-$ and $\nu_0^{--}$ oxygen vacancy sites, respectively, in both samples rGMS-400 and rGMS-600°C. For MoO$_3$–SBA-15 only Mo$^{6+}$ peaks were detected indicating the sample being fully-oxidized.
Figure 7. Oxygen reduction activity is increased through a composite electrode with less defective rGO and more highly reduced MoO$_3$–, demonstrating the importance of PDDA and thermal treatment at 600°C. (a) Linear sweep voltammetry polarization curves obtained in O$_2$-saturated 0.1 M KOH and (b) Nyquist plots for MoO$_3$–SBA-15, rGMS-400, and rGMS-600 catalysts. Rotating-disk voltammograms of the catalysts: (c) MoO$_3$–SBA-15 and (d) rGMS-600 in O$_2$-saturated 0.1 M KOH with a sweep rate of 5 mV·s$^{-1}$. 
Figure 8. The effect of a surface oxygen vacancy site on the energy barriers for ORR. DFT calculated energy barriers for the oxygen reduction reaction (ORR) with a MoO$_3$ catalyst: (a,c,e,g) with no oxygen vacancy, and (b,d,f,h) with the presence of a Mo$^{4+}$-V$_O$ surface oxygen vacancy site. The performed calculations show that the energy barriers of ORR kinetics are significantly reduced due to the presence of the surface oxygen vacancy (a,b) based on reaction (1),
(c,d) based on reaction (3), and (e,f) based on reaction (4). (g,h) The presence of the oxygen vacancy site slightly increases the barrier energy against the reduction of \( \text{Mo}^{5+} - \text{O} - \text{OH}^- \) and release of \( \text{OH}^- \) according to reaction (5). In these calculations, the products and reactants are conserved, which is required to enable direct comparison between the different states.

Table 1. Proposed reaction pathways, and their DFT calculated energy barriers for oxygen reduction reaction activity of \( \text{MoO}_3 \), and \( \text{MoO}_3-x \) with a \( \text{Mo}^{4+} - \text{O}_t \) vacancy site on the surface.

<table>
<thead>
<tr>
<th>Reaction</th>
<th>Proposed reaction pathway to create</th>
<th>Energy barrier (eV) at each step</th>
<th>Proposed reaction pathway to create</th>
<th>Energy barrier (eV) at each step</th>
</tr>
</thead>
<tbody>
<tr>
<td>(1)</td>
<td>( \text{Mo}^{6+} - \text{O}^{2-} + \text{H}_2\text{O} + \text{e}^- \rightarrow \text{Mo}^{5+} - \text{OH}^- + \text{OH}^- )</td>
<td>1.54 eV 3 eV</td>
<td>( \text{Mo}^{4+} + \text{Mo}^{6+} - \text{O}^{2-} + \text{H}_2\text{O} + \text{e}^- \rightarrow 2[\text{Mo}^{5+} - \text{OH}^-] )</td>
<td>-0.47 eV -0.55 eV</td>
</tr>
<tr>
<td>(3)</td>
<td>( \text{Mo}^{5+} - \text{OH}^- + \text{O}_\text{ads}^- \rightarrow \text{Mo}^{6+} - \text{O} - \text{O}^{2-} + \text{OH}^- )</td>
<td>0.471 eV 2.053 eV</td>
<td>( \text{Mo}^{4+} + \text{Mo}^{5+} - \text{OH}^- + \text{O}_\text{ads}^- \rightarrow \text{Mo}^{5+} - \text{OH}^- + \text{Mo}^{6+} - \text{O} - \text{O}^{2-} )</td>
<td>-1.689 eV -1.692 eV</td>
</tr>
<tr>
<td>(4)</td>
<td>( \text{Mo}^{6+} - \text{O} - \text{OH}^- + \text{e}^- \rightarrow \text{Mo}^{5+} - \text{O} - \text{OH}^- + \text{OH}^- )</td>
<td>-0.085 eV 2.158 eV</td>
<td>( \text{Mo}^{4+} + \text{Mo}^{5+} - \text{O} - \text{OH}^- + \text{H}_2\text{O} + \text{e}^- \rightarrow \text{Mo}^{5+} - \text{OH}^- + \text{Mo}^{6+} - \text{O} - \text{OH}^- )</td>
<td>-1.426 eV -1.410 eV</td>
</tr>
<tr>
<td>(5)</td>
<td>( \text{Mo}^{5+} - \text{OH}^- + \text{e}^- \rightarrow \text{Mo}^{4+} - \text{O} - \text{OH}^- + \text{OH}^- )</td>
<td>0.670 eV</td>
<td>( \text{Mo}^{4+} + \text{Mo}^{5+} - \text{O} - \text{OH}^- + \text{e}^- \rightarrow \text{Mo}^{4+} + \text{Mo}^{6+} - \text{O} - \text{OH}^- )</td>
<td>0.827 eV 0.931 eV 0.968 eV</td>
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