

1 **Dynamic intermolecular interactions control adsorption from mixtures of**
2 **natural organic matter and protein onto titanium dioxide nanoparticles**

3 Sheyda Shakiba,¹ Alireza Hakimian,¹ Luis R. Barco,¹ and Stacey M. Louie^{1,*}

4 ¹Department of Civil and Environmental Engineering,
5 University of Houston, Houston, Texas 77204, United States

6

7 ^{*}Corresponding author:

8 Phone: 713-743-8646

9 Fax: 713-743-4260

10 Email: slouie@uh.edu

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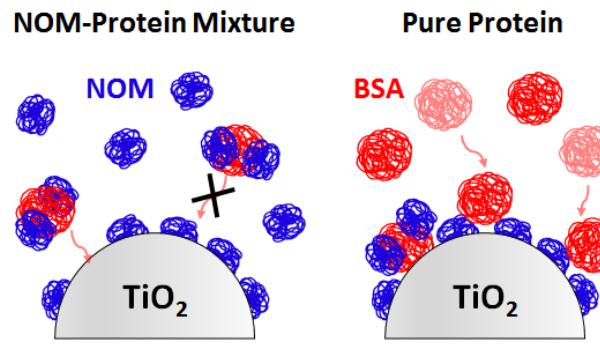
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28 **Abstract**

29 Engineered nanoparticles (NPs) will obtain macromolecular coatings in environmental systems,
30 changing their subsequent interactions. The matrix complexity inherent in natural waters and
31 wastewaters greatly complicates prediction of the corona formation. Here, we investigate corona
32 formation on titanium dioxide (TiO_2) NPs from mixtures of natural organic matter (NOM) and a
33 protein, bovine serum albumin (BSA), to thoroughly probe the role of mixture interactions in the
34 adsorption process. Fundamentally different coronas were observed under different NP exposure
35 conditions and time scales. In mixtures of NOM and protein, the corona composition was
36 kinetically determined, and the species initially co-adsorbed but were ultimately limited to
37 monolayers. On the contrary, sequential exposure of the NPs to pure solutions of NOM and protein
38 resulted in extensive multilayer formation. The intermolecular complexation between NOM and
39 BSA in solution and at the NP surface was the key mechanism controlling these distinctive
40 adsorption behaviors, as determined by size exclusion chromatography (SEC) and *in situ*
41 attenuated total reflectance – Fourier transform infrared (ATR-FTIR) spectroscopy. Overall, this
42 study demonstrates that dynamic intermolecular interactions and the history of the NP surface must
43 be considered together to predict corona formation on NPs in complex environmental media.

44 **Introduction**

45 Engineered nanoparticles (NPs) have gained attention for applications in myriad fields such
46 as water treatment and drug delivery, while concerns for potential environmental risks have also
47 arisen.¹⁻³ The adsorption of macromolecules to form a coating or corona on the NP surface
48 significantly changes the environmental fate and biological interactions of the NPs,⁴⁻¹⁷ and hence
49 surface chemistry is a critical property of the NP. In complex matrices, the corona composition is
50 difficult to characterize or predict. For example, natural organic matter (NOM) or humic
51 substances can show adsorptive fractionation, such that the composition of the adsorbed layer
52 differs from that of the bulk solution,¹⁸⁻²⁴ and extensive studies on protein corona formation in
53 physiological media have highlighted the dynamic nature of the adsorption process.¹²⁻¹⁷ To our
54 knowledge, few studies are available for NPs in environmental media comprising multiple classes
55 of macromolecules, including not only NOM but also proteins, polysaccharides, and other
56 biomolecules.^{25, 26} This research gap contributes uncertainty in interpreting NP behavior in
57 complex environmental matrices, when the ultimate NP surface composition is unknown.

58 Here, we investigate the competitive adsorption of NOM and a protein, bovine serum
59 albumin (BSA), onto titanium dioxide (TiO_2) NPs as a model system to identify the mechanisms
60 controlling corona formation on NPs in complex environmental mixtures. TiO_2 NPs are
61 photoreactive and hence of interest for water treatment applications,²⁷⁻³¹ but surface fouling (or
62 corona formation) can modify the effectiveness of the NPs.³²⁻³⁴ Our long-term goal is to predict
63 the photoreactivity of TiO_2 in complex media. To do so first requires a thorough understanding of
64 the corona formation. To our knowledge, only single-component adsorption of NOM³⁵⁻³⁸ or BSA^{37,}
65 ³⁹⁻⁴¹ onto TiO_2 NPs has previously been evaluated. Adsorption of NOM and protein together has
66 primarily been studied in the soil sciences, where zonal organic matter structures proposed by

67 Kleber et al.⁴² were attributed in part to multilayers that form upon sequential adsorption of pure
68 proteins over NOM coatings on mineral surfaces.⁴³⁻⁴⁵ However, in these studies, the influence of
69 solution-phase interactions that can occur between NOM and protein (prior to adsorption) has not
70 yet been fully explored. A recent study by Schmidt et al. identified that solution-phase
71 complexation of BSA onto DNA reduces repulsive interactions to enhance DNA adsorption to
72 goethite surfaces.⁴⁶ As proteins also complex with NOM,⁴⁷⁻⁵³ we hypothesize that complexation
73 can influence adsorption from mixtures of NOM and protein onto NPs. A comprehensive
74 understanding of the adsorption process must therefore consider all possible interactions between
75 NOM, protein, and TiO₂ NPs, including those between the uncoated NPs and macromolecules,
76 between NOM and protein in solution (e.g., complexation⁴⁸⁻⁵²), and between adsorbed and
77 dissolved macromolecules (e.g., displacement⁵⁴⁻⁵⁶ or multi-layer adsorption⁴³⁻⁴⁵).

78 The objective of this study is to achieve a mechanistic understanding of the fundamental
79 processes controlling the adsorption of mixtures of NOM and BSA onto TiO₂ NPs, by investigating
80 solution and surface interactions, as well as the kinetics and history of these interactions. Batch
81 adsorption experiments were evaluated against theoretical equilibrium and kinetic adsorption
82 models. We then focus on the influence of NOM-protein complexation on the adsorption process,
83 using size exclusion chromatography (SEC) to identify complexation and *in situ* attenuated total
84 reflectance – Fourier transform infrared (ATR-FTIR) spectroscopy to probe competitive
85 adsorption, co-adsorption, or multilayer adsorption phenomena under different NP exposure
86 conditions. We expect this fundamental knowledge will be useful to identify the range of processes
87 that can affect corona formation on NPs in complex environmental media.

88

89 **Materials and methods**

90 *Materials*

91 TiO_2 NPs (Standard Reference Material (SRM) 1898) were obtained from the National
92 Institute of Standards and Technology (NIST, Gaithersburg, MD), Suwannee River NOM (Cat.
93 No. 1R101N) from the International Humic Substances Society (IHSS, St. Paul, MN), and bovine
94 serum albumin (BSA, reagent grade pure powder) from Sera Care Life Sciences (Milford, MA).
95 Other reagents are specified in the Supporting Information (SI). BSA (1 g L^{-1}) and NOM (1 g L^{-1})
96 stock solutions were prepared in Milli-Q water, adjusted to pH 7 using (0.1 or 1) M HCl or NaOH,
97 and allowed to equilibrate overnight to dissolve. Stock solutions were filtered through $0.22 \mu\text{m}$
98 polyethersulfone membranes (EMD Millipore, Burlington, MA). Filter loss (to correct subsequent
99 concentrations) was determined against unfiltered stocks for BSA by absorbance at 280 nm on a
100 UV-2600 spectrophotometer (Shimadzu, Columbia, MD) (< 5% filter loss), and for NOM by total
101 organic carbon (TOC) analysis (Xenco Laboratories, Houston, TX) or SEC with refractive index
102 (RI) detection, described in the SI (8% to 10% filter loss). Subsequent samples containing NOM
103 or BSA were prepared in an aqueous buffer of 1.2 mM NaHCO_3 and 0.85 mM CaCl_2 (pH 7 to 7.5),
104 representing a simplified Environmental Protection Agency (EPA) moderately hard water⁵⁷
105 (matching the total monovalent and divalent cation concentrations using only NaHCO_3 and CaCl_2),
106 and provides similar pH, bicarbonate, and calcium concentrations to those reported in freshwater
107 systems.⁵⁸

108

109 *Preparation and characterization of TiO₂ suspensions*

110 Stock suspensions of TiO₂ NPs (2 g L⁻¹ in Milli-Q water) were dispersed using an
111 ultrasonication probe (TM250B Tekmar Sonic Disruptor, Cincinnati, OH) at a measured power⁵⁹
112 of (20 ± 3) W for three 5-min intervals, immediately prior to use. The NPs have reported crystallite
113 particle diameters of (19 ± 2) nm for anatase (comprising 76% of the sample) and (37 ± 6) nm for
114 rutile (comprising 24%).⁶⁰ Dynamic light scattering (DLS) measurements (Zetasizer Nano,
115 Malvern Instruments, Westborough, MA) were taken to determine the hydrodynamic size as the
116 *z*-average diameter of (155 ± 11) nm, intensity-average diameter of (182 ± 14) nm, or volume-
117 average diameter of (118 ± 8) nm for stock suspensions diluted to 0.2 g L⁻¹ TiO₂ NPs in 1 mM
118 NaCl (pH 5.6 ± 0.5), confirming good dispersion of the NPs compared to the reported volume-
119 mean diameter in the NIST SRM 1898 Certificate of Analysis (CoA).⁶⁰ After each adsorption
120 experiment, DLS size was also measured directly on samples containing 0.5 g L⁻¹ NPs in the buffer
121 stated above. A specific surface area of 54 m² g⁻¹ reported in the NIST CoA (from Brunauer–
122 Emmett–Teller (BET) analysis) was used to calculate adsorbed masses.

123

124 *Characterization of BSA and NOM solutions by SEC*

125 Solutions of BSA and NOM and their mixtures were prepared in the CaCl₂/NaHCO₃
126 medium noted above, fixing one species' concentration at 100 mg L⁻¹ and varying the other from
127 (10 to 200) mg L⁻¹. SEC analysis was performed using a Superdex 75 10/300 GL analytical SEC
128 column (GE Healthcare, Chicago, Illinois) on an Agilent 1290 Infinity system comprising a binary
129 pump, degasser, and autosampler (Agilent, Santa Clara, CA). 100 µL of sample was injected. The
130 eluent was 4 mM phosphate (pH 7) with 25 mM NaCl at a flow rate of 0.7 mL min⁻¹.^{61 62} Similar
131 results were observed in eluent matching the sample buffer (Figure S2), but column fouling by

132 NOM occurred in Ca^{2+} -containing media. A UV-vis diode array detector (Agilent 1260 UV-DAD),
133 fluorescence detector (Agilent 1260 FLD), and refractive index (RI) detector (Wyatt, Optilab T-
134 rEX) were situated in-line after the SEC column. The DAD monitored absorbance across (200 to
135 500) nm in 2 nm increments. The FLD monitored the fluorescence of BSA at excitation/emission
136 wavelengths of (295/345) nm.⁶³ Complexation of NOM onto BSA was evaluated within 1 h of
137 mixing, based on the change in UV and FLD peak areas across the BSA elution time and depletion
138 in RI peak area across the NOM elution time, on duplicate samples. The complexation kinetics of
139 BSA (100 mg L⁻¹) and NOM (100 mg L⁻¹) were also evaluated.

140

141 *Batch adsorption isotherms*

142 Adsorption isotherms onto TiO_2 NPs (0.5 g L⁻¹) were obtained in triplicate. Single-
143 component isotherms were collected for initial concentrations of BSA from (60 to 250) mg L⁻¹ or
144 NOM from (10 to 200) mg L⁻¹ in the $\text{CaCl}_2/\text{NaHCO}_3$ buffer. The buffer and adsorbates were mixed,
145 followed by NP addition within 1 h. Samples were covered with aluminum foil and rotated end-
146 over-end at 25 rpm at room temperature for approximately 24 h. Then, 1.5 mL of sample was
147 centrifuged in an Eppendorf Protein LoBind centrifuge tube at 13000 rpm (12641 $\times g$) for 23 min
148 (MiniSpin Plus, Eppendorf, Hamburg, Germany). Supernatant was collected to quantify
149 unadsorbed species. Batch adsorption samples for mixtures of BSA and NOM onto TiO_2 (0.5 g L⁻¹)
150 were prepared following the same procedures, fixing the concentration of one species at 100 mg
151 L⁻¹ while the other was varied from (10 to 200) mg L⁻¹.

152 The adsorbed mass of BSA or NOM was determined by solution depletion, i.e., subtracting
153 the remaining from the initial concentration, and dividing the depleted mass by the estimated TiO_2
154 surface area from the NIST CoA. BSA was quantified by the Bradford assay (SI);⁶⁴ for binary-

155 component solutions, corrections for interferences in the presence of NOM⁶⁵ were applied (Figure
156 S1). NOM was analyzed by SEC with refractive index (RI) detection (method description in SI)
157 to quantify solution depletion and identify adsorptive fractionation of NOM onto TiO₂. Spectral
158 analysis of the NOM by batch- and SEC-UV-vis analysis⁶⁶⁻⁶⁹ was also performed to evaluate
159 adsorptive fractionation (SI).

160

161 *Kinetic adsorption experiments*

162 *In situ* ATR-FTIR spectroscopy was used to semi-quantitatively evaluate the kinetics of
163 adsorption, displacement of adsorbed species, and multilayer adsorption processes. A Nicolet iS50
164 FTIR spectrometer (ThermoFisher Scientific, Waltham, MA) was equipped with a diamond/ZnSe
165 single reflection ATR crystal (PIKE Technologies, Fitchburg, WI). Spectra were collected from
166 (800 to 4000) cm⁻¹ with a resolution of 2 cm⁻¹ and averaged over 200 scans. 5 µL of TiO₂ (10 g L⁻¹
167 in Milli-Q water) was dried onto the ATR crystal, and a flow cell (PIKE Technologies) was
168 attached. Because the background solution chemistry and pH are important,^{41, 70, 71} buffer solution
169 with the same composition used in the adsorption experiments was flowed over the NPs to
170 equilibrate the surface chemistry and also remove loosely attached NPs.

171 Adsorption experiments were conducted separately with pure NOM, pure BSA, or
172 mixtures. For pure NOM or BSA, 100 mg L⁻¹ solutions in the buffer were flowed over the NPs,
173 and spectra were collected every 10 min and reprocessed using a background spectrum of
174 macromolecule-free buffer over the TiO₂ film. We performed the same experiment for NOM-BSA
175 mixtures (100 mg L⁻¹ of each species), injected after \approx 1 h mixing. To compare relative adsorbed
176 amounts of NOM and BSA from the mixtures, spectra across (1300 to 1800) cm⁻¹ were modeled
177 as a linear combination of the single-component adsorbed NOM and BSA spectra to obtain fitted

178 coefficients, A'_{NOM} and A'_{BSA} (details in SI). For this analysis, 1800 cm^{-1} was largely free of NOM
179 or BSA absorbance and selected as a base point to vertically align the spectra before fitting. The
180 ATR-FTIR analysis is only semi-quantitative because of the variable TiO_2 film deposited between
181 experiments; hence, fitted coefficients are not compared directly. Only ratios of coefficients, e.g.
182 $\frac{A'_{\text{BSA}}(t)}{A'_{\text{NOM}}(t)}$, were compared between samples, normalizing the TiO_2 surface area and sample volume
183 probed, roughly analogous to the use of internal standards for quantitative FTIR analysis.⁷²

184 Sequential adsorption experiments were performed to evaluate interactions between
185 adsorbed and dissolved macromolecules. Fresh TiO_2 NP films were prepared and equilibrated in
186 buffer, followed by equilibration in NOM (100 mg L^{-1}), which was identified in batch experiments
187 to preferentially adsorb. In one experiment, pure BSA (100 mg L^{-1}) was then injected over the
188 NOM-coated TiO_2 to identify displacement or overcoating. In other experiments, a mixture of
189 BSA and NOM was injected over the NOM-coated TiO_2 , followed by a solution of pure BSA, to
190 distinguish the role of solution-phase mixture interactions on BSA adsorption to NOM-coated
191 TiO_2 . Three mixtures were evaluated: BSA (50 mg L^{-1}) with NOM (100 mg L^{-1}), BSA (100 mg
192 L^{-1}) with NOM (200 mg L^{-1}), and BSA (200 mg L^{-1}) with NOM (100 mg L^{-1}).

193

194 **Results and Discussion**

195 *Batch single-component adsorption of BSA and NOM onto TiO_2 NPs*

196 Batch adsorption experiments were performed at pH 7 to 7.5, where the TiO_2 NPs have a
197 $|\zeta| < 20\text{ mV}$,^{60,73} and both BSA and NOM are negatively charged (isoelectric point of BSA ≈ 5.1 ;⁷⁴
198 zeta potential for NOM at pH 7 $\approx -40\text{ mV}$).³⁵ The adsorption behavior will be determined by
199 attractive forces, including Van der Waals forces, hydrophobic interactions, hydrogen bonding,
200 and Ca^{2+} bridging in our media, as well as repulsive electrostatic and hydrophilic forces. While

201 uncoated TiO_2 NPs aggregate rapidly in this medium, increasing concentrations of BSA and NOM
202 provided steric/electrosteric colloidal stability,^{75, 76} as observed by DLS (Figure S4). Aggregation
203 at lower adsorbate:NP ratios could reduce the available surface area for adsorption, but we
204 obtained similar BSA adsorption isotherms at different TiO_2 concentrations, (0.5 and 1) g L⁻¹,
205 suggesting the effect may be minimal. To obtain the entire isotherm with measurable solution
206 concentrations, the initial concentrations of adsorbate used were higher than typical environmental
207 concentrations, particularly for proteins which represent a small percent of dissolved organic
208 carbon (DOC) in surface waters.^{26, 77} However, the lower extent of our remaining (equilibrium)
209 solution concentrations (\approx 4 mg L⁻¹) is within the range of higher concentrations observed (e.g. up
210 to 40 mg L⁻¹ of DOC in wetlands,²⁶ or (1 to 50) mg L⁻¹ protein in urban watersheds and wastewater
211 effluents⁷⁸⁻⁸⁰).

212 A Langmuir adsorption isotherm (Equation S2) was able to fit the single-component
213 adsorption of BSA and NOM (Figure 1), with saturation adsorbed masses, q_{\max} , of (2.6 and 0.90)
214 mg m⁻², respectively, fitted by nonlinear regression. These values are higher than other reports,
215 e.g. 1.7 mg m⁻² for BSA at pH 7.3,⁸¹ and \approx 0.2 mg m⁻² for NOM at pH 7,²⁴ and likely attributable
216 to the presence of Ca^{2+} which enhances both albumin and NOM adsorption to TiO_2 by bridging.⁸²⁻
217⁸⁵ Therefore, we caution extrapolation of results to media lacking Ca^{2+} . The Langmuir isotherm
218 constant, K , for BSA (1.1 L mg⁻¹) was higher than that for NOM (0.051 L mg⁻¹). We interpret K
219 only as an empirical fitting parameter indicative of the steeper slope of the BSA isotherm and also
220 note wide 95% confidence intervals on the fitted K for BSA (Table S1).

221 We investigated the NOM adsorption in further detail, considering the heterogeneity of the
222 NOM itself. Batch UV-vis absorbance data showed an increase in the spectral slope of the NOM
223 remaining in solution after adsorption (Figure S5), indicative of preferential adsorption of higher

224 molar mass species with “activated” aromatic groups (i.e., those with polar ring substitutions, e.g.,
225 carbonyl, carboxyl, and ester groups).⁶⁸ The SEC analysis (Figure S3), along with providing
226 adsorbed mass of NOM, confirmed preferential adsorption of higher molar mass NOM, consistent
227 with prior studies.¹⁸⁻²⁰ The direct relationship between spectral slope and molar mass was also
228 verified by SEC-UV-DAD analysis^{67, 69} (Figure S6). Finally, ATR-FTIR analysis showed that the
229 non-adsorbing, lower molar mass fraction contained higher amounts of functional groups at 1120
230 cm⁻¹ (Figure S7), which are observed in hydrophilic NOM fractions and attributed to the C-O
231 stretch of alcohol or carbohydrate species.^{86, 87} The preferential adsorption was used to inform the
232 properties of adsorbing NOM when parameterizing the competitive adsorption models hereafter.

233

234 *Batch competitive adsorption from mixtures of NOM and BSA is kinetically-determined and*
235 *monolayer-limited*

236 Adsorption from mixtures of NOM and BSA onto TiO₂ was measured in two sets of batch
237 experiments: varying the concentration of BSA in the presence of 100 mg L⁻¹ NOM, and vice versa
238 (Figure 1). NOM largely outcompetes BSA for adsorption, contrary to expectations from the
239 single-component isotherms. To further explore this phenomenon, experimental observations were
240 compared to two theoretical models: an equilibrium Langmuir adsorption model, and a kinetic
241 adsorption model. Our goal is to identify a simple analytical model capable of describing the
242 competitive adsorption when parameterized using only the single-component Langmuir
243 parameters and known or measured properties of the macromolecules and NPs.

244 The competitive Langmuir adsorption model for *n* competing adsorbates is presented in
245 Equation 1:⁸⁸

246

$$q_i = \frac{q_{\max,i} K_i C_{f,i}}{1 + \sum_{j=1}^n (K_j C_{f,j})} \quad (1)$$

247
248 where q_i (mg m⁻²) is the adsorbed mass of species i , and $C_{f,i}$ (mg L⁻¹) is the final solution
249 concentration of i at the end of the adsorption experiment. $q_{\max,i}$ (mg m⁻²) and K_i (L mg⁻¹) are the
250 maximum monolayer adsorbed capacity and the Langmuir isotherm constant, respectively, from
251 each single-component isotherm. This equilibrium model was not capable of predicting adsorption
252 from the mixtures (Figure 1), significantly overestimating the adsorbed mass of BSA relative to
253 NOM. A key assumption of the Langmuir model is that adsorption is reversible, and compounds
254 with higher affinity will displace others to achieve equilibrium. Contrarily, the observed data
255 suggest that our system does not meet Langmuir assumptions.

256 The alternative limiting case is a kinetic adsorption model in which NOM and BSA adsorb
257 *irreversibly*. Irreversible attachment has been modeled by random sequential adsorption (RSA)
258 models^{89, 90} or analogously by colloid deposition models.⁹¹ For adsorption onto NPs in suspension,
259 the depletion rate of adsorbate from solution, $\frac{dN_{\infty,i}}{dt}$, can be described by the Smoluchowski
260 equation⁹² with a dynamic site blocking function, $B(\theta)$:⁹¹

261

$$262 \frac{dN_{\infty,i}}{dt} = -\alpha [4\pi D(R_1 + R_2)N_{\text{TiO}_2}]N_{\infty,i}B(\theta) = -\alpha k_{f,i}N_{\infty,i}B(\theta) \quad (2)$$

263

264 where $N_{\infty,i}$ is the number concentration of macromolecules in bulk solution at time t , D is the
265 summed diffusion coefficients for the macromolecule and NP, R_1 and R_2 are the hydrodynamic
266 radii of the macromolecule and NP, N_{TiO_2} is the number concentration of TiO₂ NPs, α is the
267 attachment efficiency, and θ represents the fractional surface coverage. The diffusion-limited rate
268 coefficient for favorable attachment (no energy barrier) is represented by $k_{f,i}$. Notably, this model
269 will always predict the same final surface coverage at infinite time, regardless of solution

270 concentration. Hence, this model is incapable of predicting the observed concentration-dependent
271 single-component adsorption isotherms without incorporating additional conditions, such as
272 spreading of macromolecules upon adsorption.^{93, 94} The paradoxical nature of observing both
273 irreversible and concentration-dependent adsorption has been discussed in the protein adsorption
274 literature.^{90, 95}

275 We do not propose to provide the most complete model to address this scenario but rather
276 to obtain a simple kinetic model capable of explaining our experimental data on final adsorbed
277 layer composition. We proceed by simplifying Equation 2 to eliminate the site-blocking function
278 and assume favorable attachment (or equivalent attachment efficiencies for NOM and BSA).
279 Incorporating site blocking requires a numerical solution and will not change the *final* adsorbed
280 layer composition predicted, since the adsorption rates of all adsorbates are affected equally.
281 Obtaining attachment efficiencies would require kinetic data or otherwise treatment of the
282 attachment efficiencies as fitting parameters in the model.

283 For favorable attachment without site blocking, integrating Equation 2 yields Equation 3:

284

285
$$\ln \left(\frac{N_{\infty,i}}{N_{0,i}} \right) = -4\pi D(R_1 + R_2)N_{\text{TiO}_2}t = -k_{f,i}t \quad (3)$$

286

287 where $N_{0,i}$ is the initial concentration of species i . The depleted concentration and adsorbed mass
288 of each species at each time t is then obtained by a mass balance. Having eliminated the site
289 blocking function, a stopping criterion is needed to end the adsorption of each species. In defining
290 this criterion, we incorporate concentration-dependent adsorption (i.e. the possibility for
291 undersaturation) by specifying that the adsorption of each species ends when it has reached

292 “equilibrium” with the surface sites that are unoccupied by the competing species j , as defined in
293 Equation 4:

294

295
$$q_i(t_{\text{stop},i}) = \frac{q_{\max,i} K_i C_i(t_{\text{stop},i})}{1 + K_i C_i(t_{\text{stop},i})} \left(1 - \sum_{j \neq i} \frac{q_j}{q_{\max,j}} \right) \quad (4)$$

296

297 In specifying $q_{\max,j}$ for the site depletion, we assume that the total available surface area
298 occupied at the saturation adsorbed mass is equivalent across all adsorbates. Equations 3 and 4 are
299 solved together to obtain different stopping times, $t_{\text{stop},i}$, for each adsorbate. Importantly, the
300 adsorption is made irreversible by holding the adsorbed mass of faster-adsorbing species fixed at
301 $q_i(t_{\text{stop},i})$ for all $t \geq t_{\text{stop},i}$. Thereafter, the slower-colliding species can continue adsorbing to any
302 remaining available sites until reaching its own stopping time. The final state is at disequilibrium
303 compared to Equation 1. Note that if the irreversibility criterion is eliminated and q and C are taken
304 at equilibrium, Equation 4 becomes equivalent to the competitive Langmuir model (Equation 1).

305 Overall, this kinetic model predicts the experimental data for the final adsorbed layer
306 composition significantly better than the equilibrium Langmuir model across all mixtures (Figure
307 1). The smaller size (higher diffusion coefficient) and higher number concentration of NOM
308 relative to BSA results in a higher adsorbed mass for NOM than predicted by the Langmuir
309 equilibrium model. Because of the high K parameter for BSA, the kinetic model predicts > 80%
310 overall surface saturation for any initial BSA concentration > 1 mg L⁻¹ (in the presence of 100 mg
311 L⁻¹ of NOM). The key assumptions of irreversible and monolayer-limited adsorption in this model
312 were then directly tested in ATR-FTIR experiments.

313

314 *Multilayers form upon sequential exposure of TiO₂ NPs to pure NOM and pure BSA*

315 *In situ* ATR-FTIR spectroscopy has previously been applied to evaluate the adsorption of
316 BSA,^{39, 41, 71, 96} NOM,⁷⁰ polymers,⁹⁷ and other compounds⁹⁸⁻¹⁰⁰ onto TiO₂ and other surfaces.¹⁰⁰⁻¹⁰³
317 This method allows semi-quantitative analysis of the kinetics and extent of adsorption onto NPs.
318 First, individual spectra of adsorbed NOM or BSA were collected during adsorption to the TiO₂
319 NP film from 100 mg L⁻¹ solutions (Figure S8). The strong peaks at (1410 and 1570) cm⁻¹ for
320 adsorbed NOM are likely attributable to deprotonated carboxyl groups (-COO⁻)^{104, 105} and also
321 include contributions from aliphatic hydrocarbons^{87, 106} and aromatic alkenes,^{87, 106} respectively,
322 that absorb in these regions. Consistent with our batch fractionation results (Figure S7), the peak
323 at 1125 cm⁻¹ (C-O stretch of carbohydrates) in the < 10 kDa NOM fraction was not observed in
324 the adsorbing NOM. For BSA, the two main peaks correspond to amide I at (1600 to 1700) cm⁻¹
325 for C=O stretching, and amide II at (1500 to 1600) cm⁻¹ for N-H bending and C-N stretching.^{106, 107}

326 Then, a sequential adsorption experiment was performed in which the surface of the
327 deposited NPs was equilibrated with NOM (100 mg L⁻¹) as the kinetically-favored adsorbate,
328 followed by pure BSA (100 mg L⁻¹). To quantify adsorption of multiple species, previous studies
329 used peak heights when peaks did not overlap significantly for adsorbed protein¹⁰⁸ and other
330 compounds.⁴⁶ Here, the broad bands for NOM and BSA overlap extensively, but peak locations
331 did not shift significantly in mixed layers compared to the single-component adsorption. Hence,
332 the mixed layer spectra were successfully modeled as a linear combination of the single-component
333 adsorbed BSA and NOM spectra in the range of (1300 to 1800) cm⁻¹ (Equation S6, Figure S9).
334 The fitted coefficients, A'_{BSA} and A'_{NOM} , are only semi-quantitative but can be evaluated for trends
335 in the adsorbed mass of each species within each experiment or when ratioed to normalize for TiO₂
336 surface or sample volume probed.

337 While in other cases, surface ligands with low affinity have been found to be displaced by
338 higher affinity species,¹⁰⁶ results here agree with adsorption irreversibility: the adsorbed amount
339 of NOM remained nearly constant during the subsequent adsorption of BSA (Figure S9). More
340 notably, the extensive BSA adsorption suggests that pure BSA significantly overcoats adsorbed
341 NOM, similar to other sequential adsorption experiments reporting multilayer formation of pure
342 proteins onto humic-coated minerals.⁴³⁻⁴⁵

343 Comparing the batch (mixture) and *in situ* ATR-FTIR (sequential) adsorption, the
344 formation of NOM-protein coronas on TiO₂ NPs then appears to be fundamentally different when
345 the NPs are exposed to a mixture (monolayer restriction) *versus* sequential exposure to pure
346 solutions (multilayer adsorption). To explain these contradictory behaviors, we hypothesize that
347 intermolecular complexation between humic substances and proteins in solution, well-known to
348 occur,⁴⁸⁻⁵² changes adsorption from mixtures compared to pure substances. Hence, we investigated
349 the role of intermolecular interactions through additional SEC and *in situ* ATR-FTIR experiments.

350

351 *Solution-phase complexation occurs between BSA and NOM*

352 SEC experiments were performed to evaluate complexation interactions between NOM
353 and BSA in the solution phase. BSA elutes from the SEC column from \approx (11 to 18) min as two
354 peaks, corresponding to BSA dimer and monomer, which were considered together in the analyses.
355 NOM elutes primarily as a broad peak from \approx (15 to 26) min. Upon increasing the ratio of NOM
356 to BSA in solution, UV absorbance and RI in the BSA region increase significantly (Figure 2),
357 indicating attachment of aromatic NOM species onto BSA. Complexation also quenches the BSA
358 fluorescence, consistent with previous reports¹⁰⁹ and possibly indicative of binding of the NOM
359 with fluorescent tryptophan residues in BSA or a change in BSA conformation. As with adsorption

360 to the TiO₂ NPs, NOM with higher molar masses have slightly higher affinity to complex with
361 BSA. The amount of NOM attached to the BSA estimated by SEC-RI analysis showed increasing
362 complexation with the ratio of NOM:BSA, and complexation was observed to proceed over \approx 5 h
363 before equilibrating (Figure S10).

364

365 *Co-adsorption is followed by suppressed multilayer formation in simultaneous adsorption from*
366 *NOM-BSA mixtures onto TiO₂ NPs*

367 *In situ* ATR-FTIR was used to investigate the simultaneous adsorption of NOM and BSA
368 onto TiO₂ NPs and evaluate the effects of complexation in solution on the adsorption from NOM-
369 BSA mixtures onto TiO₂ NPs. First, simultaneous adsorption of BSA (100 mg L⁻¹) and NOM (100
370 mg L⁻¹) onto the *uncoated* TiO₂ was evaluated. While both species increasingly adsorb over time,
371 the ratio of adsorbed BSA to NOM decreases over the first hour (Figure 3). This trend can be
372 explained either by a lower affinity of BSA to adsorb upon complexation, or increasing co-
373 adsorption of NOM with BSA as it complexes to BSA over \approx 5 h at the concentrations used here.
374 Batch adsorption experiments using isolated NOM-protein complexes suggested that
375 complexation does not largely suppress BSA adsorption onto *uncoated* TiO₂ (Figure S11); hence,
376 co-adsorption of NOM complexed with BSA may contribute more to the results observed in the
377 initial stage of adsorption to the uncoated TiO₂ NPs.

378 The larger picture from the mixture experiment is that the overall BSA adsorption does
379 indeed appear to be suppressed in the mixture relative to pure BSA: specifically, BSA adsorption
380 begins to plateau within 1 h in the mixture (Figure 4), but remains nearly linear over 1 h when
381 adsorbing from pure solution even after NOM has pre-adsorbed (Figure S9). We hypothesize that
382 over longer time scales, complexation of NOM onto dissolved BSA hinders the ability of BSA to

383 overcoat adsorbed layers *after* the TiO₂ surface has been saturated. To test this hypothesis,
384 adsorption from NOM-BSA mixtures onto NOM-coated TiO₂ NPs was evaluated (Figure 4 and
385 S12) and compared to subsequent adsorption of the pure BSA for various concentrations of BSA
386 and NOM. In all cases, after providing adequate opportunity for adsorption from the NOM-BSA
387 mixtures, subsequent injection of pure BSA led to further protein adsorption beyond that in the
388 mixtures. Hence, adsorption sites must be available to pure BSA that are not available to the
389 complexed BSA. We propose that the complexed BSA fills remaining bare TiO₂ sites (since NOM
390 is not completely saturated from 100 mg L⁻¹ starting conditions), but has little affinity to overcoat
391 the adsorbed NOM after complexing with NOM in solution. On the contrary, the pure BSA is
392 capable to attach onto the adsorbed NOM to form an overcoating. While modeling this behavior
393 without more quantitative kinetic data is outside the scope of this study, possible extensions to the
394 kinetic model are discussed in the SI that could describe this multilayer formation.

395 In summary, the complexation interaction between NOM and BSA is a critical process
396 leading to the occurrence of fundamentally different adsorption phenomena under different NP
397 exposure conditions and time scales, as depicted in Figure 5. Multilayer formation occurs upon
398 sequential exposure to *pure* solutions of NOM and BSA. In mixtures, BSA-NOM complexes can
399 co-adsorb to the *uncoated* TiO₂ at short time scales. However, after the TiO₂ surface is saturated,
400 the complexation of NOM to BSA in solution ultimately hinders any further development of
401 NOM/protein multilayers on the TiO₂ NPs, such that monolayer restrictions are reasonable when
402 modeling batch adsorption from mixtures (Figure 1). Notably, in this system, all possible mixture
403 interactions (macromolecule–NP, macromolecule–macromolecule, and macromolecule–adsorbed
404 layer) and their kinetics are important.

405

406 *Implications*

407 This study has presented a thorough investigation of the fundamental mechanisms involved
408 in the competitive adsorption of NOM and proteins (with BSA as a model protein) onto TiO₂ NPs,
409 using both modeling and experimental methods to fully evaluate the adsorption process under a
410 range of possible NP exposure conditions. The behaviors observed here further expand our
411 understanding of the role of mixture interactions and kinetics on corona formation in
412 environmental media. Just as protein corona formation in biological systems is well known to be
413 a dynamic process, so will prediction of heterogeneous corona formation in environmental systems
414 require knowledge of not only the matrix and NP composition, but also the intermolecular
415 interactions in solution and at the NP surface, and the kinetics and history of these interactions.

416 To our knowledge, this study is the first to directly identify the roles of both dynamic
417 complexation in solution and the history of the NP surface on the competitive adsorption process
418 in environmental matrices containing mixtures of NOM and protein. The influence of sequential
419 exposure observed here will be most relevant during transport of NPs between environments, e.g.
420 from surface water to a biofilm layer concentrated in proteins, or bio-uptake, where an NOM-
421 coated NP can obtain a protein corona. Diurnal or seasonal patterns also produce fluctuations in
422 the composition of organic matter in natural and engineered water treatment systems.

423 Additional research is needed to evaluate generalizability from the single solution
424 chemistry and high adsorbate and NP concentrations in this study. The presence of Ca²⁺ in our
425 samples likely enhanced the adsorption of both proteins and NOM onto TiO₂, and hence the
426 adsorbed masses and adsorption irreversibility may change in media lacking Ca²⁺. pH and ionic
427 strength also change the NP surface charge or screens charges, affecting adsorption. Using our

428 simple kinetic model to extrapolate to lower mixture concentrations (e.g. < 10 mg L⁻¹ of both
429 adsorbates), NOM is still predicted to outcompete such that the BSA adsorbed mass is relatively
430 sensitive to the NOM concentration, whereas NOM adsorption is relatively insensitive to the
431 presence of BSA. However, experiments are needed to confirm. Such studies should address
432 whether long-term conditioning of NPs in lower, environmentally relevant macromolecule
433 concentrations (but relatively high concentrations compared to relevant NP concentrations, i.e.
434 minimal solution depletion) would result in similar adsorbed layers to those measured at high
435 concentrations. True adsorption irreversibility would suggest that the final corona should not
436 depend on absolute concentrations given sufficient time for adsorption.

437 We anticipate systematic investigations for mixtures of macromolecules covering a range
438 of physicochemical properties (e.g., humic substances, proteins, polysaccharides, lipids, DNA,
439 etc.) will enable elucidation of overarching rules to predict competitive adsorption onto NPs and
440 other surfaces in complex environmental media. Future studies are needed to evaluate how the
441 corona compositions and structures formed under different conditions will affect subsequent NP
442 behavior in the environment. Most notably, we identified that exposure of the NP to a
443 homogeneous mixture of NOM and proteins that have already undergone complexation will
444 produce only a thin monolayer coating, whereas sequential or alternating exposures of the NP to
445 different ratios of NOM and protein can result in multilayer coatings. The corona thickness and
446 adsorbed mass are known to dominate the steric or electrosteric repulsion between NPs,^{11,110} and
447 hence our study suggests that the details of the history of NP exposure to various macromolecules
448 can be important to the overall fate and transport of the NPs. Corona composition, structure, and
449 thickness are also likely to change the reactivity of NPs, including photoreactive TiO₂ NPs,³²⁻³⁴
450 where the adsorbed macromolecules will interact with both organic pollutants and reactive oxygen

451 species. Finally, the degradation of the corona and transformation of the NP itself can also vary
452 with corona composition, leading to longer-term differences in NP fate and transport.¹¹¹⁻¹¹³ The
453 thoroughly characterized system presented here will be useful to investigate the effect of the
454 composition and structure of NOM/protein coronas on the photoreactivity of TiO₂ NPs and
455 reactive transformations of the corona.

456

457 ASSOCIATED CONTENT

458 Supporting Information

459 Experimental details, description of adsorption models, and additional complexation and
460 adsorption experiments are provided. This information is available free of charge via the Internet
461 at <http://pubs.acs.org>.

462

463 Notes

464 The authors declare no competing financial interest.

465

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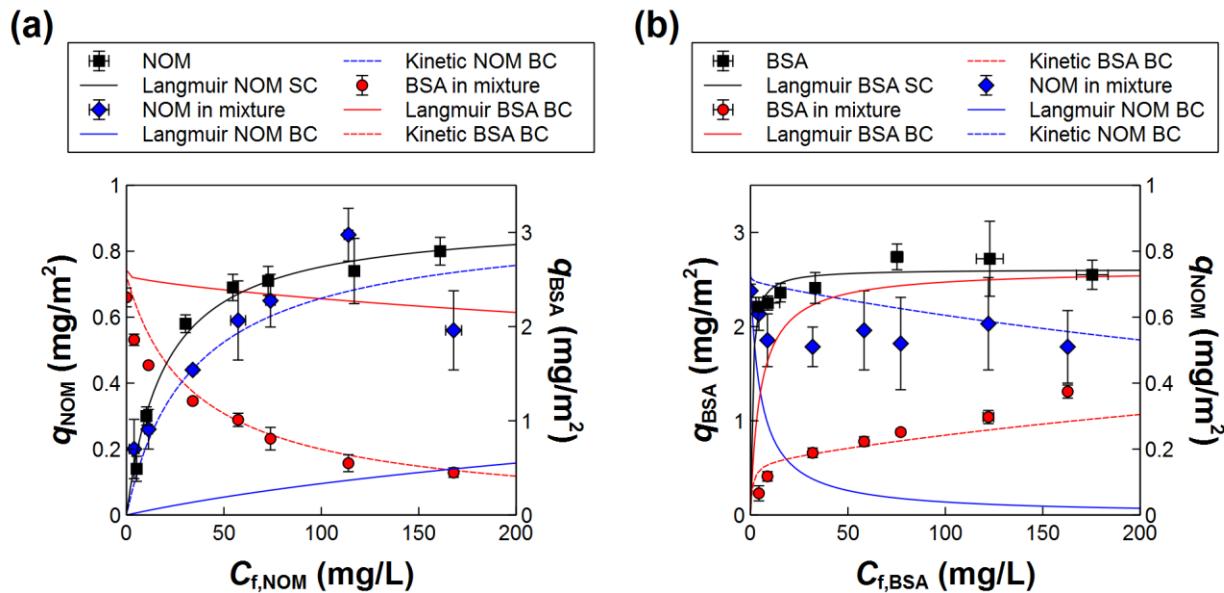
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776 **Figures**

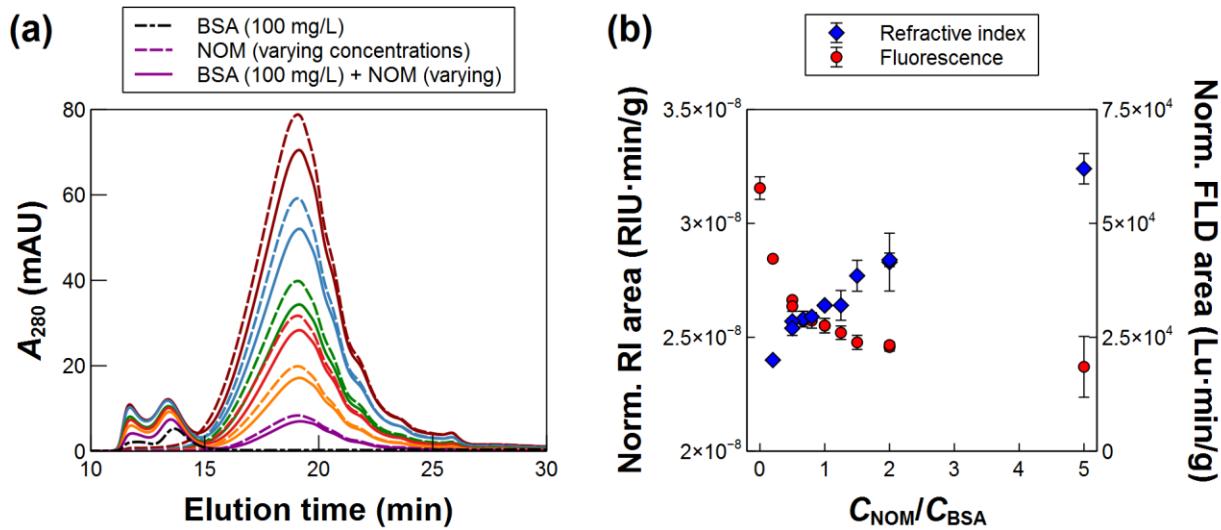
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Figure 1. Batch adsorption isotherms onto TiO_2 NPs for (a) the single-component (SC) solution of NOM and binary-component (BC) mixtures of NOM with a fixed initial concentration of BSA (100 mg L^{-1}), and (b) the SC solution of BSA and BC mixtures of BSA with a fixed initial concentration of NOM (100 mg L^{-1}). Isotherms were collected on 500 mg L^{-1} TiO_2 NPs in a background of 1.2 mM NaHCO_3 and 0.85 mM CaCl_2 (pH 7 to 7.5). Solid and dashed lines represent the Langmuir and kinetic models, respectively. Error bars represent the standard deviation of $n = 3$ samples.

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Figure 2. SEC-UV₂₈₀ chromatograms for BSA-NOM mixtures (a) were collected for BSA (100 mg L⁻¹), NOM (20, 50, 80, 100, 150, and 200 mg L⁻¹, from lower to higher UV absorbances), and their mixtures. For the BSA peaks, along with the increase in UV absorbance upon NOM complexation, addition of NOM mass onto the BSA can be identified by RI detection and quenching of the BSA fluorescence (b). Peak areas in (b) are normalized by the injected BSA mass. All samples were prepared in a buffer of 1.2 mM NaHCO₃ with 0.85 mM CaCl₂ (pH 7), then measured in an SEC mobile phase of 4 mM phosphate with 25 mM NaCl (pH 7) to avoid SEC column fouling by NOM in Ca²⁺-containing medium (SI). Additional data were also collected for mixtures of 100 mg L⁻¹ NOM with varying BSA (not shown). Error bars represent the standard deviation of $n = 2$ independently prepared samples.

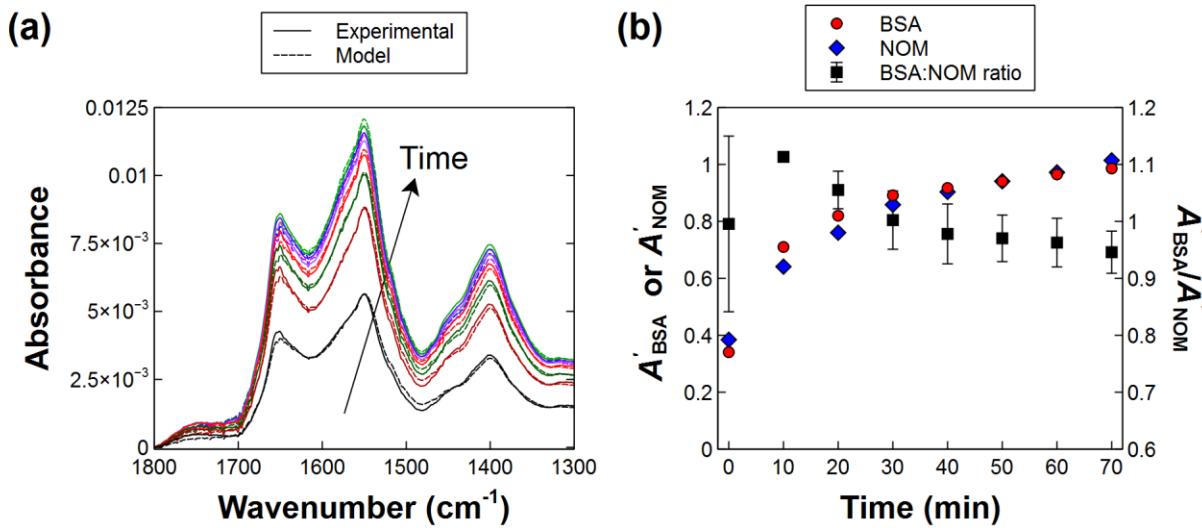
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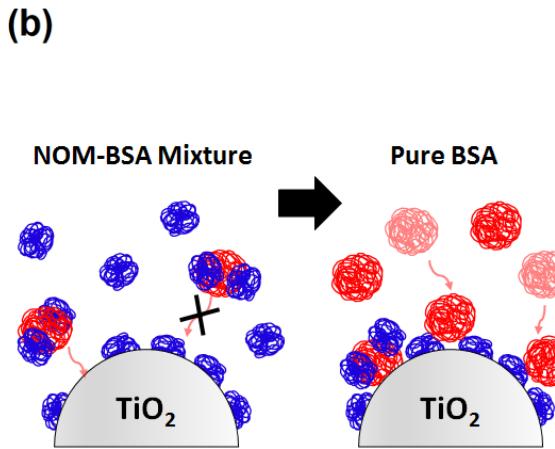
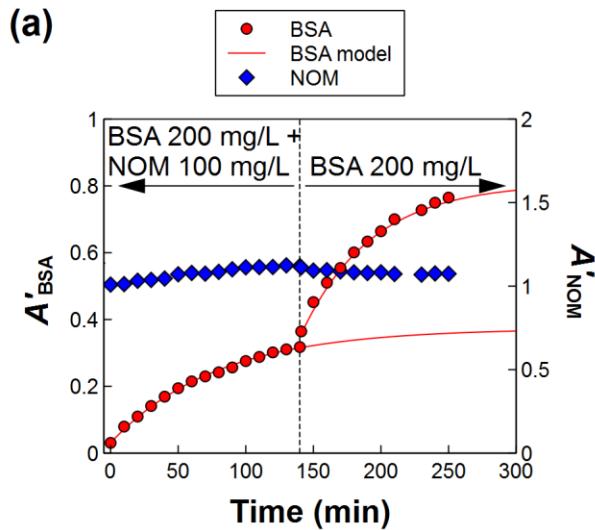
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Figure 3. *In situ* ATR-FTIR experiment for simultaneous adsorption from mixtures of BSA (100 mg L^{-1}) and NOM (100 mg L^{-1}) onto TiO_2 NPs in the same buffer as the batch adsorption experiments. The mixture was prepared immediately before injecting. (a) The measured spectra (solid lines) in the range of (1300 to 1800) cm^{-1} were modeled as a linear combination of the spectra for pure BSA and pure NOM (dashed lines). (b) Fitted adsorbed amounts (A') of BSA and NOM both increase over time, while the relative ratio of BSA:NOM decreases. Ratios plotted represent the average \pm standard deviation of the ratios determined at each time point within each of $n = 2$ independent experiments.

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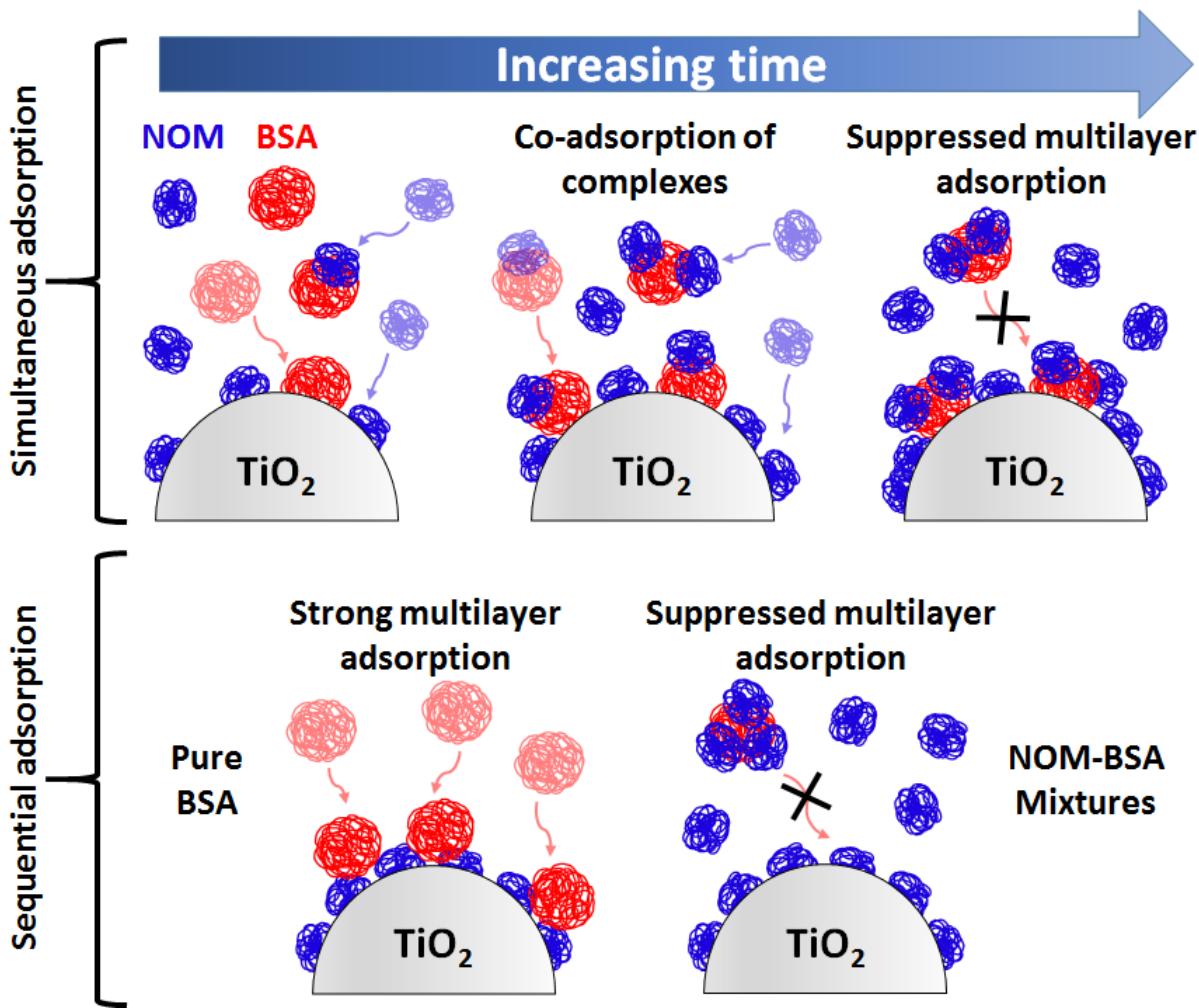
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Figure 4. *In situ* ATR-FTIR experiment for the sequential adsorption of a mixture of BSA and NOM, followed by pure BSA, onto NOM-coated TiO₂ NPs. The initial NOM layer was pre-adsorbed from a 100 mg L⁻¹ solution. Adsorption coefficients (A') were fitted as described in the SI. After the adsorption of complexed BSA from a mixture with NOM, additional protein is able to adsorb readily from a pure BSA solution. Similar results were obtained in replicate experiments. Considering the results of other combinations of concentrations (Figure S12), the conceptual model in (b) is proposed where complexed BSA fills any vacant sites on the TiO₂ surface, but multilayer formation is strongly suppressed relative to pure BSA.

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Figure 5. Conceptual model for competitive adsorption of NOM and BSA onto TiO₂ NPs, accounting for the critical role of dynamic intermolecular interactions. In simultaneous adsorption experiments (top), complexation of NOM to BSA initially results in co-adsorption to the uncoated TiO₂; however, complexation also hinders any subsequent multilayer adsorption after the TiO₂ surface is saturated. Sequential adsorption experiments (bottom) further demonstrated that pure protein readily overcoats NOM, whereas the multilayer adsorption is suppressed upon complexation of NOM to BSA.

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