

# Synergistic $\text{SO}_x/\text{NO}_x$ chemistry leading to enhanced $\text{SO}_3$ and $\text{NO}_2$ formation during pressurized oxy-combustion

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**Abstract** Pressurized oxy-combustion is a promising technology that can significantly reduce the energy penalty for  $\text{CO}_2$  capture in coal-fired power plants. However, higher pressure might enhance the production of strong acid gases, including  $\text{SO}_3$  and  $\text{NO}_2$ , which will lead to higher rates of corrosion. In this study, we investigated a reduced but combined  $\text{SO}_x$  and  $\text{NO}_x$  mechanisms and the synergistic formation of  $\text{SO}_3$  and  $\text{NO}_2$  was kinetically evaluated under different pressures and temperatures up to 15 atm and 1100 °C. The calculation results show that the interaction of  $\text{SO}_x$  and  $\text{NO}_x$  significantly accelerates the conversion rates of  $\text{SO}_2$  to  $\text{SO}_3$  and  $\text{NO}$  to  $\text{NO}_2$ , and the acceleration is much stronger at elevated pressures and comparatively low temperatures. With a strong interaction between  $\text{SO}_x$  and  $\text{NO}_x$  due to elevated pressures, the formation pathways of  $\text{SO}_3$  and  $\text{NO}_2$  through  $\text{HOSO}_2 + \text{O}_2 = \text{HO}_2 + \text{SO}_3$  and  $\text{HO}_2 + \text{O} = \text{NO}_2 + \text{OH}$ , respectively, are dramatically promoted. These two reactions are linked by the reaction  $\text{SO}_2 + \text{OH} + \text{M} = \text{HOSO}_2 + \text{M}$ , resulting in a ‘strong’ cycle, which can be represented by the global reaction  $\text{NO} + \text{SO}_2 + \text{O}_2 = \text{NO}_2 + \text{SO}_3$ . This cycle is the major route for the formation and destruction of both  $\text{SO}_3$  and  $\text{NO}_2$  at elevated pressures.

**Keywords** Elevated pressure ·  $\text{SO}_3$  ·  $\text{NO}_2$  · Kinetic mechanism · Synergistic effect

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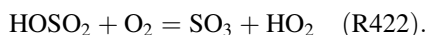
## Introduction

First-generation oxy-combustion technology, which operates under atmospheric pressure, suffers a significant penalty in net generating efficiency. By operating oxy-combustion under pressurized conditions, the plant efficiency can be increased because the latent heat in the flue gas moisture can be recovered and integrated into the steam cycle [1–3]. However, higher pressure enhances the production of strong acid gases, including  $\text{NO}_2$  and especially  $\text{SO}_3$ , which could significantly increase the rate of corrosion. Thus, the formation of  $\text{SO}_3$  during oxy-combustion has attracted attention in the past decade due to  $\text{SO}_x$  enrichment which is expected with flue gas recycle. A test conducted by Ahn et al. [4] in a pulverized coal (PC) furnace at the University of Utah found that the  $\text{SO}_3$  produced in oxy-coal combustion is several times more than that in air combustion. A recent review of sulfur impacts in oxy-coal technology indicates that the quantity of  $\text{SO}_2$  emission based on input coal mass (kg- $\text{SO}_2$ /kg-coal) is reduced by 14–30%, depending on the coal type. Based on the sulfur mass balance, this suggests that the reduced sulfur mass must either be in the fly ash that are deposited on heating surfaces in the furnace or must have condensed as sulfuric acid [5]. These studies have demonstrated significant enhancement of  $\text{SO}_3$  formation in oxy-combustion. However, previous studies were conducted at atmospheric pressures, and there are no reports on the formation of  $\text{SO}_3$  under pressurized conditions, partially because at elevated pressure, accurate sampling and measurement of  $\text{SO}_3$  is difficult. In addition, at elevated pressures, NO becomes easier to convert into  $\text{NO}_2$ , which particularly results in respiratory infections for adults and chronic lung injury for children [6].

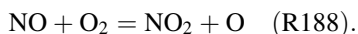
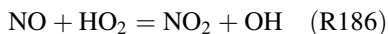
Under POC conditions, the compression of the flue gas increases residence time in the furnace in proportion to the increase in operating pressure. Thus, the residence time in a POC furnace can be an order of magnitude or longer than that in atmospheric combustion. Thus, the formation of  $\text{SO}_3$  through gas phase reactions could be significant with such a long residence time. In traditional atmospheric combustion processes,  $\text{SO}_3$  is mainly catalytically formed in the selective catalytic reduction (SCR) De- $\text{NO}_x$  unit and  $\text{SO}_3$  formation in the gas phase can be neglected. At atmospheric pressure,  $\text{SO}_3$  formation in the post-flame region is preferred via the oxidation of  $\text{SO}_2$  [7–9]:



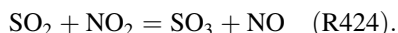
and secondary formation via  $\text{HOSO}_2$ :



As seen above,  $\text{SO}_3$  forms mainly through reactions in the O/H radical pool. Among the coexisting species in the post-flame region,  $\text{NO}_x$  has been proposed to influence  $\text{SO}_3$  formation under certain conditions. The formation routes of  $\text{NO}_2$  from NO are mostly via the following reactions, all of which affect the O/H radical pool:



On the basis of an analysis for atmospheric chemistry (1 atm), Song et al. [9] proposed a new process to oxidize NO and SO<sub>2</sub> in the flue gas simultaneously, and mentioned that reactions (R186, R376, and R422) can form a chain reaction to promote the formation of SO<sub>3</sub> and NO<sub>2</sub> if OH or HO<sub>2</sub> radicals are present. This hypothesis was verified in a recent measurement of SO<sub>3</sub> formation with NO addition in an atmospheric-pressure flow reactor [7]. Wei et al. [10] also observed the interaction between SO<sub>x</sub> and NO<sub>x</sub> when adding SO<sub>2</sub> into a coal flame in an entrained flow reactor (1 atm). Because all above studies have been performed at atmospheric pressure, the degree of this interaction was quite small. The only available measured data on SO<sub>x</sub> and NO<sub>x</sub> interaction at elevated pressures is presented by Mueller et al. [11] in a pressurized plug flow reactor at 950 K (0.5–10.0 atm) for a CO/H<sub>2</sub>O/O<sub>2</sub>/NO/SO<sub>2</sub> system. The pressurized results suggest that, at lower pressures, SO<sub>3</sub> formation occurs primarily through R1 and R3. However, the interaction via R424, given below, becomes important due to higher conversion ratio of NO to NO<sub>2</sub> at elevated pressures:



Integrated SO<sub>x</sub>/NO<sub>x</sub> removal technology is another motivation for studying SO<sub>3</sub> and NO<sub>2</sub> formation and interaction. This technology is considered a promising approach for flue gas purification and, potentially, for production of nitric and sulfuric acids in the gas processing unit of oxy-combustion systems [6, 12]. The concentrations of SO<sub>x</sub> and NO<sub>x</sub> at the inlet of the emission removal column have been shown to be critical to removal efficiency [13]. To date, the gas-phase interaction between SO<sub>x</sub> and NO<sub>x</sub> has been reported mainly for atmospheric pressure. However, at atmospheric pressure, conversion rates of NO to NO<sub>2</sub> and SO<sub>2</sub> to SO<sub>3</sub> in the post-flame region are very slow and residence times are short (e.g., 1–3 s). This is not the case at elevated pressures with a longer residence time. However, the formation of NO<sub>2</sub> and SO<sub>3</sub> in the gas phase and their interaction have not been adequately addressed for such pressurized systems.

This study seeks to understand the interaction mechanisms between SO<sub>x</sub> and NO<sub>x</sub> for evaluating the yield of strong acid gases, specifically SO<sub>3</sub> and NO<sub>2</sub>, in the post-flame region of the POC process. After validating the detailed mechanism (72 species and 428 reactions) including nitrogen and sulfur chemistry based on its comparison with the literature experimental data, the synergistic promotion of SO<sub>3</sub> and NO<sub>2</sub> was kinetically evaluated under representative post-flame conditions, and the effects of temperature and pressure on this synergistic promotion were studied. The rate of production was used to illustrate SO<sub>x</sub>/NO<sub>x</sub> interaction mechanism, and to demonstrate the formation routes of SO<sub>3</sub> and NO<sub>2</sub>.

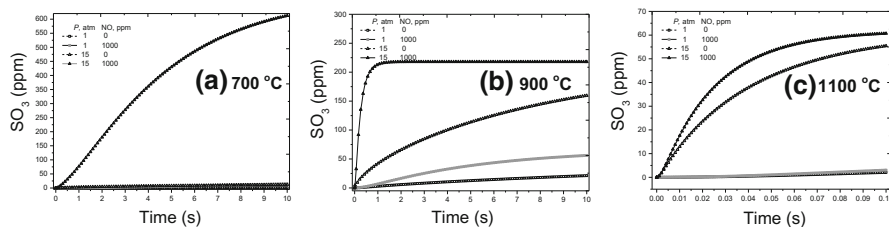
## Methods

This study adopts a detailed gas-phase mechanism including nitrogen and sulfur chemistry based on GRI-Mech 3.0 [14]. The mechanism includes 72 species and 428 steps, in which the subset of sulfur and  $\text{SO}_x/\text{NO}_x$  interactions are from Glarborg et al. [15] and Mueller et al. [11], respectively. CHEMKIN software package is employed assuming plug flow [8]. The conditions studied are chosen so as to represent the post-flame conditions of POC (1–15 atm, 700–1100 °C). Before using the detailed mechanism to predict  $\text{SO}_3$  and  $\text{NO}_2$  formation under POC conditions, nine cases are compared with experimental results from literatures [11, 16, 17]. The comparison indicates that the mechanism can accurately predict the evolution of  $\text{SO}_3$  and  $\text{NO}_2$  in the complex environment under both atmospheric and elevated pressures. In this study, rate-of-production (ROP) analysis is employed because it is a useful tool in understanding reacting-flow calculations, which determines the contribution of each reaction to the net production or destruction rates of certain species [18]. In addition, ROP analysis allows for quick identification of dominant reaction paths.

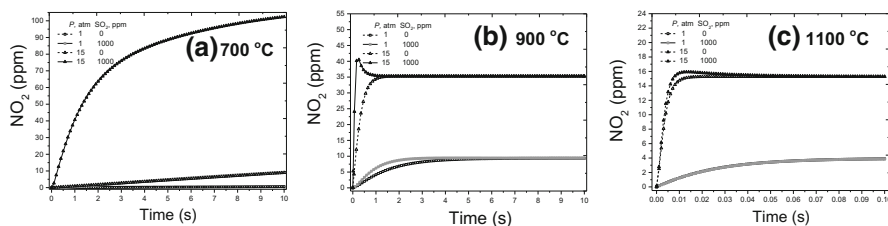
## Results and discussion

### The synergistic promotion of $\text{SO}_3$ and $\text{NO}_2$ formation at varied pressures and temperatures

To identify the synergistic effect between  $\text{SO}_x$  and  $\text{NO}_x$  at various pressures (1–15 atm) and temperatures (700–1100 °C), the formation of  $\text{SO}_3$  with and without the coexistence of NO are compared in Fig. 1. Likewise, the formation of  $\text{NO}_2$  with and without the coexistence of  $\text{SO}_2$ , are compared in Fig. 2 under the same pressures and temperatures. The major gas composition is selected as  $\text{O}_2 = 5\%$ ,  $\text{H}_2\text{O} = 15\%$ , with  $\text{CO}_2$  as the balance gas. In Fig. 1, the inlet  $\text{SO}_2$  concentration is 1000 ppm and NO concentration is shifted between 0 and 1000 ppm, while in Fig. 2, the inlet NO concentration is 1000 ppm and  $\text{SO}_2$  concentration is shifted between 0 and 1000 ppm. In Fig. 1, we observe a synergy between  $\text{SO}_3$  and  $\text{NO}_2$  formation for all conditions, with the degree of promotion significantly dependent on operating pressure and temperature. At elevated pressure and lower temperature,



**Fig. 1**  $\text{SO}_3$  formation with and without  $\text{SO}_x$ – $\text{NO}_x$  coexisting ( $\text{SO}_2 = \text{ppm}$ ,  $\text{O}_2 = 5\%$ ,  $\text{H}_2\text{O} = 15\%$ ,  $\text{CO}_2$  as the balance of the gas; for the dashed line,  $\text{NO} = 1000 \text{ ppm}$ ; for the solid line,  $\text{NO} = 0 \text{ ppm}$ )



**Fig. 2**  $\text{NO}_2$  formation with and without  $\text{SO}_x$ – $\text{NO}_x$  coexisting ( $\text{NO} = 1000$  ppm,  $\text{O}_2 = 5\%$ ,  $\text{H}_2\text{O} = \%$ ,  $\text{CO}_2$  as the balance of the gas; for the dashed line,  $\text{SO}_2 = 1000$  ppm; for the solid line,  $\text{SO}_2 = 0$  ppm)

$\text{SO}_3$  and  $\text{NO}_2$  formations are promoted. However, at higher temperatures above  $1100^\circ\text{C}$  and atmospheric pressure, the effect of this interaction is negligible. In an atmospheric-pressure coal-fired furnace, the residence time in the post-flame region is about 2 s. As shown in Fig. 1, at 1 atm and a time scale of 2 s, the maximum  $\text{SO}_3$  formation occurs at  $900^\circ\text{C}$ , and the conversion ratio from  $\text{SO}_2$  to  $\text{SO}_3$  is only 1.65% ( $\text{SO}_3$ , 16.5 ppm) and 0.60% ( $\text{SO}_3$ , 6 ppm) with and without  $\text{NO}$  addition, respectively. In contrast, under POC conditions (e.g., 15 atm), the residence time in the post-flame region can be longer than 10 s. As shown in Fig. 1, in the temperature range from 700 to  $1100^\circ\text{C}$  and at 15 atm, the conversion ratio from  $\text{SO}_2$  to  $\text{SO}_3$  can vary from about 5% ( $\text{SO}_3$ , 50 ppm) to 60% ( $\text{SO}_3$ , 600 ppm), depending on temperature. Such a high  $\text{SO}_3$  formation ratio indicates that low-temperature corrosion in the furnace and in the wet FGR unit of pressurized oxy-combustion system could be severe, and it will be necessary to implement specific measures to address  $\text{SO}_3$  before the flue gas temperature approaches acid dew point. For example, in the POC process designed by Washington University in St. Louis, a direct contact cooler (DCC) is used to remove  $\text{SO}_x/\text{NO}_x$  simultaneously before the flue gas temperature drops below the acid dew point [1, 19].

On the other hand, the synergistic effect also accelerates the formation of  $\text{NO}_2$ , as observed from Fig. 2. This acceleration is comparatively weak at temperatures above  $900^\circ\text{C}$  at which the  $\text{NO}_2$  formation reaches equilibrium within 10 s. The conversion ratio from  $\text{NO}$  to  $\text{NO}_2$  is as low as 1.5–3.5% ( $\text{NO}_2$ , 15–35 ppm) under POC conditions (15 atm). At a lower temperature of  $700^\circ\text{C}$ , the conversion ratio from  $\text{NO}$  to  $\text{NO}_2$  increases to above 10% under POC conditions (15 atm). Moreover, we observe that  $\text{NO}_2$  reaches equilibrium before  $\text{SO}_3$ , for all conditions studied. These observations are discussed further in “[Reaction pathway analysis on the formation of  \$\text{SO}\_3\$  and  \$\text{NO}\_2\$  at elevated pressure \(15 atm\)](#)” section.

### Reaction pathway analysis on the formation of $\text{SO}_3$ and $\text{NO}_2$ at elevated pressure (15 atm)

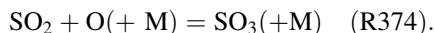
These results presented above show that the  $\text{SO}_x$ – $\text{NO}_x$  interaction promotes significantly the formation of  $\text{SO}_3$  and  $\text{NO}_2$  within a certain temperature range and at elevated pressure. In this section, to better illustrate the effect of  $\text{SO}_x$ – $\text{NO}_x$  interaction on  $\text{SO}_3$  and  $\text{NO}_2$  formation under these specific conditions, we analyze the formation pathway of  $\text{SO}_3$  and  $\text{NO}_2$  formation at elevated pressures with and

without  $\text{SO}_x\text{--NO}_x$  interaction. Based on this analysis and sensitivity studies, a 9-step reduced chemistry is developed.

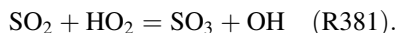
*$\text{SO}_3$  and  $\text{NO}_2$  formation pathway without  $\text{SO}_x\text{--NO}_x$  interaction at elevated pressure (15 atm)*

**$\text{SO}_3$  formation** To better illustrate the effect of  $\text{SO}_x\text{--NO}_x$  interaction on  $\text{SO}_3$  and  $\text{NO}_2$  formation at elevated pressures, we perform reaction pathway analyses on  $\text{SO}_3$  and  $\text{NO}_2$  formation without  $\text{SO}_x\text{--NO}_x$  interaction, and the results of the ROP analysis are shown in Figs. 3 and 4 for  $\text{SO}_3$  and  $\text{NO}_2$ , respectively.

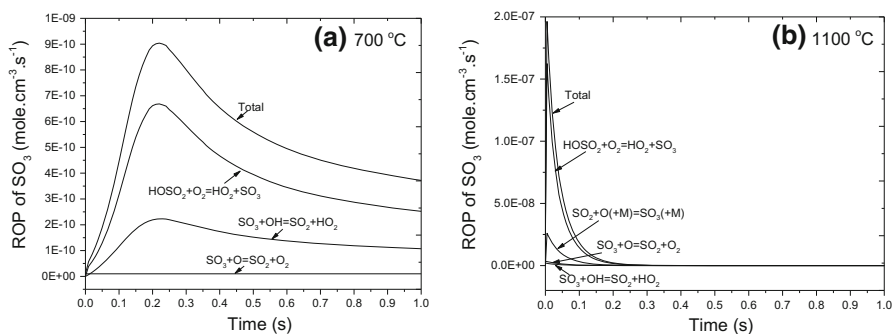
In Fig. 3 at elevated pressure of 15 atm,  $\text{SO}_3$  is formed dominantly through the oxidation of  $\text{HOSO}_2$  by  $\text{O}_2$  (R422) regardless of temperature. At 1100 °C, the preferred formation route is via the oxidation of  $\text{SO}_2$  by O radical, which is typically neglected in atmospheric conditions i.e., R374.



In addition, R381, which is the oxidizing reaction by  $\text{HO}_2$ , becomes an important route at lower temperature regions, e.g., at 700 °C,

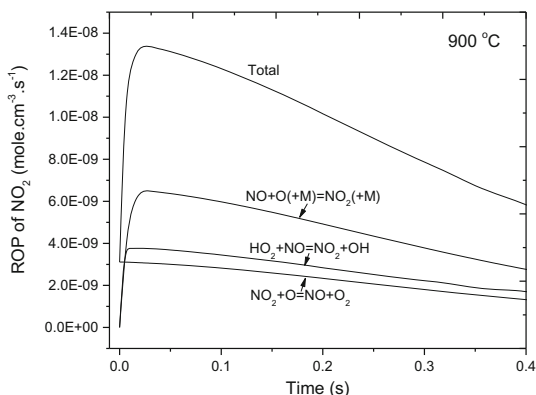


**$\text{NO}_2$  formation** As shown in Fig. 4, at elevated pressure (15 atm), the formation of  $\text{NO}_2$  is mainly via the oxidation by  $\text{HO}_2$  (R186), O (R187), and  $\text{O}_2$  (R188) independent of temperature, which are the same as the reaction routes at atmospheric pressure mentioned earlier. We also note that the contribution of each reaction varies significantly with temperatures. In this study, the route via R186 by  $\text{HO}_2$  oxidation is dominating at the higher temperature, 1100 °C and R187 and R188 by O and  $\text{O}_2$  oxidation are dominant at the lower temperatures. As shown in Fig. 4, none of these three routes (R186, R187, and R188) can be neglected at a medium temperature, say for example 900 °C.



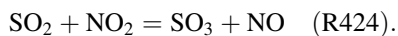
**Fig. 3** ROP analyses on  $\text{SO}_3$  formation without  $\text{SO}_x\text{--NO}_x$  interaction (15 atm,  $\text{SO}_2$  = 1000 ppm,  $\text{O}_2$  = 5%,  $\text{H}_2\text{O}$  = 15%,  $\text{CO}_2$  as the balance of the gas)

**Fig. 4** ROP analyses on  $\text{NO}_2$  formation without  $\text{SO}_x\text{--NO}_x$  interaction (15 atm,  $\text{NO} = 1000$  ppm,  $\text{O}_2 = 5\%$ ,  $\text{H}_2\text{O} = 15\%$ ,  $\text{CO}_2$  as the balance of the gas)

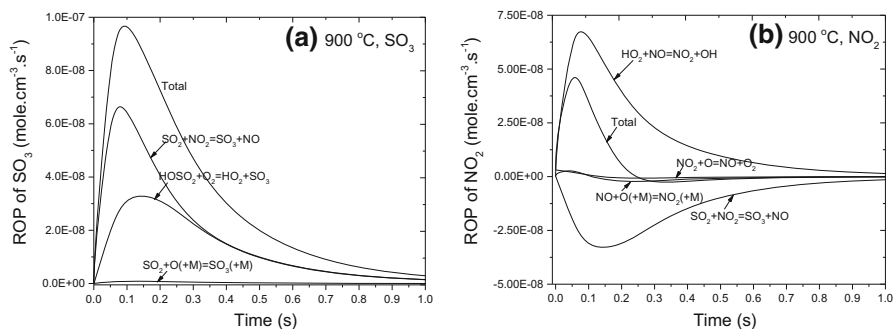


$\text{SO}_3$  and  $\text{NO}_2$  formation pathway with  $\text{SO}_x\text{--NO}_x$  interaction at elevated pressure (15 atm)

Under conditions where  $\text{SO}_x$  and  $\text{NO}_x$  coexist at elevated pressure (15 atm), ROP analysis results for  $\text{SO}_3$  and  $\text{NO}_2$  formation are shown in Fig. 5. Compared with the ROP analysis results in Figs. 3 and 4, when  $\text{SO}_x$  and  $\text{NO}_x$  do not coexist, a significant contribution to  $\text{SO}_3$  formation and  $\text{NO}_2$  destruction from reaction R424 is noticeable, and this agrees with the experimental results of Mueller et al. [11]. The net reaction rate of molecular reaction R424 is determined by the concentrations of  $\text{SO}_2$ ,  $\text{NO}_2$ ,  $\text{SO}_3$  and  $\text{NO}$ , and is important for the  $\text{SO}_x\text{--NO}_x$  system to reach equilibrium.



Under the conditions evaluated and before the system reached equilibrium, R424 retains the forward direction, producing  $\text{SO}_3$  but consuming  $\text{NO}_2$ . This explains the phenomenon observed in Fig. 2 where  $\text{NO}_2$  reaches equilibrium much earlier than  $\text{SO}_3$  in the environment with coexisting  $\text{SO}_x\text{--NO}_x$ . Routes for  $\text{NO}_2$  formation (Figs. 5b) also exhibit a big difference if  $\text{SO}_x$  and  $\text{NO}_x$  coexist in the reactive



**Fig. 5** ROP analyses on (a)  $\text{SO}_3$  and (b)  $\text{NO}_2$  formation with  $\text{SO}_x\text{--NO}_x$  interaction (15 atm,  $\text{SO}_2 = 1000$  ppm,  $\text{NO} = 1000$  ppm,  $\text{O}_2 = 5\%$ ,  $\text{H}_2\text{O} = 15\%$ ,  $\text{CO}_2$  as the balance of the gas)

**Table 1** The dominant reaction pathway of SO<sub>3</sub> and NO<sub>2</sub> formation at elevated pressures (unit: mol, s, K, cal)

| New number | Old number | Reaction                                                        | A                     | $\beta$ | E      | Source                   |
|------------|------------|-----------------------------------------------------------------|-----------------------|---------|--------|--------------------------|
| SR1        | R87, R287  | $\text{OH} + \text{HO}_2 = \text{O}_2 + \text{H}_2\text{O}$     | $2.89 \times 10^{13}$ | 0       | – 497  | Baulch et al. [20]       |
| SR2        | R186       | $\text{HO}_2 + \text{NO} = \text{NO}_2 + \text{OH}$             | $2.11 \times 10^{12}$ | 0       | – 480  | GRI-Mech 3.0 [14]        |
| SR3        | R376       | $\text{SO}_2 + \text{OH}(+\text{M}) = \text{HOSO}_2(+\text{M})$ | $5.70 \times 10^{12}$ | – 0.3   | 0      | Li et al. [21]           |
| SR4        | R422       | $\text{HOSO}_2 + \text{O}_2 = \text{HO}_2 + \text{SO}_3$        | $7.80 \times 10^{11}$ | 0       | 656    | Li et al. [21]           |
| SR5        | R424       | $\text{SO}_2 + \text{NO}_2 = \text{SO}_3 + \text{NO}$           | $6.30 \times 10^{12}$ | 0       | 27,000 | Armitage and Cullis [22] |



mixture. With  $\text{SO}_x$ – $\text{NO}_x$  coexisting at 15 atm, the only notable route for  $\text{NO}_2$  formation is via R186 by  $\text{HO}_2$  oxidation, while the routes via R187 and R188 by O and  $\text{O}_2$  oxidation become unimportant. At high temperatures of 900 and 1100 °C, because of the rapid production of  $\text{NO}_2$  at the initial stage, the backward reaction pathway of R187 is favored, leading to the consumption of  $\text{NO}_2$ , another reason for the  $\text{NO}_2$  reaching equilibrium earlier than  $\text{SO}_3$  especially at higher temperatures.

### The dominant reaction pathway of $\text{SO}_3$ and $\text{NO}_2$ formation at elevated pressures

Based on the above analysis, a dominant reaction pathway of  $\text{SO}_3$  and  $\text{NO}_2$  formation at elevated pressures can be obtained, which mainly includes five reaction steps (R87/287, R186, R376, R422, R424). These five reaction steps rearranged and renamed in Table 1 with SR# denoting the reaction number (e.g., ‘SR1’ means the first reaction in this reaction pathway). These five reactions of skeletal mechanism can be classified into three groups: (1) SR1 is the initiation reaction step that triggers production of initial OH and  $\text{HO}_2$  radicals which allows cyclic reactions to occur; (2) SR2–SR4 are the cyclic reaction group and they are important pathways for producing  $\text{SO}_3$  and  $\text{NO}_2$ , and (3) SR5 is an important pathway for more production of  $\text{SO}_3$  but the consumption of  $\text{NO}_2$ .

### Conclusions

In the present work, the synergy between  $\text{SO}_x$  and  $\text{NO}_x$  mechanisms was investigated and its role on the formation of  $\text{SO}_3$  and  $\text{NO}_2$  was kinetically evaluated under different pressures and temperatures, using a developed detailed mechanism based on GRI-Mech 3.0. The main conclusions are as follows:

The interaction of  $\text{SO}_x$  and  $\text{NO}_x$  significantly accelerates the conversion rates of  $\text{SO}_2$  to  $\text{SO}_3$  and  $\text{NO}$  to  $\text{NO}_2$ , and the acceleration is much stronger at elevated pressures and lower temperatures. Due to the strong interaction between  $\text{SO}_x$  and  $\text{NO}_x$ , the formation pathways of  $\text{SO}_3$ , through  $\text{HOSO}_2 + \text{O}_2 = \text{HO}_2 + \text{SO}_3$ , and  $\text{NO}$ , through  $\text{HO}_2 + \text{NO} = \text{NO}_2 + \text{OH}$ , are dramatically promoted. These two pathways are linked by the reaction  $\text{SO}_2 + \text{OH} + \text{M} = \text{HOSO}_2 + \text{M}$ , resulting in a ‘strong’ cycle, which can be represented by the global reaction  $\text{NO} + \text{SO}_2 + \text{O}_2 = \text{NO}_2 + \text{SO}_3$ . This cycle together with  $\text{SO}_2 + \text{NO}_2 = \text{SO}_3 + \text{NO}$  dominate the formation and destruction of both  $\text{SO}_3$  and  $\text{NO}_2$  at elevated pressures.

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