fluids

MDPI

Review

Instability and Convection in Rotating Porous Media: A Review

Peter Vadasz [1,*]

[1] Department of Mechanical Engineering, Northern Arizona University; e-mail: Peter.Vadasz@nau.edu
* Correspondence: Peter.Vadasz@nau.edu; Tel.: +1-928-523-5251

Academic Editor: Andrew S. Rees, Antonio Barletta
Received: date; Accepted: date; Published: date

Abstract: A review on instability and consequent natural convection in rotating porous media is presented. Taylor-Proudman columns and geostrophic flows exist in rotating porous media just the same as in pure fluids. The latter leads to a tendency towards two-dimensionality. Natural convection resulting from density gradients in a gravity field as well as natural convection induced by density gradients due to the centripetal acceleration are being considered. The former is the result of gravity-induced buoyancy, the latter is due to centripetally-induced buoyancy. The effect of Coriolis acceleration is also discussed. Linear stability analysis as well as weak nonlinear solutions are being derived and presented.

Keywords: Rotating Flows; Porous Media; Natural Convection; Instability; Taylor-Proudman column; Centrifugal Buoyancy, Coriolis Acceleration.

1. Introduction

The research into the effects of rotation on the flow and transport phenomena in porous media is driven by the fundamental scientific significance as well as by engineering and geophysical applications. To be specific, one refers to flows in porous geological formations subject to earth rotation, to the flow of magma in the earth mantle close to the earth crust (Fowler [1]) as geophysical applications. The food process industry, chemical process industry, centrifugal filtration processes, and rotating machinery are examples of engineering applications.

For example, packed bed mechanically agitated vessels are being used in the food processing and chemical engineering industries in batch processes. The packed bed consists of solid particles or fibers of material, which form the solid matrix while fluid flows through the pores. As the solid matrix rotates, due to the mechanical agitation, a rotating frame of reference is a necessity when investigating these flows. The role of the flow of fluid through these beds can vary from drying processes to extraction of soluble components from the solid particles. Two examples of such processes are the molasses subject to centrifugal crystal separation in the sugar milling industry and the extraction of sodium alginate from kelp. Additional industrial applications are being presented in Vadasz [2,3,4], Nield and Bejan [5,6], and Bejan [7] in comprehensive reviews of the fundamentals of heat convection in porous media.

With the emerging utilization of the porous medium approach in non-traditional fields, including some applications in which the solid matrix is subjected to rotation (like physiological processes in human body subject to rotating trajectories, cooling of electronic equipment in a rotating radar, cooling of turbo-machinery blades, or cooling of rotors of electric machines) a thorough understanding of the flow in a rotating porous medium becomes essential. Its results can then be used in the more established industrial applications like food processing, chemical

engineering or centrifugal processes, as well as to the less traditional applications of the porous medium approach.

The fundamental equations and assumptions applicable to single-phase convective heat transfer were presented by Dagan [8], Acharya [9]. A review of the effects of rotation on heat transfer in general was presented by Wiesche [10].

Reviews of the fundamentals of flow and heat transfer in rotating porous media were presented by Vadasz [2, 3, 4, 11, 12, 13, 14, 15].

No reported results were found on isothermal flow in rotating porous media prior to 1994. Research of a pioneering nature on natural convection in rotating porous media were reported by Rudraiah et al [16], Patil and Vaydianathan [17], Jou and Liaw [18, 19], and Palm and Tyvand [20]. Nield [21] found that the effect of rotation on convection in a porous medium attracted limited interest in a comprehensive review of the stability of convective flows in porous media.

The fact that isothermal flow in homogeneous porous media following Darcy law is irrotational and hence the effect of rotation on this flow is insignificant contributed to the limited interest for this type of flow. However, for natural convection in a non-isothermal homogeneous porous medium or for a heterogeneous medium with spatially dependent permeability the flow is not irrotational anymore, and therefore the effects of rotation become significant. More recent interest in this type flow, during the past three decades, led to an increased number of publications. For example, Nield [22], Auriault et al [23, 24], Govender [25, 26], Havstad and Vadasz [27], Vadasz and Havstad [28], Govender and Vadasz [29, 30, 31, 32], Vadasz [2, 3, 4, 11, 12, 13, 14, 15, 33, 34, 35, 36, 37, 38, 39, 40, 41, 42], Vadasz and Govender [43, 44], Vadasz and Heerah [45], Vadasz and Olek [46], Bhadauria [47], Malashetty, Pop, Heera [48], Vanishree and Siddheshwar [49], Agarwal et al [50], Bhadauria et al [51], Agarwall and Bhadauria [52], Malashetty et al [53], Malashetty and Swamy [54], Rana and Agarwal [55], Yadav et al [56], Rashidi et al [57], Makinde et al [58], Straughan [59], Lombardo and Mulone [60], Falsaperla, Mulone and Straughan [61, 62], Falsaperla, Giacobbe and Mulone [63], Capone and De Luca [64], Capone and Rionero [65], Capone and De Luca [66].

2. Governing Equations

The equations governing the flow and heat transfer in rotating porous media are presented in a dimensionless form subject to the assumptions of constant angular velocity of rotation, Boussinesq approximation (Boussinesq [67]), and local thermal equilibrium (LTE or Lotheq). The latter implies that the difference in the local temperature between the solid and fluid phases in the porous medium is insignificantly small and can be neglected. Boussinesq approximation [67] applicable to buoyancy flows states that the density id constant in all terms of the governing equations except the buoyancy terms in the momentum equation. The notation being used refers to symbols having an asterisk as dimensional, while symbols without an asterisk represent dimensionless quantities, except symbols carrying the subscript "c" representing characteristic values, or the subscript "o" representing reference values, both being dimensional. The continuity equation is presented in the form

$$\nabla \cdot \boldsymbol{V} = 0 \tag{1}$$

where $\boldsymbol{V} = u\,\hat{\boldsymbol{e}}_x + v\,\hat{\boldsymbol{e}}_y + w\,\hat{\boldsymbol{e}}_z$ is the filtration velocity vector presented in Cartesian coordinates, u, v, w are the components of the the filtration velocity vector in the x, y, z directions, respectively, and $\hat{\boldsymbol{e}}_x, \hat{\boldsymbol{e}}_y, \hat{\boldsymbol{e}}_z$ are unit vectors in the x, y, z directions, respectively. The operator $\nabla \cdot$ is the divergence operator defined in the form $\nabla \cdot \equiv \left[\hat{\boldsymbol{e}}_x \partial(\ )/\partial x + \hat{\boldsymbol{e}}_y \partial(\ )/\partial y + \hat{\boldsymbol{e}}_z \partial(\ )/\partial x\right] \cdot$.

The momentum transport in porous media is governed primarily by the Darcy law, which is presented in the rotating frame of reference of the solid matrix in the following dimensionless form

$$\boldsymbol{V} = -N_p \nabla p + Fr\,\rho\,\hat{\boldsymbol{e}}_g - Cn\,\rho\,\hat{\boldsymbol{e}}_\omega \times \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) - \frac{\rho}{Ek_\Delta}\hat{\boldsymbol{e}}_\omega \times \boldsymbol{V} \tag{2}$$

where four dimensionless groups emerged, i.e. a pressure number N_p (equivalent to a porous media Euler number where $\mu_* l_c / K_*$ replaces $\rho_o u_c$), a porous media Froude number Fr, a centrifugal number Cn, and a porous media Ekman number Ek_Δ defined in the form

$$N_p = \frac{K_* \Delta p_c}{\mu_* u_c l_c} \quad , \quad Fr = \frac{g_* K_*}{\nu_* u_c} \quad , \quad Cn = \frac{K_* \omega_*^2 l_c}{\nu_* u_c} \quad , \quad Ek_\Delta = \frac{\phi \nu_*}{2\omega_* K_*} \tag{3}$$

and where K_* and ϕ are the permeability and the porosity of the porous matrix, respectively, μ_* is the dynamic viscosity, ρ_o is a constant reference value of the fluid density used to convert the density into a dimensionless form, $\nu_* = \mu_* / \rho_o$ is the kinematic viscosity of the fluid, ω_* is the constant angular velocity of rotation, p and ρ are the dimensionless pressure and density, respectively, $\hat{\boldsymbol{e}}_g$ is a unit vector in the direction of the gravity acceleration, $\hat{\boldsymbol{e}}_{\boldsymbol{\omega}}$ is a unit vector in the direction of the angular velocity of roation, and $\boldsymbol{X} = x\hat{\boldsymbol{e}}_x + y\hat{\boldsymbol{e}}_y + z\hat{\boldsymbol{e}}_z$ is the position vector measured from the axis of rotation. Also l_c, u_c, p_c are constant dimensional characteristic values of length, filtration velocity, and pressure, respectively, used to convert the space variables, the filtration velocity, and the pressure into dimensionless forms. The gradient operator in equation (2) is defined in the form $\nabla \equiv \left[\hat{\boldsymbol{e}}_x \partial(\ ) / \partial x + \hat{\boldsymbol{e}}_y \partial(\ ) / \partial y + \hat{\boldsymbol{e}}_z \partial(\ ) / \partial x\right]$.

The third term in the brackets in equation (2) represents the centrifugal force while the fourth term represents the Coriolis acceleration.

When fast transients or high frequency effects are of interest there is another extension to the Darcy equation that is applicable. Then, the time resolution obtained by assuming a very fast reaction of Darcy flow to changes and therefore the quasi-steady approximation which is inherent in the formulation of the Darcy law is not sufficient and a time derivative of the filtration velocity needs to be incorporated leading to the following dimensionless form of the extended Darcy equation in a rotating frame of reference

$$\frac{DaReM_f}{\phi} \rho \frac{\partial \boldsymbol{V}}{\partial t} + \boldsymbol{V} = -N_p \nabla p + Fr\, \rho\, \hat{\boldsymbol{e}}_g - Cn\, \rho\, \hat{\boldsymbol{e}}_\omega \times \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) - \frac{\rho}{Ek_\Delta} \hat{\boldsymbol{e}}_\omega \times \boldsymbol{V} \tag{4}$$

where the additional dimensionless groups that emerged are the Darcy number Da, and the Reynolds number Re

$$Da = \frac{K_*}{l_c^2} \quad , \quad Re = \frac{u_c l_c}{\nu_*} \tag{5}$$

and M_f is a ratio of heat capacities that its the definition will follow later. The corresponding length scale is a macro-level length scale, not the pore-size, despite the fact that it is the porous media filtration velocity that emerged in the definition of the Reynolds number. However the Reynolds number appears in equation (4) in a product combination with the Darcy number, bringing therefore the pore-scale effects into account too.

Following the definition of the dimensionless temperature in the form

$$T = \frac{\left(T_* - T_o\right)}{\Delta T_c} \tag{6}$$

where T_* is the dimensional temperature, T_o is a reference value of temperature, and ΔT_c is a characteristic temperature difference, the dimensionless form of the energy equation subject to local thermal equilibrium (LTE or Lotheq) is presented in the form

$$\frac{\partial T}{\partial t} + \boldsymbol{V} \cdot \nabla T = \frac{1}{Pe} \nabla^2 T \tag{7}$$

where Peclet number emerged as an additional dimensionless group, defined in the form

$$Pe = \frac{u_c l_c}{\alpha_{e^*}} = Pr\, Re \tag{8}$$

where the porous media Prandtl number Pr is defined by

$$Pr = \frac{\nu_*}{\alpha_{e^*}} \tag{9}$$

The effective thermal diffusivity of the porous medium appearing in (8) and (9) is defined as $\tilde{\alpha}_{e^*} = k_{e^*} / \gamma_{e^*}$ and $M_f = \gamma_{f^*} / \gamma_{e^*}$ is the heat capacity ratio, i.e. the ratio between the effective heat capacity of the fluid phase and the effective heat capacity of the porous medium, where $\gamma_{e^*} = \gamma_{s^*} + \gamma_{f^*}$, $k_{e^*} = k_{s^*} + k_{f^*}$ are the effective heat capacity and effective thermal conductivity of the porous medium and subscripts "s" and "f" refer to the solid and fluid phases, respectively. Then the adjusted effective thermal diffusivity is defined as follows $\alpha_{e^*} = \tilde{\alpha}_{e^*} / M_f = k_{e^*} / \gamma_{f^*}$.

To complete the governing equations one needs a relationship between the density, temperature and pressure (and solute concentration when the fluid is a solution of soluble substances, e.g. salt in water, alcohol in water, etc., in which case an additional species equation needs to be added to). A linear approximation for this relationship is usually sufficiently accurate if the temperature and pressure differences are no excessively high. The dimensionless form of the linear approximation of the equation of state can be obtained by using the definition of the dimensionless temperature from equation (6) and the dimensionless pressure in the form $p = (p_* - p_o) / \Delta p_c$. Then the equation of state becomes

$$\rho = \left[1 - \beta_T T + \beta_p p\right] \tag{10}$$

where $\rho = \rho_* / \rho_o$ is the dimensionless density, and $\beta_T = \beta_{T^*} \Delta T_c$, $\beta_p = \beta_{p^*} \Delta p_c$ are the dimensionless thermal expansion and pressure compression coefficients, respectively. For most fluid flows and especially for incompressible flows, i.e. flows of liquids, $\beta_p \ll \beta_T$. Therefore the common approximation of the dimensionless equation of state is

$$\rho = \left[1 - \beta_T T\right] \tag{11}$$

There are some identities relevant to flows in a rotating frame of reference and in buoyancy flows that are useful in the following derivations. These identities are

$$\hat{\boldsymbol{e}}_g = \nabla\left(\hat{\boldsymbol{e}}_g \cdot \boldsymbol{X}\right) \tag{12}$$

$$\hat{\boldsymbol{e}}_\omega \times \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) = -\nabla\left[\frac{1}{2}\left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) \cdot \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right)\right] \tag{13}$$

$$\hat{\boldsymbol{e}}_\omega \times \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) = \left(\hat{\boldsymbol{e}}_\omega \cdot \boldsymbol{X}\right)\hat{\boldsymbol{e}}_\omega - \boldsymbol{X} \tag{14}$$

Their proof can be found in Vadasz [3].

Although for a significantly high number of practical instances Darcy's model (or its extension) for a rotating frame of reference is sufficient for representing the effects of rotation, non-Darcy models have been used as well. Their relevance and limitations are subject to professional discourse (e.g. Nield [68, 69, 70] and Vafai and Kim [71]).

3. Taylor-Proudman Columns and Geostrophic Flow in Rotating Porous Media

By using equations (12) and (13), considering isothermal conditions (no heat transfer) and consequently the density is constant $\rho_* = \rho_o$ hence $\rho = 1$, Darcy equation (2) becomes

$$\boldsymbol{V} = -\nabla\left[N_p p - Fr\left(\hat{\boldsymbol{e}}_g \cdot \boldsymbol{X}\right) - Cn\left(\frac{1}{2}\left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) \cdot \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right)\right)\right] - \frac{1}{Ek_\Delta}\hat{\boldsymbol{e}}_\omega \times \boldsymbol{V} \tag{15}$$

The term under the common gradient operator is a reduced pressure p_r, defined as

$$p_r = N_p p - Fr\left(\hat{\boldsymbol{e}}_g \cdot \boldsymbol{X}\right) - \frac{Cn}{2}\left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) \cdot \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right) \tag{16}$$

By using (16) and choosing the direction of the angular velocity of rotation to be aligned with the vertical axis, i.e. $\hat{\boldsymbol{e}}_{\boldsymbol{\omega}} = \hat{\boldsymbol{e}}_z$, the Darcy equation (2) can be presented in the following rearranged form

$$\left[Ek_\Delta + \hat{\boldsymbol{e}}_z \times\right]\boldsymbol{V} = -\nabla\left(Ek_\Delta p_r\right) \tag{17}$$

For typical values of viscosity, porosity and permeability the range of variation of Ekman number can be evaluated in some engineering applications. Consequently, the angular velocity may vary from 10 rpm to 10,000 rpm leading to Ekman numbers in the range from $Ek_\Delta = 1$ to $Ek_\Delta = 10^{-3}$. The latter value is very small, pertaining to the conditions considered here. Therefore, in the limit of $Ek_\Delta \to 0$, say $Ek_\Delta = 0$, equation (17) takes the simplified form

$$\hat{\boldsymbol{e}}_z \times \boldsymbol{V} = -\nabla\left(Ek_\Delta p_R\right) \tag{18}$$

and the effect of permeability variations disappears. Taking the "curl" of equation (18) leads to

$$\nabla \times \left(\hat{\boldsymbol{e}}_z \times \boldsymbol{V}\right) = 0 \tag{19}$$

Evaluating the "curl" operator on the cross product of the left-hand side of equation (19) leads to

$$\left(\hat{\boldsymbol{e}}_z \cdot \nabla\right)\boldsymbol{V} = 0 \tag{20}$$

Equation (20) is identical to the Taylor-Proudman theorem for pure fluids (non-porous domains); it thus represents the proof of the Taylor-Proudman theorem in porous media, and can be presented in the following simplified form

$$\frac{\partial \boldsymbol{V}}{\partial z} = 0 \tag{21}$$

The conclusion expressed by equation (21) is that $\boldsymbol{V} = \boldsymbol{V}(x, y)$, i.e. it cannot be a function of z, where z is the direction of the angular velocity vector. This means that all filtration velocity components can vary only in the plane perpendicular to the angular velocity vector. This result leads to the existence of Taylor-Proudman columns in rotating porous media as presented in detail by Vadasz [3]. The consequence of this result can be demonstrated by considering a particular example that was presented by Vadasz [36] (see Greenspan [72] for the corresponding example in pure fluids).

A further significant consequence of equation (21) is represented by a geostrophic type of flow. Taking the z-component of equation (21) yields $\partial w/\partial z = 0$, and the continuity equation (1) becomes two dimensional

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{22}$$

Therefore the flow at high rotation rates has a tendency towards two-dimensionality and a stream function, ψ, can be introduced for the flow in the $x - y$ plane in the form

$$u = -\frac{\partial \psi}{\partial y}; \quad v = \frac{\partial \psi}{\partial x} \tag{23}$$

which satisfies identically the continuity equation (1). Substituting u and v with their stream function representation given by equation (23) into equation (18) yields

$$\frac{\partial \psi}{\partial x} = \frac{\partial\left(Ek_\Delta p_R\right)}{\partial x} \tag{24}$$

$$\frac{\partial \psi}{\partial y} = \frac{\partial\left(Ek_\Delta p_R\right)}{\partial y} \tag{25}$$

As both the pressure and the stream function can be related to an arbitrary reference value, the conclusion from equations (24) and (25) is that the stream function and the pressure are the same in the limit of high rotation rates ($Ek \to 0$). This type of geostrophic flow means that isobars represent streamlines at the leading order, for $Ek \to 0$.

4. Natural Convection due to Centrifugal Buoyancy

Natural convection is the effect of flow and convection heat transfer due to the existence of density gradients in a body force field (such as gravity or centrifugal force field). As density depends on temperature as demonstrated in the derivation of the equation of state, temperature

gradients may create natural convective flows when a body force field is present. What characterizes natural convection is the lack of a known value of characteristic filtration velocity that can be applied upfront in a problem. No characteristic velocity can be specified because the latter is dictated by the temperature gradients and their resulting buoyancy rather than being known upfront. Therefore a sensible choice of u_c would be $u_c = \alpha_{e^*}/l_c$. With this choice of u_c the Froude number Fr, the pressure number N_p, and the centrifugal dimensionless group Cn in equations (12) and (14) become $Fr = g_* K_* l_c / \nu_* \alpha_{e^*}$, $N_p = K_* \Delta p_c / \mu_* \alpha_{e^*}$, $Cn = \omega_*^2 l_c^2 K_* / \nu_* \alpha_{e^*}$. Without loss of generality for the same reason as for the filtration velocity one can chose the characteristic pressure difference to be such that the pressure number N_p becomes unity, i.e. $\Delta p_c = \mu_* \alpha_{e^*} / K_*$ leading to $N_p = 1$. Also the Reynolds number in equation (5) renders into the reciprocal Prandtl number $Re = \alpha_{e^*}/\nu_* = 1/Pr$ and the Peclet number in equations (7) and (8) becomes equal to one by definition $Pe = u_c l_c / \alpha_{e^*} = \alpha_{e^*} l_c / l_c \alpha_{e^*} = 1$. One may define the effective Prandtl number in terms of the effective thermal diffusivity $\tilde{\alpha}_{e^*}$ (see the equation and the text following equation (9)) $Pr_e = \nu_* / \tilde{\alpha}_{e^*} = Pr / M_f$. Then the coefficient to the time derivative term in equation (4) becomes $DaReM_f / \phi = DaM_f / \phi Pr = Da / \phi Pr_e = 1/Va$ a new dimensionless group that Straughan [73] named the Vadasz number (Va), or the Vadasz coefficient named by Straughan [73] (see also Sheu [74] and Govender [26]). By using equations (11), (12) and (13) leads to transforming equations (2) and (4) into the following form

$$\boldsymbol{V} = -\nabla p_r + Ra_g T\,\hat{\boldsymbol{e}}_{\boldsymbol{g}} - Ra_\omega T\left[\left(\hat{\boldsymbol{e}}_\omega \cdot \boldsymbol{X}\right)\hat{\boldsymbol{e}}_\omega - \boldsymbol{X}\right] - \frac{1}{Ek_\Delta}\hat{\boldsymbol{e}}_\omega \times \boldsymbol{V} \tag{26}$$

$$\frac{1}{Va}\frac{\partial \boldsymbol{V}}{\partial t} + \boldsymbol{V} = -\nabla p_r + Ra_g T\,\hat{\boldsymbol{e}}_{\boldsymbol{g}} - Ra_\omega T\left[\left(\hat{\boldsymbol{e}}_\omega \cdot \boldsymbol{X}\right)\hat{\boldsymbol{e}}_\omega - \boldsymbol{X}\right] - \frac{1}{Ek_\Delta}\hat{\boldsymbol{e}}_\omega \times \boldsymbol{V} \tag{27}$$

The product of β_T by Fr and Cn produced two new dimensionless groups in the form of the gravity related Rayleigh number and the centrifugal Rayleigh number, respectively in the form

$$Ra_g = Fr\,\beta_T = \frac{\beta_{T^*} \Delta T_c g_* K_* l_c}{\nu_* \alpha_{e^*}} \tag{28}$$

$$Ra_\omega = Cn\,\beta_T = \frac{\beta_{T^*} \Delta T_c \omega_*^2 l_c^2 K_*}{\nu_* \alpha_{e^*}} \tag{29}$$

The particular cases when $\hat{\boldsymbol{e}}_{\boldsymbol{g}} = -\hat{\boldsymbol{e}}_z$ and $\hat{\boldsymbol{e}}_\omega = \hat{\boldsymbol{e}}_z$ will be considered later. Subject to this orientation of the gravity and angular velocity of rotation equations (26) and (27) take the form

$$\boldsymbol{V} = -\nabla p_r + Ra_g T\,\hat{\boldsymbol{e}}_z - Ra_\omega T\left(x\,\hat{\boldsymbol{e}}_{\boldsymbol{x}} + y\,\hat{\boldsymbol{e}}_{\boldsymbol{y}}\right) - \frac{1}{Ek_\Delta}\hat{\boldsymbol{e}}_z \times \boldsymbol{V} \tag{30}$$

$$\frac{1}{Va}\frac{\partial \boldsymbol{V}}{\partial t} + \boldsymbol{V} = -\nabla p_r + Ra_g T\,\hat{\boldsymbol{e}}_z - Ra_\omega T\left(x\,\hat{\boldsymbol{e}}_{\boldsymbol{x}} + y\,\hat{\boldsymbol{e}}_{\boldsymbol{y}}\right) - \frac{1}{Ek_\Delta}\hat{\boldsymbol{e}}_z \times \boldsymbol{V} \tag{31}$$

The vector $\boldsymbol{r} = (x\,\hat{\boldsymbol{e}}_x + y\,\hat{\boldsymbol{e}}_y)$ in equations (30) and (31) represents the perpendicular radius vector from the axis of rotation to any point in the flow domain.

Three dimensionless groups emerged in equation (30) when fast transients or high frequencies are not of interest. These dimensionless groups control the significance of the different phenomena. Therefore, the value of Ekman number (Ek_Δ) controls the significance of the Coriolis effect, and the ratio between the gravity related Rayleigh number (Ra_g) and centrifugal Rayleigh number (Ra_ω) controls the significance of gravity with respect to centrifugal forces as far as natural convection is concerned. This ratio is $Ra_g / Ra_\omega = g_* / \omega_*^2 l_c$. When fast transients or high frequencies are of interest equation (27) is to be considered. In such a case one additional dimensionless group emerged, the Va number representing the ratio between two characteristic frequencies, i.e. the fluid flow frequency $\omega_{\nu^*} = \phi \nu_* / K_*$ and the thermal diffusion frequency $\omega_{\alpha^*} = \tilde{\alpha}_{e^*} / l_c^2$, i.e.

$Va = \omega_{v^*}/\omega_{\alpha^*} = \phi\nu_* l_c^2/K_*\tilde{\alpha}_{e^*} = \phi Pr_e/Da$, or alternatively the ratio between two time scales, i.e. the thermal diffusion time scale $\tau_{\alpha^*} = l_c^2/\tilde{\alpha}_{e^*}$, and the fluid flow time scale $\tau_{v^*} = K_*/\phi\nu_*$, i.e. $Va = \tau_{\alpha^*}/\tau_{v^*} = \phi\nu_* l_c^2/K_*\tilde{\alpha}_{e^*} = \phi Pr_e/Da$. In addition to such cases equation (27) should be used also when the effective Prandtl number is of the order of magnitude of Darcy number, i.e. $Pr_e = O(Da)$ i.e. a very small number (as $Da << 1$ in most porous media). Such small values of the Prandtl number are typical for liquid metals. In such cases too the time derivative term in equation (27) should be retained.

Considering the Darcy regime subject to a centrifugal body force and by neglecting gravity effects ($Ra_g/Ra_\omega << 1$) equations (1), (7) and (26) with $Ra_g = 0$ and $Pe = 1$ represent the mathematical model for this case. The objective in the first instance is to establish the convective flow under small rotation rates, then $Ek >> 1$, and as a first approximation the Coriolis effect can be neglected, i.e., $Ek \to \infty$. Following these conditions the governing equations become (by using identity (14))

$$\nabla \cdot \boldsymbol{V} = 0 \tag{32}$$

$$\boldsymbol{V} = -\left[\nabla p - Ra_\omega T\, \hat{\boldsymbol{e}}_\omega \times \left(\hat{\boldsymbol{e}}_\omega \times \boldsymbol{X}\right)\right] \tag{33}$$

$$\frac{\partial T}{\partial t} + \boldsymbol{V} \cdot \nabla T = \nabla^2 T \tag{34}$$

There are three cases corresponding to the relative orientation of the temperature gradient with respect to the centrifugal body force as presented in Figure 1. Case 1(a) in Figure 1 corresponds to a temperature gradient, which is perpendicular to the direction of the centrifugal body force and leads to unconditional convection. The solution representing this convection pattern is presented by Vadasz [34, 3, 4]. Cases 1(b) and 1(c) in Figure 1 corresponding to temperature gradients collinear with the centrifugal body force represent stability problems and hence our present focus. The objective is then to establish the stability condition as well as the convection pattern when this stability condition is not satisfied.

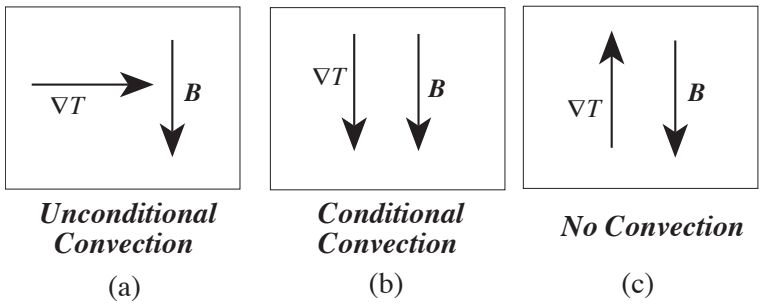


Figure 1. The effect of the relative orientation of the temperature gradient with respect to the body force on the setup of convection.

An example of a case when the imposed temperature is perpendicular to the centrifugal body force is a rectangular porous domain rotating about the vertical axis, heated from above and cooled from below. For this case the centrifugal buoyancy term in equation (33) becomes $Ra_\omega T\, x\, \hat{\boldsymbol{e}}_x$ leading to

$$\boldsymbol{V} = -\nabla p - Ra_\omega T\, x\, \hat{\boldsymbol{e}}_x \tag{35}$$

An analytical two-dimensional solution to this problem (see Figure 2) for a small aspect ratio of the domain was presented by Vadasz [34, 3, 4]. The solution to the non-linear set of partial differential equations was obtained through an asymptotic expansion of the dependent variables in terms of a small parameter representing the aspect ratio of the domain.

The convection in the core region far from the sidewalls was the objective of the investigation. To first order accuracy, the heat transfer coefficient represented by the Nusselt number was evaluated in the form

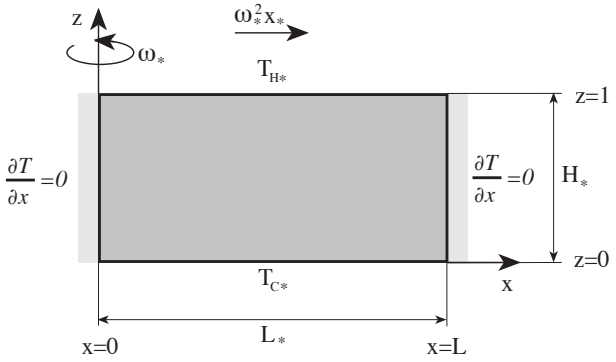


Figure 2: A rotating rectangular porous domain heated from above, cooled from below, and insulated on its sidewalls. (courtesy Elsevier Science Ltd.)

$$Nu = -\left[1 + \frac{Ra_\omega}{24} + O\left(H^2\right)\right] \tag{36}$$

where Nu is the Nusselt number and the length scale used in the definition of Ra_ω, equation (54), was $l_c = H_*$. Vadasz [37] used a different approach to solve a similar problem without the restriction of a small aspect ratio. A direct extraction and substitution of the dependent variables was found to be useful for de-coupling the non-linear partial differential equations, resulting in a set of independent non-linear ordinary differential equations, which was solved analytically. To obtain an analytical solution to the non-linear convection problem we assume that the vertical component of the filtration velocity, w, and the temperature T are independent of x, i.e., $\partial w/\partial x = \partial T/\partial x = 0 \quad \forall x \in (0, L)$, being functions of z only. It is this assumption that will subsequently restrict the validity domain of the results to moderate values of Ra_ω (practically $Ra_\omega < 5$). Subject to the assumptions of two-dimensional flow $v = 0$ and $\partial(\cdot)/\partial y = 0$ and that w and T are independent of x the governing equations take the form

$$\frac{\partial u}{\partial x} + \frac{\mathrm{d}w}{\mathrm{d}z} = 0 \tag{37}$$

$$u = -\frac{\partial p}{\partial x} - Ra_\omega \, xT \tag{38}$$

$$w = -\frac{\partial p}{\partial z} \tag{39}$$

$$\frac{\mathrm{d}^2 T}{\mathrm{d}z^2} - w\frac{\mathrm{d}T}{\mathrm{d}z} = 0 \tag{40}$$

The method of solution consists of extracting T from equation (38) and expressing it explicitly in terms of $u, \partial p/\partial x$ and x. This expression of T is then introduced into equation (40) and the derivative $\partial/\partial x$ is applied to the result. Then, substituting the continuity equation (37) in the form $\partial u/\partial x = -\mathrm{d}w/\mathrm{d}z$ and equation (39) into the results yields a non-linear ordinary differential equation for w in the form

$$\frac{\mathrm{d}^3 w}{\mathrm{d}z^3} - w\frac{\mathrm{d}^2 w}{\mathrm{d}z^2} = 0 \tag{41}$$

An interesting observation regarding equation (41) is the fact that it is identical to the Blasius equation for boundary layer flows of pure fluids (non-porous domains) over a flat plate. To observe this, one simply has to substitute $w(z) = -f(z)/2$ to obtain $2f''' + ff'' = 0$, which is the Blasius equation. Unfortunately, no further analogy to the boundary layer flow in pure fluids exists, predominantly due to the different boundary conditions and because the derivatives $[\mathrm{d}(\cdot)/\mathrm{d}z]$ and the flow (w) are in the same direction. The solutions for the temperature T and the horizontal

component of the filtration velocity u, are related to the solution of the ordinary differential equation

$$\varphi'\varphi''' - \varphi''^2 + \varphi\,\varphi'^2 = 0 \tag{42}$$

where $(\cdot)'$ stands for $\mathrm{d}(\cdot)/\mathrm{d}z$ and

$$u = x\varphi(z) \tag{43}$$

$$T(z) = -\frac{1}{Ra_\omega}\left[P + \varphi(z)\right] \tag{44}$$

where P is a constant defined by

$$P = -Ra_\omega \int_0^1 T(z)\,\mathrm{d}z \tag{45}$$

The relationship (45) is a result of imposing a condition of no net flow through any vertical cross-section in the domain, stating that $\int_0^1 u\,\mathrm{d}z = 0$.

The following boundary conditions are required to the solution of (41) for w: $w = 0$ at $z = 0$ and $z = 1$ representing the impermeability condition at the solid boundaries and $T = 0$ at $z = 0$ and T=1 at $z = 1$. Since $\partial u/\partial x = \varphi$ according to equation (43), then following the continuity equation (37) $\varphi = -\mathrm{d}w/\mathrm{d}z$ and the temperature boundary conditions can be converted into conditions in terms of w by using equation (44), leading to the following complete set of boundary conditions for w:

$$z = 0:\ w = 0 \quad \text{and} \quad \frac{\mathrm{d}w}{\mathrm{d}z} = P \tag{46}$$

$$z = 1:\ w = 0 \quad \text{and} \quad \frac{\mathrm{d}w}{\mathrm{d}z} = P + Ra_\omega \tag{47}$$

Equations (46) and (47) represent four boundary conditions, while only three are necessary to solve the third order equation (41). The reason for the fourth condition comes from the introduction of the constant P, whose value remains to be determined. Hence, the additional two boundary conditions are expressed in terms of the unknown constant P and the solution subject to these four conditions will determine the value of P as well. A method similar to Blasius's method of solution was applied to solve equation (41). Therefore, $w(z)$ was expressed as a finite power series and the objective of the solution was to determine the power series coefficients. Once the solution for $w(z)$ and the value of P were obtained, u and T were evaluated by using $\varphi(z) = -\mathrm{d}w/\mathrm{d}z$ and equations (43) and (44).

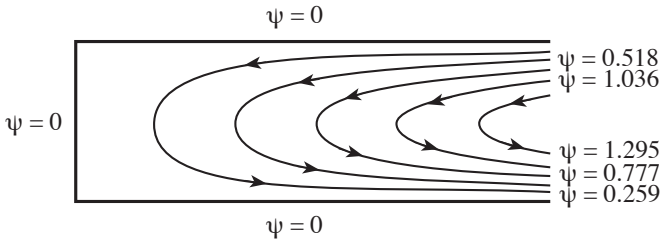


Figure 3: Graphical description of the resulting flow field; five streamlines equally spaced between their minimum value $\psi_{\min} = 0$ at the rigid boundaries and their maximum value $\psi_{\max} = 1.554$. The values in the figure correspond to every other streamline. (courtesy Elsevier Science Ltd.)

For presentation purposes a stream function ψ was introduced to plot the results ($u = \partial\psi/\partial z$, $w = -\partial\psi/\partial x$). An example of the flow field represented by the streamlines is presented in Figure 9 for $Ra_\omega = 4$ and for an aspect ratio of 3 (excluding a narrow region next to the sidewall at $x = L$). Outside this narrow region next to $x = L$ the streamlines remain open on the right hand side. They are expected to close in the end region. On the left-hand side, however, the streamlines close throughout the domain. The reason for this, is the centrifugal acceleration,

which causes u to vary linearly with x, thus creating (due to the continuity equation) a non-vanishing vertical component of the filtration velocity w at all values of x. The local Nusselt number Nu, representing the local vertical heat flux was evaluated as well by using the definition $Nu = \left| -\partial T / \partial z \right|_{z=0}$ and using the solution for T. A comparison between the heat flux results obtained from this solution and the results obtained by Vadasz [34] using an asymptotic method was presented graphically by Vadasz [37]. The two results compare well as long as Ra_ω is very small. However, for increasing values of Ra_ω the deviation from the linear relationship pertaining to the first order asymptotic solution ($Nu = 1 + Ra_\omega / 24$, according to Vadasz [34]) was evident. The stability of this convection flow was not evaluated, although it is of extreme interest. This would be an interesting though not simple task recommended for future research.

The problem of stability of free convection in a rotating porous layer when the temperature gradient is collinear with the centrifugal body force was treated by Vadasz [38] and Vadasz [40] for a narrow layer adjacent to the axis of rotation (Vadasz [38]) and distant from the axis of rotation (Vadasz [40]), respectively. The problem formulation corresponding to the latter case is presented in Figure 4. In order to include explicitly the dimensionless offset distance from the axis of rotation x_0, and to keep the coordinate system linked to the porous layer, equation (33) was presented in the form

$$\boldsymbol{V} = -\nabla p - \left[Ra_{\omega o} + Ra_\omega x \right] T \hat{\boldsymbol{e}}_x \tag{48}$$

Two centrifugal Rayleigh numbers appear in equation (48); the first one, representing the contribution of the offset distance from the rotation axis to the centrifugal buoyancy is $Ra_{\omega o} = \beta_{T*} \Delta T_c \omega_*^2 x_{0*} L_* K_o / \alpha_{e*} \nu_*$, while the second, $Ra_\omega = \beta_{T*} \Delta T_c \omega_*^2 L_*^2 K_o / \alpha_{e*} \nu_*$, represents the contribution of the horizontal location within the porous layer to the centrifugal buoyancy. The ratio between the two centrifugal Rayleigh numbers is dimensionless reciprocal distance from the axis of rotation

$$\eta = \frac{Ra_\omega}{Ra_{\omega o}} = \frac{1}{x_0} \tag{49}$$

and can be introduced as a parameter in the equations transforming equation (48) into the form

$$\boldsymbol{V} = -\nabla p - Ra_{\omega o} \left[1 + \eta x \right] T \hat{\boldsymbol{e}}_x \tag{50}$$

From equation (50) it is observed that when the porous layer is far away from the axis of rotation then $\eta << 1$ ($x_0 >> 1$) and the contribution of the term ηx is not significant, while for a layer close enough to the rotation axis $\eta >> 1$ ($x_0 << 1$) and the contribution of the first term becomes insignificant. In the first case the only controlling parameter is $Ra_{\omega o}$ while in the latter case the only controlling parameter is $Ra_\omega = \eta Ra_{\omega o}$. The flow boundary conditions are $\boldsymbol{V} \cdot \hat{\boldsymbol{e}}_n = 0$ on the boundaries, where $\hat{\boldsymbol{e}}_n$ is a unit vector normal to the boundary. These conditions stipulate that all boundaries are rigid and therefore non-permeable to fluid flow. The thermal boundary conditions are: $T = 0$ at $x = 0$, $T = 1$ at $x = 1$ and $\nabla T \cdot \hat{\boldsymbol{e}}_n = 0$ on all other walls representing the insulation condition on these walls.

The governing equations accept a basic motionless conduction solution in the form

$$\left[\boldsymbol{V}_b, T_b, p_b \right] = \left[0, x, \left(-Ra_{\omega o} (x^2/2 + \eta x^3/3) + C \right) \right] \tag{51}$$

The objective of the investigation was to establish the condition when the motionless solution (51) is not stable and consequently a resulting convection pattern appears. Therefore a linear stability analysis was employed, representing the solution as a sum of the basic solution (51) and small perturbations in the form

$$\left[\boldsymbol{V}, T, p \right] = \left[\boldsymbol{V}_b + \boldsymbol{V}', \; T_b + T', \; p_b + p' \right] \tag{52}$$

where $(\cdot)'$ stands for perturbed values. Solving the resulting linearized system for the perturbations by assuming a normal modes expansion in the y and z directions, and $\theta(x)$ in

the x direction, i.e., $T' = A_\kappa \theta(x) \exp\left[\sigma t + i\left(\kappa_y y + \kappa_z z\right)\right]$, and using the Galerkin method to solve for $\theta(x)$ one obtains at marginal stability, i.e., for $\sigma = 0$, a homogeneous set of linear algebraic equations. This homogeneous linear system accepts a non-zero solution only for particular values of $Ra_{\omega o}$ such that its determinant vanishes. The solution of this system was evaluated up to order 7 for different values of η, representing the offset distance from the axis of rotation.

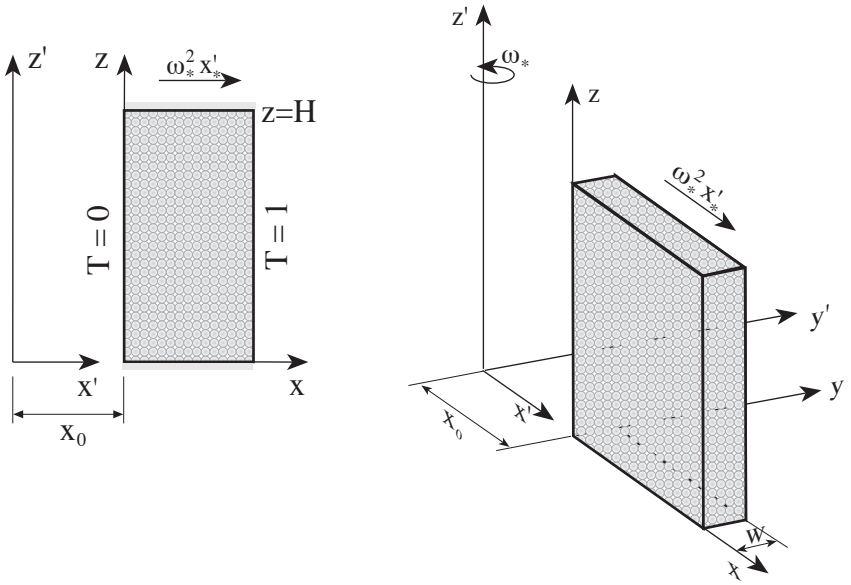


Figure 4: A rotating fluid saturated porous layer distant from the axis of rotation and subject to different temperatures at the sidewalls.

However, useful information was obtained by considering the approximation at order 2. At this order the system reduces to two equations, which lead to the characteristic values of $Ra_{\omega o}$ in the form

$$R_{0,c} = \frac{\beta\left[(1+\alpha)^2 + (4+\alpha)^2\right]}{2\alpha\left(\beta^2 - \gamma^2\right)} \pm \frac{\sqrt{\beta^2\left[(1+\alpha)^2 + (4+\alpha)^2\right]^2 - 4\left(\beta^2 - \gamma^2\right)(1+\alpha)^2(4+\alpha)^2}}{2\alpha\left(\beta^2 - \gamma^2\right)} \quad (53)$$

where the following notation was used

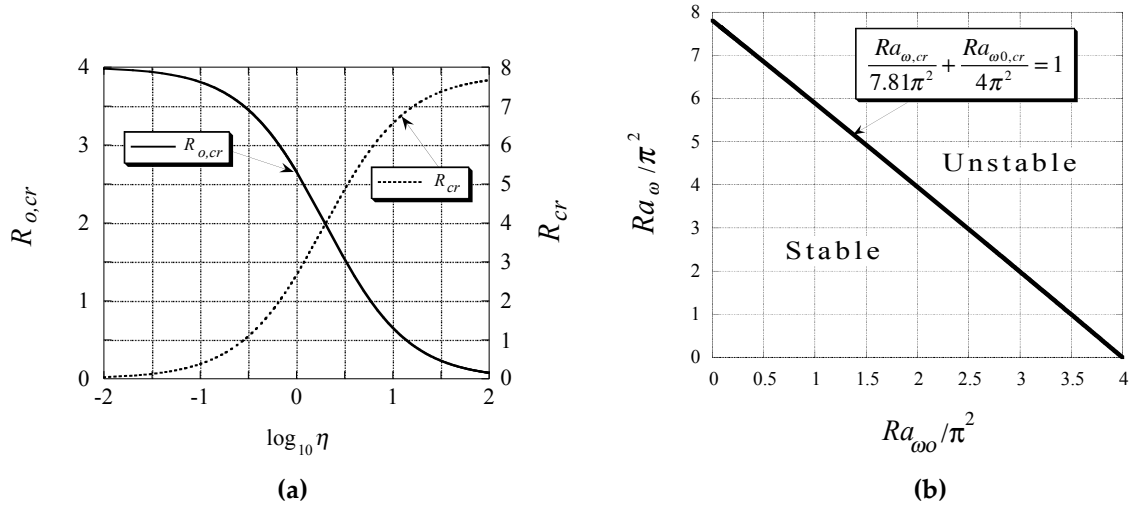
$$R_o = \frac{Ra_{\omega o}}{\pi^2}; \quad R = \frac{Ra_\omega}{\pi^2}; \quad \alpha = \frac{\kappa^2}{\pi^2}; \quad \beta = 1 + \frac{\eta}{2}; \quad \gamma^2 = \frac{256\eta^2}{81\pi^4} \quad (54)$$

and κ is the wavenumber such that $\kappa^2 = \kappa_y^2 + \kappa_z^2$ while the subscript c in equation (53) represents characteristic (neutral) values (values for which $\sigma = 0$). A singularity in the solution for $R_{o,c}$, corresponding to the existence of a single root for $R_{o,c}$, appears when $\beta^2 = \gamma^2$. This singularity persists at higher orders as well. Resolving for the value of η when this singularity occurs shows that it corresponds to negative η values implying that the location of the rotation axis falls within the boundaries of the porous domain (or to the right side of the hot wall - a case of little interest due to its inherent unconditional stability). This particular case will be discussed later in this section. The critical values of the centrifugal Rayleigh number as obtained from the solution up to order 7 are presented graphically in Figure 5(a) in terms of both $R_{o,cr}$ and R_{cr} as a function of the offset parameter η. The results presented in Figure 5 are particularly useful in order to indicate the stability criterion for all positive values of η. It can be observed from the figure that as the value of η becomes small, i.e. for a porous layer far away from the axis of rotation, the critical centrifugal Rayleigh number approaches a limit value of $4\pi^2$. This corresponds to the critical Rayleigh number in a porous layer subject to gravity and heated from below. For high values of η

it is appropriate to use the other centrifugal Rayleigh number R, instead of R_o, by introducing the relationship $R = \eta R_o$ (see equations (49) and (54)) in order to establish and present the stability criterion. It is observed from Fig. 5(a) that as the value of η becomes large, i.e. for a porous layer close to the axis of rotation, the critical centrifugal Rayleigh number approaches a limit value of $7.81\pi^2$. This corresponds to the critical Rayleigh number for the problem of a rotating layer adjacent to the axis of rotation as presented by Vadasz [38]. The stability map on the $Ra_\omega - Ra_{\omega o}$ plane is presented in Figure 5(b), showing that the plane is divided between the stable and unstable zones by the straight line $\left(Ra_{\omega,cr}/7.81\pi^2\right)+\left(Ra_{\omega o,cr}/4\pi^2\right)=1$.

The results for the convective flow field are presented graphically in Figure 6 following Vadasz [40], where it was concluded that the effect of the variation of the centrifugal acceleration within the porous layer is definitely felt when the box is close to the axis of rotation, corresponding to an eccentric shift of the convection cells towards the sidewall at $x=1$. However, when the layer is located far away from the axis of rotation (e.g. $x_0 = 50$) the convection cells are concentric and symmetric with respect to $x = 1/2$ as expected for a porous layer subject to gravity and heated from below (here "below" means the location where $x=1$).

Although the linear stability analysis is sufficient for obtaining the stability condition of the motionless solution and the corresponding eigenfunctions describing qualitatively the convective flow, it cannot provide information regarding the values of the convection amplitudes, nor regarding the average rate of heat transfer. To obtain this additional information, Vadasz and Olek [46] analyzed and provided a solution to the non-linear equations by using Adomian's decomposition method to solve a system of ordinary differential equations for the evolution of the amplitudes.



(a) **(b)**

Figure 5: (a) The variation of the critical values of the centrifugal Rayleigh numbers as a function of η; **(b)** The stability map on the $Ra_\omega - Ra_{\omega o}$ plane showing the division of the plane.

This system of equations was obtained by using the first three relevant Galerkin modes for the stream function and the temperature in the form

$$\psi = 2\theta\sqrt{2\overline{\gamma}(R-1)}\,X(t)\sin(\pi x)\sin\left(\frac{\pi z}{H}\right) \tag{55}$$

$$T = x + \frac{2\sqrt{2\overline{\gamma}(R-1)}}{\pi R}Y(t)\sin(\pi x)\cos\left(\frac{\pi z}{H}\right)+\frac{(R-1)}{\pi R}Z(t)\sin(2\pi x) \tag{56}$$

where $\overline{\gamma} = H^2/\left(H^2+1\right)$, $\theta = \left(H^2+1\right)/H$, H being the layer's aspect ratio, $R = \xi/\pi^2\theta^2$, $\xi = Ra_{\omega o} + Ra_\omega/2$, and X, Y, Z the possibly time dependent amplitudes of convection. In this

model it was considered of interest including the time derivative term in Darcy's equation in the form $(1/Va)\partial \mathbf{V}/\partial t$, where $Va = \phi Pr_e/Da$, and Da, Pr_e are the Darcy and the effective Prandtl numbers, respectively, defined as $Da = K_*/L_*^2$ and $Pr_e = \nu_*/\tilde{\alpha}_{e^*}$ (see equation (58) with $Ra_g = 0$ and $Ek \to \infty$). The reason for including the time derivative term in the Darcy equation was the fact that one anticipates oscillatory and possibly chaotic solutions for which very high frequencies may occur. Then, the following equations were obtained for the time evolution of the amplitudes $X(t), Y(t), Z(t)$

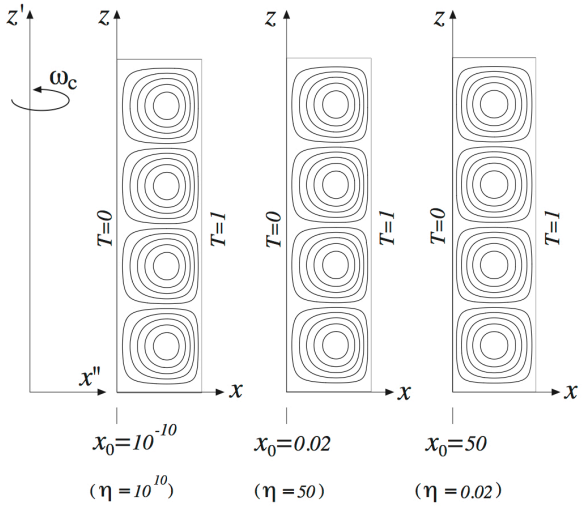


Figure 6: The convective flow field at marginal stability for three different values of x_0; 10 stream lines equally divided between $\psi_{\min}$ and $\psi_{\max}$. At $x_0 = 10^{-10}$: $\psi_{\min} = -1.378$; $\psi_{\max} = 1.378$, at $x_0 = 0.02$: $\psi_{\min} = -1.374$; $\psi_{\max} = 1.374$ and at $x_0 = 50$: $\psi_{\min} = -1.319$; $\psi_{\max} = 1.319$.

$$\dot{X} = \alpha(Y - X) \tag{57}$$

$$\dot{Y} = R\,X - Y - (R-1)XZ \tag{58}$$

$$\dot{Z} = 4\overline{\gamma}(XY - Z) \tag{59}$$

where $\alpha = \overline{\gamma} Va/\pi^2$, and R is a rescaled Rayleigh number introduced above according to the definitions in the text following equation (56). The results obtained are presented in Figure 7 in the form of projection of trajectories data points onto the $Y - X$ and $Z - X$ planes. Different transitions as the value of R varies are presented and they relate to the convective fixed point which is a stable simple node in Figure 7(a), a stable spiral in Figures 7(b) and 7(c), and loses stability via an inverse Hopf bifurcation in Figure 7(d), where the trajectory describes a limit cycle, moving towards a chaotic solution presented in Figures 7(e) and (f). A further transition from chaos to a periodic solution was obtained at a value of R slightly above 100, which persists over a wide range of R values. This periodic solution is presented in Figures 7(g) and 7(h) for $R = 250$.

Previously in this section (see equation (53)) a singularity in the solution was identified and associated with negative values of the offset distance from the axis of rotation. It is this resulting singularity and its consequences, which were investigated by Vadasz [41] and are the objective of the following presentation. As this occurs at negative values of the offset distance from the axis of rotation it implies that the location of the rotation axis falls within the boundaries of the porous domain, as presented in Fig. 8. This particular axis location causes positive values of the centrifugal acceleration on the right side of the rotation axis and negative values on its left side. The rotation axis location implies that the value of x_0 is not positive.

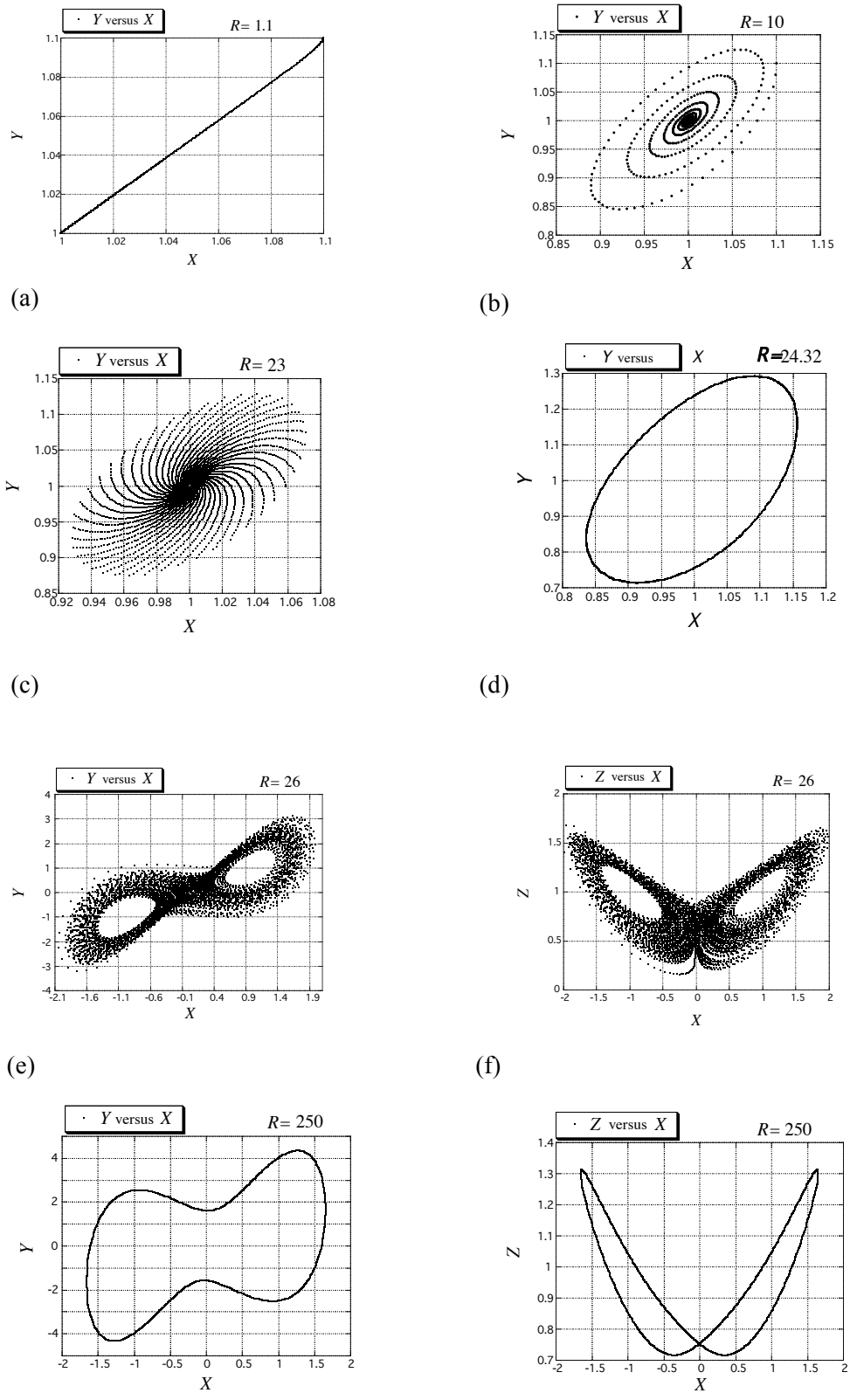


Figure 7: Different transitions in natural convection in a rotating porous layer. (courtesy Elsevier Science Ltd.)

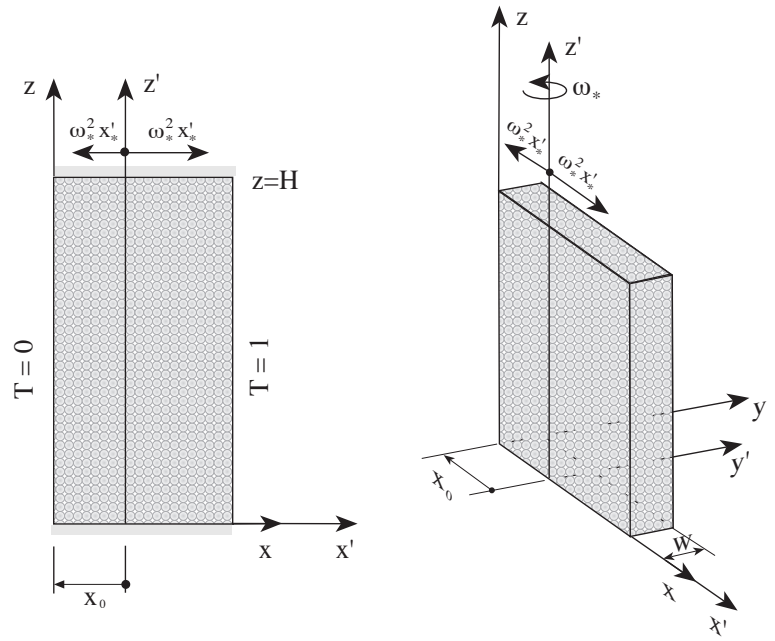


Figure 8: A rotating porous layer having the rotation axis within its boundaries and subject to different temperatures at the sidewalls. (courtesy Elsevier Science Ltd.)

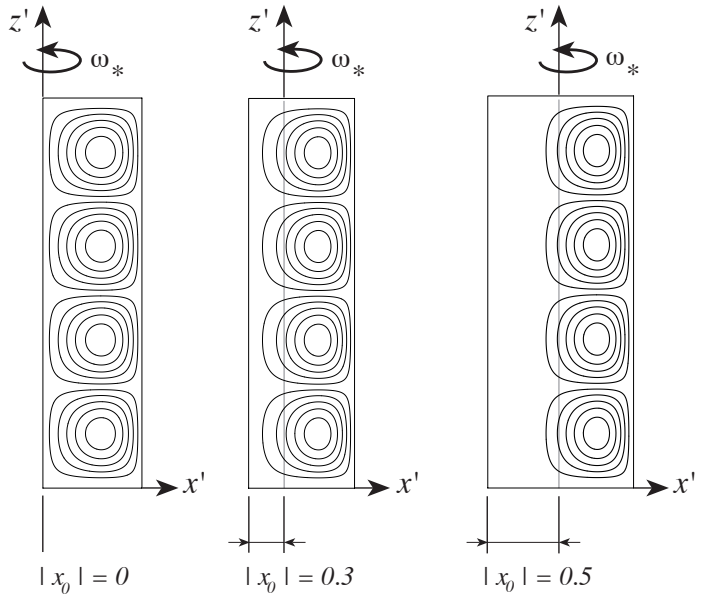


Figure 9: The convective flow field at marginal stability for three different values of $|x_0|$; 10 streamlines equally divided between $\psi_{\min}$ and $\psi_{\max}$. (courtesy Elsevier Science Ltd.)

It is therefore convenient to explicitly introduce this fact in the problem formulation specifying explicitly that $x_0 = -|x_0|$. As a result equation (50) can be expressed in the form

$$\boldsymbol{V} = -\nabla p - Ra_\omega \left[x - |x_0|\right] T \hat{\boldsymbol{e}}_x \tag{60}$$

The solution for this case is similar to the previous case leading to the same characteristic equation for R_c at order 2 as obtained previously in equation (53) for $R_{o,c}$, with the only difference appearing in the different definition of β and γ as follows

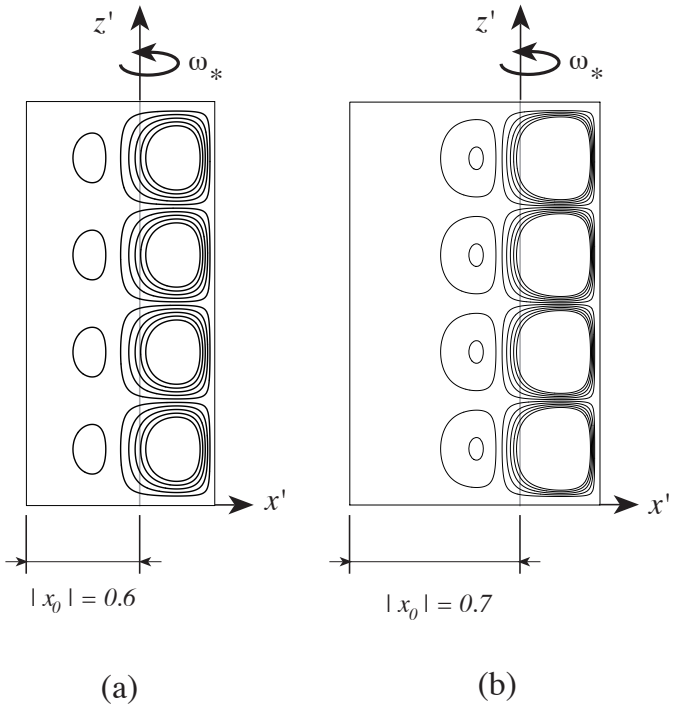
$$\beta = \left(\frac{1}{2} - |x_0| \right); \qquad \gamma^2 = \frac{256}{81\pi^4} \tag{61}$$

The singularity is obtained when $\beta^2 = \gamma^2$, corresponding to $\beta = \gamma$ or $\beta = -\gamma$. Since β is uniquely related to the offset distance $|x_0|$ and $\gamma = 16/9\pi^2$ is a constant, one can relate the singularity to specific values of $|x_0|$. At order 2 this corresponds to $|x_0| = 0.3199$ and $|x_0| = 0.680$. It was shown by Vadasz [41] that the second value $|x_0| = 0.680$ is the only one, which has physical consequences. This value corresponds to a transition beyond which, i.e., for $|x_0| \geq 0.68$, no positive roots of R_c exist. It therefore implies an unconditional stability of the basic motionless solution for all values of R if $|x_0| \geq 0.68$. The transitional value of $|x_0|$ was investigated at higher orders showing $|x_0| \geq 0.765$ at order 3 and the value increases with increasing the order. The indications are that as the order increases the transition value of $|x_0|$ tends towards the limit value of 1. The results for the critical values of the centrifugal Rayleigh number expressed in terms of R_{cr} vs. $|x_0|$ are presented graphically by Vadasz [41], who concluded that increasing the value of $|x_0|$ has a stabilizing effect. The results for the convective flow field as obtained by Vadasz [41] are presented in Figures 9, 10 and 11 for different values of $|x_0|$. Keeping in mind that to the right of the rotation axis the centrifugal acceleration has a destabilizing effect while to its left a stabilizing effect is expected; the results presented in Figures 9(b) and (c) reaffirm this expectation showing an eccentric shift of the convection cells towards the right side of the rotation axis. When the rotation axis is moved further towards the hot wall, say at $|x_0| = 0.6$ as presented in Figure 10(a), weak convection cells appear even to the left of the rotation axis. This weak convection becomes stronger as $|x_0|$ increases, as observed in Figure 10(b) for $|x_0| = 0.7$ and formation of boundary layers associated with the primary convection cells is observed to the right of the rotation axis. These boundary layers become more significant for $|x_0| = 0.8$ as represented by sharp streamlines gradients in Figure 11(a). When $|x_0| = 0.9$ Figure 11(b) shows that the boundary layers of the primary convection are well established and the whole domain is filled with weaker secondary, tertiary and further convection cells. The results for the isotherms corresponding to values of $|x_0| = 0, 0.5, 0.6 \text{ and } 0.7$ are presented in Figure 12 where the effect of moving the axis of rotation within the porous layer, on the temperature is evident.

Previously the discussion focused on centrifugally driven natural convection under conditions of small rotation rates, i.e. $Ek >> 1$. Then, as a first approximation the Coriolis effect was neglected. In this section the effect of the Coriolis acceleration on natural convection is presented even when this effect is small, i.e., $Ek >> 1$. A long rotating porous box where the temperature gradient was perpendicular to the centrifugal body force was considered by Vadasz [35]. The possibility of internal heat generation was included but the case without heat generation, i.e., when the box is heated from above and cooled from below was dealt with separately. The leading order basic flow was evaluated analytically. From the solutions it was concluded that the Coriolis effect on natural convection is controlled by the combined dimensionless group

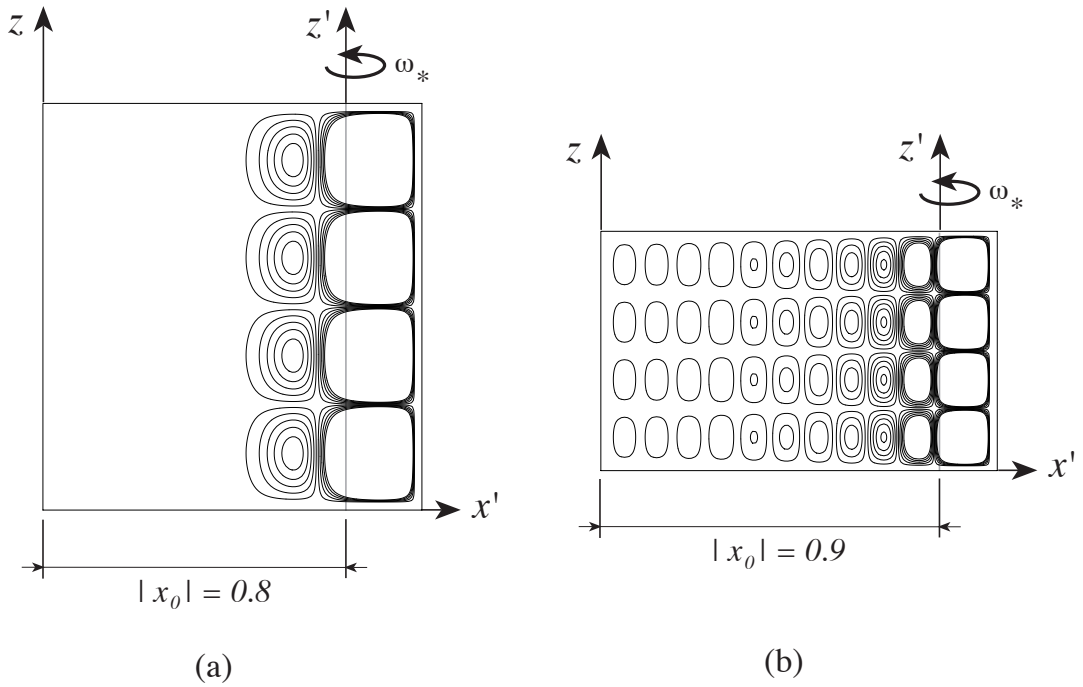
$$\sigma = \frac{Ra_\omega}{Ek} = \frac{2\beta_{T*}\Delta T_c \omega_*^3 L_* H_* K_o^2}{\alpha_{e*} \nu_*^2 \phi} \tag{62}$$

The flow and temperature fields in the plane $y - z$, perpendicular to the leading order natural convection plane as evaluated through the analytical solution shows single or double vortices secondary flow in this plane, perpendicular to the basic flow.



564

565 **Figure 10:** The convective flow field at marginal stability for two different values of $|x_0|$; 10 streamlines
566 equally divided between ψ_{min} and ψ_{max}. (courtesy Elsevier Science Ltd.)
567



568

569 **Figure 11:** The convective flow field at marginal stability for two different values of $|x_0|$; 10 streamlines
570 equally divided between ψ_{min} and ψ_{max}. (courtesy Elsevier Science Ltd.)
571

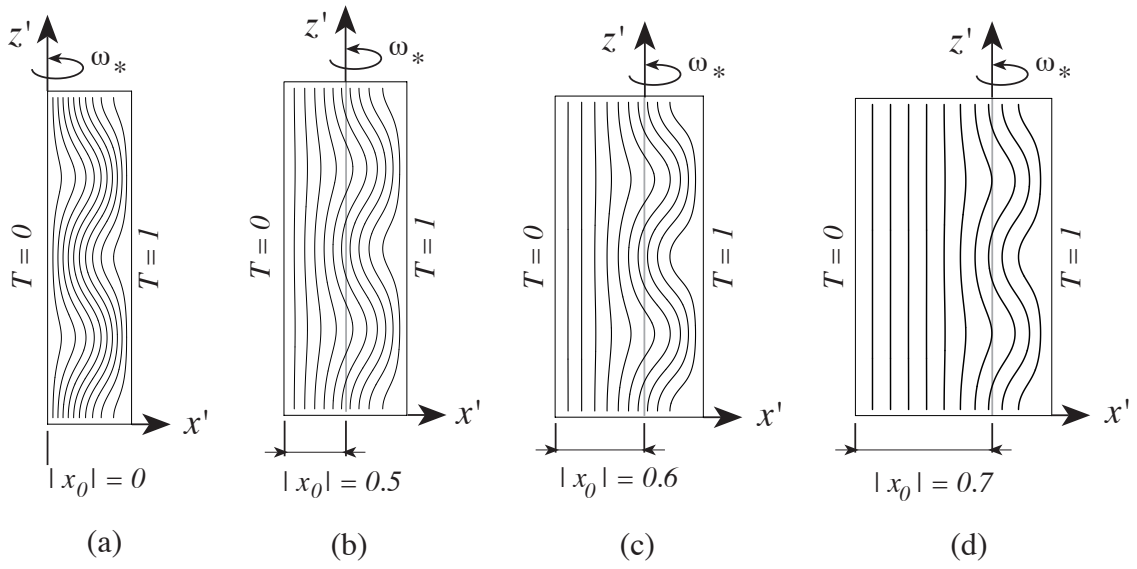


Figure 12: The convective temperature field at marginal stability for four different values of $|x_0|$; 10 isotherms equally divided between $T_{min} = 0$ and $T_{max} = 1$. (courtesy Elsevier Science Ltd.)

5. Coriolis Effect on Natural Convection due to Gravity Buoyancy

The problem of a rotating porous layer subject to gravity and heated from below (see Figure 13) was originally investigated by Friedrich [75] and by Patil and Vaidyanathan [17]. Both studies considered a non-Darcy model, which is probably subject to the limitations as shown by Nield [68]. Friedrich [74] focused on the effect of Prandtl number on the convective flow resulting from a linear stability analysis as well as a non-linear numerical solution, while Patil and Vaidyanathan [17] dealt with the influence of variable viscosity on the stability condition. The latter concluded that variable viscosity has a destabilizing effect while rotation has a stabilizing effect. Although the non-Darcy model considered included the time derivative in the momentum equation the possibility of convection setting-in as an oscillatory instability was not explicitly investigated by Patil and Vaidyanathan [17]. It should be pointed out that for a pure fluid (non-porous domain) convection sets in as oscillatory instability for a certain range of Prandtl number values (Chandrasekhar [76, 77]). This possibility was explored by Friedrich [75], which presents stability curves for both monotonic and oscillatory instability. Jou and Liaw [19] investigated a similar problem of gravity driven thermal convection in a rotating porous layer subject to transient heating from below. By using a non-Darcy model they established the stability conditions for the marginal state without considering the possibility of oscillatory convection.

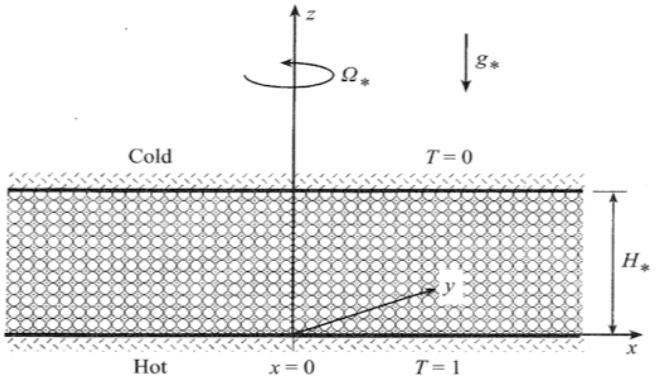


Figure 13: A rotating fluid saturated porous layer heated from below. (courtesy: Cambridge University Press.)

An important analogy was discovered by Palm and Tyvand [20] who showed, by using a Darcy model, that the onset of gravity driven convection in a rotating porous layer is equivalent to the case of an anisotropic porous medium. The critical Rayleigh number was found to be

$$Ra_{g,cr} = \pi^2 \left[(1+Ta)^{1/2} + 1 \right]^2 \tag{63}$$

where Ta is the Taylor number defined here as

$$Ta = \left(\frac{2\omega_* K_o}{\phi \nu_*} \right)^2 \tag{64}$$

and the corresponding critical wave number is $\pi(1+Ta)^{1/4}$. The porosity is missing in Palm and Tyvand [20] definition of Ta. Nield [21, 22] has pointed out that these authors and others have omitted the porosity from the Coriolis term. This result, eq. (63) (amended to include the correct definition of Ta), was confirmed by Vadasz [41] for a Darcy model extended to include the time derivative term (see equation (31) with $Ra_\omega = 0$), while performing linear stability as well as a weak non-linear analyses of the problem to provide differences as well as similarities with the corresponding problem in pure fluids (non-porous domains). As such, Vadasz [42] found that, in contrast to the problem in pure fluids, overstable convection in porous media at marginal stability is not limited to a particular domain of Prandtl number values (in pure fluids the necessary condition is $Pr < 1$). Moreover, it was also established by Vadasz [42] that in the porous media problem the critical wave number in the plane containing the streamlines for stationary convection is not identical to the critical wave number associated with convection without rotation, and is therefore not independent of rotation, a result which is quite distinct from the corresponding pure-fluids problem. Nevertheless, it was evident that in porous media, just as in the case of pure fluids subject to rotation and heated from below, the viscosity at high rotation rates has a destabilizing effect on the onset of stationary convection, i.e. the higher the viscosity the less stable is the fluid. An example of stability curves for overstable convection is presented in Figure 14 for $Ta = 5$, where κ is the wave number. The upper bound of these stability curves is represented by a stability curve corresponding to stationary convection at the same particular value of the Taylor number, while the lower bound was found to be independent of the value of Taylor number and corresponds to the stability curve for overstable convection associated with $Va = 0$.

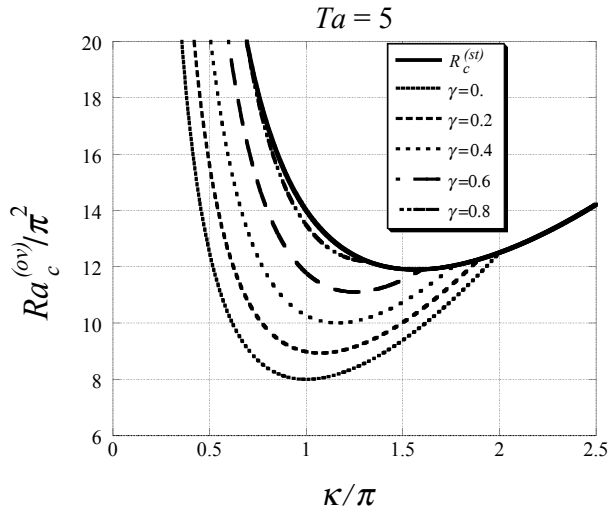


Figure 14: Stability curves for overstable gravity driven convection in a rotating porous layer heated from below ($\gamma = Va/\pi^2$, $R = Ra_g/\pi^2$). (courtesy: Cambridge University Press.)

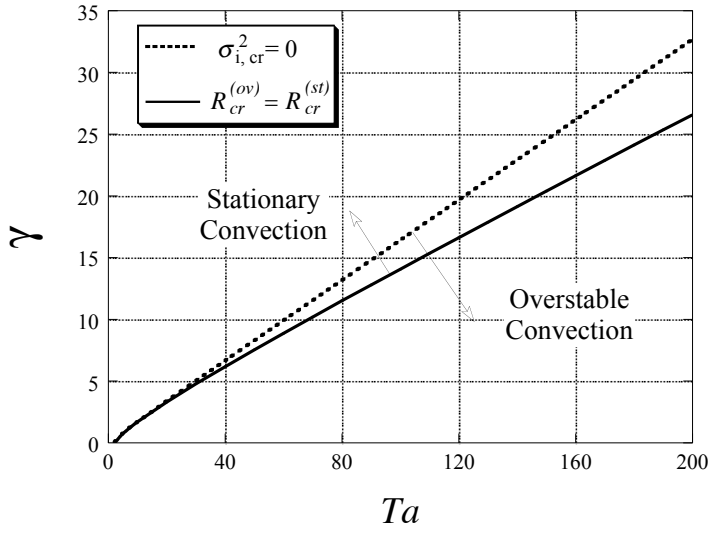


Figure 15: Stability map for gravity driven convection in a rotating porous layer heated from below ($\gamma = Va/\pi^2$, $R = Ra_g/\pi^2$). (courtesy: Cambridge University Press.)

Two conditions have to be fulfilled for overstable convection to set in at marginal stability, i.e., (i) the value of Rayleigh number has to be higher than the critical Rayleigh number associated with overstable convection, and (ii) the critical Rayleigh number associated with overstable convection has to be smaller than the critical Rayleigh number associated with stationary convection. The stability map obtained by Vadasz [42] is presented in Figure 15, which shows that the $Ta-\gamma$ ($\gamma = Va/\pi^2$) plane is divided by a continuous curve (almost a straight line) into two zones, one for which convection sets in as stationary, and the other where overstable convection is preferred. The dotted curve represents the case when the necessary condition (i) above is fulfilled but condition (ii) is not. Weak non-linear stationary as well as oscillatory solutions were derived, identifying the domain of parameter values consistent with supercritical pitchfork (in the stationary case) and Hopf (in the oscillatory case) bifurcations. Unfortunately due to a typo affecting the sign of one of the nonlinear terms in the weak nonlinear analysis the direction of the bifurcations presented seems to be incorrect. The identification of the tricritical point corresponding to the transition from supercritical to subcritical bifurcations was presented on the $\gamma - Ta$ parameter plane. The possibility of a codimension-2 bifurcation, which is anticipated at the intersection between the stationary and overstable solutions, although identified as being of significant interest for further study, was not investigated by Vadasz [42].

6. Natural Convection due to Combined Centrifugal and Gravity Buoyancy

Previous sections dealt with natural convection due to centrifugal buoyancy, when the gravity body force contribution was negligible, $Ra_g = 0$, satisfying the condition: $Ra_g/Ra_\omega = g_*/\omega_*^2 L_* << 1$, or with gravity buoyancy when the centrifugal body force contribution was insignificant, $Ra_\omega = 0$, satisfying the condition: $Ra_\omega/Ra_g = \omega_*^2 L_*/g_* << 1$. In the present section the focus is on conditions when both centrifugal buoyancy as well as gravity buoyancy effects are significant, $Ra_g \sim Ra_\omega$, but at small rotation rates, i.e. $Ek >> 1$. Then, as a first approximation the Coriolis effect can be neglected. Figure 4 still applies to the present problem, subject to a slight modification of drawing the gravity acceleration g_* in the negative z direction. The notation remains the same and equation (50) becomes

$$\boldsymbol{V} = -\nabla p - Ra_{\omega o}\left[1+\eta x\right]T\hat{\boldsymbol{e}}_x + Ra_g T\hat{\boldsymbol{e}}_z \tag{65}$$

where $\eta = 1/x_0 = Ra_\omega / Ra_{\omega o}$ represents the reciprocal of the offset distance from the axis of rotation. The approach being the same as before, the solution is expressed as a sum of a basic solution and small perturbations as presented in equation (52). However, because of the presence of the gravity component in equation (65), a motionless conduction solution is not possible any more. Therefore, the basic solution far from the top and bottom walls is obtained in the form

$$u_b = v_b = 0;\ w_b = Ra_g\left(x - \frac{1}{2}\right);\quad T_b = x;\ \ p_b = \frac{1}{2}Ra_g z - Ra_{\omega o}x^2\left[\frac{1}{2} + \frac{1}{3}\eta x\right] + \text{const.} \tag{66}$$

Substituting this basic solution into the governing equations and linearizing the result by neglecting terms that include products of perturbations, which are small, yields a set of partial differential equations for the perturbations. Assuming a normal modes expansion in the y and z directions in the form

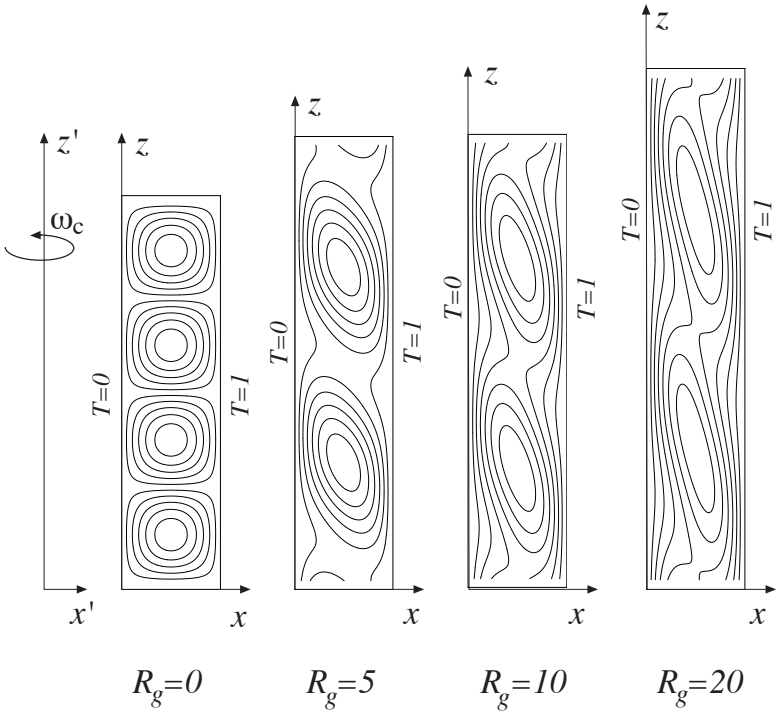
$$T' = A_\kappa \theta(x)\exp\left[\sigma t + i(\kappa_y y + \kappa_z z)\right] \tag{67}$$

where κ_y and κ_z are the wave numbers in y and z directions respectively, i.e., $\kappa^2 = \kappa_y^2 + \kappa_z^2$, and using the Galerkin method, the following set of linear algebraic equations is obtained at marginal stability (i.e., for $\sigma = 0$)

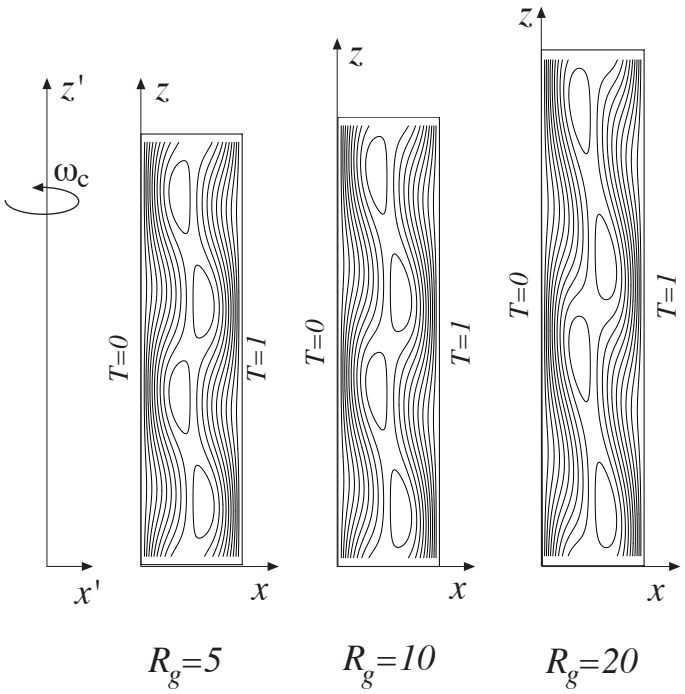
$$\sum_{m=1}^{M}\left\{\left[2\left(m^2\pi^2 + \kappa^2\right)^2 - \kappa^2 Ra_{\omega o}\left(2 + \eta\right)\right]\delta_{ml} + \left[\frac{16ml\kappa^2 Ra_{\omega o}}{\pi^2\left(l^2 - m^2\right)} - i\frac{8ml\kappa_z Ra_g}{\pi^2\left(l^2 - m^2\right)^2}\left[\pi^2\left(l^2 + m^2\right) + 2\kappa^2\right]\right]\delta_{m+l,2p-1}\right\} a_m = 0 \tag{68}$$

for $l = 1, 2, 3, \ldots, M$ and $i = \sqrt{-1}$. In equation (68) δ_{ml} is the Kronecker delta function and the index p can take arbitrary integer values, since it stands only for setting the second index in the Kronecker delta function to be an odd integer. A particular case of interest is the configuration when the layer is placed far away from the axis of rotation, i.e. when the length of the layer L_* is much smaller than the offset distance from the rotation axis x_{0*}. Therefore for $x_0 = \left(x_{0*}/L_*\right) \to \infty$ or $\eta \to 0$ the contribution of the term ηx in equation (65) is not significant. Substitution of this limit into equation (68) and solving the system at the second order, i.e. $M = 2$, yields a quadratic equation for the characteristic values of $Ra_{\omega o}$. This equation has no real solutions for values of $\alpha = \kappa_z^2/\pi^2$ beyond a transitional value $\alpha_{tr} = (27\pi^3/16\,Ra_g)^2$. This value was evaluated at higher orders too, showing that for $M = 10$ the transitional value varies very little with Ra_g, beyond a certain Ra_g value around 50π. The critical values of $Ra_{\omega o}$ were evaluated for different values of $R_g\ (= Ra_g/\pi)$ and the corresponding two-dimensional convection solutions in terms of streamlines are presented graphically for the odd modes in Figure 16(a), showing the perturbation solutions in the $x - z$ plane as skewed convection cells when compared with the case without gravity. The corresponding convection solutions for the even modes are presented in Figure 16(b), where it is evident that the centrifugal effect is felt predominantly in the central region of the layer, while the downwards and upwards basic gravity driven convection persists along the left and right boundaries, respectively, although not in straight lines. Beyond the transition value of α, the basic gravity driven convective flow (equation (66)) is unconditionally stable. These results were shown to have an analogy with the problem of gravity driven convection in a non-rotating, inclined porous layer (Govender and Vadasz [29]). Qualitative experimental confirmation of these results was presented by Vadasz and Heerah [45] by using a thermo-sensitive liquid-crystal tracer in a rotating Hele-Shaw cell. When the layer is placed at an arbitrary finite distance from the axis of rotation no real solutions exist for the characteristic values of $Ra_{\omega o}$ corresponding to any values of γ other than $\gamma = \kappa_z Ra_g = 0$. In the presence of gravity $Ra_g \neq 0$, and $\gamma = 0$ can be satisfied only if $\kappa_z = 0$. Therefore the presence of gravity in this case has no other role but to exclude the vertical modes of convection. The critical centrifugal Rayleigh numbers and the corresponding critical wave numbers

are the same as in the corresponding case without gravity as presented in section 4.3. However, the eigenfunctions representing the convection pattern are different as they exclude the vertical modes replacing them with a corresponding horizontal mode in the y direction. Therefore, a cellular convection in the $x-y$ plane is superimposed to the basic convection in the $x-z$ plane.



(a)



(b)

Figure 16: The convective flow field (streamlines) at marginal stability for different values of R_g $(= Ra_g/\pi)$; **(a)** the odd modes; **(b)** the even modes.

7. Additional Effects on Flow and Natural Convection in Rotating Porous Media

Not much research results are available for thermo-haline convection in porous media subject to rotation. Chakrabarti and Gupta [78] investigated a non-Darcy model, which includes the Brinkman term as well as a non-linear convective term in the momentum equation (in the form $(\boldsymbol{V}\cdot\nabla)\boldsymbol{V}$). Therefore the model's validity is subject to the limitations pointed out by Nield [69]. Both linear and non-linear analyses were performed and overstability was particularly investigated. Overstability is affected in this case by both the presence of a salinity gradient and by the Coriolis effect. Apart from the thermal and solutal Rayleigh numbers and the Taylor number, two additional parameters affect the stability. These are the Prandtl number $Pr = \nu_* / \alpha_{e^*}$, and the Darcy number $Da = K_o / H_*^2$, where H_* is the layer's height. The authors found that, in the range of values of the parameters, which were considered, the linear stability results favor setting-in of convection through a mechanism of overstability. The results for non-linear steady convection show that the system becomes unstable to finite amplitude steady disturbances before it becomes unstable to disturbances of infinitesimal amplitude. Thus the porous layer may exhibit subcritical instability in the presence of rotation. These results are surprising at least in the sense of their absolute generality and the authors mention that further confirmation is needed in order to increase the degree of confidence in these results. A similar problem was investigated by Rudraiah et al [16] while focusing on the effect of rotation on linear and non-linear double-diffusive convection in a sparsely packed porous medium. A non-Darcy model identical to the one used by Chakrabarti and Gupta [78] was adopted by Rudraiah et al [16], however the authors spelled out explicitly that the model validity is limited to high porosity and high permeability which makes it closer to the behavior of a pure fluid system (non-porous domain). It is probably for this reason that the authors preferred to use the non-porous medium definitions for Rayleigh and Taylor numbers which differ by a factor of Da and Da^2, respectively, from the corresponding definitions for porous media. It is because of these definitions that the authors concluded that for small values of Da number the effect of rotation is negligible for values of $Ta < 10^6$. This means that rotation has a significant effect for large rotation rates, i.e., $Ta > 10^6$. If the porous media Taylor number had been used instead, i.e., the proper porous media scales, then one could have significant effects of rotation at porous media Taylor numbers as small as $Ta > 10$. Hence, the results presented by Rudraiah et al [16] are useful provided $Da = O(1)$ which is applicable for high permeability (or sparsely packed) porous layers. Marginal stability as well as overstability were investigated and the results show different possibilities of existence of neutral curves by both mechanisms, i.e., monotonic as well as oscillatory instability. In this regard the results appear more comprehensive in the study by Rudraiah et al [16] than in Chakrabarti and Gupta [78]. The finite amplitude analysis was performed by using a severely truncated representation of a Fourier series for the dependent variables. As a result a seventh-order Lorenz model of double diffusive convection in a porous medium in the presence of rotation was obtained. From the study of steady, finite amplitude analysis the authors found that subcritical instabilities are possible, depending on the parameter values. The effect of the parameters on the heat and mass transport was investigated as well, and results presenting this effect are discussed in Rudraiah et al [16]. The onset of double-diffusive convection in a rotating porous layer was investigated by Lombardo and Mulone [60], Malashety, Pop, and Heera [48], Falsaperla, Giacobbe and Mulone [63]. Triple-diffusion effects in rotating porous layers were investigated by Capone and De Luca [64]. They evaluated the ultimate boundedness of the solutions and found a necessary and sufficient condition for the global nonlinear asymptotic L^2-stability of the motionless conduction solution.

Lack of local thermal equilibrium (LaLotheq) or local thermal non-equilibrium (LTNE) means that distinct temperature values exist between the solid and fluid phases within the same Representative Elementary Volume (REV). Malashetty et al [53] presented the linear stability and the onset of convection in a porous layer heated from below and subject to rotation, accounting for the Coriolis effect as in Vadasz [42] but allowing for distinct temperature values between the solid and fluid phases, i.e. lack of local thermal equilibrium (LaLotheq), or local thermal non-equilibrium

(LTNE). The nonlinear part of the analysis was undertaken by using a truncated mode spectral system, such as the one used by Vadasz and Olek [46] but adapted for the LaLotheq conditions. The effect of finite heat transfer between the phases leading to lack of local thermal equilibrium was investigated also by Govender and Vadasz [32] while investigating also the effect of mechanical and thermal anisotropy on the stability of a rotating porous layer heated from below and subject to gravity. The topic of anisotropic effects is discussed in the next section. Bhadauria [47] investigated the effect of temperature modulation on the onset of thermal instability in a horizontal fluid-saturated porous layer heated from below and subject to uniform rotation. An extended Darcy model, which includes the time derivative term, has been considered, and a time-dependent periodic temperature field was applied to modulate the surfaces' temperature. A perturbation procedure based on small amplitude of the imposed temperature modulation was used to study the combined effect of rotation, permeability, and temperature modulation on the stability of the fluid saturated porous layer. The correction of the critical Rayleigh number was calculated as a function of amplitude and frequency of modulation, the porous media Taylor number, and the Vadasz number. It was found that both rotation and permeability suppress the onset of thermal instability. Furthermore, the author concluded that temperature modulation could either promote or retard the onset of convection.

The effect of anisotropy on the stability of convection in a rotating porous layer subject to centrifugal body forces was investigated by Govender [25]. The Darcy model extended to include anisotropic effects and rotation was used to describe the momentum balance and a modified energy equation that included the effects of thermal anisotropy was used to account for the heat transfer. The linear stability theory was used to evaluate the critical Rayleigh number for the onset of convection in the presence of thermal and mechanical anisotropy. It was found that the convection was stabilized when the thermal anisotropy ratio (which is a function of the thermal and mechanical anisotropy parameters) increased in magnitude. Malashetty and Swamy [54], and Govender and Vadasz [32] investigated the Coriolis effect on natural convection in a rotating anisotropic fluid-saturated porous layer heated from below and subject to gravity as the body force. Malashetty and Swamy [54] assumed local thermal equilibrium while Govender and Vadasz [32] dealt with lack of local thermal equilibrium (LaLotheq), or local thermal non-equilibrium (LTNE). Malashetty and Swamy [54] used the linear stability theory as well as a nonlinear spectral method. The linear theory was based on the usual normal mode technique and the nonlinear theory on a truncated Galerkin analysis. The Darcy model extended to include a time derivative and the Coriolis terms with an anisotropic permeability was used to describe the flow through the porous media. A modified energy equation including the thermal anisotropy was used. The effect of rotation, mechanical and thermal anisotropy parameters and the Prandtl number on the stationary and overstable convection was discussed. It was found that the effect of mechanical anisotropy is to prefer the onset of oscillatory convection instead of the stationary one. It was also found, just as in Vadasz [42], that the existence of overstable motions in case of rotating porous media is not restricted to a particular range of Prandtl number as compared to the pure viscous fluid case. The steady finite amplitude analysis was performed using the truncated Galerkin modes to find the Nusselt number. The effect of various parameters on heat transfer was investigated. Govender and Vadasz [32] analyzed the stability of a horizontal rotating fluid saturated porous layer exhibiting both thermal and mechanical anisotropy, subject to lack of local thermal equilibrium (LaLotheq), or local thermal non-equilibrium (LTNE). All of the results were presented as a function of the scaled inter-phase heat transfer coefficient. The results of the linear stability theory have revealed that increasing the conductivity ratio and the mechanical anisotropy has a destabilizing effect, whilst increasing the fluid and solid thermal conductivity ratios is stabilizing. In general it was found that rotation has a stabilizing effect in a porous layer exhibiting mechanical or thermal (or both mechanical and thermal) anisotropy. Additional results for the effect of rotation on thermal convection in an anisotropic porous medium were presented by Vanishree and Siddheshwar [49].

An interesting, more recent, application is related to nanofluids. A nanofluid is a suspension of nanoparticles or nanotubes in a liquid. When the liquid is saturating a porous matrix one deals with

820 nanofluids in porous media. Chand and Rana [79] analyzed the Coriolis effect on natural
821 convection in a rotating porous layer saturated by a nanofluid. Agarwal an Bhadauria [52], Rana
822 and Agarwal [55], investigated the natural convection in a rotating porous layer saturated by a
823 nanofluid and a binary mixture. This implies that the nanoparticles are suspended in a binary
824 mixture, e.g. in a water and salt solution. Therefore double-diffusive convection is anticipated. The
825 model used for the nanofluid incorporates the effects of Brownian motion and thermophoresis,
826 while the Darcy model is used for the porous medium. The neutral and critical Rayleigh numbers
827 for stationary and oscillatory convection have been obtained in terms of various dimensionless
828 parameters. The authors concluded that the principle of exchange of stabilities is applicable in the
829 present problem, while more amount of heat is required in the nanofluid case for convection to
830 set-in. Agarwal et al [50] considered the convection in a rotating anisotropic porous layer saturated
831 by a nanofluid. The model used for nanofluid combines the effect of Brownian motion along with
832 thermophoresis, while for a porous medium the Darcy model has been used. Using linear stability
833 analysis the expression for the critical Rayleigh number has been obtained in terms of various
834 dimensionless parameters. Agarwal et al [50] indicate that bottom-heavy and top-heavy
835 arrangements of nanoparticles tend to prefer oscillatory and stationary modes of convection,
836 respectively. The onset of double-diffusive nanofluid convection in a rotating porous layer was
837 investigated by Yadav et al [56].
838 During solidification of binary alloys the solidification front between the solid and the liquid
839 phases is not a sharp front but rather a mushy layer combining liquid and solid phases each one
840 being interconnected. It is not surprising therefore that the treatment of this mushy layer follows all
841 the rules applicable to a porous medium. Natural convection due to thermal as well as
842 concentration gradients occurs in the mushy layer resulting in possible creation of freckles that
843 might affect the quality of the cast. When such a process occurs in a system that is subject to
844 rotation, centrifugal buoyancy as well as Coriolis effects are relevant and essential to be included in
845 any model of this process. Govender and Vadasz [31] investigated such a system via a weak
846 nonlinear analysis for moderate Stefan numbers applicable to stationary convection in a rotating
847 mushy layer. Consequently Govender and Vadasz [30] investigated a similar system via a weak
848 nonlinear analysis for moderate Stefan numbers applicable to oscillatory convection in a rotating
849 mushy layer. A near-eutectic approximation and large far-field temperature were employed in both
850 papers in order to decouple the mushy layer from the overlying liquid melt. The parameter regimes
851 in terms of Taylor number for example where the bifurcation is subcritical or supercritical were
852 identified. In the case of oscillatory convection increasing the Taylor number lead to a supercritical
853 bifurcation.
854 Linear stability was the primary method used in previous sections to establish the stability
855 criteria for the onset of natural convection in a rotating porous layer. Straughan [73] pioneered the
856 introduction of a nonlinear analysis producing a sharp nonlinear stability threshold in rotating
857 porous convection. The application and generalization of this method was presented by Lombardo
858 and Mulone [60], while deriving necessary and sufficient conditions of global nonlinear stability for
859 double-diffusive convection in rotating porous media. The nonlinear method was expanded and
860 summarized by Straughan [59]. The application of this nonlinear method to natural convection in
861 non-rotating porous media was expanded showing the coincidence between linear and global
862 nonlinear stability of non-constant through-flows was presented by Capone and De Luca [66] by
863 using the "Rionero Auxiliary System Method". Weak nonlinear solutions were presented by
864 Bhadauria et al [51]. Investigations into the effects of inertia on rotating porous convection were
865 undertaken by Falsaperla, Mulone, and Straughan [62], and by Capone and Rionero [65]. The latter
866 used again the "Rionero Auxiliary System Method" to derive a set of conditions for the significance
867 of inertia in this problem and for global nonlinear stability in terms of the porous media Taylor
868 number as well as Vadasz number.
869 Other studies considered effects of rotation for a combination of previously presented
870 conditions. For example Capone and Gentile [80] presented sharp stability results in a rotating
871 anisotropic porous layer subject to lack of local thermal equilibrium (LaLotheq, LTNE). Double

872 diffusive convection in a rotating anisotropic porous layer was presented by Galkwad and Kouser
873 [81], Malashetty and Heera [82], and Malashetty and Begum [83]. Double diffusive convection in a
874 rotating porous medium saturated with a coupled stress fluid was considered by Malashetty et al
875 [84], while double diffusive convection in a rotating porous layer saturated by a viscoelastic fluid
876 was investigated by Kumar and Bhadauria [85]. The effect of rotation on a micropolar
877 ferromagnetic fluid heated from below saturating a porous medium was presented by Sunil et al
878 [86]. Rotation effects on convection in a porous layer saturated by nanofluids was further
879 considered by Bhadauria and Agrawal [87], for a porous medium model including the Brinkman
880 term. A similar model was presented by Yadav and Lee [88] for the case of lack of local thermal
881 equilibrium (LaLotheq, LTNE), and by Yadav et al [89] for a Darcy model Soret driven convection
882 in a rotating porous medium saturated by a nanofluid. Brinkman convection induced by internal
883 heating in a rotating porous medim layer saturated by a nanofluid was investigated by Yadav et al
884 [90], while thermal instability in a rotating porous layer saturated by a non-Newtonian nanofluid
885 was considered by Yadav et al [91]. Yadav et al [92] presented the conditions for the onset of
886 convection in a rotating porous layer due internal heating by using a Brinkman model. The effects
887 of thermal modulation, i.e. top and bottom imposed temperatures are allowed to vary slightly in
888 time, were considered by Malashetty and Swamy [93] using a Darcy model and Bhadauria [94]
889 using a Brinkman model. A similar Brinkman model was applied for investigating the effects of
890 centrifugal buoyancy in a rotating porous layer far away from the center of rotation subject to
891 modulation of rotation by Om et al [95], i.e. the angular velocity was allowed to slightly vary
892 periodically in time. The same conditions applied to a rotating porous layer distant an arbitrary
893 distance from the center of rotation was presented by Om et al [96]. Coriolis effect on thermal
894 convective instability of viscoelastic fluids in a rotating porous cylindrical annulus was investigated
895 by Kang et al [97]. Küppers-Lortz instability in rotating Rayleigh-Benard convection in a porous
896 medium was studied by Rameshwar et al. [98].

897

898 **8. Conclusions**

899 A review of the variety of instability problems linked to natural convection in rotating porous
900 media was presented. The effect of centrifugal buoyancy was investigated separately, and later in
901 combination with gravitational buoyancy. The cases when the Coriolis effect is significant were also
902 analyzed and the corresponding results were discussed. The diversity of additional effects linked to
903 natural convection in rotating porous media, such as thermo-solutal and double-diffusive
904 convection, the effect of anisotropy of the porous medium, the inclusion of nanofluids in rotating
905 porous media, solidification of binary alloys, and lack of local thermal equilibrium are examples
906 that were also shortly reviewed. The pioneering studies on global nonlinear analyses and
907 investigations of the effect of inertia on natural convection in rotating porous media concluded the
908 present review.

909

910 **Author Contributions:** N/A

911 **Conflicts of Interest:** "The author declares no conflict of interest.".

912

913 **References**

914 1. Fowler, A.C. A compaction model for melt transport in the earth asthenosphere Part I: The base model. In
915 *Magma Transport and Storage*, ed. Michael P. Raya, John Wiley & Sons, Chichester, 1990, pp. 3-14.
916 2. Vadasz, P., Fluid Flow and Thermal Convection in Rotating Porous Media. In *Handbook of Porous Media*,
917 Kambiz Vadfai (ed.), Marcel Dekker, New York, Basel, 2000, pp. 395-439.

3. Vadasz, P. *Fluid Flow and Heat Transfer in Rotating Porous Media*, Springer (Springer Briefs in applied Science and Engineering, series editor: F.A. Kulacki), Cham, Heidelberg, New York, Dordrecht, London, 2016.
4. Vadasz, P. Natural Convection in Rotating Flows, in *Handbook of Thermal Science and Engineering*, F. A. Kulacki (ed.), Chapter 11, Springer International Publishing AG, 2018, pp. 691-758.
5. Nield, D.A.; Bejan, A. *Convection in Porous Media*, 4th edition, Springer, New York, Heidelberg, Dordrecht, London, 2013.
6. Nield, D.A.; Bejan, A. *Convection in Porous Media*, 5th edition, Springer, New York, Heidelberg, Dordrecht, London, 2017.
7. Bejan, A. *Convection Heat Transfer*, 4th edition, John Wiley & Sons, Hoboken, New Jersey, 2013.
8. Dagan, G. Some aspects of heat and mass transfer in porous media. In *Fundamentals of Transport Phenomena in Porous Media* (ed. J. Bear), Int. Association for Hydraulic Research, Elsevier, New York, 1972, pp. 55-64.
9. Acharya, S. Single-phase convective heat transfer: Fundamental equations and foundational assumptions. In *Handbook of Thermal Science and Engineering*, (ed. F. A. Kulacki), Springer, 2017.
10. Wiesche, S. Heat Transfer in Rotating Flows, in *Handbook of Thermal Science and Engineering*, (ed. F. A. Kulacki), Springer, 2017.
11. Vadasz, P. Fundamentals of Flow and Heat Transfer in Rotating Porous Media. In *Heat Transfer PA 5*, Taylor and Francis, Bristol, 1994, pp. 405-410.
12. Vadasz, P. Flow in rotating porous media. In *Fluid Transport in Porous Media* from the series Advances in Fluid Mechanics 13, ed. P. du Plessis & series ed. M. Rahman, Computational Mechanics Publications, Southampton, 1997, pp. 161-214.
13. Vadasz, P. Free convection in rotating porous media. In *Transport Phenomena in Porous Media*, ed. D.B. Ingham and I. Pop, Elsevier Science, Oxford, 1998, pp. 285-312.
14. Vadasz, P. Heat Transfer and Fluid Flow in Rotating Porous Media. In *Computational Methods in Water Resources 1*, S.M. Hassanizadeh, R.J. Schotting, W.G. Gray & G.F. Pinder (eds.), Development in Water Science 47, Elsevier, Amsterdam, 2002, pp. 469-476.
15. Vadasz, P. Thermal Convection in Rotating Porous Media. in *Trends in Heat, Mass & Momentum Transfer 8*, Research Trends, Trivandrum, Kerala, India, 2002, pp. 25-58.
16. Rudraiah, N.; Shivakumara, I.S.; and Friedrich, R. The effect of rotation on linear and non-linear double-diffusive convection in a sparsely packed porous medium. *Int. J. Heat Mass Transfer* **1986**, 29, pp. 1301-1317.
17. Patil, P.R.; Vaidyanathan, G. On setting up of convection currents in a rotating porous medium under the influence of variable viscosity. *Int. J. Engineering Science* **1983**, 21, pp. 123-130.
18. Jou, J.J.; Liaw, J.S. Transient thermal convection in a rotating porous medium confined between two rigid boundaries. *Int. Comm. Heat and Mass Transfer* **1987**, 14, pp. 147-153.
19. Jou, J.J.; Liaw, J.S. Thermal convection in a porous medium subject to transient heating and rotation. *Int. J. Heat Mass Transfer* **1987**, 30 pp. 208-211.
20. Palm, E.; Tyvand, A. Thermal convection in a rotating porous layer. *J. Appl. Math. & Physics (ZAMP)* **1984**, 35, pp. 122-123.
21. Nield, D.A. The stability of convective flows in porous media, in *Convective Heat and Mass Transfer in Porous Media*, ed. S. Kakaç, B. Kilkis, F.A., Kulacki & F. Arniç, Kluwer Academic Publ., Dordrecht, 1991a, pp. 79-122.
22. Nield DA. Modeling the effect of a magnetic field or rotation on flow in a porous medium: momentum equation and anisotropic permeability analogy. *Int. J. Heat Mass Transfer* **1999**, 42: 3715-3718.
23. Auriault, J.L.; Geindreau, C.; Royer, P. Filtration law in rotating porous media. *C.R. Acad. Sci. Paris* **2000**, t. 328 Serie II b, pp. 779-784.
24. Auriault, J.L.; Geindreau, C.; Royer, P. Coriolis effects on filtration law in rotating porous media. *Transport in Porous Media* **2002**, 48, pp. 315-330.
25. Govender, S. On the effect of anisotropy on the stability of convection in rotating porous media. *Transport in Porous Media* **2006**, 64 (4), pp. 413-422.
26. Govender, S. Vadasz number influence on vibration in a rotating porous layer placed far away from the axis of rotation. *J. Heat Transfer* **2010**, 132, pp. 112601/1-4.

971 27. Havstad, M.A.; Vadasz, P. Numerical Solution of the Three Dimensional Fluid Flow in a Rotating
972 Heterogeneous Porous Channel, *Int. J. for Numerical Methods in Fluids* **1999**, 31 (2), pp.411-429.
973 28. Vadasz, P.; Havstad, M.A. The Effect of Permeability Variations on the Flow in a Rotating Porous
974 Channel, *ASME J. Fluids Engineering* **1999**, 121 (3), pp. 568-573.
975 29. Govender, S.; Vadasz, P. Centrifugal and gravity driven convection in rotating porous media - An
976 analogy with the inclined porous layer. *ASME-HTD* **1995**, 309, pp. 93-98.
977 30. Govender, S.; Vadasz, P. Weak non-linear analysis of moderate Stefan number oscillatory convection in
978 rotating mushy layers. *Transport in Porous Media* **2002**, 48 (3), pp. 353-372.
979 31. Govender, S.; Vadasz, P. Weak non-linear analysis of moderate Stefan number stationary convection in
980 rotating mushy layers. *Transport in Porous Media* **2002**, 49 (3), pp. 247-263.
981 32. Govender, S.; Vadasz, P., The effect of mechanical and thermal anisotropy on the stability of gravity
982 driven convection in rotating porous media in the presence of thermal non-equilibrium. *Transport in*
983 *Porous Media* **2007**, 69 (1), pp. 55-66.
984 33. Vadasz, P. On the evaluation of heat transfer and fluid flow by using the porous media approach with
985 application to cooling of electronic equipment. *Proceedings of the 5th Israeli Conference on Packaging of*
986 *Electronic Equipment*, Herzlia, Israel, 1991, pp. D.4.1-D.4.6.
987 34. Vadasz, P. Natural convection in rotating porous media induced by the centrifugal body force: The
988 solution for small aspect ratio. *ASME J. Energy Resources Technology* **1992**, 114, pp. 250-254.
989 35. Vadasz, P. Three-dimensional free convection in a long rotating porous box. *ASME J. Heat Transfer* **1993**,
990 115, pp. 639-644.
991 36. Vadasz, P. On Taylor-Proudman columns and geostrophic flow in rotating porous media. *SAIMechE*
992 *R&D Journal* **1994**, 10 (3), pp. 53-57.
993 37. Vadasz, P. Centrifugally generated free convection in a rotating porous box. *Int. J. Heat and Mass Transfer*
994 **1994**, 37 (16), pp. 2399-2404.
995 38. Vadasz, P. Stability of free convection in a narrow porous layer subject to rotation. *Int. Comm. Heat Mass*
996 *Transfer* **1994**, 21 (6), pp. 881-890.
997 39. Vadasz, P. Coriolis effect on free convection in a rotating porous box subject to uniform heat generation.
998 *Int. J. Heat and Mass Transfer* **1995**, 38 (11), pp. 2011-2018.
999 40. Vadasz, P. Stability of free convection in a rotating porous layer distant from the axis of rotation.
1000 *Transport in Porous Media* **1996**, 23, pp. 153-173.
1001 41. Vadasz, P. Convection and stability in a rotating porous layer with alternating direction of the centrifugal
1002 body force. *Int. J. Heat Mass Transfer* **1996**, 39 (8), pp. 1639-1647.
1003 42. Vadasz, P. Coriolis effect on gravity-driven convection in a rotating porous layer heated from below. *J.*
1004 *Fluid Mechanics* **1998**, 376, pp. 351-375.
1005 43. Vadasz, P.; Govender, S. Two-dimensional convection induced by gravity and centrifugal forces in a
1006 rotating porous layer far away from the axis of rotation. *Int. J. Rotating Machinery* **1998**, 4 (2), pp. 73-90.
1007 44. Vadasz, P.; Govender, S. Stability and stationary convection induced by gravity and centrifugal forces in
1008 a rotating porous layer distant from the axis of rotation. *Int. J. Engineering Science* **2001**, 39 (6), pp. 715-732.
1009 45. Vadasz, P.; Heerah, A. Experimental confirmation and analytical results of centrifugally-driven free
1010 convection in rotating porous media. *J. Porous Media* **1998**, 1 (3), pp. 261-272.
1011 46. Vadasz, P.; Olek, S. Transitions and chaos for free convection in a rotating porous layer. *Int. J. Heat Mass*
1012 *Transfer* **1998**, 41 (11), pp. 1417-1435.
1013 47. Bhadauria, B.S. Effect of temperature modulation on the onset of Darcy convection in a rotating porous
1014 medium. *Journal of Porous Media* **2008**, 11 (4), pp. 361-375.
1015 48. Malashetty, M.S.; Pop, I.; Heera, R. Linear and nonlinear double diffusive convection in a rotating
1016 sparsely packed porous layer using a thermal non-equilibrium model, *Continuum Mechanics and*
1017 *Thermodynamics* **2009**, 21 (4), pp. 317-339.
1018 49. Vanishree, R. K.; Siddheshwar, P. G. Effect of Rotation on Thermal Convection in an Anisotropic Porous
1019 Medium with Temperature-dependent Viscosity, *Transport in Porous Media* **2010**, 81 (1), pp.73-87.
1020 50. Agarwal, S.; Bhadauria, B.S.; Siddheshwar, P.G. Thermal instability of a nanofluid saturating a rotating
1021 anisotropic porous medium. *Special Topics & Reviews in Porous Media — An International Journal* **2011**, 2 (1),
1022 pp. 53–64.

51. Bhadauria, B. S.; Siddheshwar, P. G.; Kumar, J.; Suthar, O.P. Weakly nonlinear stability analysis of temperature/gravity-modulated stationary Rayleigh–Bénard convection in a rotating porous medium, *Transport in Porous Media* **2012**, 92 (3), pp. 633-647.
52. Agarwal, S.; Bhadauria, B.S. Flow patterns in linear state if Rayleigh-Benard convection in a rotating nanofluid layer. *Applied Nanoscience* **2014**, 4 (8), pp. 935-941.
53. Malashetty, M.S.; Swamy, M.; Kulkarni, S. Thermal convection in a rotating porous layer using a thermal nonequilibrium model. *Physics of Fluids* **2007**, 19, pp. 054102/1-16.
54. Malashetty, M.S.; Swamy, M. The effect of rotation on the onset of convection in a horizontal anisotropic porous layer. *Int. J. Thermal Sciences* **2007**, 46 (10), 1023–1032.
55. Rana, P.; Agarwal, S. Convection in a binary nanofluid saturated rotating porous layer. *J. Nanofluids* **2015**, 4, pp. 1–7.
56. Yadav, D.; Lee, D.; Hee Cho, H.; Lee, J. The Onset of Double Diffusive Nanofluid Convection in a Rotating Porous Medium Layer with Thermal Conductivity and Viscosity Variation: A Revised Model, *J. Porous Media* **2016**, 19 (1), pp. 31-46.
57. Rashidi, M.M.; Mohimanian Pour, S.A.; Hayat, T.; Obaidat, S. Analytic Approximate Solutions for Steady Flow over a Rotating Disk in Porous Medium with heat Transfer by Homotopy Analysis Method, *Computers & Fluids* **2012**, 54, pp. 1-9.
58. Makinde, O.D.; Beg, O.A.; Takhar, H.S. Magnetohydrodynamic Viscous Flow in a Rotating Porous Medium Cylindrical Annulus with a Applied Radial Magnetic Field, *Int. J. Appl. Mathematics and Mechanics* **2009**, 5 (6), pp. 68-81.
59. Straughan, B. *Stability and Wave Motion in Porous Media*. (Applied Mathematical Sciences Series 165), Springer, New York, 2008.
60. Lombardo, S.; Mulone, G. Necessary and sufficient conditions of global nonlinear stability for rotating double-diffusive convection in a porous medium, *Continuum Mechanics and Thermodynamics* **2002**, 14 (6), pp. 527-540.
61. Falsaperla, P.; Mulone, G.; Straughan, B. Rotating porous convection with Prescribed Heat Flux, *Int. J. Engineering Science* **2010**, 48 (7-8), pp. 685–692.
62. Falsaperla, P.; Mulone, G.; Straughan, B. Inertia effects on rotating porous convection, *Int. J. Heat and Mass Transfer* **2011**, 54 (7-8), pp. 1352–1359.
63. Falsaperla, P.; Giacobbe, A.; Mulone, G., Double Diffusion in Rotating Porous Media under General Boundary Conditions , *Int. J. Heat and Mass Transfer* **2012**, 55 (9-10), pp. 2412–2419.
64. Capone, F.; De Luca, R. Ultimately boundedness and stability of triply diffusive mixtures in rotating porous layers under the action of Brinkman law. *Int. J. Non-Linear Mechanics* **2012**, 47 (7), pp. 799-805.
65. Capone, F.; Rionero, S. Inertia effect on the onset of convection in rotating porous layers via the "auxiliary system method". *Int. J. Non-Linear Mechanics* **2013**, 57, pp. 192-200.
66. Capone, F.; De Luca, R. Coincidence between linear and global nonlinear stability of non-constant throughflows via the Rionero ''Auxiliary System Method''. *Meccanica* **2014**, 49 (9), pp. 2025-2036.
67. Boussinesq, J. *Theorie Analitique de la Chaleur*. 2, Gutheir-Villars, Paris, 1903, p. 172.
68. Nield, D.A. The boundary correction for the Rayleigh-Darcy problem: limitations of the Brinkman equation. *J. Fluid Mechanics* **1983**, 128, pp. 37-46.
69. Nield, D.A. The limitations of the Brinkman-Forchheimer equation in modeling flow in a saturated porous medium and at an interface. *Int. J. Heat and Fluid Flow* **1991**, 12 (3), pp. 269-272.
70. Nield, D.A. Discussion on "Analysis of heat transfer regulation and modification employing intermittently emplaced porous cavities". *J. Heat Transfer* **1995**, 117, pp. 554-555.
71. Vafai, K.; Kim, S.J., Analysis of surface enhancement by a porous substrate. *ASME J. Heat Transfer* **1990**, 112, pp. 700-706.
72. Greenspan, H.P. *The Theory of Rotating Fluids*, Cambridge Univ. Press, Cambridge, 1980, pp. 5-18.
73. Straughan, B. A sharp nonlinear stability threshold in rotating porous convection. *Proc. Royal Society of London A* **2001**, 457, pp. 87-93.
74. Sheu, Long-Jye An autonomous system for chaotic convection in a porous medium using a thermal non-equilibrium model. *Chaos, Solitons & Fractals* **2006**, 30, pp. 672-689.
75. Friedrich, R. The effect of Prandtl number on the cellular convection in a rotating fluid saturated porous medium. *ZAMM* **1983**, 63, pp. 246-249. (in German)

76. Chandrasekhar, S. The instability of a layer of fluid heated from below and subject to Coriolis forces, *Proc. Royal Society of London A* **1953**, 217 (1130), pp. 306-327.
77. Chandrasekhar, S. *Hydrodynamic and Hydromagnetic Stability*. Oxford Univ. Press, Oxford (1961), reprint by Dover Publications Inc., New York, 1981.
78. Chakrabarti, A.; Gupta, A.S. Nonlinear thermohaline convection in a rotating porous medium. *Mechanics Research Communications* **1981**, 8 (1), pp. 9-22.
79. Chand, R.: Rana, G.C. On the onset of thermal convection in rotating nanofluid layer saturating a Darcy-Brinkman porous medium, *Int. J. Heat and Mass Transfer* **2012**, 55, pp. 5417-5424.
80. Capone, F.; Gentile, M. Sharp stability results in LTNE rotating anisotropic porous layer. *Int. J. Thermal Sciences* **2018**, 134, pp. 661-664.
81. Galkwad, S.N.; Kouser, S. Analytical study of linear and nonlinear double diffusive convection in a rotating anisotropic porous layer with Soret effect. *J. Porous Media* **2012**, 12(8), pp. 745-761.
82. Malashetty, M.S.; Heera, R. The effect of rotation on the onset of double diffusive convection in a horizontal anisotropic porous layer. *Transport in Porous Media* **2008**, 74, pp. 105-127.
83. Malashetty, M.S.; Begum, I. The effect of rotation on the onset of double diffusive convection in a sparsely packed anisotropic porous layer. *Transport in Porous Media* **2011**, 88, pp. 315-345.
84. Malashetty, M.S.; Kollur, P.; Sidram, W. Effect of rotation on the onset of double diffusive convection in a Darcy porous medium saturated with a couple stress fluid. *Applied Mathematical Modelling* **2013**, 37 (1-2), pp. 172-186. (The effect of rotation on the onset of double diffusive convection in a horizontal couple stress fluid-saturated porous layer, which is heated and salted from below, is studied ana- lytically using both linear and weak nonlinear stability analyses. The extended Darcy model, which includes the time derivative and Coriolis terms, has been employed in the momentum equation. The onset criterion for stationary, oscillatory and finite amplitude convection is derived analytically. The effect of Taylor number, couple stress parameter, solute Rayleigh number, Lewis number, Darcy–Prandtl number, and normalized porosity on the stationary, oscillatory, and finite amplitude convection is shown graphically.)
85. Kumar, A.; Bhadauria, B.S. Non-linear two dimensional double diffusive convection in a rotating porous layer saturated by a viscoelastic fluid. *Transport in Porous Media* **2011**, 87, pp. 229-250.
86. Sunil; Sharma, A.; Bharti, P.K.; Shandil, R.G. Effect of rotation on a layer of micropolar ferromagnetic fluid heated from below saturating a porous medium. *Int. J. Engineering Sciences* **2006**, 44 (11-12), pp. 683-698.
87. Bhadauria, B.S.; Agarwal, S. Natural convection in a nanofluid saturated rotating porous layer: a nonlinear study. *Transport in Porous Media* **2011**, 87, pp. 585-602.
88. Yadav, D.; Lee, J. The effect of local thermal non-equilibrium on the onset of Brinkman convection in a nanofluid saturated rotating porous layer. *J. of Nanofluids* **2015**, 4 (3), pp. 335-342.
89. Yadav, D.; Kim, M.C. The effect of rotation on the onset of transient Soret-driven buoyancy convection in a porous layer saturated by a nanofluid. *Microfluidics and Nanofluidics* **2014**, 17, pp. 1085-1093.
90. Yadav, D.; Lee, J.; Cho, H.H. Brinkman convection induced by purely internal heating in a rotating porous medium layer saturated by a nanofluid. *Powder Technology* **2015**, 286, pp. 592-601.
91. Yadav, D.; Bhargava, R.; Agrawal, G.S.; Yadav, N.; Lee, J., Kim, M.C. Thermal instability in a rotating porous layer saturated by a non-Newtonian nanofluid with thermal conductivity and viscosity variation. *Microfluidics and Nanofluidics* **2014**, 16, pp. 425-440.
92. Yadav, D.; Wang, J.; Lee, J. Onset of Darcy-Brinkman convection in a rotating porous layer induced by purely internal heating. *J. Porous Media* **2017**, 20 (8), pp. 691-706.
93. Malashetty, M.S.; Swamy, M. Combined effect of thermal modulation and rotation on the onset of stationary convection in a porous layer. *Transport in Porous Media* **2007**, 69, pp. 313-330.
94. Bhadauria, B.S. Fluid convection in a rotating porous layer under modulated temperature on the boundaries. *Transport in Porous Media* **2007**, 67, pp. 297-315.
95. Om; Bhadauria, B.S.; Khan, A. modulated centrifugal convection in a vertical rotating porous layer distant from the axis of rotation. *Transport in Porous Media* **2009**, 79, pp. 255-264.
96. Om; Bhadauria, B.S.; Khan, A. Rotating Brinkman-Lapwood convection with modulation. *Transport in Porous Media* **2011**, 88, pp. 369-383.
97. Kang, J.; Niu, J.; Fu, C.; Tan, W. Coriolis effect on thermal convective instability of viscoelastic fluids in a rotating porous cylindrical annulus. *Transport in Porous Media* **2013**, 98, pp. 349-362.

98. Rameshwar, Y.; Sultana, S.; Tagare, S.G. Küppers-Lortz instability in rotating Rayleigh-Benard convection in a porous medium, *Meccanica* **2013**, 48 (10), pp. 2401-2414.