

Preferential Oxidation of CO in Hydrogen at Nonmetal Active Sites with High Activity and Selectivity

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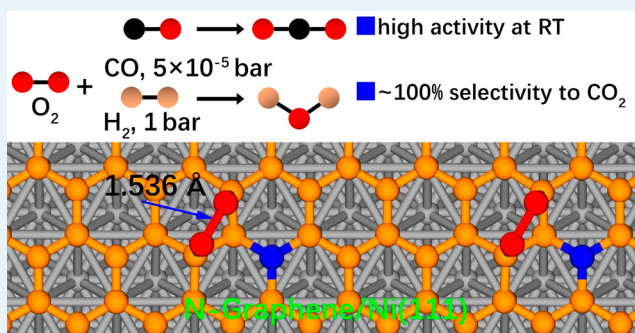
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ABSTRACT: Preferential oxidation of CO in hydrogen (PROX) is an effective process for purification of H₂ gas streams containing CO. Conventional PROX catalysts are usually a platinum group or Au-based. However, low-cost PROX catalysts with high CO conversion and a wide operating temperature window are rare. Here, we design a PROX catalyst by harnessing the electronic atomic monolayer–metal support interaction between a single layer 2-D material and a metallic support. O₂ is physisorbed on nitrogen-doped graphene, while it adsorbs highly activated on Ni(111)-supported nitrogen-doped graphene where the O–O bond can dissociate readily. The adsorbed atomic oxygen can subsequently react with CO or H₂. The proposed catalyst is expected to maintain its activity in the presence of water. Microkinetic modeling results suggest that the turnover frequency of O₂ consumption with a CO partial pressure of 0.01 bar is over 2/s at room temperature and the selectivity to CO₂ is ~100%. As an oxidation catalyst, Ni(111)-supported nitrogen-doped graphene is predicted to be also highly active for ethylene epoxidation at 423 K. Thus, the present study suggests a direction for the design of various selective oxidation catalysts.

KEYWORDS: CO oxidation, PROX, oxidation catalyst, ethylene epoxidation, graphene, DFT calculations



1. INTRODUCTION

Hydrogen produced through methane steam reforming and water gas-shift (WGS) reactions contains ~1% CO, which should be further purified to reduce the CO concentration below 50 ppm for applications in proton-exchange-membrane fuel cells (PEMFCs).^{1–3} PROX is a promising cost-effective process for the removal of CO, as compared to CO methanation ($\text{CO} + 3\text{H}_2 \rightarrow \text{CH}_4 + \text{H}_2\text{O}$), which can consume up to 15% of the available H₂.² A benchmark goal of 50/50 was proposed for PROX catalysts, which means that the CO concentration in the product should be below 50 ppm and the O₂ selectivity to CO₂ should be above 50%.^{1,2} Apart from the 50/50 goal, a good PROX catalyst should also have a wide operating temperature window (~353–473 K) and high thermal stability.⁴ Currently, platinum group metal (PGM) and Au-based catalysts are the most extensively explored PROX catalysts.⁴ Pt catalysts typically possess high water stability, but the activity is low. To improve the activity of Pt catalysts, different preparation methods, oxide supports, and promoters were explored.⁴ A Pt/Fe₂O₃ PROX catalyst featuring subnanometer Pt clusters⁵ was found to be ~100 times more active than a commercially available Pt/Al₂O₃ catalyst.⁶ A recently reported inverse Pt-supported Fe₁(OH)_x catalyst is about 10 times more active than a Pt/Fe₂O₃ PROX catalyst.³ Other supported PGM catalysts including Ir,⁷ Ru,⁸ and Rh⁹ were also explored as PROX catalysts. Au catalysts

exhibit high PROX activity, but the selectivity to CO₂ decreases with an increase in temperature due to the oxidation of H₂. A single-atom Au/CeO₂ catalyst was found to suppress the oxidation of H₂, but it still suffers from a drop in CO₂ selectivity after 20 h of operation.¹⁰ Apart from the activity loss of the catalyst, the presence of water can significantly affect the performance of Au catalysts. A recent study suggests that a commercial Au/Al₂O₃ catalyst exhibits optimal performance when two monolayers of water are adsorbed on the catalyst surface.²

Despite the remarkable progress in Au and PGM PROX catalysts, cost-effective PROX catalysts with high activity are still rare. For example, Cu-based catalysts have been extensively explored, but high conversion of CO is usually achieved only in a narrow temperature range.^{11,12} To design a novel PROX catalyst, we consider the effect of a metal support, which manifests its importance in inverse catalysts.¹³ It was, for example, revealed that a metal support enables electrocatalytic water oxidation on graphene monolayers by changing the

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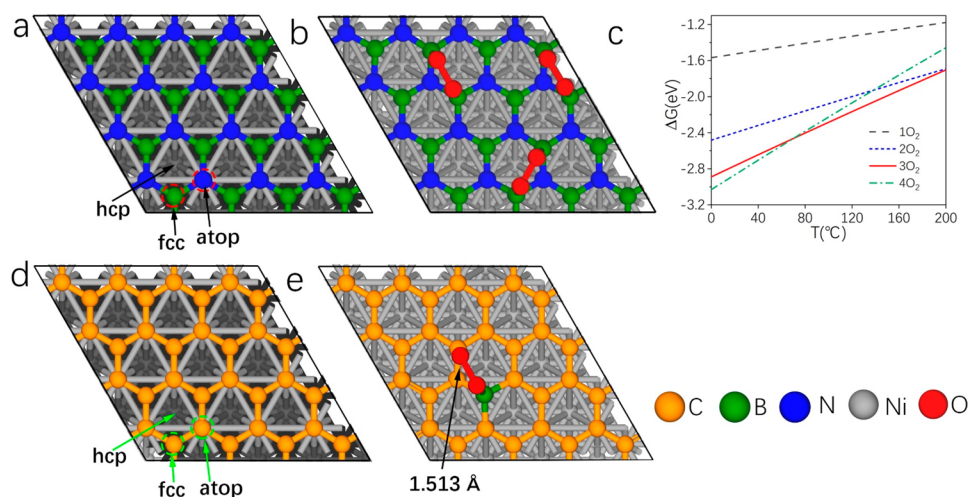


Figure 1. (a) Adsorption configuration of hBN on a five-layer (4×4) Ni(111) support; (b) adsorption of three O₂ molecules on hBN/Ni(111); (c) Gibbs free energies of O₂ adsorption on hBN/Ni(111) at various coverages, with the O₂ partial pressure set to 0.01 bar; (d) adsorption of graphene on a 4×4 Ni(111) support; and (e) adsorption of one O₂ molecule on B-GR/Ni(111).

electronic properties of graphene (GR).¹⁴ Also, we have recently shown that Ni(111)-supported Rh-doped graphene exhibits comparatively high activity for direct methane to methanol oxidation and that overoxidation of methanol can be significantly reduced. In contrast, free-standing Rh-doped graphene has high reaction barriers for methane C–H activation, highlighting the importance of the effect of the Ni(111) support.¹⁵ The tunability of the catalytic activity of doped graphene by a metal support offers enormous opportunities for the design of new catalysts. In the present study, we seek to design Ni(111)-supported monolayer catalysts for PROX reaction. While Ni(111)-supported pristine GR¹⁶ is not able to chemisorb O₂ and hexagonal boron nitride (hBN)¹⁷ is not able to catalyze CO oxidation with a reasonably high reaction rate (vide infra), we show in this Article that boron-¹⁸ or nitrogen-doped¹⁹ graphene (B-GR or N-GR) supported on Ni(111) can chemisorb O₂ with a moderate adsorption energy. We therefore examined CO and H₂ oxidation on B-GR/Ni(111) and N-GR/Ni(111). After determining various reaction pathways, we developed a microkinetic reaction model to understand the activity and selectivity of the catalyst. Finally, we demonstrate that N-GR/Ni(111) is potentially an oxidation catalyst for various reactions by examining the energy profiles of ethylene epoxidation.

2. COMPUTATION METHODS AND MODEL

First-principles calculations were performed using periodic density functional theory (DFT), as implemented in the Vienna Ab initio Simulation Package (VASP 5.4.4).^{20,21} The spin-polarized generalized gradient approximation (GGA) with the PBE functional²² was used to treat exchange-correlation effects. A plane wave basis set with a cutoff energy of 400 eV was selected to describe the valence electrons. The energy difference between reaction energies computed with a 400 and 500 eV cutoff was found to be smaller than 5 meV. The electron–ion interactions were described by the projector augmented wave (PAW)^{23,24} method. Brillouin zone integration was performed with a $3 \times 3 \times 1$ Monkhorst–Pack²⁵ (MP) k-mesh and Gaussian smearing ($\sigma = 0.1$ eV). We used Grimme's DFT-D3²⁶ scheme to treat the van der Waals

interactions semiempirically. PBE-D3 calculations suggest that a graphene layer is 2.17 Å above the outermost plane of the Ni(111) support, which agrees well with the experimental value of 2.1 Å.¹⁶ Other functionals such as RPBE²⁷ or revPBE²⁸ fail to describe the chemisorption of graphene on Ni(111). Because the graphene–Ni(111) interactions can also be well described by the SCAN functional with a long-range van der Waals interaction from rVV10,²⁹ we compared the energetics of selected reaction steps computed with SCAN+rVV10 and PBE-D3. While the chemisorption energy of O₂ is stronger when computed with SCAN+rVV10 by 0.34 eV, the physisorption energy of CO is not sensitive to the choice of functional, and, as discussed in more detail in the [Supporting Information](#), the overall kinetics is only marginally affected by the choice of functional.

The SCF and force convergence criteria for structural optimization were set to 1×10^{-5} eV and 0.01 eV/Å, respectively. The climbing image nudged elastic band (CI-NEB)³⁰ and dimer methods^{31,32} were used to optimize the transition state structures to achieve a force criteria of 0.03 eV/Å. All transition states have been confirmed with the existence of one imaginary frequency whose corresponding eigenvector points in the direction of the reactant and product state.

Neighboring slabs were separated by at least 13 Å of vacuum. The adsorption energy of a gas-phase molecule is defined as $E_{\text{ads}} = E(\text{surface+adsorbent}) - E(\text{surface}) - E(\text{adsorbent})$. Next, the Ni(111) surface is represented by a five-layer (4×4) slab. The lattice parameter of Ni(111) is close to that of graphene (Ni(111), 2.49 Å; graphene, 2.46 Å). To construct a Ni(111) supported graphene, the lattice parameter of Ni(111) is adopted for our calculations. Such a small tensile strain does essentially not change the electronic properties of graphene as shown in [Figure S1](#). Also, the change in lattice parameter from 2.46 to 2.49 Å leads to only a small energy penalty of 0.16, 0.10, and 0.26 eV for a pristine (4×4) graphene, a boron-doped graphene, and a nitrogen-doped graphene, respectively, which is easily overcome by chemisorption on Ni(111). We also considered a six-layer Ni(111)-support model, and the calculated adsorption energy difference of O₂ on N-GR/Ni(111) using the six-layer and the five-layer model is less than 0.01 eV. Thus, we used the five-layer model for all subsequent calculations.

Next, the harmonic transition state theory was used to calculate all elementary rate constants of surface processes. Collision theory with a sticking coefficient of 1 was used to estimate the rate constants for adsorption processes. Using the obtained rate constants of each elementary step, we developed a chemical master equation of probability densities for the system to occupy each discrete state and solved for the steady-state solution. No assumption of active site coverage was made in the kinetic model. Details of our rate constant are provided in the [Supporting Information](#). Finally, the energy of O_2 is adjusted to fit the experimental reaction energy of hydrogen combustion, $2H_2 + O_2 \rightarrow 2H_2O$, and increased by 0.49 eV to correct the overbinding³³ of O_2 predicted by the PBE functional.¹⁵ A correction to the energy of O_2 lowers the free energy of each intermediate and transition state along the energy profile by 0.49 eV, while the energy barriers are not affected.

3. RESULTS AND DISCUSSION

3.1. Adsorption of O_2 on B-GR/Ni(111). Our attempt of identifying promising PROX catalysts starts from hBN/Ni(111) ([Figure 1a](#)) where boron is situated at the hcp site and nitrogen is situated at the atop site, respectively.³⁴ The chemisorption energy of hBN on a (4×4) Ni(111) was calculated to be -3.93 eV. O_2 molecules were found to be chemisorbed strongly on hBN/Ni(111) with the neighboring boron atoms occupied by two oxygen atoms ([Figure 1b](#)), which contrasts the case of free-standing hBN where O_2 is only physisorbed. Bader charge analysis³⁵ suggests that a (4×4) hBN layer has a total negative charge of -1.13 e $^-$, indicative of the formation of chemical bonds between hBN and Ni(111). Upon the chemisorption of O_2 , Ni(111) can serve as an electron reservoir and compensate the loss of electrons transferred from hBN to O_2 . Each chemisorbed O_2 has a negative charge of ca. -1.8 e $^-$ and the O–O bond length is elongated to a range of 1.46–1.50 Å, depending on the number of O_2 molecules on hBN/Ni(111). Therefore, the presence of a Ni(111) support leads to a significant modification of the properties of hBN. Constrained thermodynamics calculations suggest that up to three O_2 molecules can be accommodated on a (4×4) hBN/Ni(111) at 80 °C and at a O_2 partial pressure of 0.01 bar ([Figure 1c](#)), following the typical operation conditions of the PROX reaction.¹⁰ We therefore investigated the oxidation of CO on hBN/Ni(111) loaded with three O_2 molecules ([Figure S2](#)). However, we observed a free energy barrier of 1.19 eV (80 °C, CO partial pressure is 0.01 bar), corresponding to a forward rate constant of only 7.89×10^{-5} /s, suggesting that hBN/Ni(111) is not a good candidate for catalyzing CO oxidation under PROX reaction conditions. Next, we considered the case of Ni(111)-supported graphene. Our calculations suggest that GR is preferably adsorbed on Ni(111) with an atop/fcc configuration ([Figure 1d](#)), consistent with a previous study.¹⁶ The adsorption energy is calculated to be -2.10 eV for a (4×4) graphene layer. However, O_2 can only be physisorbed on GR/Ni(111). Considering that in the case of hBN/Ni(111) O_2 can be adsorbed strongly on a boron site, we speculated that the presence of a boron dopant in GR/Ni(111) can also lead to the chemisorption of O_2 . We note that boron-doped graphene (B-GR) has previously been synthesized and used as an electrocatalyst.¹⁸ A carbon atom on top of the Ni fcc site was replaced with a boron atom to construct our atomistic model shown in [Figure 1d](#), which is the most favorable

adsorption configuration ([Figure S3](#)), and the adsorption energy of B-GR on Ni(111) was calculated to be -4.03 eV. A Bader charge calculation suggests that B-GR gains 1.39 e $^-$ from Ni(111).

The O–O bond is elongated to 1.513 Å upon adsorption on B-GR/Ni(111) (see [Figure 1e](#)). One oxygen binds to a fcc carbon, while the other one binds to boron. The chemisorption of O_2 on B-GR/Ni(111) contrasts that on free-standing B-GR where O_2 is only physisorbed. Apart from O_2 , all other investigated molecules in the present study (including CO) are physisorbed on B-GR/Ni(111).

3.2. CO Oxidation on B-GR/Ni(111). [Figure 2](#) illustrates the free energy diagram of CO oxidation on B-GR/Ni(111)

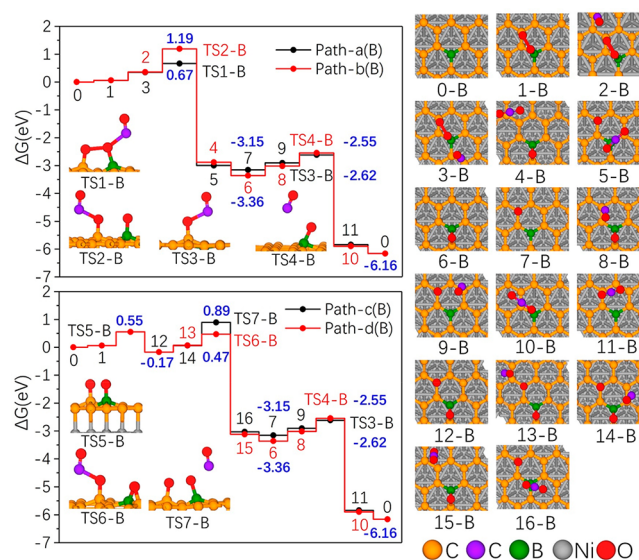


Figure 2. Free energy profiles of CO oxidation on B-GR/Ni(111) at 353 K. The partial pressures of all gas-phase molecules are set to be 1 bar. In **Paths-a(B)** and **-b(B)**, CO reacts with oxygen before O_2 dissociation occurs; in **Paths-c(B)** and **-d(B)**, CO reacts with atomic O. Boron doping is denoted as B in each intermediate and transition state. The B in each intermediate state along the energy profile is omitted for clarity. The description of each elementary is also presented in [Table S1](#).

calculated at 353 K. CO can react with the pristine O_2 on B-GR/Ni(111) (see [Figure 2](#), **Paths-a(B)** and **-b(B)**) or atomic O after the dissociation of the O–O bond (**Paths-c(B)** and **-d(B)**). The adsorption of O_2 is only slightly endergonic by 0.06 eV. In **Path-a(B)**, CO reacts with the O adsorbed at the boron site first, which is concomitant with the dissociation of the O–O bond and has an effective barrier of 0.67 eV ($3-B \rightarrow 5-B$); following the concept of the energy span model,³⁶ an effective barrier is calculated as the energy difference between a transition state and the lowest-energy intermediate preceding it). $5-B \rightarrow 7-B$ and $4-B \rightarrow 6-B$ correspond to the desorption of CO_2 . The second CO reacts with the O adsorbed on the C site, and the effective barrier amounts to 0.53 eV ($9-B \rightarrow 11-B$). In **Path-b(B)**, CO reacts first with the O adsorbed at the carbon site. The effective barriers for CO oxidation along **Path-b(B)** are 1.19 and 0.81 eV, respectively.

The dissociation of the O–O bond has an effective barrier of 0.55 eV, whose free energy of reaction is exergonic by -0.17 eV ($1-B \rightarrow 12-B$). After O–O bond dissociation, one oxygen atom binds to one carbon atom in an upright configuration, while the other oxygen is shared by a boron and a carbon atom

(12-B, called B-bonded oxygen hereafter). The comparatively weak adsorption of oxygen on B-GR/Ni(111) is beneficial for the removal of oxygen by CO. The reaction of the C-bonded O with the first CO (13-B \rightarrow 15-B) has an effective barrier of 0.64 eV (Path-d(B)), while the reaction for the B-bonded O (14-B \rightarrow 16-B) has a barrier of 1.06 eV (Path-c(B)). The remaining parts of Paths-c(B) and -d(B) are identical to those of Paths-a(B) and -b(B), respectively. Because an oxygen atom can migrate from a boron site to a carbon site (6-B \rightarrow 7-B) by overcoming a barrier of 0.84 eV (Table S4), the second CO oxidation can also occur through the pathway 6-B \rightarrow 7-B \rightarrow 9-B \rightarrow 11-B. Throughout the process, an Eley–Rideal mechanism of CO oxidation is followed. Considering the energy profiles of Paths-a, -b, -c, and -d(B), we can deduce that the first CO oxidation mainly proceeds through the path 12-B \rightarrow 13-B \rightarrow 15-B. For the second CO oxidation, if the effective barrier of 6-B \rightarrow TS4-B \rightarrow 10-B (possible when the CO partial pressure is noticeably lower than 1 bar) is higher than that of the oxygen migration (6-B \rightarrow 7-B), then a 6-B \rightarrow 7-B \rightarrow 9-B \rightarrow 11-B pathway is followed, which lowers the effective barrier by 0.07 eV relative to the pathway through TS4-B. In other words, the oxygen migration from the boron site to the carbon site can possibly lower the effective barrier of the second CO oxidation at lower partial pressures of CO due to the fact that TS3-B is 0.07 eV lower than TS4-B.

3.3. H₂ Oxidation on B-GR/Ni(111). For the reaction of H₂ with O₂ adsorbed on B-GR/Ni(111), we were unable to find an elementary reaction step involving the dissociation of O₂ and the formation of H₂O. In other words, O₂ dissociation has to occur prior to the reaction of atomic O with H₂. Because the H₂ molecule is only weakly physisorbed on B-GR/Ni(111), an Eley–Rideal mechanism is again followed. Figure 3 illustrates that the reaction of the first H₂ with the O at the

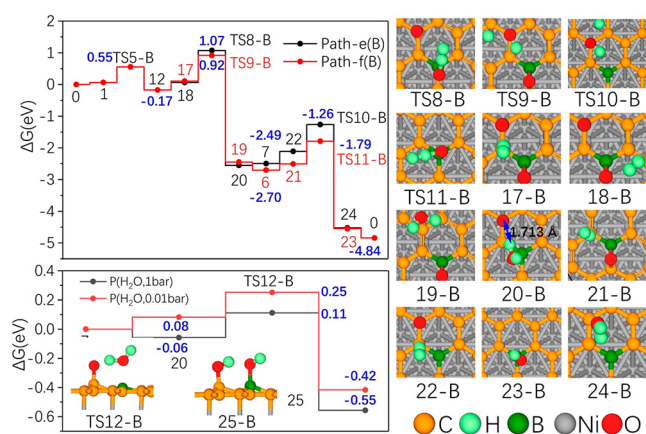


Figure 3. Free energy profiles of H₂ oxidation (above) as well as the formation of two hydroxyls by an oxygen atom and water (below) on B-GR/Ni(111) at 353 K. The partial pressures of all gas-phase molecules are set to be 1 bar. The description of each elementary is also presented in Table S1.

boron site has an effective barrier of 1.24 eV (18-B \rightarrow 20-B, Path-e(B)), as compared to the O on the carbon site, which has a barrier of 1.09 eV (17-B \rightarrow 19-B, Path-f(B)). Along Path-e(B), the reaction of the second H₂ and the C-bonded O (7-B \rightarrow 24-B) has an effective barrier of 1.23 eV, while the reaction of the second atomic O (6-B \rightarrow 23-B) along Path-f(B) has a lower barrier of 0.91 eV. The reactions of H₂ with the boron-bonded oxygen feature early transition states (TS8-

B and TS11-B, see TS configurations in Figures 3 and S4), while those involving the carbon-bonded oxygen feature late transition states (TS9-B and TS10-B). For the reaction of each oxygen atom, we observe that CO has a higher reactivity than does H₂, which is due to the fact that the formation of H₂O requires the insertion of the oxygen atom into the H–H bond of the physisorbed H₂, while CO₂ is formed simply by the approach of CO to the adsorbed oxygen. Moreover, we examined the dissociation of H₂ on B-GR/Ni(111) in the absence of adsorbed oxygen, which has a high barrier of 2.40 eV and is endergonic by 1.12 eV (see Figure S5). From the above discussions, it is obvious that an oxygen atom bonded to a boron and a carbon has distinct reactivities. This can be traced back to the different adsorption configurations of oxygen in 6-B and 7-B where an oxygen atom binds to both boron and carbon atoms in the case of 6-B and only to a carbon atom in the latter case of 7-B (see Figure 2).

Under PROX reaction conditions, the presence of water is unavoidable. Therefore, we incorporated the presence of water in the reaction pathways on B-GR/Ni(111). 20-B \rightarrow 25-B corresponds to the reaction of an adsorbed water and an oxygen atom, which produces two hydroxyl groups and has a low barrier of 0.17 eV at a water pressure of 1 bar (see Figure 3). At a water partial pressure of 0.01 bar, which is more typical for PROX reactors, the energy profile shown in Figure 3 suggests that 25-B is 0.42 eV lower than 7-B. The reaction of 25-B and a physisorbed CO may proceed through a COOH mechanism of CO oxidation,³⁷ which is common for chemisorbed CO and OH that can produce a COOH intermediate, followed by cleavage of the O–H bond to produce CO₂. However, we were not able to identify a COOH mechanism in the present case, likely because the approach of the CO to the B-GR/Ni(111) surface is energetically unfavorable. To react with CO, the two hydroxyl groups need to form an adsorb oxygen and a water molecule (25-B \rightarrow 20-B), followed by facile water desorption (25-B \rightarrow 7-B). Considering that the effective barrier of 6-B \rightarrow TS4-B \rightarrow 10-B at a CO partial pressure of 0.01 bar (PROX condition) is calculated to be 0.95 eV (i.e., it is higher than the oxygen migration barrier of 0.84 eV; see Table S4), the second CO oxidation preferably proceeds through 6-B \rightarrow 7-B \rightarrow 9-B \rightarrow 11-B with an effective barrier of 0.88 eV. However, in the presence of H₂O (0.01 bar), the effective barrier of the second CO oxidation on B-GR/Ni(111) is increased by 0.42 eV, being 1.30 eV, which is translated to a low forward reaction rate of 2.03×10^{-6} /s. Thus, we can conclude that CO oxidation on B-GR/Ni(111) is poisoned by water dissociation under PROX reaction conditions.

3.4. CO and H₂ Oxidation on N-GR/Ni(111). Because B-GR/Ni(111) appears to be not a good active site model for a PROX catalyst, we next examined the PROX reaction on nitrogen-doped graphene supported on Ni(111). Again, various reaction pathways involving the dissociation of water were considered. We first identified the most favorable adsorption configuration of N-GR on Ni(111) shown in Figures 4a and S6, whose adsorption energy is -2.35 eV. Bader charge calculations suggest that the N-GR unit cell gains $1.58 e^-$ from Ni(111). We found that an O₂ molecule can be chemisorbed on N-GR/Ni(111) in three different configurations (Modes-a, -b, and -c in Figure 4b). In all cases, one or two next-nearest carbon atoms of the nitrogen site (C1–C6 in Figure 4a) are occupied by oxygen. We were unable to identify other chemisorption configurations of O₂ for which other

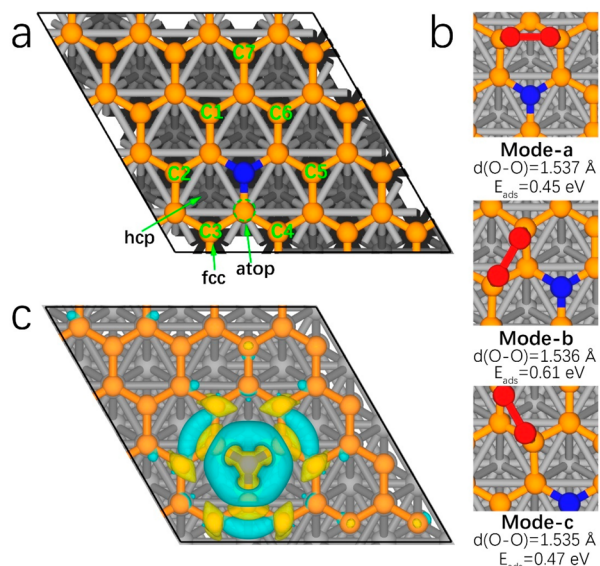


Figure 4. (a) Adsorption configuration of nitrogen-doped graphene on a five-layer (4 × 4) Ni(111) support. C1–C6 are equivalent carbon atoms. (b) Chemisorption configurations of O₂ on N-GR/Ni(111). (c) Charge density difference upon the deposition of nitrogen at Ni(111)-supported graphene with a carbon defect. The accumulation (depletion) of electrons is denoted by yellow (blue). The isosurface value is 0.003 e[−]/Å³.

carbon atoms or the nitrogen site are adsorption sites of oxygen. A charge density difference plot suggests that, upon the deposition of nitrogen at the carbon defect site of GR/Ni(111), the charge surrounding the nitrogen atom redistributes and charge accumulation occurs on the six next-nearest carbon atoms (Figure 4c), C1–C6. In the case of free-standing N-GR, O₂ is only physisorbed.

To further understand the activation of an O₂ molecule by the carbon atoms of N-GR/Ni(111), we plotted the projected density of states of carbon (PDOS, Figure 5a) for the free-standing and Ni(111)-supported GR, B-GR, and N-GR. The PDOS of carbon moves toward lower energies due to the interaction with Ni(111), which is indicative of electronic interaction between GR (or doped-GR) and Ni(111). Inspection of the PDOS near the Fermi level suggests that the electrons of carbon (supported on Ni(111)) have a small spin-polarization, which can be attributed to the broken sublattice symmetry of graphene^{38,39} due to the presence of Ni(111). The spin-polarization of carbon is also reflected in the spin-density plot (Figure 5b), and each carbon atom has a magnetic moment of ~0.03 μ_B. For the case of supported boron nitride, each boron has a magnetic moment of ~0.02 μ_B. The spin-polarized carbon or boron facilitates the activation of O₂. However, an O₂ molecule is not chemisorbed (practically no change in O–O bond distance) on GR/Ni(111), likely due to the weaker adsorption of an oxygen atom on GR/Ni(111) (−0.71 eV) relative to the C1–C6 sites on N-GR/Ni(111) (Figure 4a, −0.87 eV) where the O–O bond distance is increased to 1.54 Å upon O₂ adsorption. Carbon atoms (e.g., C7 in Figure 4a) distant from the nitrogen-dopant have an oxygen adsorption of ~−0.73 eV (close to pristine graphene) and are not able to activate O₂. This is consistent with the fact that charge-redistribution due to the nitrogen-doping occurs at C1–C6.

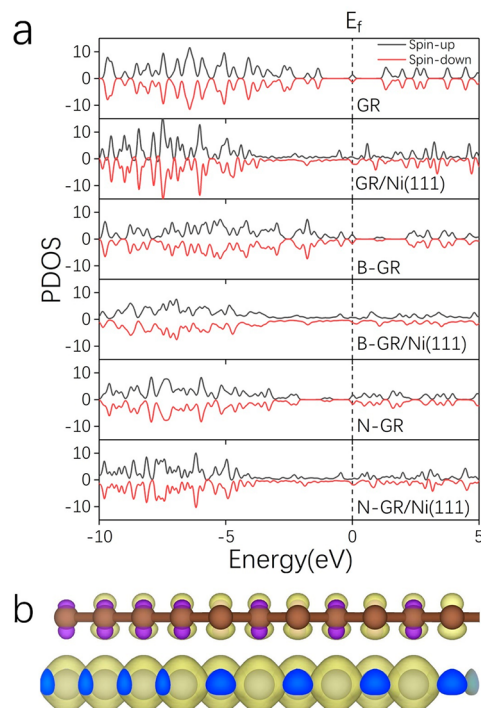


Figure 5. (a) Projected density of states of carbon for free-standing GR, B-GR, and N-GR as well as the Ni(111)-supported counterpart. The Fermi level is set to 0 eV. (b) Spin density of Ni(111)-supported pristine graphene. Spin-up (spin-down) electrons are denoted by yellow (purple). The isosurface value is 0.003 e[−]/Å³.

We next examined the energy profiles (Paths-a(N) and -b(N)) of CO and H₂ oxidation for the most favorable O₂ adsorption configuration Mode-b, as displayed in Figure 6. O₂ adsorption is slightly endergonic at 353 K (1-N), followed by O–O dissociation, which involves a vanishingly small barrier. As compared to the O–O bond dissociation on B-GR/Ni(111), the more favorable O–O dissociation on N-GR/Ni(111) can be attributed to the fact that an upright

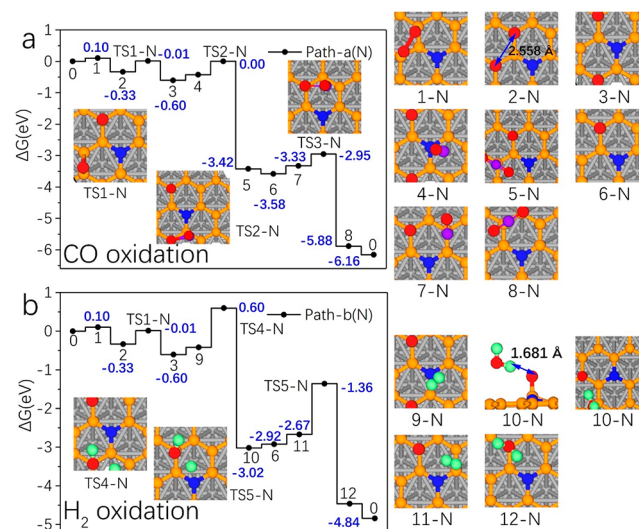


Figure 6. Free energy profiles of CO (a) and H₂ oxidation (b) on N-GR/Ni(111) at 353 K without the dissociation of H₂O. The partial pressures of all gas-phase molecules are set to be 1 bar. The description of each elementary is also presented in Table S2.

adsorption configuration of oxygen on boron in TS5-B is unfavorable for the B-GR/Ni(111). The two oxygen atoms of 2-N have a comparatively short distance of 2.558 Å, and the migration of one oxygen to another carbon site leads to a decrease in free energy of 0.27 eV, which we attribute to a decrease in electrostatic repulsion between the negatively charged oxygen atoms. The physisorbed CO can react with oxygen atoms adsorbed on N-GR/Ni(111) through the paths 3-N → 4-N → 5-N and 6-N → 7-N → 8-N, whose effective barrier we calculated to be 0.60 and 0.57 eV at 353 K, respectively. The H₂ oxidation possesses a significantly higher activation barrier than does the CO counterpart, being 1.20 eV for 3-N → 9-N → 10-N and 1.56 eV for 6-N → 11-N → 12-N, respectively. Note that the desorption of H₂O (10-N → 9-N) is slightly endergonic at a high H₂O partial pressure of 1 bar due to the relatively strong hydrogen bond between hydrogen and oxygen (denoted as 10-N in Figure 6b).

We also investigated reaction pathways (Paths-c(N) and -d(N)) of H₂ and CO oxidation on N-GR/Ni(111) involving the dissociation of water shown in Figure 7. Starting from 3-N,

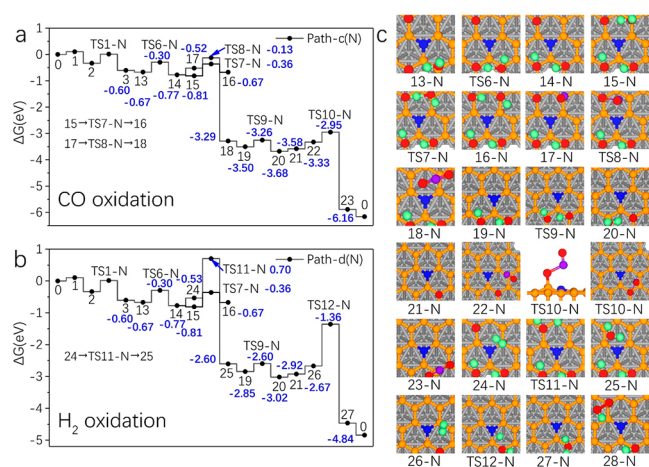


Figure 7. Free energy profiles of CO (a) and H₂ oxidation (b) on N-GR/Ni(111) at 353 K involving the dissociation of H₂O. (c) Configurations of all intermediate and transition states. The partial pressures of all gas-phase molecules are set to be 1 bar. The description of each elementary is also presented in Table S2.

oxygen can react with adsorbed H₂O to form hydroxyl groups. 14-N featuring two hydroxyl groups is 0.17 eV lower in free energy than is 3-N, whereas 16-N featuring four hydroxyl groups is 0.10 eV higher in energy than is 14-N. Therefore, the formation of hydroxyl groups on N-GR/Ni(111) is less thermodynamically favorable than the 7-B → 20-B → 25-B counterpart of B-GR/Ni(111). 14-N can react with CO by overcoming an effective barrier of 0.64 eV to form 18-N. Upon the formation of the first CO₂, the two hydroxyl groups of 19-N can form an adsorbed oxygen and H₂O, which is energetically downhill by 0.18 eV. While the 21-N → 22-N → 23-N path occurs at an active site different from that of the 6-N → 7-N → 8-N path (see Figures 6a and 7a), the energy profiles of the two processes are the same because the oxygen atoms of 21-N and 6-N are equivalent (see Figure 4). H₂ can also be oxidized on N-GR/Ni(111) in the same vein as CO through 14-N → 24-N → 25-N and 21-N → 26-N → 27-N, respectively, with noticeably higher activation energies than the CO oxidation. We emphasize here that the energetically uphill process of 14-N → 15-N → 16-N and downhill process of

19-N → 20-N → 21-N (even if the H₂O partial pressure is 1 bar) ensure that no hydroxyl group poisoning occurs for the N-GR/Ni(111) catalyst. Apart from the reaction pathways in the absence/presence of H₂O, we also considered a reaction pathway involving an OOH species, which is a possible active species for CO oxidation.⁴⁰ Here, we found that the formation of an OOH species is energetically uphill by 1.25 eV (14-N → 28-N), which is significantly higher than the effective barrier of CO oxidation (~0.6 eV) mentioned above. Therefore, an OOH pathway is unlikely to occur on N-GR/Ni(111).

To this end, we have examined the energy profiles of the CO and H₂ oxidation on B-GR/Ni(111) and N-GR/Ni(111). We found that, at 353 K, CO oxidation by an adsorbed oxygen at a carbon site has an effective barrier of around 0.60 eV, which is not sensitive to the environment of the active sites. In comparison, the effective barrier of H₂ oxidation at the carbon site ranges from 1.09 eV (12-B → TS9-B → 19-B) to 1.56 eV (6-N → TS5-N → 12-N), which can be correlated with the oxygen adsorption energy (see Figure 8). Hence, a lower

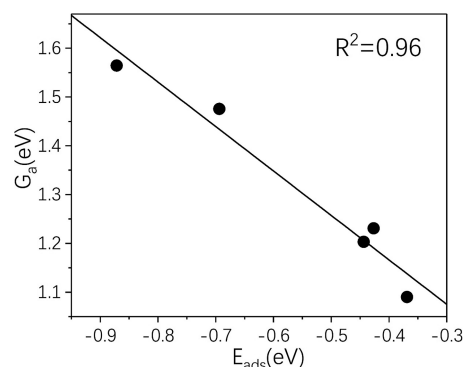


Figure 8. Scaling relation between the effective barrier (G_a , 353 K, the H₂ pressure is 1 bar) of H₂ oxidation by O adsorbed at the carbon site on B-GR/Ni(111) and N-GR/Ni(111) versus the O adsorption energy (E_{ads}). $G_a = 0.911 \times E_{ads} + 0.802$. The reference state of E_{ads} is the clean surface and 0.5O₂ in the vapor phase.

oxygen adsorption energy is favorable for the formation of water. We note here that the scaling relation of H₂ oxidation on the C-bonded oxygen is not applicable for the B-bonded oxygen shown in Figure S7; that is, the scatter in the data is large, probably due to the different adsorption configuration of the B-bonded oxygen.

3.5. Microkinetic Modeling of CO and H₂ Oxidation on N-GR/Ni(111). A microkinetic model was developed to understand the PROX reaction kinetics (see Tables S5–S8 for the rate constants of each elementary step). The microkinetic model was solved for a H₂ partial pressure of 1 bar. The CO partial pressure was set to be in the range of 5×10^{-5} and 0.01 bar.¹⁰ A low CO pressure of 5×10^{-5} bar was considered due to the need to reduce the CO concentration to ~50 ppm.^{1,2} The partial pressures of O₂, H₂O, and CO₂ were all set to be 0.01 bar. At 353 K and a CO partial pressure of 0.01 bar, the turnover frequency (TOF) of O₂ consumption was calculated to be 33.46/s, and the selectivity to CO₂ is ~100%. At a CO pressure of 5×10^{-5} bar, the selectivity to CO₂ still reaches ~100%. Figure 9 shows a low apparent activation energy of 0.45 eV for the oxygen consumption. The reaction orders of CO (from 5×10^{-5} to 0.01 bar) and O₂ (0.01–1 bar) were calculated to be 1 and 0 at 353 K, respectively. Even if the temperature decreases to 300 K, a high TOF of 2.38/s was

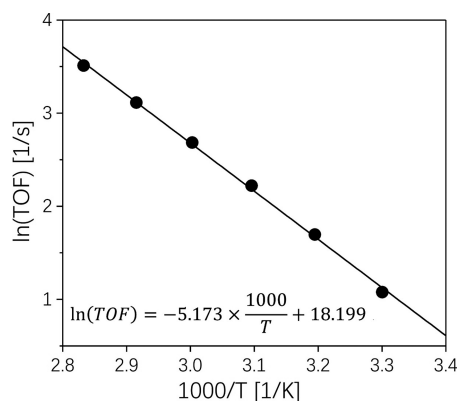


Figure 9. Arrhenius plot for CO/H₂ oxidation, that is, O₂ consumption, over N-GR/Ni(111) in the temperature range 300–353 K.

obtained, which is comparable to that found for Pt-supported Fe₁(OH)_x (2.1/s).³

To better understand the high activity and selectivity of CO oxidation obtained from the microkinetic analysis, we plotted in Figures S8 and S9 the free energy profiles with a CO partial pressure of 0.01 bar. Along **Paths-a(N)** and **-b(N)**, the effective barriers of the first and second CO oxidation were calculated to be 0.74 and 0.77 eV, respectively, as compared to 1.20 and 1.56 eV for the oxidation of the first and the second H₂. If the dissociation of H₂O is involved in the reaction, the effective barrier for the first CO oxidation along **Path-c(N)** is 0.78 eV, as compared to 1.47 eV for the H₂ along **Path-d(N)**. The effective barriers of the second CO and H₂ oxidation along **Path-c(N)** and **Path-d(N)** are the same as those along **Path-a(N)** and **Path-b(N)**, respectively. Even if the CO partial pressure is reduced to 5×10^{-5} bar, the effective barriers of CO oxidation are only ~ 0.94 eV (see Figure S10), noticeably lower than those of the H₂ oxidation, which hence leads to the high selectivity to CO₂.

To summarize, we have shown that N-GR/Ni(111) is a highly active and selective catalyst for PROX. Key to this process is the activation of O₂ enabled by the Ni(111) support that covalently binds with the N-GR monolayer. As the nitrogen-doped graphene has been explored extensively in heterogeneous catalysis^{41–44} and the encapsulation of metals by a graphene-like atomic monolayer was realized experimentally through a chemical vapor deposition process in mesoporous silica,¹⁴ it can be expected that the N-GR/Ni(111) model catalyst proposed here can also be fabricated. Our prediction of N-GR/Ni(111) as oxidation catalyst is further supported by a recent experimental observation that cobalt nanoparticles encapsulated by nitrogen-doped carbon nanotubes are efficient catalysts for selective oxidation of hydrocarbons.⁴³ Apart from the favorable electronic interaction between N-GR and Ni, an advantage of the encapsulated structure is that N-GR can prevent Ni from being oxidized. Also, H₂ cannot easily diffuse through the N-GR layer and dissociate into adsorbed H atoms (the diffusion barrier is ~ 4 eV).

3.6. Ethylene Epoxidation on N-GR/Ni(111). Finally, we examined the possibility of N-GR/Ni(111) as a more general oxidation catalyst, and we investigated the ethylene epoxidation reaction over N-GR/Ni(111), which is commercialized over Ag/ α -Al₂O₃ at 473–513 K using O₂ as the oxidant.^{45,46} Because the annual production of ethylene oxide is over 20

million tons, increasing the selectivity to ethylene oxide and lowering the reaction temperature is highly desirable and an active area of research.⁴⁷ As an example, low-temperature (308 K) ethylene epoxidation was achieved over a mesoporous silicate using H₂O₂ as the oxidant.⁴⁶ Here, we present in Figure 10 the calculated energy profiles of ethylene epoxidation on N-

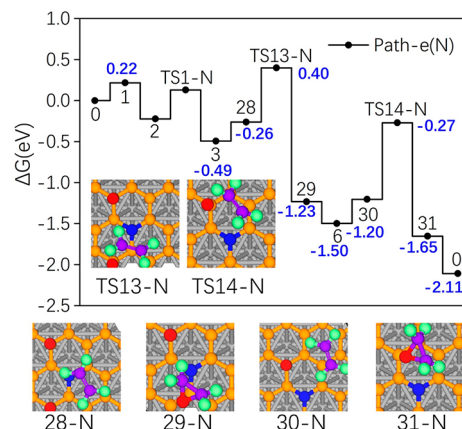


Figure 10. Free energy profiles of ethylene epoxidation on N-GR/Ni(111) at 423 K. The partial pressures of all gas-phase molecules are set to be 1 bar. The description of each elementary is also presented in Table S3.

GR/Ni(111). The physisorbed ethylene on N-GR/Ni(111) reacts with oxygen through an Eley–Rideal mechanism after the facile dissociation of the chemisorbed O₂. Interestingly, because ethylene is not chemisorbed, an oxametallacycle intermediate⁴⁷ of ethylene epoxidation typical for silver catalysts that processes both ethylene oxide and acetaldehyde is avoided in the present case. Ethylene can react with the first oxygen readily with an effective energy barrier of 0.89 eV, while the second ethylene epoxidation has a higher barrier of 1.23 eV. The relatively difficult epoxidation of the second ethylene is due to the stronger adsorption energy of the second oxygen (see Table 1). Next, we developed and solved a steady-state

Table 1. Adsorption Energy (Not Zero-Point Corrected in eV) of One Oxygen Atom ($E_{\text{ads}}(\text{O})$) on Each Surface and One Hydrogen Atom on a Preadsorbed Oxygen ($E_{\text{ads}}(\text{H})$)^a

	$E_{\text{ads}}(\text{O})$	$E_{\text{ads}}(\text{H})$
first oxygen of N-GR/Ni(111)	−0.44	−1.64
second oxygen of N-GR/Ni(111)	−0.87	−1.25
Ag(111)	−0.87	−1.53
Pd(111)	−1.72	−0.56
Pt(111)	−1.52	−0.38
Rh(111)	−2.41	−0.31

^aThe reference state is the clean surface and 0.5O₂ and 0.5H₂ molecules in the gas phase, respectively.

microkinetic model for the epoxidation at 423 K with ethylene, oxygen, and ethylene oxide partial pressures of 10, 1, and 1 bar, respectively (see Table S9 for the model parameters). The TOF of ethylene oxide formation was calculated to be 0.41/s. The appreciable TOF suggests that N-GR/Ni(111) might also be a promising low-temperature ethylene epoxidation catalyst.

To understand the high activity of ethylene epoxidation on N-GR/Ni(111), we computed the adsorption energies of an oxygen atom and one hydrogen atom on a preadsorbed oxygen

on several surfaces. Table 1 shows that the adsorption behavior of O and H on N-GR/Ni(111) resembles that on Ag(111), while it contrasts those on Pd(111), Pt(111), and Rh(111). The similarity of oxygen and hydrogen adsorption on N-GR/Ni(111) and Ag(111) might be the origin for the high catalytic oxidation activity of N-GR/Ni(111).

4. CONCLUSIONS

We designed a N-GR/Ni(111) PROX catalyst through first-principles calculations. Ni(111)-supported boron-doped graphene was found to chemisorb O₂ with a significantly elongated O–O bond, leading to facile O–O dissociation. A carbon atom and its neighboring boron are the active sites for adsorption and reaction. While the CO oxidation on B-GR/Ni(111) is facile and the H₂ oxidation is much less active, we found that B-GR/Ni(111) is likely not a good PROX catalyst due to the energetically favorable formation of stable hydroxyl groups from the reaction of H₂O and adsorbed oxygen atoms on B-GR/Ni(111) that poison the catalyst. By contrast, N-GR/Ni(111) is highly active for CO oxidation in the presence of water. The two next-nearest carbon atoms of the nitrogen site are the active sites. Microkinetic modeling suggests that N-GR/Ni(111) is highly active and selective for PROX, with a TOF of O₂ consumption (300 K, CO pressure is 0.01 bar) and selectivity to CO₂ of 2.38/s and ~100%, respectively. The effective free energy barrier of H₂ oxidation (at 1 bar H₂ pressure) is over 0.2 eV higher than that of CO (at 5 × 10^{−5} bar CO pressure) oxidation, ensuring the high selectivity to CO₂. N-GR/Ni(111) is also highly active for ethylene epoxidation at 423 K, and the TOF was calculated to be 0.41/s. The chemisorption of O₂ on B-GR/Ni(111) and N-GR/Ni(111) contrasts the physisorption of O₂ on free-standing B-GR and N-GR, which highlights the potential of the electronic atomic monolayer–metal support interaction for the design of novel oxidation catalysts.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acscatal.0c00743>.

Additional discussions on the choice of DFT functional, free energy profile of CO oxidation on hBN/Ni(111), relative energies for different B-GR adsorption configurations, transition state configurations of H₂ oxidation on B-GR/Ni(111), free energy profile of H₂ dissociation on B-GR/Ni(111), relative energies for different N-GR adsorption configurations, free energy profiles of CO and H₂ oxidation at various temperatures and pressures, and details of the microkinetic model (PDF)

DFT structures of surface intermediates and transition states (PDF)

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Notes

The authors declare no competing financial interest.

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