

# Elucidating Secondary Metal Cation Effects on Nickel Olefin Polymerization Catalysts

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**Keywords:** olefin polymerization, coordination insertion, nickel catalysts, cation tuning, polyethylene

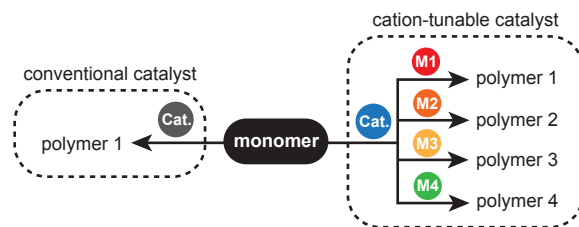
**ABSTRACT:** Secondary metal cations, such as alkali and transition metal ions, have been shown to enhance the catalytic performance of nickel and palladium olefin polymerization catalysts. Their beneficial effects can manifest in different ways, such as increasing rates of polymerization, altering polymer microstructures, enhancing catalyst thermal stability, or a combination of these effects. We have systematically quantified secondary metal ion influences on nickel phenoxyphosphine polyethylene glycol (PEG) complexes. We demonstrate that cation-tuning could readily achieve three-dimensional structures and electronic environments that are not easily accessible through conventional ligand-tuning. This study led to the development of extremely active ethylene polymerization catalysts. For example, the nickel-lithium complex gave activity and turnover number as high as  $7.0 \times 10^4$  kg PE/mol Ni·h and  $2.5 \times 10^6$  mol ethylene/mol Ni, respectively and the nickel-cesium complex showed unusual thermal stability up to 90 °C (activity =  $2.3 \times 10^4$  kg/mol·h, turnover number =  $\sim 4.1 \times 10^5$  mol ethylene/mol Ni,  $M_n = 1.6 \times 10^4$  g/mol). We provide both experimental and computational data showing that secondary metals impact the relative stability of *cis* and *trans* isomers, which is a phenomenon not shown previously. Unlike in our earlier work, which was limited by poor nuclearity control and/or secondary metals that were too far from the catalyst center, the nickel phenoxyphosphine-PEG complex is an ideal platform for future studies of cation-controlled polymerization.

## Introduction

Our society's long-standing fascination with polyethylene stems in part from the low cost of ethylene and the broad range of materials properties attainable by tailoring its microstructure and composition.<sup>1</sup> The discovery in the 1990s that Ni and Pd diimine complexes are excellent catalysts for olefin polymerization<sup>2,3</sup> led to several decades of research to create new variants with expanded capabilities,<sup>4-12</sup> such as those that could produce ultra high molecular weight polymers<sup>13-15</sup> or incorporate high percentages of polar olefins.<sup>16-18</sup> Traditional polymer synthesis typically follows the "one catalyst one material" paradigm, in which a single catalyst produces a single type of polymer structure (Scheme 1, left). This strategy is limiting because it does not allow for user control of the polymerization process.<sup>19</sup> For example, conventional catalysts are incapable of generating block copolymers from a single monomer pool or forming gradient polymers without external control.<sup>20</sup> For practical applications, catalysts that could easily produce different polymer structures *on demand* would make customized polymer synthesis more accessible to non-chemists, who might lack the expertise to create derivatives of the coordination catalyst. Furthermore, although exhaustive work has been invested in developing large libraries of olefin polymerization catalysts, there are limits to what molecular structures could be reasonably synthesized even by skilled chemists. Thus, significant gaps in the polyolefins space still exist, which represents exciting areas for further research and development in polymerization catalysis.

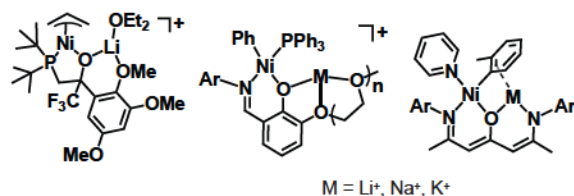
Toward the goal of realizing the "one catalyst many materials" concept,<sup>19</sup> researchers have pursued innovative approaches to control the polymerization process. One such

strategy relies on varying the reaction parameters and/or components. For example, Arriola and coworkers took advantage of chain transfer agents to shuttle polymer chains between distinct Hf and Zr catalysts to produce olefin block copolymers with unique elastomeric properties.<sup>21</sup> The amount of chain transfer agents used relative to ethylene was varied to obtain materials with different crystallinity and transparency. Coates and coworkers demonstrated that living Ni diimine catalysts could be subjected to alternating changes in temperature and pressure to synthesize tetrablock polymers directly from ethylene.<sup>22</sup> These tetrablock materials enhanced the toughness of low-density and high-density polyethylene blends at ratios in which they would otherwise be phase separated. Finally, Coates, Fors, and coworkers used metered catalyst addition to control the shape of polyethylene molecular weight distributions.<sup>23</sup> This study showed that molecular weight distribution shape affects a material's viscosity but not tensile strength.



**Scheme 1.** Comparison of conventional versus cation-tunable polymerization catalysts.

An alternative strategy that has emerged in recent years is the application of tunable catalysts in polymerization.<sup>24–30</sup> Tunable catalysts are complexes that could be toggled between different reactivity states in response to external stimuli.<sup>31</sup> For example, catalysts bearing ferrocene groups<sup>32–34</sup> or redox active ligands<sup>35</sup> were shown to exhibit different olefin polymerization rates and polymer branching density upon the addition of chemical reductants or oxidants. Redox switching is operationally simple and does not require changes in reaction conditions. Tunable catalysts that rely on light as photo-triggers are also being developed to prepare polyolefins<sup>36</sup> and related hybrid materials.<sup>37,38</sup>



**Chart 1.** Representative examples of nickel-alkali complexes studied in ethylene polymerization catalysis. The examples shown were reported by Brookhart/Johnson (left),<sup>39</sup> Do (middle),<sup>40,41</sup> and Tonks (right)<sup>42</sup> groups.

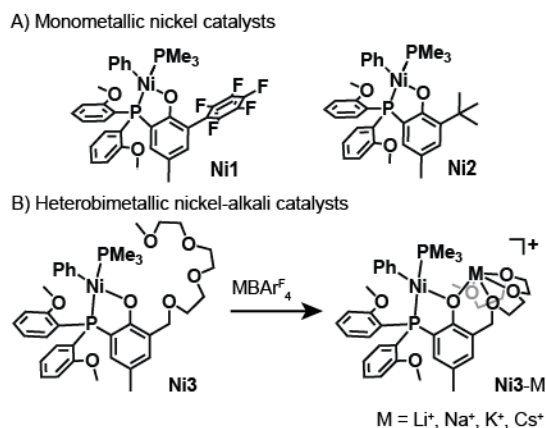
Our laboratory has been interested in a subset of tunable catalysts that take advantage of secondary metal binding.<sup>43</sup> Unlike redox- and light-tuning that typically toggles between 2–3 catalyst states, cation-tuning could potentially access a wider range because  $M^{n+}$  can differ in size, charge, Lewis acidity, redox activity, and other characteristics. In 2003, Johnson, Brookhart, and coworkers were the first to report that external cations were beneficial to olefin polymerization (Chart 1, left).<sup>39</sup> They found that addition of  $\text{Li}^+$  to nickel alkoxypyridine catalysts provided a significant boost in catalyst activity. Other investigators have also taken advantage of secondary metals in coordination catalyst designs. For example, Tonks and coworkers demonstrated that alkali ions could influence the tautomeric structure of nickel  $\beta$ -oxo- $\delta$ -diimine catalysts (Chart 1, right).<sup>42</sup> Jordan and coworkers showed that lithium<sup>44–47</sup> and zinc<sup>48</sup> ions could induce the spontaneous self-assembly of catalyst cages that exhibited unique polymerization behavior. These examples illustrate beautifully the diverse chemistry that could be leveraged by integrating secondary metals into polymerization systems.

Because of their highly tunable nature, cation-tunable catalysts are ideal platforms to test the feasibility of a user-customizable polymer synthesis approach, where different polymer structures could be obtained by pairing the catalyst with different secondary metals (Scheme 1, right).<sup>43</sup> Toward this goal, our research group has developed several catalyst prototypes supported by ligands featuring polyethylene glycol (PEG) side chains (Chart 1, middle). They include complexes based on phenoxypyridine,<sup>40,41</sup> phosphine phosphonate ester,<sup>49,50</sup> and phenoxypyridine.<sup>51</sup> The PEG groups are integral to our catalyst design because they provide well-defined secondary metal binding pockets for a variety of metal cations. It has also been used successfully as a ligand substituent by Chen and coworkers.<sup>52</sup> In our ethylene polymerization studies, we observed that combining secondary metals with either Ni or Pd catalyst often gave favorable polymerization results, such as rate acceleration or changes to the polymer architecture. Some of the most confounding questions that arose out of our inves-

tigations were: What were the roles of the secondary metals in polymerization? Are cation effects simply manifestations of steric and electronic effects? To investigate these fundamentally important questions, we have undertaken a systematic study to determine how binding of alkali ions to nickel phenoxypyridine-PEG complexes impacts their catalyst properties and polymerization tendencies. We quantified secondary metal cation effects using a variety of spectroscopic and analytical tools, and applied computational methods to explore possible catalyst structures. We discovered that our nickel-alkali complexes are among some of the most productive late transition metal coordination catalysts reported to date and the identity of the alkali ions strongly influences the polymerization outcome. Our results suggest that steric and electronic parameters are useful descriptors of metal cation effects but that other factors such as coordination interactions could have possible roles in catalysis. Importantly, we show that our Ni phenoxypyridine-PEG construct has overcome previous catalyst design issues, which allowed us to extract useful lessons for future developments in cation-controlled catalysis.

## Results and Discussion

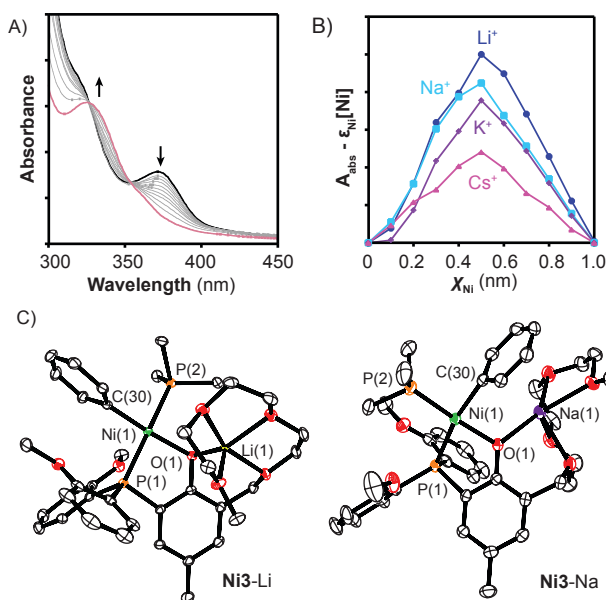
**Catalyst Selection and Secondary Metal Binding.** One of the major challenges in creating cation-tunable catalysts is coupling secondary metal binding with programmed changes in form and function. Although we showed that pendant metal binding sites could be installed in different olefin polymerization catalyst platforms, we had encountered various challenges. For example, we found that Ni phenoxypyridine-PEG complexes could dimerize in the presence of stoichiometric amounts of alkali ions,<sup>40</sup> Ni triazolecaboxamidate-pyridine complexes formed ill-defined species upon addition of zinc ions,<sup>53</sup> and Ni phosphine phosphonate-PEG complexes gave heterobimetallic structures that have non-interacting nickel and alkali centers.<sup>50</sup> In contrast, the Ni phenoxypyridine-PEG complexes (**Ni3**) gave well-behaved molecular species in the presence of sodium salts.<sup>51</sup> Because of these encouraging results, we focused our current investigations on **Ni3** and its nickel-alkali derivatives (**Ni3-M**, where  $M = \text{Li}^+, \text{Na}^+, \text{K}^+, \text{and } \text{Cs}^+$ ). As representative examples of conventional mononickel catalysts,<sup>54–56</sup> we also studied **Ni1**<sup>54</sup> and **Ni2**<sup>51</sup> bearing pentafluorophenyl and *tert*-butyl groups, respectively, at the *ortho* positions of their phenolate moieties (Scheme 2).



**Scheme 2.** Monometallic nickel (conventional) and heterobimetallic nickel-alkali complexes used in this study.

We had shown previously that conventional nickel phenoxyposphine complexes lacking *ortho* PEG groups do not bind secondary metals to an appreciable extent.<sup>51</sup> In contrast, **Ni3** produced discrete 1:1 nickel-sodium species in solution and the solid state. To investigate whether **Ni3** could form adducts with other alkali ions, we performed metal ion titrations using UV-visible absorption spectroscopy. We observed that addition of 1.0 equiv. of  $\text{MBAr}^{\text{F}_4}$  ( $\text{M} = \text{Li}^+, \text{Na}^+, \text{K}^+, \text{Cs}^+$ ;  $\text{BAr}^{\text{F}_4} = \text{tetrakis}(3,5\text{-bis}(\text{trifluoromethyl})\text{phenyl})\text{borate}$ ) to **Ni3** in  $\text{Et}_2\text{O}$  led to clear optical changes with the appearance of multiple isosbestic points, suggesting of **Ni3** and  $\text{M}^+$  binding (Figure S1). For example, when aliquots of  $\text{LiBAr}^{\text{F}_4}$  were combined with **Ni3**, the band at 372 nm decreased concomitant with an increase at 326 nm (Figure 1A). Interestingly, when  $\text{LiOTf}$  ( $\text{OTf}^- = \text{triflate anion}$ ) was used instead of  $\text{LiBAr}^{\text{F}_4}$ , the spectra of **Ni3** only showed minor changes (Figure S1E). Presumably, the more coordinating triflate can compete with **Ni3** for alkali ion binding whereas the less coordinating tetraarylborate cannot. As expected, the spectra of the nickel-alkali species all showed slightly different  $\lambda_{\text{max}}$  values, consistently with the different electronic effects of  $\text{M}^+$  on **Ni3**.

To ascertain the optimal nickel:alkali binding stoichiometry in solution, the method of continuous variation was employed. Although the polymerization studies below were conducted in toluene,  $\text{Et}_2\text{O}$  was used for these studies because polar solvents are needed to dissolve high concentrations of alkali salts. As shown in Figure 1B, the Job plots for **Ni3** +  $\text{M}^+$  all gave peak maxima at  $\chi_{\text{Ni}} = 0.5$ , which is indicative of 1:1 nickel to alkali ion binding. Their curvatures suggest that the affinities of **Ni3** for alkali metals are approximately in the order  $\text{Li}^+ > \text{Na}^+ \sim \text{K}^+ > \text{Cs}^+$ .<sup>57</sup> However, further binding studies are needed to confirm this order. These results are consistent with other studies showing that the PEG group has different association constants with different metal ions.<sup>40,58,59</sup>



**Figure 1.** A) UV-vis absorbance spectra of **Ni3** (black trace, 100  $\mu\text{M}$  in  $\text{Et}_2\text{O}$ ) after the addition of 1.0 equiv. of  $\text{LiBAr}^{\text{F}_4}$  (red trace); B) Job plots obtained from binding studies of **Ni3** +  $\text{MBAr}^{\text{F}_4}$ ; C) Molecular structures of **Ni3-Li** and **Ni3-Na** (ORTEP view, displacement ellipsoids drawn at 50% probability). Hydrogen atoms and  $\text{BAr}^{\text{F}_4}$  have been omitted for clarity.

**Characterization of Nickel-Alkali Complexes.** To gain insight into the structures of the heterobimetallic species, single crystals of the **Ni3-M** complexes were grown and analyzed by X-ray crystallography. Their nickel centers all showed square planar geometries, although **Ni3-Li** (Figure 1C), **Ni3-K** (Figure S37), and **Ni3-Cs** (Figure S38) displayed *cis* arrangements of their P(1) and C(30) donors (isomer A) whereas **Ni3-Na** displayed a *trans* arrangement (isomer B).<sup>51</sup> Isomer A is typically more thermodynamically favored because its strongest  $\sigma$ -donors, P(1) and C(30), prefer being *cis* to each other rather than *trans* to avoid sharing the same nickel *d*-orbital.<sup>60,61</sup> A distinct feature of the solid state structure of **Ni3-Na** is the close contact between  $\text{Na}^+$  and the nickel-coordinated phenyl ring ( $\text{Na}(1)\text{--C}(30) = 2.98 \text{ \AA}$ ,  $\text{Na}(1)\text{--C}(31) = 3.04 \text{ \AA}$ ),<sup>62</sup> which suggests that metal- $\pi$  interactions could provide enough stabilization energy to overcome the *trans* influence (vide infra). This type of alkali- $\pi$  interactions has been observed in the solid state by us<sup>40,51</sup> and others.<sup>42</sup>

The coordination spheres of the alkali metals in **Ni3-M** are slightly different due to variations in their ionic radii and coordination numbers. For example, the  $\text{Li}^+$  ion in **Ni3-Li** is ligated by the phenolate oxygen donor and four ether oxygen atoms from PEG (Figure 1C). Complex **Ni3-Na** also has an oxygen-rich environment around  $\text{Na}^+$ , except for an additional sodium- $\pi$  interaction as described above.<sup>51</sup> Interestingly, the alkali ions in **Ni3-K** (Figure S37) and **Ni3-Cs** (Figure S38) are surrounded by five oxygen donors as well tetrahydrofuran and benzene molecules, respectively. Although the presence of external adducts may be artifacts of the crystallization solvents used, the increasing coordination numbers observed going from  $\text{Li}^+ \rightarrow \text{Na}^+ \rightarrow \text{K}^+ \rightarrow \text{Cs}^+$  is consistent with the atomic size of the secondary ions.<sup>63</sup>

**Table 1.** Comparison of Atomic Distances<sup>a</sup>

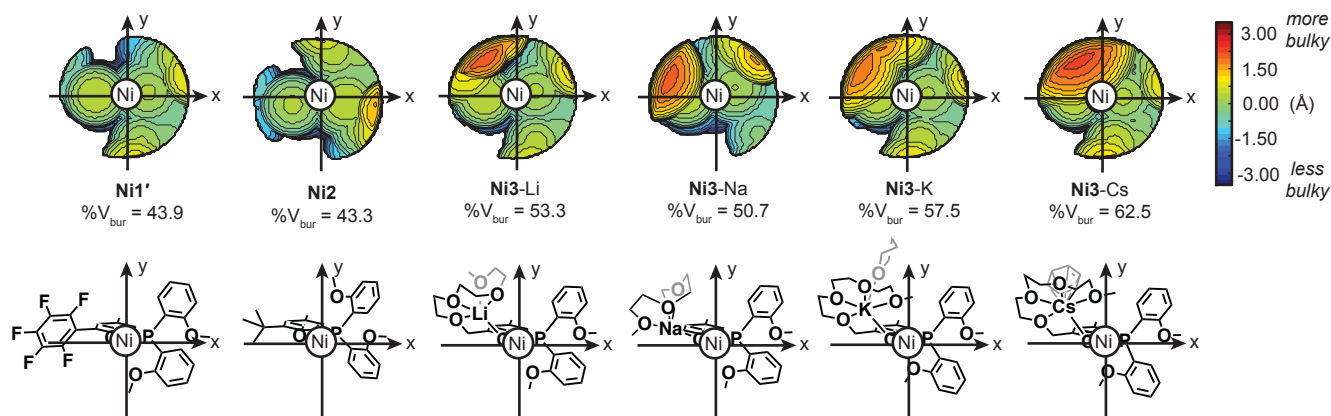
Isomer A	Isomer B					
	<b>Ni1</b> <sup>b,c</sup>	<b>Ni2</b> <sup>c</sup>	<b>Ni3-Li</b>	<b>Ni3-Na</b> <sup>c</sup>	<b>Ni3-K</b>	<b>Ni3-Cs</b>
Isomer	-	A	A	B	A	A
Ni(1)–P(1)	2.176	2.186	2.194	2.221	2.203	2.167
Ni(1)–O(1)	1.938	1.913	1.936	1.936	1.936	1.921
Ni(1)–C(30)	-	1.895	1.889	1.916	1.899	1.902
Ni(1)–P(2)	-	2.186	2.192	2.135	2.182	2.192
M(1)–O(1)	-	-	1.933	2.313	2.592	3.121
Ni(1)–M(1)	-	-	3.208	3.486	3.899	3.831

<sup>a</sup>All atomic distances are given in angstroms. <sup>b</sup>Complex **Ni1'** does not have phenyl and trimethylphosphine ligands coordinated to nickel. <sup>c</sup>X-ray structures previously reported.

Next, we compared the bond metrics of **Ni3-M** to those of their mononickel counterparts (Table 1). Although the X-ray structure of **Ni3** could not be obtained because the complex is not crystalline, the structures of **Ni1**<sup>54</sup> (Chart S1) and **Ni2**<sup>51</sup> were readily available. Complex **Ni1'** is supported by a phe-

noxyphosphine donor similar to that in **Ni1**, except that it is also chelated by cyclooctene instead of phenyl and trimethylphosphine donors.





**Figure 2.** Top: topographic steric maps of the nickel complexes calculated from their X-ray structures using SambVca 2.1. Only the phenoxyposphine ligands were considered in the calculation of % $V_{bur}$ . The nickel atom was set as the center of the coordination sphere, the nickel square plane defined the  $xz$ -plane, and the  $z$ -axis bisects the  $P(1)-Ni(1)-O(1)$  angle. The crystallographic data for **Ni1'**, **Ni2**, and **Ni3-Na** were obtained from published data. Bottom: chemical structures corresponding to the steric maps above shown in the same front view perspective.

Complex **Ni2** has the standard formula  $[Ni(Ph)(PMe_3)(L)]$  (where  $L$  = compound **4**, see Scheme S1) and was crystallized in the isomer **A** form. Comparison of the atomic distances in the nickel complexes showed only slight differences. For example, the  $Ni(1)-O(1)$  length in **Ni3-M** was about 1.92–1.94 Å whereas that in **Ni2** was 1.91 Å. Variations in the other bond lengths between **Ni3-M** and **Ni2** were typically less than 0.05 Å. As expected, the most pronounced differences are in the  $M(1)-O(1)$  separations, which ranged from 1.93 to 3.12 Å going from **Ni3-Li** to **Ni3-Cs** in accordance with the increasing ionic radii of  $M^+$ .<sup>63</sup> Surprisingly, the  $Ni(1)-K(1)$  distance is slightly longer than that of  $Ni(1)-Cs(1)$  (3.90 vs. 3.83 Å, respectively), which might be due to effects of their different solvent adducts (e.g., differences in electronic donation from THF vs. toluene).

Having crystallographic characterization of the complete **Ni3-M** series allowed us to compare the steric congestion in their active site pockets. Although a variety of descriptors have been used to define steric bulk, we prefer percentage of buried volume (% $V_{bur}$ ) because it could be applied to many catalyst structures and is simple to determine using the SambVca 2.1 program.<sup>64,65</sup> In addition, % $V_{bur}$  values have been reported for other olefin polymerization catalysts so direct comparisons could be made with those complexes.<sup>17,18,66</sup> In our calculations, % $V_{bur}$  only took into account the fraction of the first coordination sphere occupied by the phenoxyposphine-PEG ligand + alkali ion. As shown in the topographic steric maps in Figure 2, the nickel-alkali complexes displayed % $V_{bur}$  values in the order **Ni3-Na** (50.7) < **Ni3-Li** (53.3) < **Ni3-K** (57.5) < **Ni3-Cs** (62.5). Although the % $V_{bur}$  for **Ni3-Li** does not seem to follow the atomic size trend (ionic radii = 76 pm for  $Li^+$ , 102 pm for  $Na^+$ , 138 pm for  $K^+$ , and 167 pm  $Cs^+$ ),<sup>63</sup> we attributed this apparent discrepancy to shorter alkali-PEG bonds in **Ni3-Li** compared to those in **Ni3-Na**, which brought the pendant lithium-PEG unit closer to Ni and consequently, led to enhanced % $V_{bur}$ . Interestingly, when the **Ni3-M** structures were viewed from the side (looking down the  $x$ -axis, Figure S11), the alkali-PEG groups afforded varying amount of axial site coverage. Specifically, the  $Li^+$  and  $Cs^+$  cations appeared to provide greater steric protection than  $Na^+$  and  $K^+$ .

However, the southwest quadrants (when viewed down the  $z$ -axis, front view) of the **Ni3-M** complexes are open to the external environment, suggesting that this space could be protected better in future catalyst designs.

The % $V_{bur}$  for **Ni1'** and **Ni2** were determined to be 43.9 and 43.3, respectively (Figure 2). These values are similar to those reported for related palladium  $P,O$ -ligated polymerization catalysts (% $V_{bur}$  = 41.5–49.6<sup>17</sup> and 45.3–47.8<sup>67</sup>). Although much higher % $V_{bur}$  values could be achieved using symmetric diimine ligands with ultra bulky groups (e.g., up to 87.6% buried volume),<sup>66</sup> many asymmetric ligand platforms such as phosphine sulfonates could only be bulked up on the phosphine side.<sup>8</sup> Comparison of our % $V_{bur}$  data revealed the alkali-PEG units could enhance steric protection by up to ~19% in volume compared to that by common ligand substituents such as pentafluorophenyl (**Ni1'**) or *tert*-butyl (**Ni2**) groups. In addition, **Ni1'** and **Ni2** are devoid of steric protection at their axial positions (side view, Figure S10), which could prevent efficient polymerization and reduce thermal stability.<sup>4</sup> These results clearly indicate the **Ni3-M** structures are unique and cation binding as a way of fine-tuning steric bulk could be advantageous over conventional methods that rely on synthetic ligand modifications.

**Table 2.** Electrochemical Data for Nickel Complexes<sup>a</sup>

Complex	$E$ (vs. $Fc/Fc^+$ , mV)	$\Delta E$ (cf. <b>Ni3</b> , mV)
<b>Ni1</b>	26	+76
<b>Ni2</b>	-49	+1
<b>Ni3</b>	-50	0
<b>Ni3-Li</b>	56	+106
<b>Ni3-Na</b>	-14	+36
<b>Ni3-K</b>	-16	+34
<b>Ni3-Cs</b>	-24	+26

<sup>a</sup>The cyclic voltammograms of the nickel complexes were measured in THF with 0.09 M *n*Bu<sub>4</sub>NBPh<sub>4</sub> supporting electrolyte and 200 mV/s scan rate. The oxidation potentials were references to ferrocene/ferrocenium.

Next, we evaluated how secondary metal binding impacts the nickel electron density using cyclic voltammetry (Table 2, Figure S19). The heterobimetallic species were formed in situ by combining **Ni3** with 1 equiv. of  $\text{MBAr}^{\text{F}}_4$  in THF with  $n\text{Bu}_4\text{NBPh}_4$  as the supporting electrolyte. Both mononickel and nickel-alkali complexes showed irreversible anodic waves, which were tentatively ascribed to the one-electron oxidation of Ni(II) to Ni(III).<sup>68,69</sup> The oxidation peak for **Ni3** occurred at -50 mV (vs.  $\text{Fc}/\text{Fc}^+$ ) and was used as reference for comparison with the other complexes. Complex **Ni2** with a slightly electron-donating *tert*-butyl group had a similar oxidation potential as that of **Ni3** ( $E = -49$  mV), whereas **Ni1** with an electron-withdrawing pentafluorophenyl group oxidized at a more positive potential ( $E = +26$  mV). The presence of secondary alkali ions shifted the anodic peak in accordance to their relative Lewis acid strength,<sup>70</sup> giving  $E$  in the order **Ni3**-Li (+56 mV) > **Ni3**-Na (-14 mV) ~ **Ni3**-K (-16 mV) > **Ni3**-Cs (-24 mV). Interestingly, the  $\Delta E$  of **Ni3**-Li (vs. **Ni3**) is larger than that of **Ni1** (+106 mV vs. +76 mV, respectively), which suggests  $\text{Li}^+$  binding reduces the electron density of Ni to a greater extent than electronic induction by pentafluorophenyl substituents.

On the basis of their structural and electronic features, **Ni3**-M complexes are clearly distinct from conventional nickel phenoxyphosphine complexes (e.g., **Ni1** and **Ni2**). Because the alkali-PEG units in **Ni3**-M vary in shape and size, depending on the identity of  $\text{M}^+$  and possible solvent interactions, they have different space filling capacity within the nickel coordination sphere (Figure 2). At the same time, the alkali ions increase the effective charge of the nickel centers, which provides a convenient way to tune their electron density and electrophilicity. We will discuss in the last section that pendant metal cations are also capable of secondary coordination interactions, which could impact the relative stability of *cis* and *trans* isomers.

**Table 3.** Ethylene Polymerization by Nickel Catalysts at Various Temperatures<sup>a</sup>

Entry	Catalyst	Salt	Temp. (°C)	Polymer Yield (g)	Activity (kg/mol·h)	Branches <sup>b</sup> (/1000 C)	$M_n^c$ ( $\times 10^3$ )	$M_w/M_n^c$
1	<b>Ni1</b>	none	30	0.77	1500	9	3.06	2.1
2	<b>Ni2</b>	none	30	1.32	2600	15	5.20	1.9
3	<b>Ni3</b>	none	30	trace	0	—	—	—
4 <sup>d</sup>	<b>Ni3</b>	$\text{Li}^+$	30	3.53	35000	12	40.10	1.3
5	<b>Ni3</b>	$\text{Na}^+$	30	9.07	18000	27	1.72	1.4
6	<b>Ni3</b>	$\text{K}^+$	30	1.46	2900	25	4.53	1.6
7	<b>Ni3</b>	$\text{Cs}^+$	30	0.18	360	9	33.93	1.5
8 <sup>d</sup>	<b>Ni3</b>	$\text{Li}^+$	50	3.84	38000	7	12.10	1.3
9	<b>Ni3</b>	$\text{Na}^+$	50	6.52	13000	30	1.60	1.2
10	<b>Ni3</b>	$\text{K}^+$	50	2.73	5500	9	11.50	1.5
11	<b>Ni3</b>	$\text{Cs}^+$	50	0.72	1400	8	34.98	1.3
12 <sup>d</sup>	<b>Ni3</b>	$\text{Li}^+$	70	1.82	18000	10	6.20	1.3
13	<b>Ni3</b>	$\text{Na}^+$	70	4.61	9200	27	1.03	1.4
14 <sup>e</sup>	<b>Ni3</b>	$\text{K}^+$	70	2.89	12000	27	1.39	1.3
15 <sup>e</sup>	<b>Ni3</b>	$\text{Cs}^+$	70	9.12	36000	9	15.12	1.7
16	<b>Ni1</b>	none	90	10.3	21000	15	0.97	3.7
17	<b>Ni2</b>	none	90	12.8	26000	12	1.46	3.4
18 <sup>d</sup>	<b>Ni3</b>	$\text{Li}^+$	90	1.31	13000	17	2.09	2.2
19	<b>Ni3</b>	$\text{Na}^+$	90	2.41	4800	30	0.86	1.5
20 <sup>e</sup>	<b>Ni3</b>	$\text{K}^+$	90	2.49	10000	29	1.06	1.6
21 <sup>e</sup>	<b>Ni3</b>	$\text{Cs}^+$	90	5.73	23000	10	15.74	1.4

<sup>a</sup>Polymerization conditions: Ni catalyst (0.5  $\mu\text{mol}$ ),  $\text{MBAr}^{\text{F}}_4$  (1  $\mu\text{mol}$ , if any),  $\text{Ni}(\text{COD})_2$  (4  $\mu\text{mol}$ ), ethylene (450 psi), 100 mL toluene, 1h. Temperature was controlled by manual external cooling when necessary to ensure the reaction temperature does not exceed greater than 5 °C from the starting temperature. Reported yields are the average of 2-3 runs and standard deviations are less than 10%. <sup>b</sup>The total number of branches per 1000 carbons was determined by  $^1\text{H}$  NMR spectroscopy. <sup>c</sup>Determined by GPC in trichlorobenzene at 140 °C. <sup>d</sup>**Ni3** (0.1  $\mu\text{mol}$ ),  $\text{LiBAr}^{\text{F}}_4$  (0.2  $\mu\text{mol}$ ),  $\text{Ni}(\text{COD})_2$  (0.8  $\mu\text{mol}$ ). <sup>e</sup>Reaction was run for 30 min.

**Ethylene Polymerization.** We had demonstrated previously that **Ni3** in combination with  $\text{NaBAr}^{\text{F}}_4$  was a highly efficient catalyst for ethylene polymerization.<sup>51</sup> To expand our studies to include other alkali ions, we carried out polymerization reactions using both conventional and PEGylated nickel

complexes (Table 3). Our standard reactions were conducted in high-pressure reactors using 0.5  $\mu\text{mol}$  nickel complex in 100 mL of toluene under 450 psi of ethylene. The Ni complexes were activated by treatment with  $\text{Ni}(\text{COD})_2$  (COD = 1,5-cyclooctadiene) as a phosphine scavenger and the reac-

tions were allowed to proceed for 1 h. To establish a baseline for comparison, the mononickel complexes **Ni1** and **Ni2** were tested first. At 30 °C, **Ni1** (entry 1) and **Ni2** (entry 2) showed moderate activities of  $1.5 \times 10^3$  and  $2.6 \times 10^3$  kg/mol·h, respectively. Because **Ni1** and **Ni2** are similar in their steric bulk ( $\%V_{\text{bur}} = 43.9$  and  $43.3$ , respectively), the different rates observed were attributed to differences in their electronic properties ( $E = +26$  mV for **Ni1** vs.  $-49$  mV for **Ni2**). This result is contrary to commonly observed trends that electron-poor catalysts are typically faster than electron-rich ones,<sup>71-73</sup> but is consistent with this family of catalysts.<sup>74</sup> Electron-poor complexes could exhibit longer induction periods due to slower dissociation of the coordinated phosphine. In fact, we found that at 90 °C when presumably phosphine abstraction is more facile, the activity of **Ni1** ( $2.1 \times 10^4$  kg/mol·h, entry 16) was similar to that of **Ni2** ( $2.6 \times 10^4$  kg/mol·h, entry 17). The polyethylene (PE) products obtained from both **Ni1** and **Ni2** have low branching ( $\leq 15$  branches/1000 C) and low molecular weight ( $M_n = \sim 10^3$  g/mol), which are similar to those reported for nickel phenoxyposphine catalysts.<sup>56</sup>

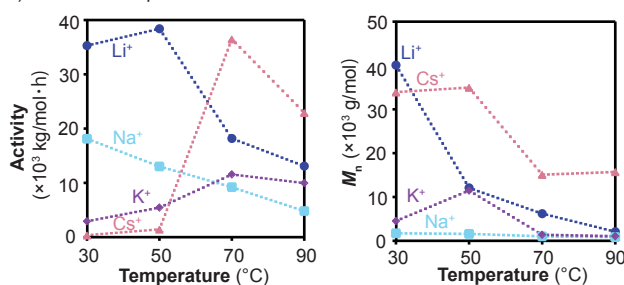
When **Ni3**/Ni(COD)<sub>2</sub> were combined under 450 psi of ethylene, negligible amounts of PE were obtained (Table 3, entry 3). In the absence of alkali ions, the free PEG chain in **Ni3** is believed to be capable of inhibiting the catalyst via nickel coordination. When  $M^+$  was added, the catalyst “switched on” dramatically and large quantities of PE were produced. At 30 °C (entries 4-7), the catalyst activities were observed in the order **Ni3**-Li > **Ni3**-Na > **Ni3**-K > **Ni3**-Cs, which tracks with the electron-withdrawing abilities of their  $M^+$  ions.<sup>75</sup> The fastest catalyst **Ni3**-Li ( $3.5 \times 10^4$  kg/mol·h, entry 4) showed 23× and 13× higher activity than that of the mononickel catalysts **Ni1** (entry 1) and **Ni2** (entry 2), respectively. In some reactions, mass transport issues were significant due to the formation of large amounts of insoluble PE.<sup>13</sup>

The PEs obtained from **Ni3**-M showed an inverse relationship between molecular weight and branching (i.e., polymers with higher  $M_n$  have fewer branches and vice versa). It is generally found that bulkier catalysts give polymers with higher molecular weight because they could prevent associative chain transfer pathways in favor of chain propagation.<sup>6</sup> Despite not having the largest  $\%V_{\text{bur}}$  in the series, **Ni3**-Li yielded PE with the highest molecular weight ( $4.0 \times 10^4$  g/mol, Table 3, entry 4). The bulkiest catalyst **Ni3**-Cs afforded PE with only a slightly lower  $M_n$  of  $3.4 \times 10^4$  g/mol (entry 7). To rationalize these results, it should be noted that electronic effects could also lead to enhanced polymer molecular weight if the rate of chain propagation increases more significantly than the rate of chain transfer. In fact, the chain growth rate of **Ni3**-Li was about 20× faster than that of **Ni3**-Cs (assuming they are proportional to their polymer yields of 3.53 and 0.18 g, respectively), but its chain transfer rate was about 16× slower.<sup>76</sup> We cannot compare these rates to those of their parent complex **Ni3** because it is catalytically inactive. In a separate Lewis acid study, Jordan and coworkers found that addition of boranes to Pd catalysts increased chain growth rates by only about 3× but increased chain transfer rates by up to 80×.<sup>77</sup> These changes were attributed to electronic perturbations that placed more partial positive charge at the palladium center. In contrast, because both structural and electronic changes occur in our catalysts as a result of secondary metal binding, both contributions must be considered *together* to fully explain the cation effect.

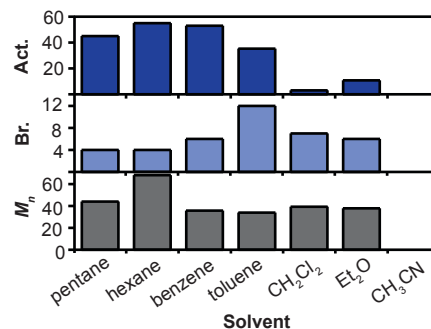
The **Ni3**-M catalysts produced PEs with branches ranging from 9–27/1000 C, indicating the alkali ions also affected chain-walking processes (i.e.,  $\beta$ -hydride elimination/reinsertion) to different degrees. Although nickel catalysts typically furnish polymers with fewer branches than their palladium analogues, which could have as many as 100+ branches/1000 C,<sup>6</sup> our results clearly showed that cation-tuning is a viable strategy to prepare PE with customized morphologies (Scheme 1).

Next, we investigated how various reaction parameters affected polymerization. We observed that the **Ni3**-M catalysts had different optimal temperatures. Using a standard catalyst loading of 0.5  $\mu\text{mol}$ , we found **Ni3**-Li was most active at 50 °C, **Ni3**-Na was most active at 30 °C, and both **Ni3**-K and **Ni3**-Cs were most active at 70 °C (Figure 3A, Table 3). Their PE molecular weights generally decreased, whereas their branching densities were only minimally affected by increasing temperatures (Figure S6).

A) Effects of Temperature on **Ni3**-M



B) Effects of Solvent on **Ni3**-Li



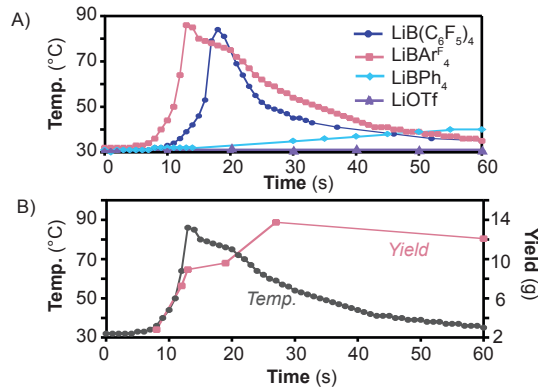
**Figure 3.** Plots showing A) the effects of temperature on **Ni3**-M ( $M = \text{Li}^+, \text{Na}^+, \text{K}^+$  or  $\text{Cs}^+$ , see Table 3 for details) and B) the effects of solvent on **Ni3**-Li (30 °C, see Table S7 for details). Abbreviations used: Act. = Activity ( $\times 10^3$  kg/mol·h), Br. = Branches (/1000 C),  $M_n$  = average number molecular weight ( $\times 10^3$  g/mol).

Surprisingly, **Ni3**-Cs showed impressive catalytic performance even at 90 °C (activity =  $2.3 \times 10^4$  kg/mol·h and turnover number or TON =  $4.1 \times 10^5$  mol ethylene/mol Ni), exceeding that of other thermally stable nickel catalysts reported in the literature (Table S12). For example, the nickel diimine cyclophane catalyst **Ni13** gave lower activity ( $1.8 \times 10^4$  kg/mol·h) and TON ( $1.6 \times 10^5$  mol ethylene/mol Ni) at 90 °C.<sup>78</sup> However, catalyst **Ni13** furnished PE with an order of magnitude higher molecular weight ( $M_n = 2.9 \times 10^5$  g/mol) than that of **Ni3**-Cs ( $M_n = 1.6 \times 10^4$  g/mol). However, in preliminary work we found that our nickel phenoxyposphine-PEG catalysts could be derivatized with bulkier groups to produce PE with  $M_n$  of  $\sim 10^6$  g/mol so polymer molecular weight is not a

limiting feature of our catalyst. Although **Ni1** and **Ni2** also exhibited high activity at 90 °C ( $\sim 10^4$  kg/mol·h), their  $M_w/M_n$  increased to  $\geq 3.4$  (Table 3, entries 16 and 17), suggesting that these complexes were no longer single site catalysts or were decomposing at high temperatures.

The effects of solvent on polymerization were also investigated. In general, **Ni3**-M was more active in non-polar than in polar solvents (Table S5). For example, **Ni3**-Li displayed the highest activity in hexane ( $5.5 \times 10^4$  kg/mol·h) and benzene ( $5.30 \times 10^4$  kg/mol·h) but was completely inhibited in acetonitrile (Figure 3B), probably because the latter could compete with ethylene for catalyst binding. Interestingly, hexane gave PE with the highest molecular weight ( $6.81 \times 10^4$  g/mol) and toluene gave PE with the highest number of branches (12/1000 C) using **Ni3**-Li. As observed in the solid-state structures of **Ni3**-K (Figure S37) and **Ni3**-Cs (Figure S38), the alkali-PEG units are capable of forming solvent adducts, which means the structures of **Ni3**-M might be different in different solvents. The advantage of performing polymerizations in polar solvents, such as ether, is that higher charged cations (e.g.,  $M^{2+}$  or  $M^{3+}$ ) could potentially be used as secondary metals.<sup>50</sup>

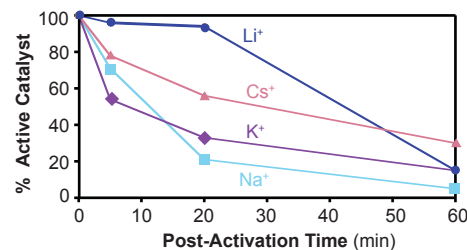
Because **Ni3**-Li showed the highest activity in our studies, we sought to optimize its reaction conditions even further (Table S6). We found that at 40 °C using a reduced catalyst loading of 0.1  $\mu$ mol in 200 mL of toluene for 1 h, **Ni3**-Li gave an activity of  $7.0 \times 10^4$  kg/mol·h (entry 3). Its TON of  $2.5 \times 10^6$  mol ethylene/mol Ni greatly surpassed that of other highly active nickel ethylene polymerization catalysts reported in the literature (Table S11). For example, the nickel diimine catalyst **Ni4**<sup>79</sup> and nickel tris(adamantyl)phosphine **Ni12**<sup>14</sup> gave TONs of  $\sim 4.0 \times 10^5$  and  $2.2 \times 10^5$  mol ethylene/mol Ni, respectively.



**Figure 4.** A) Reaction temperatures changes in ethylene polymerization catalyzed by **Ni3**-Li generated from **Ni3** and various lithium salts in toluene. See Table S9 for details. B) Temperature vs. yield plot of ethylene polymerization catalyzed by **Ni3**/LiBARF<sub>4</sub>. See Table S10 for details.

The counteranion also seemed to have significant effects on the performance of **Ni3**-Li. In terms of catalyst activity, the order observed was  $\text{BARF}_4^- > \text{B(C}_6\text{F}_5)_4^- > \text{BPh}_4^- \gg \text{OTf}^-$  (Table S9). This trend correlated well with their metal coordinating abilities, since tetraarylborates are considered spectator ions<sup>80</sup> whereas triflate is not.<sup>81</sup> Monitoring the temperature profiles of **Ni3** and various lithium salts during polymerization allowed us to differentiate the subtle effects of the anions (Figure 4A). For example, **Ni3**+LiBARF<sub>4</sub> showed a preactivation period of  $\sim 5$  min before a large exotherm occurred, which

maximized at  $\sim 13$  min (86 °C). A time-dependent plot of temperature vs. PE yield for **Ni3**+LiBARF<sub>4</sub> suggested the catalyst deactivated after  $\sim 30$  min since no additional polymer was produced (Figure 4B). The temperature profile of **Ni3**+LiB(C<sub>6</sub>F<sub>5</sub>)<sub>4</sub> was similar to that of **Ni3**+LiBARF<sub>4</sub>, except the preactivation period lasted  $\sim 10$  min before the temperature increased exponentially. Interestingly, **Ni3**+LiBPh<sub>4</sub> showed a slow linear increase in temperature up to 40 °C during the 60 min run. As expected, because **Ni3**+LiOTf was not active in polymerization, this reaction showed no changes in temperature. Although the reasons for the different effects of anions have not been studied in detail, we hypothesize that solubility and metal coordinating ability might be major contributing factors.



**Figure 5.** Comparison of **Ni3**-M complexes in ethylene polymerization after various post-activation times. The % active catalyst = [(yield of polymer after x min post-activation)/(yield of polymer after 0 min post-activation)] $\times 100\%$ . See Table S13 for details.

**Relative Catalyst Stability.** To study the relative stability of the nickel-alkali catalysts, a reactivity-based method was used.<sup>14</sup> The **Ni3**-M complexes were dissolved in 100 mL of toluene/Et<sub>2</sub>O (4:1) and then combined with 3 equiv. of B(C<sub>6</sub>F<sub>5</sub>)<sub>3</sub><sup>82</sup> under  $\sim 5$  psi of ethylene. The reaction mixtures were allowed to stir for various post-activation times and then the ethylene pressure was increased to 450 psi for 1 h (Table S13). The % active catalyst was determined based on the quantity of PE obtained after 5, 20, or 60 min post-activation relative to that of the control with no waiting period. It is important to note these experiments provide only an estimate of the *relative* amounts of active species present rather than the *actual* amounts, which would require more rigorous techniques such as active site labeling.<sup>83,84</sup> A summary of the data is shown in Figure 5. As expected, the amount of PE obtained decreased as the post-activation time increased. After 5 min,  $\sim 96$ , 71, 54, and 78% of active catalysts were observed for **Ni3**-Li, **Ni3**-Na, **Ni3**-K, and **Ni3**-Cs, respectively. The apparent high percentage of **Ni3**-Li calculated ( $\geq 94\%$  up to 20 min) was not likely due to its greater stability, but rather, to the fact that it is slower to activate than the other **Ni3**-M species (in other words, fresh active species were generated as others decayed). After 60 min, the % active catalyst was observed in the order **Ni3**-Cs > **Ni3**-K  $\sim$  **Ni3**-Li > **Ni2**-Na. This experiment most likely overestimates the stability of **Ni3**-Li due to its slower phosphine abstraction rate (vide infra).

Because phosphine abstraction is the first step in catalyst activation, we measured how quickly PMe<sub>3</sub> was removed from the nickel center using <sup>31</sup>P NMR spectroscopy. In our reactions, **Ni3** was premixed with MBarF<sub>4</sub>, and then combined with 3 equiv. of B(C<sub>6</sub>F<sub>5</sub>)<sub>3</sub> (Figures S12-S18). The time required for complete consumption of the starting nickel complex was considered the “phosphine abstraction time” (Table 4). We found that at 30 °C, the initial **Ni3**, **Ni3**-Na, **Ni3**-K, and



**Ni3**-Cs species disappeared in less than 5 min. Surprisingly, phosphine abstraction from **Ni3**-Li took > 2 h at 30 °C (entry 2) and < 30 min at 50 °C (entry 4). It should be noted that under actual polymerization conditions, this activation step is expected to be much faster because higher ethylene pressure (450 instead of 5 psi) and vigorous stirring are used. When **Ni3** was mixed with B(C<sub>6</sub>F<sub>5</sub>)<sub>3</sub> first and then treated with LiBAR<sup>F</sup><sub>4</sub>, no starting nickel was left after 5 min (entry 3). Because the nickel center in **Ni3**-Li is the most electron-deficient, its Ni-PMe<sub>3</sub> bond is stronger than those in other **Ni3**-M species. Thus, removal of phosphine from **Ni3**-Li is expected to be correspondingly slower.<sup>71</sup>

**Table 4.** Summary of Phosphine Abstraction Study<sup>a</sup>

$\text{Ni3} + \text{MBAr}^{\text{F}}_4 \xrightarrow{+\text{B}(\text{C}_6\text{F}_5)_3} \text{Changes observed by } ^{31}\text{P NMR spectroscopy?}$ (1 equiv.) (5 equiv.) (3 equiv.)			
Entry	Complex	Temp. (°C)	Activation Time <sup>b</sup>
1	<b>Ni3</b>	30	< 5 min
2	<b>Ni3</b> -Li	30	> 2h
3	<b>Ni3</b> + (LiBAR <sup>F</sup> <sub>4</sub> ) <sup>c</sup>	30	< 5 min
4	<b>Ni3</b> -Li	50	< 30 min
5	<b>Ni3</b> -Na	30	< 5 min
6	<b>Ni3</b> -K	30	< 5 min
7	<b>Ni3</b> -Cs	30	< 5 min

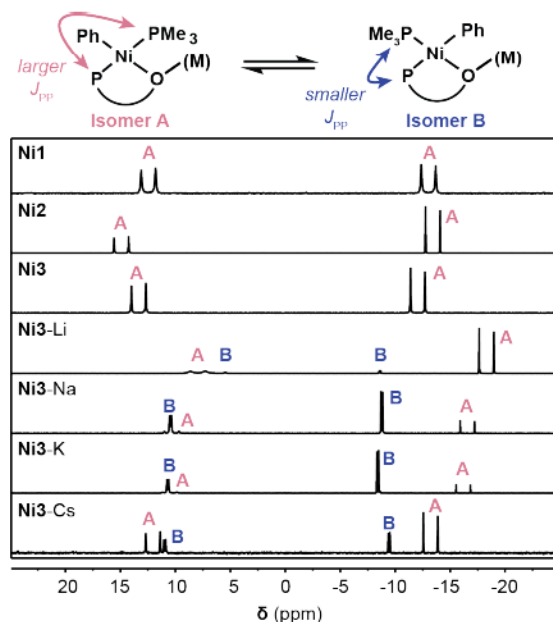
<sup>a</sup>Activation study: Complex **Ni3** (7 μmol) and MBAr<sup>F</sup><sub>4</sub> (35 μmol, if any) were dissolved in 0.5 mL of toluene-*d*<sub>8</sub>/diethyl ether (4:1) and characterized by <sup>31</sup>P NMR spectroscopy. The B(C<sub>6</sub>F<sub>5</sub>)<sub>3</sub> activator (21 μmol) was added and the NMR tube was shaken to mix. <sup>b</sup>The activation time was estimated based on the amount of time it took for the starting complex to convert completely to a new species upon the addition of borane. <sup>c</sup>In this experiment, **Ni3** and B(C<sub>6</sub>F<sub>5</sub>)<sub>3</sub> were combined first to activate the complex before the addition of LiBAR<sup>F</sup><sub>4</sub>.

Our variable temperature polymerization studies (Figure 3A) and post-activation studies (Figure 5) both support the catalyst stability ranking **Ni3**-Cs > **Ni3**-K > **Ni3**-Li > **Ni2**-Na. Interestingly, this trend correlates well with their %V<sub>bur</sub> values (Figure 2), which is reasonable given that greater steric protection should protect the catalysts from undesired decomposition modes. Nickel coordination catalysts are known to degrade through a variety of ways, such as formation of inactive nickel bis(ligand) species or protonolysis of the supporting ligands.<sup>83,86</sup> Since **Ni3**-Cs is the most chemically robust, it is the fastest catalyst at high temperatures (70–90 °C, Table 3). On the other hand, since **Ni3**-Li has the highest intrinsic reactivity, it is the fastest catalyst under conditions in which thermal decay is minimal (e.g., at 30–50 °C). We hypothesize that the short induction period observed during polymerization using **Ni3**-Li (Figure 4) is in part due to slow phosphine abstraction (Table 4).

#### Cis/Trans Isomerization and Mechanistic Implications.

Because the solid-state structures showed that both isomers **A** (e.g., **Ni2**, **Ni3**-Li, **Ni3**-K, **Ni3**-Cs) and **B** (e.g., **Ni3**-Na) were isolable, we next investigated their relative distributions in solution. When the <sup>31</sup>P NMR spectra of the nickel complexes were recorded in a mixture of toluene-*d*<sub>8</sub>/diethyl ether (4:1) at RT, signals corresponding to the phosphine donors were clear-

ly detected (Figure 6). Because *trans* phosphines (isomer **A**) have larger *J*<sub>PP</sub> coupling constants than *cis* phosphines (isomer **B**), isomers **A** and **B** were easily differentiated.<sup>87</sup> The data showed the mononickel complexes all adopted the **A** form in solution. Because **Ni1** is more electron-deficient than **Ni2**, it seems that the electronic nature of nickel *does not* impact its *cis* and *trans* isomer preference (i.e., the *trans* influence is the dominating effect). In fact, there are numerous literature examples of asymmetric square planar nickel complexes that favor having phosphine *trans* to another phosphine rather than to a stronger donor such as alkyl or aryl.<sup>88–91</sup>

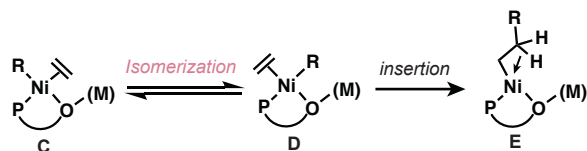


**Figure 6.** <sup>31</sup>P NMR spectra (toluene-*d*<sub>8</sub>/diethyl ether (4:1), 243 MHz) of various nickel complexes showing the equilibrium distribution of isomers **A** and **B** in solution at RT.

Interestingly, **Ni3**-M gave both isomers in various ratios in toluene-*d*<sub>8</sub>/diethyl ether (4:1) (Figure 6). Based on their NMR peak integrations, the equilibrium constants (*K*<sub>eq</sub> = [B]/[A]) were calculated to be 0.1, 9.0, 7.3, and 0.5 for **Ni3**-Li, **Ni3**-Na, **Ni3**-K, and **Ni3**-Cs, respectively. The relatively large amounts of isomer **B** observed in these samples suggest additional forces must be responsible for their greater stability. Based on their *K*<sub>eq</sub> values, the free energy change associated with converting isomer **A** to **B** (Δ*G*<sub>obs</sub>) was determined to be 1.4, -1.3, -1.2, and 0.4 kcal/mol for **Ni3**-Li, **Ni3**-Na, **Ni3**-K, and **Ni3**-Cs, respectively. Clearly the different alkali ions affect the equilibrium distribution of **A** and **B** differently.

To identify the factors underlying the thermodynamic preference for isomer **A** vs. **B**, we performed density functional theory (DFT) calculations on the nickel complexes. Qualitatively, the calculated results were consistent with our experimental data. We found that Δ*G*<sub>calc</sub> for isomerization of **A** to **B** was 9.3, 6.6, and 6.2 kcal/mol for the mononickel complexes **Ni1**, **Ni2**, and **Ni3**, respectively (Table S15), which indicates the equilibrium is strongly in favor of isomer **A**. In contrast, the Δ*G*<sub>calc</sub> was 2.0, -2.8, -1.1, and 3.3 kcal/mol for **Ni3**-Li, **Ni3**-Na, **Ni3**-K, and **Ni3**-Cs, respectively. These free energy terms indicate a slight preference of **A** over **B** for **Ni3**-Li and **Ni**-Cs, whereas there is a slight preference of **B** over **A** for

**Ni3**-Na and **Ni**-K, which was shown by  $^{31}\text{P}$  NMR spectroscopic measurements (Figure 6). Although we have confidence in the calculated trends, the accuracy of the  $\Delta G_{\text{calc}}$  values is somewhat limited because we did not include solvent coordination and solvation models in the calculations, which may be different for each complex and would require further experimental studies to guide computational models. The most intriguing result from our DFT studies was that the structures of isomer **B** for **Ni3**-M all showed metal- $\pi$  interactions between the nickel-coordinated phenyl ring and the neighboring alkali ion (Figure S39). For example, the M(1)–C(30) distances were computed to be 3.27 and 3.22 Å in the optimized **B** structures for **Ni3**-Na and **Ni3**-K, respectively (sum of Van der Waals radii: Na–C = 4.1 Å and K–C = 4.5 Å<sup>92</sup>). These distances were shorter than those in **Ni3**-Li and **Ni3**-Cs, which suggests that Na<sup>+</sup> and K<sup>+</sup> ions have greater  $\pi$  orbital overlap with the phenyl group than Li<sup>+</sup> and Cs<sup>+</sup>. It appears that if the stabilization provided by alkali- $\pi$  interactions exceeds the energy penalty for having unfavorable square planar nickel arrangements, then isomer **B** is thermodynamically accessible.



**Scheme 3.** Proposed pathway for chain propagation involving a key isomerization step from **C** to **D**.

Although the propagating nickel species during polymerization will not have a coordinated phenyl group to participate in alkali- $\pi$  interactions, the results above led us to wonder whether alkali ions could be involved in *cis/trans* isomerization in other ways. In particular, might such behavior account for their polymerization rate enhancing effects? A prevailing mechanistic hypothesis in the literature is that nickel and palladium complexes with asymmetric supporting ligands undergo polymerization mechanisms that alternate between two different geometric isomers.<sup>93,94</sup> For example, it is believed that ethylene coordination to a nickel( $\beta$ -agostic alkyl) complex leads to formation of isomer **C** because it avoids positioning the better phosphine and alkyl donors *trans* to each other (Scheme 3).<sup>95-97</sup> Given that our polymerization data clearly showed significant rate enhancements due to addition of M<sup>+</sup> to **Ni3**, we speculate alkali ions must play integral roles in the reaction beyond just electronic tuning. Although further studies are needed to differentiate between possible isomerization mechanisms,<sup>98-101</sup> such complex undertakings are beyond the scope of this paper. In fact, the tentative nickel(alkyl)(ethylene) species (**C** or **D**) of any catalyst system has not been observed experimentally, presumably due to their extraordinarily reactive nature. Reported studies of such intermediates have been done either computationally<sup>94</sup> or using less reactive palladium analogs.<sup>13</sup> It is entirely possible that *cis/trans* isomerization is not responsible for the rate enhancing effects of M<sup>+</sup> but this hypothesis is worthy of further scrutiny. An alternative explanation is that the **Ni3**-M complexes are formally cationic species so their greater charge compared to that of **Ni3** might lead to improved ethylene binding and insertion efficiency.

## Conclusion

We have developed a cation-tunable nickel catalyst capable of furnishing polyethylene with distinct morphologies. In previous work, we had encountered design difficulties such as undesirable catalyst bridging,<sup>40</sup> uncontrollable nuclearity,<sup>53</sup> and far nickel-alkali distances.<sup>50</sup> However, we have overcome these synthetic challenges using a nickel phenoxyposphine-PEG catalyst platform. For the first time, we were able to obtain crystallographic characterization of the complete nickel-alkali series (M = Li<sup>+</sup>, Na<sup>+</sup>, K<sup>+</sup>, and Cs<sup>+</sup>), which allowed us to quantify their steric bulk by calculating the percentage buried volumes. The topographic steric maps of **Ni3**-M revealed the complexes not only have greater %V<sub>bur</sub> than that of the conventional catalysts **Ni1** and **Ni2** but their alkali-PEG units also protect the nickel axial sites better than pentafluorophenyl or *tert*-butyl groups. Our cyclic voltammetry measurements suggested the alkali ions also decreased the electron density of the nickel complexes, with Li<sup>+</sup> having greater electron-withdrawing capability than even pentafluorophenyl. The impact of alkali ions on polymerization was remarkable as evident by the catalysts' record-breaking performance (quantified by activity and turnover number) and unusual thermal stability. At moderate temperatures (30–50 °C), the activity of **Ni3**-M correlated with the Lewis acidity of M<sup>+</sup> but polymer branching and molecular weight were most likely controlled by both steric and electronic factors. At high temperatures (70–90 °C), the **Ni3**-M complexes with greater steric protection were more active, presumably due to their reduced susceptibility toward decomposition. To explain the rate enhancing effects of alkali ions, we prefer mechanistic models in which M<sup>+</sup> participates directly in polymerization. For example, one possibility is that alkali ions promote isomerization of nickel(alkyl)(ethylene) intermediates from the more to less stable isomer by coordinating to the dissociated phenolate in a three-coordinate transition state. However, this hypothesis still needs to be tested.

Our work on cation-tunable complexes suggests that such systems are much too complicated to fully describe using any single molecular descriptor (e.g., steric or electronic). In fact, some of our observations defy established trends. For example, the addition of borane Lewis acids to conventional catalysts led to significant *decrease* in polymer molecular weight whereas addition of alkali Lewis acids to our tunable catalysts often led to significant *increase* (while also enhancing catalyst activity). Furthermore, secondary metals have other functional properties such as ligand or monomer coordinating ability that could play important roles in catalysis. Despite the complicated nature of secondary metals, we propose that advanced statistical techniques could be used to develop predictive models for guiding cation selection in future polymerization studies.<sup>102</sup>

We anticipate that our cation tuning strategy will allow us to achieve more sophisticated polymer synthesis capabilities. For example, we envision it might be feasible to prepare multi-modal polymers by using two different secondary metals simultaneously or obtain block polymers from a single monomer feed by adding or removing secondary metals in living polymerization reactions. These possibilities suggest that cation-regulated polymerization could be highly versatile and potentially offer improved efficiency and control over existing methods.

## Experimental

**General Procedures.** Commercial reagents were used as received. All air- and water-sensitive manipulations were performed using standard Schlenk techniques or under a nitrogen atmosphere using a drybox. Anhydrous solvents were obtained from an Innovative Technology solvent drying system saturated with argon. High-purity polymer grade ethylene was obtained from Matheson TriGas without further purification. Complexes **Ni2**, **Ni3**, and  $\text{NiPhBr(PMe}_3)_2$  were prepared according to our previous report.<sup>51</sup> The  $\text{LiBar}^{\text{F}}_4$ ,  $\text{NaBar}^{\text{F}}_4$ ,  $\text{KBar}^{\text{F}}_4$  and  $\text{CsBar}^{\text{F}}_4$  salts were prepared according to literature procedures.<sup>103,104</sup>

NMR spectra were acquired using JEOL spectrometers (ECA-400, -500, and -600) and referenced using residual solvent peaks. All  $^{13}\text{C}$  NMR spectra were proton decoupled.  $^{31}\text{P}$  NMR spectra were referenced to phosphoric acid.  $^1\text{H}$  NMR spectroscopic characterization of polymers: each NMR sample contained ~20 mg of polymer in 0.5 mL of 1,1,2,2-tetrachloroethane- $d_2$  (TCE- $d_2$ ) and was recorded on a 500 MHz spectrometer using standard acquisition parameters at 120 °C.

Gel permeation chromatography (GPC) data were obtained using a Malvern high temperature GPC instrument equipped with refractive index, viscometer, and light scattering detectors at 150 °C with 1,2,4-trichlorobenzene (stabilized with 125 ppm BHT) as the mobile phase. A calibration curve was established using polystyrene standards in triple detection mode. All molecular weights reported are based on the triple detection method.

**General Procedure for Ethylene Polymerization.** Inside the drybox, the nickel complex (0.5  $\mu\text{mol}$ ) and  $\text{MBar}^{\text{F}}_4$  (1  $\mu\text{mol}$ , if any) were dissolved in 10 mL of toluene in a 20 mL vial and stirred for 10 min. Solid  $\text{Ni(COD)}_2$  (4  $\mu\text{mol}$ ) was added and stirred until a clear solution was obtained (4–5 min). The mixture was loaded into a 10 mL syringe equipped with an 8-inch stainless steel needle. The loaded syringe was sealed by sticking the needle tip into a rubber septum and brought outside of the drybox. To prepare the polymerization reactor, 90 mL of dry toluene was placed in an empty autoclave. The autoclave was pressurized with ethylene to 80 psi, stirred for 5 min, and then the reactor pressure was reduced to 5 psi. This process was repeated 3 times to remove trace amounts of oxygen inside the reaction vessel. The reactor was then heated to the desired temperature and the catalyst solution was injected into the autoclave through a side arm. The autoclave was sealed and purged with ethylene at 40 psi (no stirring) three times. Finally, the reactor pressure was increased to the desired pressure, and the contents were stirred vigorously. To stop the polymerization, the autoclave was vented and cooled in an ice bath. A solution of MeOH (700 mL) was added to precipitate the polymer. The polymer was collected by vacuum filtration, rinsed with MeOH, and dried under vacuum at 80 °C overnight. The reported yields are average values obtained from duplicate or triplicate runs. The standard deviations are typically within 7% but no more than 10%.

**Computational Methods.** All geometries were optimized at B3LYP-D3 using the 6-31G(d) basis set for the H, Li, C, O, F, Na, P and K atoms, and the Lanl2DZ basis set with effective core potential for Ni and Cs, employing the Gaussian16 program. This choice of method and basis set combination has

been applied in computational studies of ethylene polymerization as well as other mechanistic studies involving Ni atoms.<sup>94,105</sup> Vibrational frequency analyses verified the nature of the minima and transition state structures. Gas-phase Gibbs free energies were computed at 298.15 K and verified the *cis/trans* conformational preferences of the nickel complexes. Three dimensional structures were produced with the CYL-View 1.0.1 software.<sup>106</sup>

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### Notes

The authors declare no competing financial interest.

## ASSOCIATED CONTENT

### Supporting Information.

Experimental procedures, spectroscopic data, metal binding studies, polymerization data, and DFT calculations. This material is available free of charge via the Internet at <http://pubs.acs.org>.

## ACKNOWLEDGMENT

We are extremely grateful to the Welch Foundation (E-1894 to L.H.D.), the National Science Foundation (CHE-1750411 to L.H.D. and CHE-1751370 to J.I.W.), and the National Institute of General Medical Sciences of the National Institutes of Health (R35GM133548 to J.I.W.) for grant support. We acknowledge the use of the Sabine cluster and support from the Research Computing Data Core at the University of Houston. We thank Prof. Tom Teets for allowing us to use a potentiostat for electrochemical measurements.

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