



# Synthesis of high molecular weight poly(*n*-butyl acrylate) macromolecules via *se*ATRP: From polymer stars to molecular bottlebrushes

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## ABSTRACT

Poly(*n*-butyl acrylate) (PBA) branched polymers have interesting properties and potential applications as super soft materials and pressure sensitive adhesives. Herein, star and comb polymers with long PBA sidechains were synthesized by a simplified electrochemically-mediated ATRP (*se*ATRP) utilizing ca. 100 ppm of Cu catalyst. Grafting-from (or core-first) synthesis of PBA stars using a multifunctional sucrose initiator (Sucrose-Br<sub>8</sub>) was best controlled using moderately negative applied potentials. This method was also applied to the synthesis of molecular bottlebrushes with long sidechains to a relatively high conversion. The prepared molecular bottlebrushes had low dispersity, with length distributions of 1.01 for the shorter bottlebrushes (backbone DP = 316) and 1.03 for the longer brushes (backbone DP = 1,632), as determined by atomic force microscopy (AFM) imaging.

## 1. Introduction

Compared to linear polymers of the same molecular weight, graft/comb polymers have less chain entanglement, lower viscosity, and a higher local concentration of polymer chain ends [1,2]. These properties enable graft polymers to be used as drug delivery vehicles, lubricants, molecular nanotemplates, supersoft materials, and stimuli-responsive materials [3–8]. Comb/graft polymer architectures can be synthesized by the “grafting-through” (polymerization of macromonomers) [9,10], “grafting-onto” (coupling sidechains onto a backbone) [11,12], or “grafting-from” (polymerization from a multifunctional macroinitiator) methods [12,13]. The grafting-onto and grafting-through methods can leave behind residual linear impurities which can be difficult to separate from a chemically similar graft polymer. The “grafting-from” method alleviates this issue by polymerizing “small” monomers from an already prepared multifunctional macroinitiator.

Controlled radical polymerization (CRP) techniques, such as reversible addition-fragmentation chain transfer polymerization (RAFT) [14,15], nitroxide mediated polymerization (NMP) [16–18], and atom transfer radical polymerization (ATRP) [19,20], have significantly simplified the synthesis of complex grafted architectures by the

grafting-from method. A well-controlled CRP will suppress most radical termination (RT) by reducing radicals' concentration *via* equilibration with dormant polymer species. Excessive bimolecular radical termination by coupling will lead to the formation of higher molecular weight products, and eventually crosslinking, if a grafting-from polymerization is uncontrolled. The synthesis of large, multifunctional, molecular bottlebrushes by the grafting-from method has been previously conducted under dilute conditions with low activity catalysts used at high concentrations to suppress the undesired termination. Grafting-from polymerizations have seen some success by polymerization in dispersed media or by promoting alternative termination pathways [13,21].

Attempts have been made to reduce copper loading in grafting-from ATRP to prepare polymer stars and bottlebrushes with chemical reducing agents (ARGET ATRP) [22,23], external radical sources (ICAR ATRP) [24], zero-valent metals (SARA ATRP) [24,25], electrical current (eATRP) [26–30], and UV light (photoATRP) [31]. Lowering the concentration of Br-Cu<sup>I</sup>/L catalyst in grafting-from ATRP while maintaining control over polymerization presents a unique challenge in the synthesis of well-defined graft polymers. A lower concentration of Br-Cu<sup>I</sup>/L can lead to slower deactivation and less efficient initiation at the beginning of a grafting-from polymerization [32,33]. Inefficient deactivation can broaden distribution of side chains, causing long side

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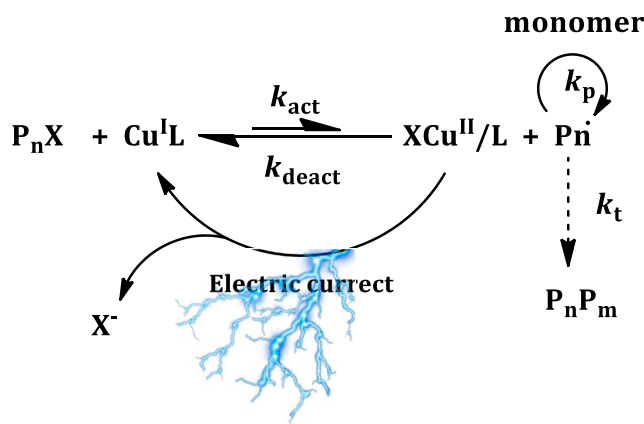
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**Scheme 1.** Mechanism of eATRP ( $P_nX$  - initiator,  $Cu^I L$  - activator,  $XCu^{II}/L$  - deactivator,  $P_n\cdot$  - growing radicals,  $P_nP_m$  - terminated polymer chain,  $X\cdot$  - halogen anion,  $k_{act}$  - activation rate constant,  $k_{deact}$  - deactivation rate constant,  $k_p$  - propagation rate constant,  $k_t$  - termination rate constant).

chains to sterically shield nearby initiators and reduce graft density [34]. A lower graft density will alter the bulk and solution conformations of a graft polymer and will affect the materials properties [35,36].

It is important to investigate new methods of grafting-from synthesis which could both decrease bimolecular RT and produce well-defined graft polymers at low loadings of  $Br-Cu^{II}/L$ . Polyacrylate stars of low molecular weight prepared by grafting-from SARA ATRP could reach near quantitative conversion by  $^1H$  NMR without coupling detectable by gel permeation chromatography (GPC) [25]. Similarly, simplified electrochemically mediated solution ATRP (seATRP) with low ppm of  $Br-Cu^{II}/L$  was employed to form poly(*n*-butyl acrylate) (PBA) polymer stars up to moderately high conversion (~80%) with little evidence of coupling by gel permeation chromatography (GPC) [28]. Both methods relied on a judicious selection of polymerization conditions to compensate for lower loadings of copper catalyst (see Scheme 1).

Electrochemically mediated ATRP (eATRP) allows for highly precise tuning of the  $Cu^I/Cu^{II}$  ratio by variation of the applied potential ( $E_{app}$ ) and current ( $I$ ) [37,38]. A more negative  $E_{app}$  gives a higher  $Cu^I/Cu^{II}$  ratio, which results in a higher rate of propagation ( $R_p$ ) and can also lead to an increased rate of catalyzed radical termination if formation of organometallic species is favored [39]. Decreasing  $Br-Cu^{II}/L$  will also raise dispersity and lower initiation efficiency [40].

In this work, the effect of the applied potential in the simplified electrochemically mediated ATRP of *n*-butyl acrylate was investigated. The findings were then utilized to synthesize high molecular weight polymer stars and bottlebrushes with long arms from multifunctional sucrose (Sucrose- $Br_8$ ) core and poly(2-(2-bromoisobutyryloxy)ethyl methacrylate) (PBiBEM) backbone.

## 2. Results and discussion

### 2.1. Synthesis of PBA stars

The sucrose-based octafunctional ATRP initiator (Scheme S1, Figs. S1 and S2,  $M_{n,app} = 1,534.3$ ,  $\bar{D} = 1.07$ ) was prepared and utilized to synthesize polymer stars as shown in Scheme S3. A series of polymerizations were conducted to examine the effect of the applied potential ( $E_{app}$ ,  $E_{app} = E_{pc}-30$  mV,  $E_{app} = E_{pc}-80$  mV,  $E_{app} = E_{pc}-140$  mV and  $E_{app} = E_{pc}-170$  mV, where  $E_{pc}$  is cathodic peak potential, Fig. S7) on grafting-from polymerization kinetics (Table 1, Figs. 1 and S9). Each seATRP polymerization exhibited a rapid decay of the cathodic current at the beginning of the polymerization due to the initial presence of only  $Br-Cu^{II}/L$  deactivator. Then, the equilibrium  $[Cu^{II}]/[Cu^I]$  ratio was (Table S2) adjusted by the applied  $E_{app}$  to achieve constant current (Fig. S8).

**Table 1**  
Effect of applied potential on seATRP polymerization of BA from Sucrose- $Br_8$  octafunctional initiator.<sup>a</sup>

Entry	$E_{app}$ [V]	$[Cu^I]/[Cu^{II}]$	conv <sup>c</sup> [%]	$k_p^{app}$ [h <sup>-1</sup> ]	$M_{n,th}^d$ ( $\cdot 10^{-3}$ )	$DP_{n,th}^e$ (arm)	$M_{n,app}^g$ ( $\cdot 10^{-3}$ )	$M_w/M_n^g$	$DP_{n,app}^f$ (arm)	$M_w/M_n^g$	LMW impurities (wt%)
S1	$E_{pc}-30$ mV	77	60	0.048 $\pm$ 0.159 <sup>b</sup>	586.0	570	373.1	1.09	499	1.05	9.3
S2	$E_{pc}-80$ mV	92	66	0.057 $\pm$ 0.214 <sup>b</sup>	644.4	627	330.6	1.11	669	1.04	8.4
S3	$E_{pc}-140$ mV	88	65	0.055 $\pm$ 0.196 <sup>b</sup>	634.7	617	374.0	1.09	517	1.07	8.4
S4	$E_{pc}-170$ mV	80	61	0.050 $\pm$ 0.189 <sup>b</sup>	592.8	580	221.6	1.17	536	1.07	9.0

<sup>a</sup> General reaction conditions:  $[BA]_0/[Sucrose-Br_8]_0/[Cu^{II}Br_2/TPMA]_0 = 950/1/0.1$ ,  $T = 50^\circ C$ ;  $V_{tot} = 25$  mL;  $t = 20$  h;  $[BA]_0 = 3.6$  M;  $[CuL]_0 = 105$  ppm; Constant potential seATRP (WE = Pt, CE = Al, RE = SCE).

<sup>b</sup>  $E_{app}$  were selected based on CV analysis of  $Cu^{II}Br_2/TPMA$  catalytic complexes (Fig. S7).

<sup>c</sup> Monomer conversion, apparent rate constant of propagation ( $k_p^{app}$ ) and apparent theoretical degree of polymerization of monomer unit per arm ( $DP_{n,theo}$ ) were determined by NMR [10].

<sup>d</sup>  $M_{n,th} = ([BA]_0/[Sucrose-Br_8]_0) \times conversion \times M_{BA} + M_{Sucrose-Br_8}$ .

<sup>e</sup> Apparent  $M_n$  and  $M_w/M_n$  were determined by GPC.

<sup>f</sup>  $DP_{n,app}$  (per arm) =  $M_{n,app}/M_{BA}$  [27].

<sup>g</sup> Apparent  $M_n$  and  $M_w/M_n$  of the arms cleaved from the star polymers executed by GPC [27].

<sup>h</sup> Apparent rate constant of propagation at the initial stage of the polymerization reaction.

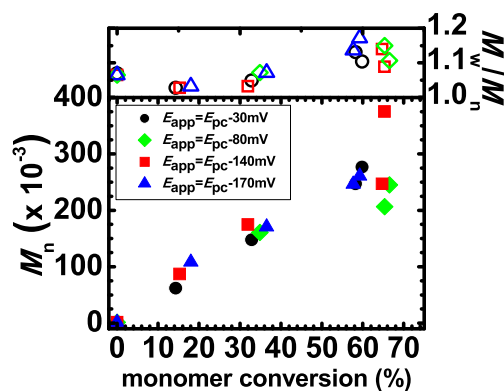


Fig. 1.  $M_n$  and  $M_w/M_n$  vs. monomer conversion showing the effect of applied potential on the synthesis of macromolecular star-like polymers with sucrose core via *se*ATRP.

In an *e*ATRP, more negative potential causes larger cathodic currents and thus provides faster  $R_p$  and thereby larger  $k_p^{app}$  [27]. In the absence of mass transfer limitations,  $R_p$  is directly proportional to the  $E_{app}$  and  $Cu^I/L$  to  $Br-Cu^{II}/L$  ratio [41]. When a highly negative potential is applied, the diffusion of catalyst to the working electrode surface becomes rate limiting. This can be observed as the point when  $R_p$  becomes independent on  $\eta$  ( $\eta = E_{app} - E_{1/2}$ ;  $E_{1/2} = (E_{pc} + E_{pa})/2$ ) and reaches a plateau; the application of more negative  $E_{app}$  values does not increase the polymerization rate [41]. This phenomenon was observed during preparative electrolysis when BA was grafted from the multifunctional Sucrose- $Br_8$  initiator under potentiostatic conditions.

Increasing the  $Cu^I/Cu^{II}$  ratio resulted in a small increase of polymerization rate with comparable control. When the applied potential was increased from  $E_{pc}$ -30 mV to  $E_{pc}$ -80 mV (Entries S1 and S2), the  $Cu^I/Cu^{II}$  ratio was increased from 10 to 11. This resulted in an increase in  $k_p^{app}$  from 0.159 to 0.214  $h^{-1}$  and a small decrease of arm dispersity from  $M_w/M_n = 1.05$  to 1.04. An even more negative  $E_{app}$  of  $E_{pc}$ -140 mV (Entry S3) kept the  $Cu^I/Cu^{II}$  ratio at 11, resulting in a slightly lower  $k_p^{app}$  of 0.196  $h^{-1}$ . This can be attributed to the applied current reaching the upper limit of mass transport at the working electrode. High molecular weight shouldering and higher  $M_w/M_n$  values were observed for polymerizations conducted at  $E_{pc}$ -140 mV and  $E_{pc}$ -170 mV, indicating radical termination was more prominent after the overpotential was achieved (Figs. S10c and S10d) [27]. The predicted percent of chains terminated by biradical termination was estimated using the dead chain fraction (DCF) and is listed in the supplementary information (Table S3). All polymerizations from the Sucrose- $Br_8$  core were calculated to have less than 1% of chains terminated by radical

termination.

Low molecular weight (LMW) impurities were observed in the polymerization product (Fig. S11). Their content increased with time – suggesting transfer to solvent, monomer or more attributed to preparative electrolysis – to an electrolyte were significant (Fig. S11e). The low molecular weight impurity prevented accurate assessment of number of arms by cleavage experiments, resulting in the overestimation of the initiation efficiency values. Branched architectures prepared by grafting-from ATRP under ppm concentrations of copper could have lower initiation efficiency than analogous reactions at higher catalyst loadings. Employing a low concentration of  $Br-Cu^{II}/L$  can cause non-uniform deactivation in a grafting-from polymerization, which can lower initiation efficiency due to uneven growth of side-chains [33].

Summarizing these results, an  $E_{app}$  at  $\sim E_{pc}$ -80 mV had the highest  $k_p^{app}$  and lowest  $M_w/M_n$  out of all tested conditions in the *se*ATRP of *n*-butyl acrylate from octafunctional Sucrose- $Br_8$  cores. These conditions were then utilized to prepare molecular bottlebrushes with relatively long sidechains using the same approach.

## 2.2. Synthesis of molecular bottlebrushes

The synthesis of bottlebrushes by grafting-from *se*ATRP was carried with two multifunctional linear ATRP macroinitiators, PBiBEM<sub>316</sub> (Scheme S2, Table S1, entry 1, Figs. S3 and S4,  $M_n = 88,200$ ,  $D = 1.12$ ) and PBiBEM<sub>1632</sub> (Scheme S2, Table S1, entry 2, Figs. S5 and S6,  $M_n = 455,000$ ,  $D = 1.28$ ), using  $E_{pc}$ -80 mV in the presence of 105 ppm of  $Cu/TPMA$  catalyst. The reactions are outlined in Table 2.

Synthesis of both P(BiBEM-g-(PBA))<sub>316</sub> and P(BiBEM-g-(PBA))<sub>1632</sub> bottlebrushes exhibited excellent control (Entries B1 and B2). Both reactions had linear first-order kinetic plots (Figs. 2a and 3a, respectively) and  $M_{n,app}$  increased with conversion. GPC traces appear to be monomodal, indicating insignificant termination by coupling (Figs. 2c and 3c, respectively).  $M_{n,app}$  of prepared bottlebrushes was significantly lower than  $M_{n,th}$  due to the large difference in hydrodynamic volume of P(BiBEM-g-(PBA)) bottlebrushes and linear polystyrene used for GPC calibrations. The molecular brushes had low dispersity of 1.07 for P(BiBEM-g-(PBA))<sub>316</sub> and 1.18 for P(BiBEM-g-(PBA))<sub>1632</sub>, respectively. The results confirm *se*ATRP could be utilized to prepare well-defined molecular bottlebrushes with minimal bimolecular radical termination.

However, again low molecular weight impurities were observed in the polymerization products (Figs. 13d and 14d). This prevented accurate assessment of initiation efficiency in grafting-from synthesis. Reaction B1 showed 22 wt% of LMW impurities. The P(BiBEM-g-(PBA))<sub>1632</sub> bottlebrush with shorter arms had only 2 wt% of homopolymer impurities (B2, Fig. S14d). Nevertheless, sidechain cleavage

Table 2

Preparation of high molecular weight bottlebrushes with the use of macromolecular initiators.<sup>a</sup>

Entry	[BA] <sub>0</sub> /[BiBEM] <sub>0</sub> / [Cu <sup>II</sup> Br <sub>2</sub> /TPMA] <sub>0</sub>	DP <sub>target</sub>	Conv <sup>b</sup> [%]	$k_p^{app}$ <sup>b</sup> [h <sup>-1</sup> ]	$M_{n,th}$ <sup>c</sup> (·10 <sup>-3</sup> )	DP <sub>n,th</sub> <sup>b</sup> (arm)	$M_{n,app}$ <sup>d</sup> (·10 <sup>-3</sup> )	$M_w/M_n$ <sup>d</sup>	$M_{n,app}$ <sup>e</sup> (·10 <sup>-3</sup> )	DP <sub>n,app</sub> <sup>e</sup> (arm)	$M_w/M_n$ <sup>f</sup>	LMW impurities (wt%)
B1	500/1/0.05 <sup>g</sup>	500	33	0.127	6,707.4	163	645.0	1.11	20.8	163	1.32	22
B2	60/1/0.05 <sup>h</sup>	60	34	0.127	4,685.9	20	945.0	1.30	4.31	34	1.07	2

<sup>a</sup> General reaction conditions:  $T = 50^\circ C$ ;  $V_{tot} = 25$  mL;  $t = 3.25$  h, except entry 2:  $t = 3.5$  h;  $[BA]_0 = 0.73$  M; entry 1:  $[MI]_0 = 4.6$   $\mu$ M calculated per 316 Br initiation sites, entry 2:  $[MI]_0 = 7.5$   $\mu$ M calculated per 1632 Br initiation sites;  $[Cu^{II}Br_2/TPMA] = 0.08$  mM; 105 ppm. Constant potential *se*ATRP (WE = Pt, CE = Al, RE = SCE);  $E_{app} = -0.286$  V ( $E_{app} = E_{pc}$ -80 mV), except entry 2:  $E_{app} = -0.288$  V ( $E_{app} = E_{pc}$ -80 mV),  $E_{app}$  were selected based on CV analysis of  $Cu^{II}Br_2/TPMA$  catalytic complexes (Figs. S13a and S14a).

<sup>b</sup> Monomer conversion, apparent rate constant of propagation ( $k_p^{app}$ ) and apparent theoretical degree of polymerization of monomer unit per arm ( $DP_{n,theo}$ ) were determined by NMR [41].

<sup>c</sup>  $M_{n,th} = ([BA]_0/[MI]_0) \times conversion \times M_{BA} + M_{MI}$ .

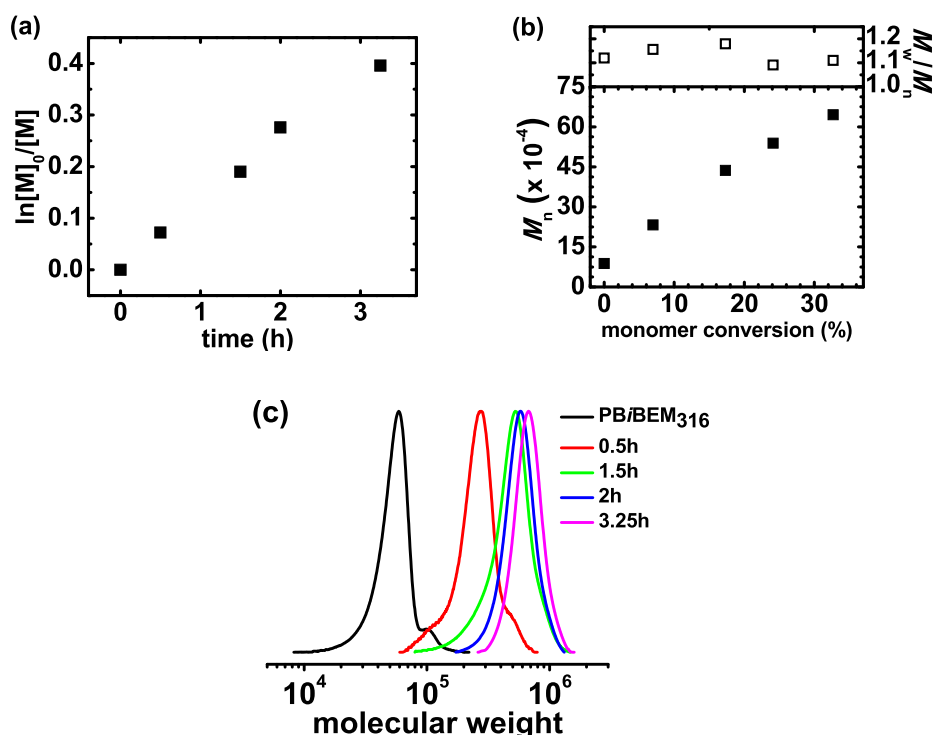
<sup>d</sup> Apparent  $M_n$  and  $M_w/M_n$  were determined by GPC.

<sup>e</sup>  $DP_{n,app}$  (per arm) =  $M_{n,app}/M_{BA}$  [27].

<sup>f</sup> Apparent  $M_n$  and  $M_w/M_n$  of the chains cleaved from the molecular bottlebrushes determined by GPC.

<sup>g</sup> MI: PBiBEM<sub>316</sub>.

<sup>h</sup> MI: PBiBEM<sub>1632</sub>.

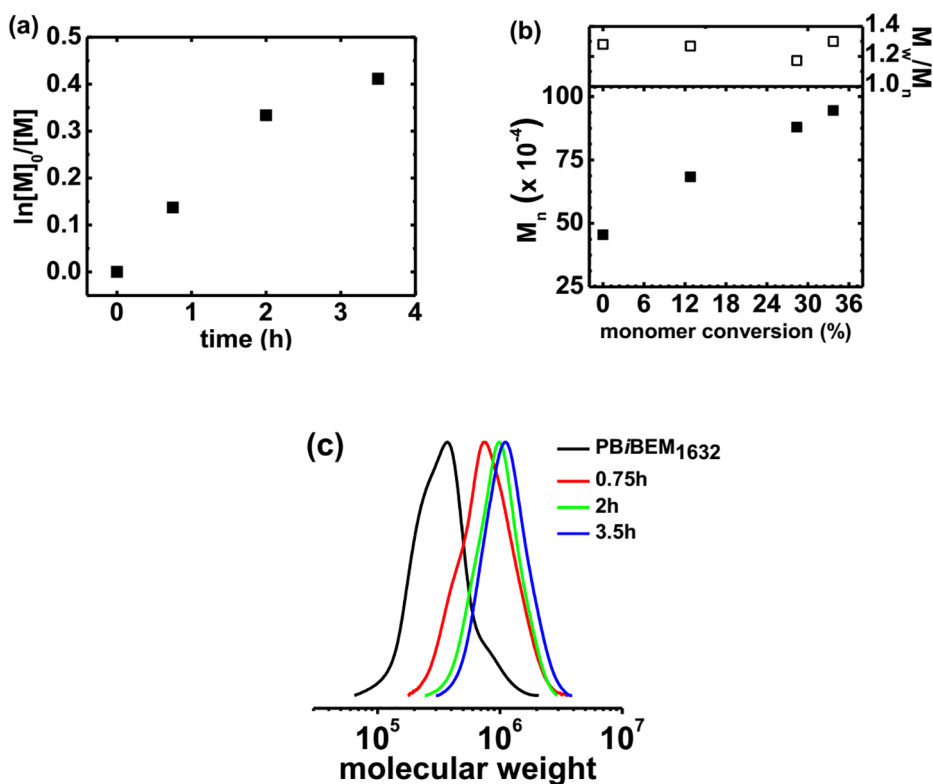


**Fig. 2.** Preparation of macromolecular bottlebrushes with the use of PBiBEM<sub>316</sub>: (a) first-order kinetic plot of monomer conversion vs. time; (b)  $M_n$  and  $M_w/M_n$  vs. monomer conversion; (c) GPC traces of BA polymerization according to Table 2, entry 1. LMW impurities are not included for clarity, but can be found in Fig. S13d.

experiments were used to assess overall control of polymerization (Fig. S13c and S14c for B1 and B2, respectively). The mixture of cleaved sidechains and LMW impurities had low dispersity, suggesting good control in both grafting-from polymerizations.

### 2.3. AFM characterization of the prepared molecular brushes

AFM measurements (Fig. 4) confirmed the successful formation of molecular brushes with different degree of polymerization for the main



**Fig. 3.** Preparation of macromolecular bottlebrushes with the use of PBiBEM<sub>1632</sub>: (a) first-order kinetic plot of monomer conversion vs. time; (b)  $M_n$  and  $M_w/M_n$  vs. monomer conversion; (c) GPC traces of BA polymerization according to Table 2, entry B2. LMW impurities not included for clarity, but can be found in Fig. S14d.



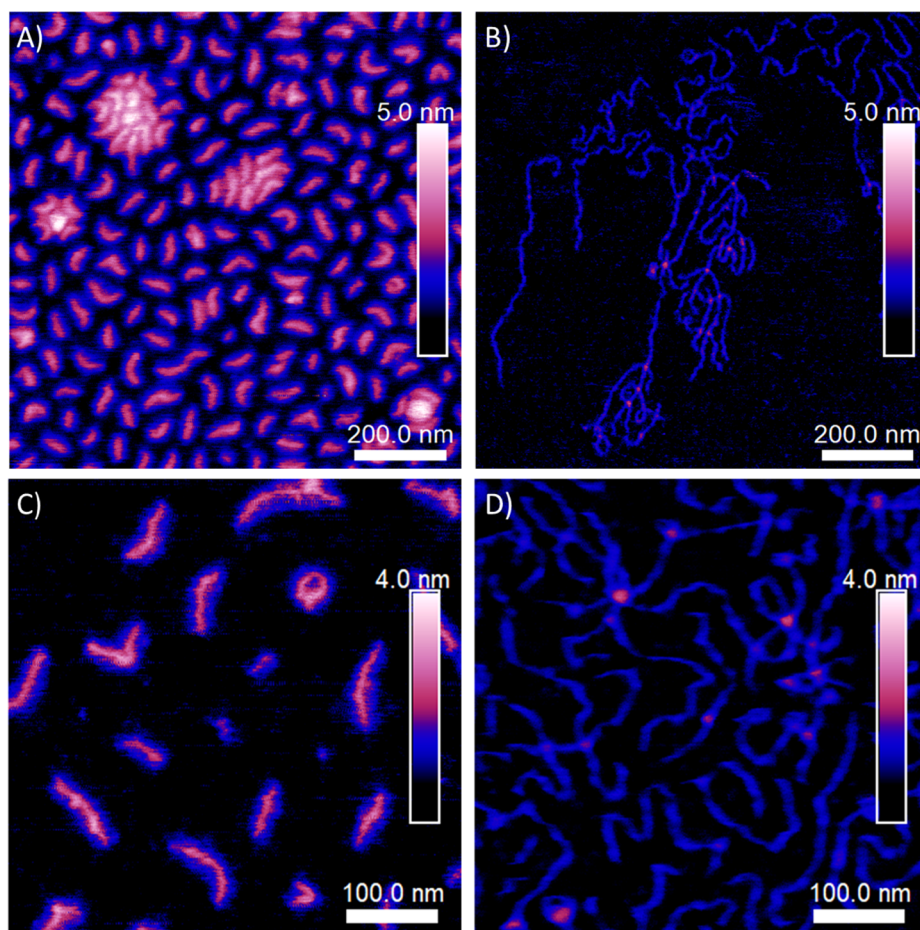


Fig. 4. AFM topography images of: (A), (C) PBiBEM<sub>316</sub>-based brushes and (B), (D) PBiBEM<sub>1632</sub>-based brushes spin-casted on flat silicon substrate.

backbone and grafted polymer chains. In the case of bottlebrushes prepared from PBiBEM<sub>316</sub> initiator, the number-average contour length ( $L_n$ ) was  $93.0 \pm 8.6$  nm, while the width was  $48.2 \pm 4.8$  nm and the length distribution ( $L_w/L_n$ ) of backbone was 1.01, see Figs. S17 and Table S4. If the main backbone adapted a fully extended conformation, and the length of the C—C monomeric unit is equal to 0.25 nm, the contour length of the bottlebrush should be around 79 nm. However, as visualized in the Fig. 4C, the main backbone is shorter than the entire molecule, and one must take into account the contribution of the side chains to the final value of the brush length.

The brushes obtained from much longer macroinitiator (PBiBEM<sub>1632</sub>) had  $L_n$  value  $452 \pm 68$  nm, Fig. 4B and D, Table S4, which correlates well with the results obtained for shorter molecules. However, the PBiBEM<sub>1632</sub>-based brushes were much thinner, due to lower DP of the side chains with the average width =  $17.2 \pm 2$  nm, Fig. S17C. The  $L_w/L_n$  was calculated to be 1.03 (Table S4).

### 3. Conclusion

Star and molecular bottlebrush polymers with poly(*n*-butyl acrylate) side chains were prepared by seATRP using ca. 100 ppm of copper catalyst. A more negative applied potential resulted in faster controlled polymerization. Applied potentials more negative than  $E_{pc}$ -140 mV caused a decrease in polymerization rate and loss of control. An applied potential of  $E_{pc}$ -80 mV provided the fastest polymerization and small contribution of radical termination. This resulted in sucrose-based star polymers with low dispersity of both star polymers ( $M_w/M_n = 1.11$ ) and cleaved arms ( $M_w/M_n = 1.04$ ), as well as molecular bottlebrushes with narrow MW distributions. Low molecular weight impurities were present in all samples and likely originated from transfer reactions or

arm cleavage. The electric current as an external stimulus was proved is a useful synthetic tool which can be used to prepare advanced materials with desired functions and properties.

### Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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### Data availability

The raw/processed data required to reproduce these findings cannot be shared at this time due to technical or time limitations.

### Appendix A. Supplementary material

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.eurpolymj.2020.109566>.

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