



## Biochar derived from red algae for efficient remediation of 4-nonylphenol from marine sediments

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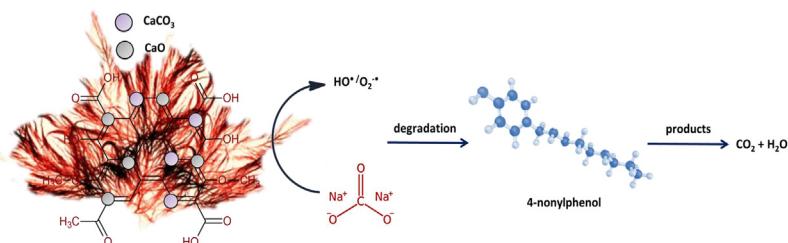
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### HIGHLIGHTS

- RAB was successfully prepared from red algae biomass.
- Real marine sediments were treated with SPC oxidation for 4-NP removal.
- Calcium-enriched RAB efficiently activated SPC to generate reactive radicals.
- pH and RAB dose controlled 4-NP degradation.
- Langmuir–Hinshelwood model described well the kinetics of 4-NP degradation.

### GRAPHICAL ABSTRACT



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### ABSTRACT

4-Nonylphenol (4-NP), a phenolic endocrine disruptor chemical (EDC), is known to have high toxicity to aquatic organisms and humans. The remediation of 4-NP-contaminated marine sediments was studied using red algae-based biochar (RAB) thermochemically synthesized from *Agardhiella subulata* with simple pyrolysis process under different temperatures of 300–900 °C in CO<sub>2</sub> atmosphere. The RAB was characterized by XRD, Raman, FTIR spectroscopy, and zeta potential measurements. The calcium in RAB efficiently activated sodium percarbonate (SPC) to generate reactive radicals for the catalytic degradation of 4-NP at pH 9.0. The oxygen-containing functional groups reacted with H<sub>2</sub>O<sub>2</sub>, which increased the generation of reactive radicals under alkaline pH condition. Ca<sup>2+</sup> ion was the active species responsible for 4-NP degradation. CaO/CaCO<sub>3</sub> on RAB surface enhanced direct electron transfer, increased HO<sup>•</sup> production, and 4-NP degradation in marine sediments. Langmuir–Hinshelwood type kinetics well described the 4-NP degradation process. Remediation of contaminated sediments using RAB could be a sustainable approach toward closed-loop biomass cycling in the degradation of 4-NP contaminants.

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### 1. Introduction

The frequent presence of nonylphenol ethoxylate (NPEO), nonionic surfactant discharged from various anthropogenic sources such as household, industrial, and agricultural activities, in marine and freshwater ecosystems is one of the most common emerging substances of concern (ESOC) in the sediments (Fang et al., 2019;

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Wang et al., 2019). 4-Nonylphenol (4-NP) is a metabolite of NPEO, which is more recalcitrant than its parent compound. 4-NP is an important environmental phenolic endocrine disruptor chemical (EDC) and an indicator of seafood contamination (Chang et al., 2019; Zhou et al., 2019). At elevated concentrations in different environmental systems such as reservoirs, rivers, lakes, wetlands, streams, and marine matrices, 4-NP exhibited high toxicity, in terms of estrogenic activity and teratogenicity, to aquatic organisms and humans (Gong et al., 2019). Effective techniques such as bioremediation and advanced oxidation process (AOP) for 4-NP degradation are urgently needed to safeguard ecological and human health (Hussain et al., 2017; Dong et al., 2019a; Kent and Tay, 2019; Mtibaà et al., 2020).

AOP is effective in oxidizing and mineralizing many toxic and biorefractory organic compounds due to of high oxidation potential from possible reactive oxygen species (ROS) (Qi et al., 2013; Hung et al., 2016a,b; Danish et al., 2017; Dong et al., 2018a,b; 2019a,b; Dong et al., 2020). Among all HO<sup>•</sup> generation systems, sodium percarbonate ( $2\text{Na}_2\text{CO}_3 \cdot 3\text{H}_2\text{O}_2$ , SPC), a solid carrier of hydrogen peroxide ( $\text{H}_2\text{O}_2$ ), can produce oxidizing species, i.e. hydroxyl ( $\text{HO}^{\bullet}$ ) and superoxide anion ( $\text{O}_2^{\bullet}$ ) radicals, which exhibit strong oxidation ability toward the degradation of organic contaminants (Cravotto et al., 2007). SPC is alkaline and has high pH buffer capacity over a wide pH range (Fu et al., 2015). Zuo et al. (2020) reported that the degradation of carbamazepine (CBZ) in wastewater by radical-based (specifically, HO<sup>•</sup> and  $\text{SO}_4^{\bullet}$ ) techniques using microwave-ultraviolet catalyzed oxidation systems followed the order: SPC >  $\text{H}_2\text{O}_2$  > persulfate (PS) > peroxyomonosulfate (PMS). SPC is a strong oxidant capable of removing a wide list of refractory contaminants. Cravotto et al. (2007) studied the treatment of *p*-nonylphenol (NP) by SPC under microwave (MW) irradiation. Miao et al. (2015) used hydroxylamine hydrochloride modified Fe-catalyzed SPC process to enhance the removal of tetrachloroethene (PCE). The Fe(III)/Fe(II) redox couple, yielding a relatively steady Fe(II) and higher of HO<sup>•</sup>/O<sub>2</sub><sup>•</sup> radicals, which resulted in almost complete PCE removal. Moreover, Cui et al. (2017) studied ethylbenzene (EB) removal in aqueous solutions by SPC oxidation over (S,S)-ethylenediamine-N,N-disuccinic acid (EDDS)-Fe(III) catalyst and complete oxidation occurred at pH 5.5 in 90 min and HO<sup>•</sup> was the predominant species responsible for EB degradation. Farooq et al. (2017) investigated the degradation of trichloroethane (TCA) by SPC over binary Fe–Cu/reduced graphene oxide (rGO). Results showed that the combination of Fe and Cu supported on rGO greatly enhanced TCA degradation because of high surface area ( $119.2 \text{ m}^2/\text{g}$ ) that provided more active sites for the generation of ROS in the SPC system. Additionally, Chen et al. (2018) studied the degradation of Rhodamine B (RhB) dye by SPC over iron oxychloride (FeOCl) catalyst under visible light (FeOCl/SPC/Vis) and reported that the degradation of RhB increased with active iron sites. Although above studies have addressed the issue that combining SPC with catalyst can enhance the degradation efficiency of organic contaminants synergistically, but high cost of metallic catalysts, leaching of metal ions, incomplete removal of the organic contamination, and the formation of the toxic byproducts still remain engineering challenges (De Luna et al., 2020). Therefore, it is necessary to develop eco-friendly and cost-effective bio-based materials, such as biochar, as SPC activators to produce radicals, i.e., HO<sup>•</sup> and O<sub>2</sub><sup>•</sup>, for improving the degradation efficiency of hazardous chemicals.

Biochar is a highly porous material rich in varying surface functional groups, polarity and crystallinity. However, feedstock, thermos-chemical process and pretreatment of biomass and post treatment of biocahr determined the surface heterogeneity and thus reactivity. Del Bubba et al. (2020) studied the adsorption of 4-

t-octylphenol (4-t-OP) and 4-nonylphenol (4-NP) on a wide list of biochars prepared from wide list of biomaterials and pyrolysis temperature and reported that pyrolysis temperature was the most influential parameter on surface properties and thus reactivity of biochar.

Algae are main primary producers in most ecosystems. Algae, both autotrophic and heterotrophic, which biomass contains proteins, polysaccharides and lipids, are capable of generating substantial biomass (Duan et al., 2019). The potential benefits of marine algal biomass, both microalgae and macroalgae, as algal-based foods, phycocolloids, biomedicinals, fertilizers, biofuels, soil amendment, and nutrient scavengers in wastewater treatment systems, in terms of circular bioeconomy framework, has received increasing attention in recent years (Alobwede et al., 2019; Amin and Chetpattananondh, 2019; Jaafari and Yaghmaeian, 2019a,b; Thiyva and Vijayaraghavan, 2019; Nagarajan et al., 2020). De Bhowmick et al. (2018) reported that microalgae could be grown in wastewater for simultaneous production of high-value products and biochar. Red algal (*Agardhiella subulata*) is a common bioresource with that can be produced at large quantity rapidly. The algal biomass can be used to produce polysaccharides, such as agars or carrageenan, valuable gelling and stabilizing reagents for pharmaceutical applications (Murnao et al., 1997; Rorrer and Cheney, 2004; Sudhakar et al., 2018). De Bhowmick et al. (2019) reported that algae will be next generation feedstock. Algal biomass can be environmentally sustainable material for the production of biochar catalyst, an attractive option to enhance the capacity of remediating contaminated waters and soils (Roberts et al., 2015). Moreover, the alkaline nature of algal biochar can be ideal acid soils conditioner and the inorganic ash components, namely, P, K, Mg and Ca, can be beneficial soil amendments to enhance crop productivity (Yu et al., 2017). One potential end-use of algal biomass, especially, the fast-growing calcium oxide-rich red algae, is for the production of biochar (Bird et al., 2011; Sharma et al., 2019). Red algal is a potential Ca source that is suitable for the preparation of Ca-modified biochar for use as heterogeneous catalyst. Moreover, calcium is an alkaline earth metal ion having weak Lewis acidity due to its small electronegativity (Bazargan et al., 2015). Hence, calcium ion contributes to high activity in transesterification reaction during biodiesel production, and enhances adsorption phosphate due to its high basicity (Wang et al., 2019; Liu et al., 2019). This study aims at the preparation, characterization and applications of red algal biochar as catalyst for the degradation of refractory contaminants in sediments. We have previously studied the treatment of PAHs and 4-NP contaminated sediments using bamboo biochar modified by Fe<sub>3</sub>O<sub>4</sub> (Dong et al., 2017, 2019c). To the best of our knowledge, the preparation and testing of calcium oxide-rich macroalgal biochar, in one-step pyrolysis, for SPC activation toward the remediation of 4-NP-contaminated sediments has not yet been studied. Major factors, such as pyrolysis temperature, SPC and RAB dosages, and pH affecting the kinetics of 4-NP degradation were investigated.

## 2. Materials and methods

### 2.1. Sediment samples

Sediment samples were collected from the Jen-Gen River, Kaohsiung City, Taiwan (longitude 120°18.12' E, latitude 22°35.13' N). The samples were immediately placed in pre-cleaned amber bottles (with Teflon gasket and screw cap) upon dredging. The collected sediments were frozen while being transported to the laboratory. The samples were air-dried at room temperature and

then freeze-dried for 72 h prior to laboratory experiments. The sand, silt, and clay content of typical sediment samples were 24, 68, and 8%, respectively.

## 2.2. Chemicals

Chemicals used included sodium percarbonate ( $2\text{Na}_2\text{CO}_3 \cdot 3\text{H}_2\text{O}_2$ , SPC) (20–30%  $\text{H}_2\text{O}_2$ ) from Sigma-Aldrich Co. Ltd. (St. Louis, USA), acetone, methanol, dichloromethane, and *n*-hexane (99.8% purity, HPLC grade) from Echo Chemical Co., Ltd. (Miaoli, Taiwan), 4-nonylphenols ( $\text{C}_{15}\text{H}_{24}\text{O}$ , NP) and branched side-chain-mixed compounds (99.5% purity) from Tokyo Kasei Kogyo Co., Ltd. (Tokyo, Japan), and internal standard (p-terphenyl, 99.5% purity) from Chem Service Inc. (Pennsylvania, U.S.A). The above reagents were of analytical grade. The biochar was produced by the pyrolysis of red algae (*Agardhiella subulata*) as raw biomass material. Red algae samples were provided by Po-Wu Botechnology Co. Ltd (Pingtung, Taiwan). The collected red algae was washed several times with deionized water to remove the epiphytes, microbes, sand particles, and other impurities, dried in air for 1 h, again at 60 °C in oven for 24 h, then dried algae material was ground to powder form. The powdered red algae was pyrolyzed at temperature ranging from 300 to 900 °C and heating rate of 10 °C min<sup>-1</sup> in a furnace in  $\text{CO}_2$  atmosphere to produce red algae biochar (RAB). The RAB was washed thoroughly, oven-dried at 60 °C for 24 h, and then stored in a desiccator for future use. The solid products was denoted as RAB300, RAB500, RAB700, and RAB900, for pyrolysis temperature of 300, 500, 700 and 900 °C, respectively. Raw red algae had a CaO content of about 734 mg g<sup>-1</sup> reported previously (Su et al., 2014).

## 2.3. 4-NP degradation experiments

All experiments were conducted at room temperature (303 K). To 40-mL borosilicate glass vial, it was added 1 g of dry sediment sample, 1.0–5.0 g L<sup>-1</sup> of RAB, and 25 mL of solution containing SPC and 4-NP at molar ratio of 1–1000 : 1. Then all sample vials were gently shaken for 30 s before placing in a water bath shaker (SB-9D, Taiwan Hipoint Corporation, Kaohsiung, Taiwan) and continuously shaken at a speed of 200 rpm for 6 h. At the end of preselected time interval, i.e., 1–6 h, the solution was quenched with methanol to terminate the oxidation reaction. Then the sediment slurry was extracted for residual 4-NP with dichloromethane to determine the amount of 4-NP degraded. The 4-NP concentration was detected using gas chromatography–mass spectrometry (GC–MS) (Agilent 6890 N GC/5975 MS). The initial solution pH was adjusted with HCl (0.1 M) and NaOH (0.1 M) to the desired value. Parameters such as dosage of RAB and pH on 4-NP degradation were investigated. Each degradation experiment was performed in triplicate.

## 2.4. Chemical analyses

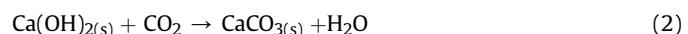
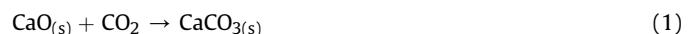
XRD analysis was performed using a Diano-8536 diffractometer equipped with  $\text{CuK}\alpha$  radiation source. Raman spectroscopy analysis was conducted using a visible Raman system (Nanofinder 30, Tokyo Instruments, Japan) with a 632.8 nm He–Ne laser. Fourier transform infrared (FTIR) spectra were collected in the range of 400–4000 cm<sup>-1</sup> with FTIR spectrometer (FT-700, Horiba, Japan) using potassium bromide (KBr) pellet. Zeta potential of the catalyst was measured with Zetasizer Nano ZS90 (Malvern Instruments, Worcestershire, UK). The suspension pH was adjusted from pH 3 to 11 using 0.1 M of  $\text{HNO}_3$  or 0.1 M of NaOH. The 4-NP concentration was analyzed using GC–MS. The transfer line and ion source temperature were 280 and 230 °C, respectively. The 4-NP was separated using an HP-5MS (30 m × 0.25 mm i. d. × 0.25  $\mu\text{m}$  film

thickness) capillary column (Hewlett-Packard, Palo Alto, CA, USA). Helium was the carrier gas at a flow rate of 1.5 mL min<sup>-1</sup>. The GC oven temperature was initially set to 70 °C for 2 min, increased to 240 °C at 20 °C min<sup>-1</sup>, then to 300 °C at 5 °C min<sup>-1</sup>, and finally maintained at 300 °C for 5 min. The mass spectrometer was operated in selected ion monitoring (SIM) mode. The 4-NP concentration was quantified based on the internal standard method. The final concentration was corrected based on the recovery. The results showed remarkable repeatability and reproducibility of 4-NP measurement.

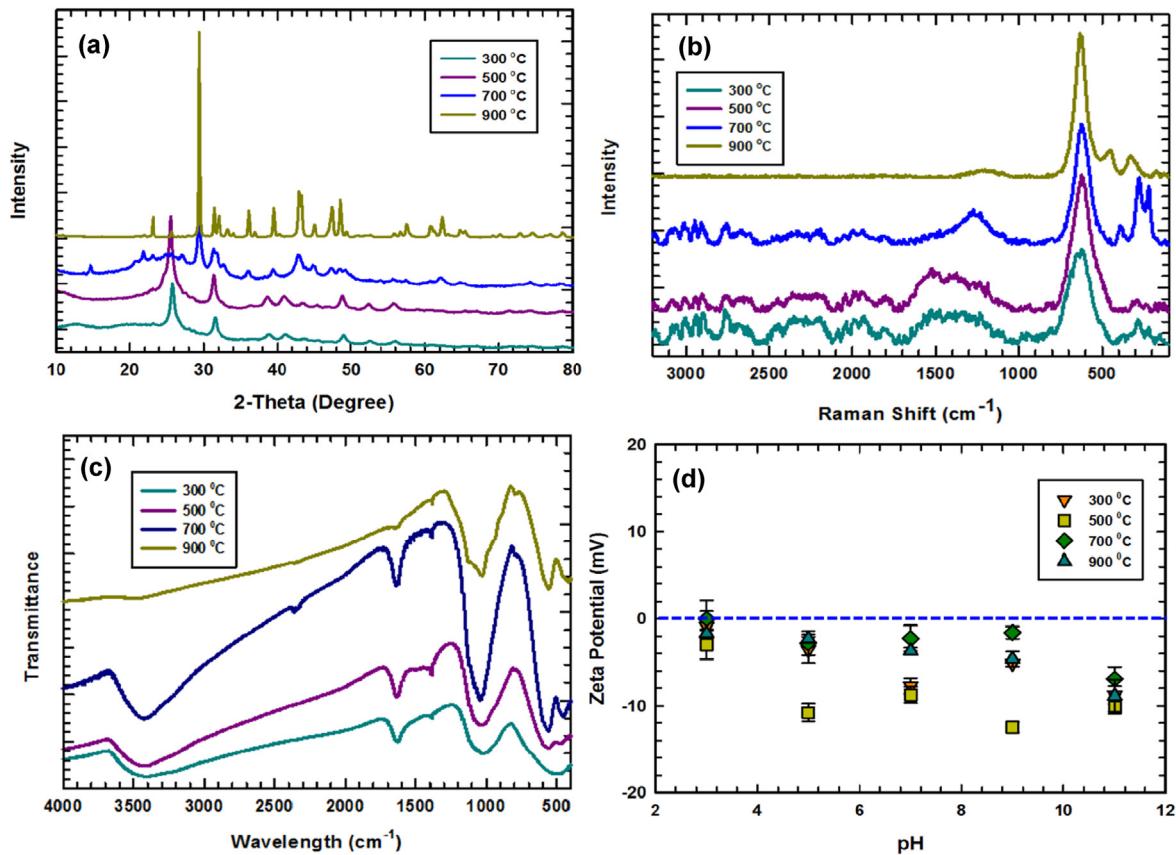
## 3. Results and discussion

### 3.1. Characterization of RAB

The XRD peaks of typical graphite-like crystalline carbon in RAB were at  $2\theta = 25.9^\circ$  and  $43.9^\circ$ , which were characteristic of (002) and (100) planes (Fig. 1a). Significant CaO peaks of were at  $2\theta = 31.6^\circ$ ,  $36.3^\circ$ ,  $47.3^\circ$ ,  $52.9^\circ$ , and  $64.1^\circ$ , which were corresponding to the lattice planes (111), (200), (220), and (222) (Liu et al., 2019). The XRD peaks of RAB appeared at  $2\theta = 23.0^\circ$ ,  $29.4^\circ$ ,  $35.9^\circ$ ,  $43.2^\circ$ ,  $47.5^\circ$ ,  $48.5^\circ$ ,  $57.4^\circ$ ,  $60.6^\circ$ , and  $64.6^\circ$ , representing the lattice planes of (012), (104), (110), (202), (018), (116), (122), (119), and (300) of  $\text{CaCO}_3$  (Chang et al., 2011). The results showed the presence of CaO and  $\text{CaCO}_3$  in RAB900, along with low intensity peaks of graphite-like structures, which suggested that RAB was carbonated with  $\text{CO}_2$  and  $\text{CaCO}_3$  was formed. However, moisture and  $\text{CO}_2$  easily reacted with CaO to form  $\text{Ca(OH)}_2$  and  $\text{CaCO}_3$ , respectively. These inactive phases could reduce the activity and basicity of RAB (Wang et al., 2019).  $\text{CO}_2$  reacted with CaO and  $\text{Ca(OH)}_2$  to form a thermodynamically stable  $\text{CaCO}_3$  according to Eqs. (1) and (2).  $\text{CO}_2$  acted as an activation agent and generated a large number of small porous structures in biochar (Shi et al., 2020). As the pyrolysis temperature increased from 700 to 900 °C, the intensity of CaO and  $\text{CaCO}_3$  peaks increased gradually while the intensity of C peaks decreased sharply, due to the chemical reaction between CaO and graphite-like phases and the coverage of RAB by CaO and  $\text{CaCO}_3$ .



Raman analysis provides more information about the surface properties of RAB (Fig. 1b). The peaks in the region of 1360 cm<sup>-1</sup> corresponding to D bands (carbon  $\text{sp}^3$  hybridization) and peaks in the range of 1586 cm<sup>-1</sup> was associated with the G bands (carbon  $\text{sp}^2$  hybridization). The results of the FTIR analyses for RAB, obtained in the wavenumber region between 4000 and 400 cm<sup>-1</sup>, which indicated changes in their surface functional groups in relation to the different pyrolysis temperatures for the positive or negative catalytic effects of RAB for the degradation of 4-NP (Fig. 1c). The samples exhibited these peaks at 1470, 689, and 907 cm<sup>-1</sup>, representing the asymmetric stretch modes of Ca–O bonds, respectively (Wang et al., 2019). Moreover, three peaks were observed at 1385, 1160, and 1040 cm<sup>-1</sup> corresponding to the O–H stretching in the plane of free hydroxyl groups, surface C–O–C, and C–O bonds, respectively (Shi et al., 2020). The peak at 1430 cm<sup>-1</sup> was assigned to the antisymmetric stretching of carboxylic acid ( $-\text{COOH}$ ) and carboxylate ( $-\text{COO}^-$ ) groups in RAB due to aromatic ring modes, which were important to maintain hydrophilicity of catalyst. The band of the C=O group appeared at 1556 cm<sup>-1</sup>. The band at 1100 cm<sup>-1</sup> corresponded to the polysaccharide rings and became most prominent at higher temperature (Bird et al., 2011). The increase in band intensity of oxygen-containing functional groups (OFGs) was observed for RAB900,



**Fig. 1.** The (a) XRD pattern, (b) Raman, (c) FTIR and (d) zeta potential of RAB catalyst.

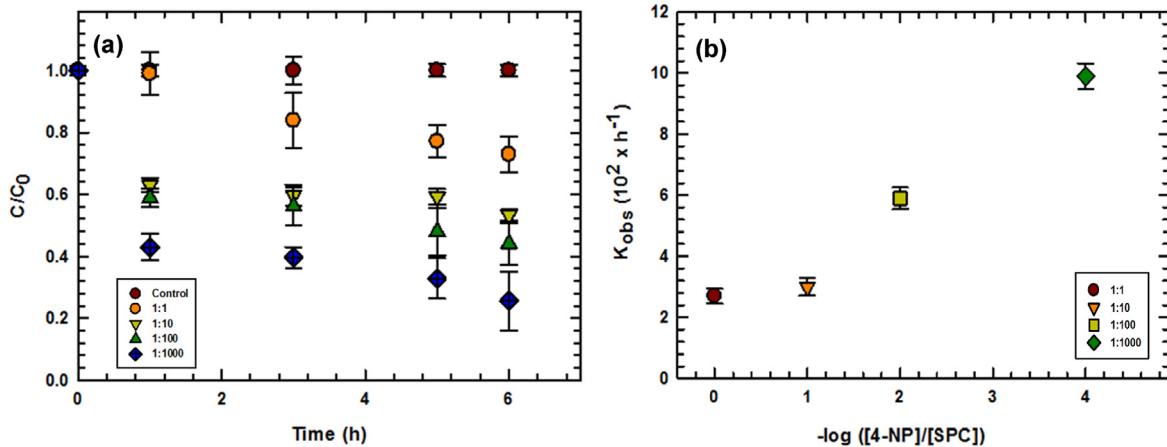
which provided information on the surface functionalization process. Poo et al. (2018) reported that the OFG density of marine macro-algae biochar was larger than that of woody biochar. Therefore, OFGs were active catalytic sites and electron acceptors for the oxidation of 4-NP. In addition, the RAB surface charge was determined by zeta potential measurements over the pH range of 3–11 to further explore the catalytic mechanism (Fig. 1d). The zeta potential of RAB900 was approximately  $-24$  mV at pH 3 and decreased to  $-39$  mV at pH 11, which clearly indicated that RAB was negatively charged. Electronic interactions between 4-NP and RAB might play a role on the adsorption and the catalytic activity of RAB. This behavior could be attributed, in part, to surface functionalization; that is, OFGs, including  $-\text{COO}^-$ ,  $-\text{COOH}$ , and  $-\text{OH}$ , onto the RAB surface thus decreased the surface potential. Results of zeta potential and FTIR analyses suggested that 4-NP degradation over RAB involved electrostatic attraction and hydrophobic interactions between 4-NP and OFGs. FTIR results confirmed the successful deposition of CaO phase on to the carbon framework through Ca–O–C linkages between CaO and porous carbon support. The formation of Ca–O–C bond enhanced the stability of the Ca-based composite catalysts and reduced the loss of  $\text{Ca}^{2+}$  ions (Wang et al., 2019). Thus, results of the XRD, Raman, and FTIR clearly indicated the presence of CaO on RAB surface.

### 3.2. The activity of RAB toward 4-NP degradation

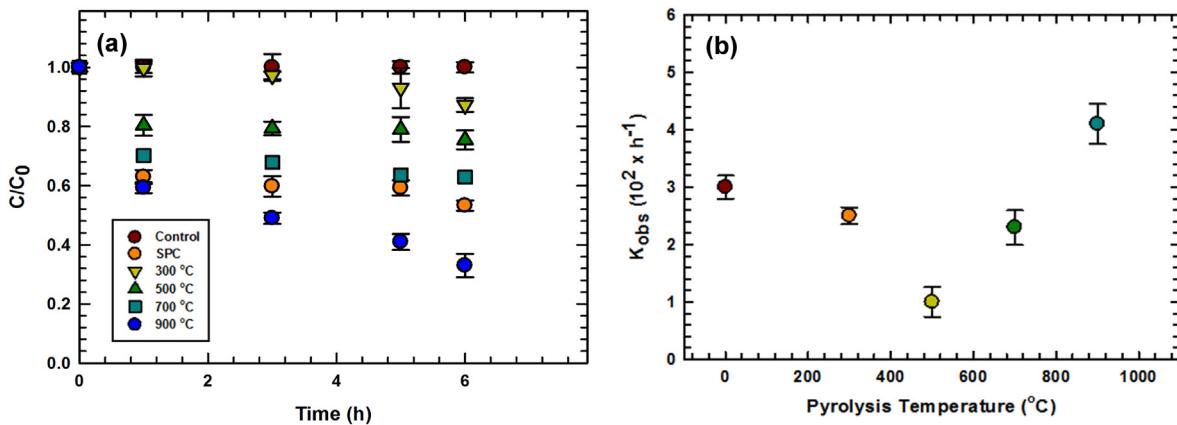
The 4-NP concentration observed in sediments was approximately  $56,136 \pm 7342$  ng g<sup>-1</sup> dry weight (dw). Fig. 2a shows the degradation of 4-NP as affected by SPC concentration. Results show less than 5% loss of 4-NP in the absence of SPC. 4-NP degradation

increased significantly at higher SPC concentration. At the highest SPC concentration of  $2 \times 10^{-2}$  M (or  $\Sigma[4\text{-NP}]/[\text{SPC}]$  molar ratio of 1:1000),  $\Sigma$ 4-NP removal reached 75%. Results indicated that adequate SPC must be available to produce of  $\text{HO}^\bullet$  radicals for 4-NP degradation. As shown in Fig. 2b,  $\Sigma[4\text{-NP}]/[\text{SPC}]$  ratio of 1:1000 gave rate constant,  $k_{\text{obs}}$ , of  $9.9 \times 10^{-2}$  h<sup>-1</sup>, which was almost 3.7 times that  $2.7 \times 10^{-2}$  h<sup>-1</sup> of  $\Sigma[4\text{-NP}]/[\text{SPC}]$  ratio 1:1. After reaction, SPC was converted to bicarbonate and carbonate ions ( $\text{HCO}_3^-$  and  $\text{CO}_3^{2-}$ ), which might scavenge  $\text{HO}^\bullet$  and  $\text{O}_2^\bullet$  to form carbonate radical ( $\text{CO}_3^\bullet$ ) (Gao et al., 2020).  $\text{CO}_3^\bullet$  could react with the aromatic substrates through an electrophilic addition, substitution, or direct electron transfer reaction but at a lower rate than  $\text{HO}^\bullet$  (Miao et al., 2015; Cui et al., 2017). Therefore,  $2 \times 10^{-4}$  M (at  $\Sigma[4\text{-NP}]/[\text{SPC}]$  molar ratio of 1:10) was selected as the optimal reaction concentration and used for further study.

Further experiments were conducted to examine 4-NP degradation by SPC on RAB prepared at different pyrolysis temperature. The results showed that RAB900 effectively activated SPC, to yield a maximum 4-NP degradation of 67%, which was greater than that of SPC (47%) alone (Fig. 3a). The findings demonstrated that RAB played a critical role toward 4-NP degradation owing to the synergistic effects exhibited by CaO and the porous carbon support of biochar. Yin et al. (2013) reported that natural CaO-rich sepiolite calcined at 900 °C exhibited remarkable phosphorus removal capacity. Furthermore, high calcination temperature could significantly govern the formation of graphitized carbon skeleton of biochar, which resulted in high surface functionality and porosity (Liu et al., 2015). Therefore, the role of RAB in the RAB/SPC system included direct decomposition of SPC and accelerating SPC oxidation mediated by reactive Ca-phases. Therefore, CaO, the main



**Fig. 2.** (a) Effect of percarbonate concentration and (b) rate constant of 4-NP degradation. Experimental conditions: sediment = 1.00 g, reaction volume = 40 mL,  $T = 30^\circ\text{C}$ ,  $\text{pH}_0 = 9.0$ ,  $\sum[4\text{-NP}]: [\text{SPC}]$  (molar ratio) = 1:  $10^0\text{--}10^3$ .

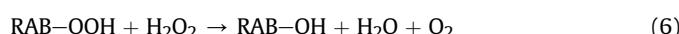
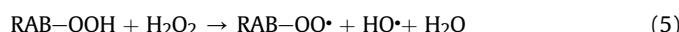


**Fig. 3.** (a) Effect of pyrolysis temperature of the RAB and (b) rate constant of 4-NP degradation. Experimental conditions: sediment = 1.00 g, reaction volume = 40 mL,  $T = 30^\circ\text{C}$ ,  $\text{pH}_0 = 9.0$ ,  $[\text{RAB}] = 3.0 \text{ g L}^{-1}$ ,  $[\text{SPC}] = 2 \times 10^{-4} \text{ M}$ ,  $\sum[4\text{-NP}]: [\text{SPC}]$  (molar ratio) = 1 : 10.

active mineral phase, provided sufficient catalytic sites with sufficient amount of  $\text{Ca}^{2+}$  ions to facilitate the electron transfer reaction at the RAB surface toward catalytic 4-NP decomposition. The catalytic activity of  $\text{CaO}$  was derived from the basic sites and spatial dispersion defining  $\text{Ca}^{2+}$  availability (Marinković et al., 2016). The basic sites quickly reacted with ambient  $\text{H}_2\text{O}$  and  $\text{CO}_2$  to form  $\text{O}^{2-}$  and initiated base-catalyzed reaction. Efficient electron transfer process among 4-NP, SPC, and the RAB network via  $\text{Ca}^{2+}$  (Eq. (3)), initiated the oxidation-reduction reaction to generate ROS (Granados et al., 2007).

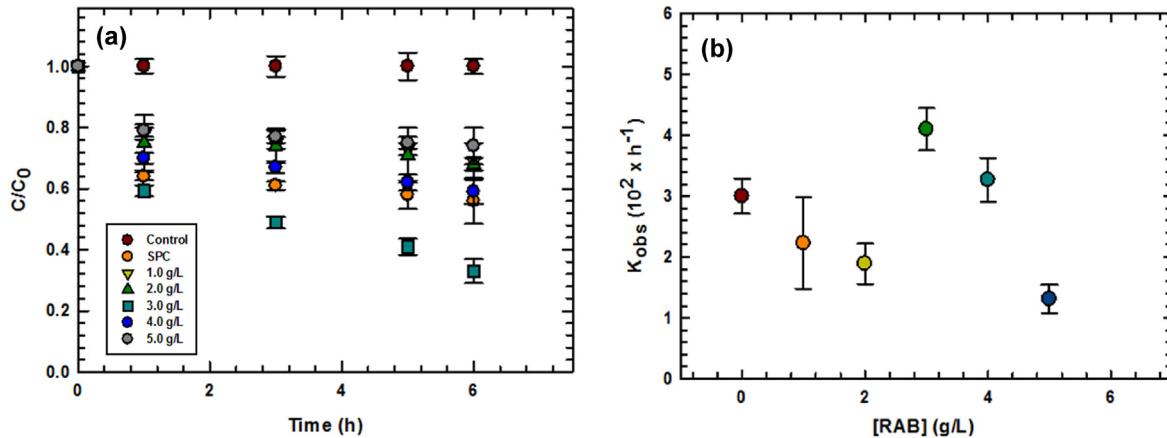


Moreover, the presence of OFGs on the RAB surface, such as electron-rich groups of hydroxyl ( $-\text{OH}$ ) and carboxyl ( $-\text{COOH}$ ) enhanced the generation of  $\text{HO}^\bullet$  according to the following reactions (Eqs. (4)–(6)), the outcome of which enhanced 4-NP degradation.



Sharma et al. (2019) reported that high specific surface area, porosity, and OFGs of the algal biomass effectively promoted the adsorption/photocatalytic of organic pollutants from the aqueous medium. The degradation of 4-NP oxidation by SPC over the RAB catalyst followed the pseudo-first-order kinetics. The rate constant ( $k_{obs}$ ) was determined from the slope of linear  $\ln (C/C_0)$  vs. time ( $t$ ) plot, where  $C_0$  and  $C$  are the 4-NP concentration at initial ( $t = 0$ ) and at time  $t$ , respectively (Fig. 3b). The  $k_{obs}$  were  $2.5 \times 10^{-2}$ ,  $1.0 \times 10^{-2}$ ,  $2.3 \times 10^{-2}$ , and  $4.1 \times 10^{-2} \text{ h}^{-1}$  for RAB300, RAB500, RAB700, and RAB900, respectively. The results revealed that the RAB900/SPC process achieved the highest 4-NP degradation rate with respect to SPC at pH 9.0. Therefore, RAB and  $\text{HO}^\bullet$  exhibited a synergistic effect on 4-NP degradation. Further study is needed still on the effect of calcium content of RAB as a function of pyrolysis temperature and how calcium ion may govern the catalytic activity of RAB during field applications.

The degradation of 4-NP was evaluated at different RAB900 dosage from 1.0 to 5.0  $\text{g L}^{-1}$ , while keeping constant the concentration of SPC at  $2 \times 10^{-4} \text{ M}$  and initial pH at 9.0 (Fig. 4a). Specifically, results showed that 3.0  $\text{g L}^{-1}$  of RAB was able to generate enough  $\text{HO}^\bullet$  for effective degradation of 4-NP with a maximum conversion of 67%. However, higher dosage (5.0  $\text{g L}^{-1}$ ) decreased 4-NP degradation due to excess generation of  $\text{H}_2\text{O}_2$ , the higher RAB dosage enabled the graphitic structure and OFGs to scavenge the radicals and subsequently decreased the catalytic activity. The

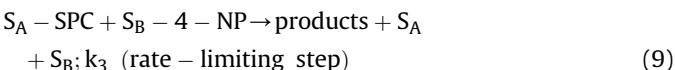


**Fig. 4.** (a) Effect of RAB dosage and (b) rate constant of 4-NP degradation. Experimental conditions: sediment = 1.00 g, reaction volume = 40 mL,  $T = 30$  °C,  $pH_0 = 9.0$ ,  $[SPC] = 2 \times 10^{-4}$  M,  $\sum[4-NP]:[SPC]$  (molar ratio) = 1 : 10.

optimum 4-NP degradation rate must be achieved at a suitable RAB dose. Reaction between HO<sup>•</sup> and organic pollutants was responsible for the degradation of the latter by  $H_2O_2$  oxidation (Wang et al., 2019). Ruan et al. (2019) proposed that biochar effectively activated  $H_2O_2$  to produce environmentally persistent free radicals (EPFRs), such as, oxygen-, carbon-, and oxygenated carbon-centered radicals, which are powerful and promising oxidants for the degradation of organic contaminants. Nevertheless, the decomposition of 4-NP in the RAB/SPC system increased with the amount of HO<sup>•</sup> due to increasing direct electron transfer between the constituents of the CaO/CaCO<sub>3</sub> oxide surface and target contaminants. Moreover, the  $k_{obs}$  were  $2.2 \times 10^{-2}$ ,  $1.9 \times 10^{-2}$ ,  $4.1 \times 10^{-2}$ ,  $3.3 \times 10^{-2}$ , and  $1.3 \times 10^{-2} h^{-1}$  at RAB dosages of 1.0, 2.0, 3.0, 4.0, and 5.0 g L<sup>-1</sup>, respectively (Fig. 4b). The increase in the reaction rate with increasing RAB dosage could be ascribed to the increased availability of SPC for reaction with Ca<sup>2+</sup> in solution to produce a large amount of HO<sup>•</sup> for the oxidation of 4-NP. According to the Langmuir-Hinshelwood mechanism of heterogeneous catalysis reaction, rapid adsorption of reactants, i.e., SPC and 4-NP onto the catalyst surface was the first reaction step (Dobaradaran et al., 2018; Dong et al., 2019d). Accordingly, at the onset of the reaction, SPC and 4-NP adsorbs onto the active site,  $S_A$  and  $S_B$ , respectively, as showing in the following reactions:



where  $K_1$  and  $K_2$  are the equilibrium adsorption constants of SPC and 4-NP on the different active sites of the RAB, respectively.  $S_A - SPC$  and  $S_B - 4 - NP$  are the adsorbed SPC and 4-NP species on the RAB surface, respectively. The reaction between the adsorbed SPC and 4-NP species is assumed the rate-limiting step, that is:



From Eq. (9), one can obtain the following rate expression:

$$\text{rate } (r) = - \frac{d[4 - NP]}{dt} = k_3 [S_A - SPC][S_B - 4 - NP] \quad (10)$$

where  $k_3$  is the reaction rate constant. From Eqs. (7) and (8), one has:

$$[S_A - SPC] = K_1 [S_A][SPC] \quad (11a)$$

and

$$[S_B - 4 - NP] = K_2 [S_B][4 - NP] \quad (11b)$$

The mass balance relationship gives the following equations:

$$S^T = S_A^T + S_B^T \quad (12)$$

$$S_A^T = [S_A] + [S_A - SPC] \quad (13a)$$

and

$$S_B^T = [S_B] + [S_B - 4 - NP] \quad (13b)$$

Combining Eq. (11a) and Eq. (13a), and Eq. (11b) and Eq. (13b) gives:

$$[S_A - SPC] = \frac{S_A^T K_1 [SPC]}{1 + K_1 [SPC]} \quad (14a)$$

and

$$[S_B - 4 - NP] = \frac{S_B^T K_2 [4 - NP]}{1 + K_2 [4 - NP]} \quad (14b)$$

By substituting Eqs. (14a) and (14b) into Eq. (10), the reaction rate expression becomes:

$$r = - \frac{d[4 - NP]}{dt} = k_3 \times \frac{S_A^T K_1 [SPC]}{1 + K_1 [SPC]} \times \frac{S_B^T K_2 [4 - NP]}{1 + K_2 [4 - NP]} \quad (15)$$

If  $1 \gg K_1 [SPC]$  and  $1 \gg K_2 [4 - NP]$ , Eq. (15) becomes:

$$r = k_3 S_A^T K_1 [SPC] S_B^T K_2 [4 - NP] = k_{app} [SPC][4 - NP] \quad (16)$$

where  $k_{app} = k_3 S_A^T K_1 [SPC] S_B^T K_2$ . At a constant SPC concentration and  $[SPC] \gg [4 - NP]$ , the catalytic oxidation of 4-NP follows the pseudo-first-order kinetics, as follows:

$$r = k_{obs} [4 - NP] \quad (17)$$

where  $k_{obs} = k_{app} [SPC]$ .

Note that  $k_{obs}$  is a function of the product of  $S_A$  and  $S_B$ . By expressing both sites as a function of the total surface sites,  $S_T$ , as  $\theta_A$

and  $\theta_B$ , where  $\theta_A + \theta_B = 1$ , one can obtain:

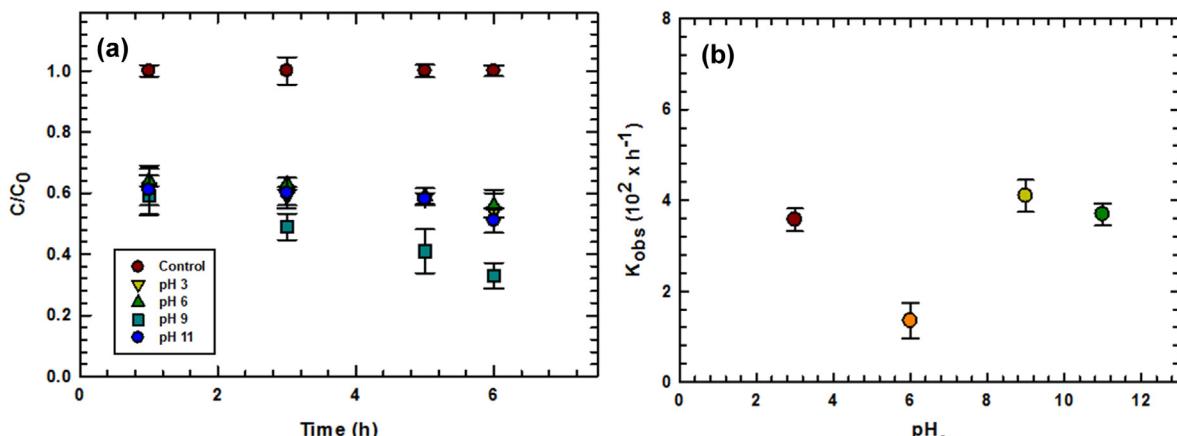
$$k_{obs} \propto S_T^2 \theta_A \theta_B = S_T^2 (1 - \theta_A) \theta_A \quad (18)$$

Eq. (18) predicts that  $k_{obs}$  as a function of RAB dosage with a maximum  $k_{obs}$  near  $\theta_A = \theta_B = 0.5$ . Therefore it is expected that the rate constant will be at the maximum when the surface site for the specific adsorption of SPC and 4-NP are equal. Fig. 4b shows that the maximum  $k_{obs}$  was at RAB dosage of  $3.0 \text{ g L}^{-1}$ , which agreed well with Eq. (18).

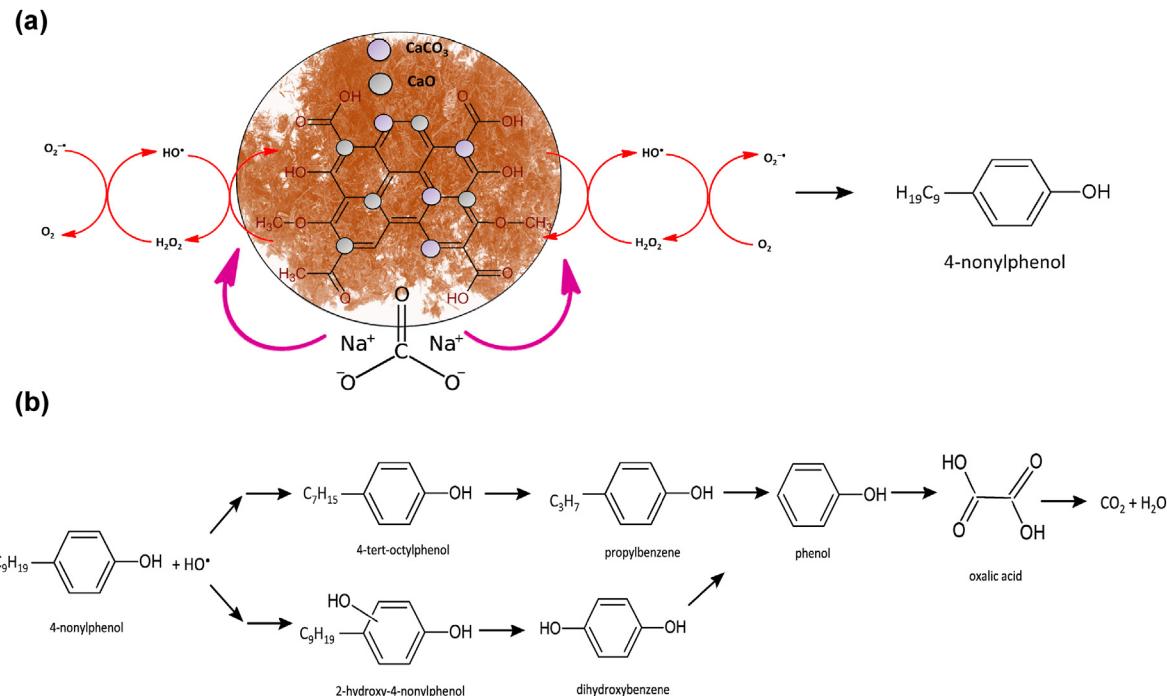
The degradation of 4-NP in the RAB/SPC system was evaluated at different initial pH value (3.0, 6.0, 9.0, and 11.0). The as well degradation percent 4-NP followed the order: pH 9.0 (67%) > pH 11.0 (49%) > pH 3.0 (46%) > pH 6.0 (44%) (Fig. 5a). SPC need to replace  $\text{H}_2\text{O}_2$  for the chemical oxidation of 4-NP in this study. SPC, having similar function as liquid  $\text{H}_2\text{O}_2$ , released free  $\text{H}_2\text{O}_2$  into the solution when SPC was in contact with water (Eq. (19a)), which initiated a series of reaction forming several reactive species (Eqs. 19b-19i). Bicarbonate is believed to be a hydroxyl radical scavenger in the aqueous phase via reactions as shown in Eqs. 19j-19k.  $\text{HCO}_4^-$  can be generated through the equilibrium reaction between  $\text{HCO}_3^-$  and  $\text{H}_2\text{O}_2$  in aqueous solution, as shown in Eq. 19l-19m (Fu et al., 2015). SPC, as a weak Brønsted base, raised the solution pH upon its introduction to the sediment matrix.  $\text{CO}_3^{2-}$  from SPC or inherently present in natural or slightly alkaline water systems could compete for  $\text{HO}^\bullet$  radicals with the organic contaminants. It has been reported that  $\text{CO}_3^{2-}$  was more stable at near-neutral pH than acidic (Cui et al., 2017). The initial solution pH in the RAB/SPC system was 9.0, therefore the amount of  $\text{CO}_3^{2-}$  in this system would be rather small. Thus, it was concluded that the effect of  $\text{CO}_3^{2-}$  on 4-NP degradation might be insignificant in the present system. Moreover, pH significantly affected the activity of SPC during the generation of ROS such as  $\cdot\text{OH}$ ,  $\text{O}_2^\bullet$ , and  $\text{HO}_2^\bullet$ , according to the following reactions (Miao et al., 2015; Lin et al., 2017).



Furthermore, more  $\text{HO}^\bullet$  would be formed due to the increases in dissolution of  $\text{Ca}^{2+}$  from the alkaline calcareous RAB, which enhanced the activation of SPC, under alkaline conditions (Granados et al., 2007). The results confirmed that alkaline conditions were more reactive than acidic conditions, which was consistent with the results of other reports on 4-NP degradation (Dong et al., 2019c). Moreover, the biochar surface had the capacity to activate SPC toward  $\text{HO}^\bullet$  generation even in the absence of  $\text{CaO}$  because of the presence of  $\text{C}-\text{OOH}$  and  $\text{C}-\text{OH}$  groups on RAB surface acting as electron shuttle to mediate electron transfer reactions between the  $\text{CaO}$  constituent on the RAB surface and target contaminants in marine sediments (Hussain et al., 2017). Further, the pH of algal biochar increased with increase in pyrolysis temperature, which increased the relative ash content in the biochar and raised the pH of biochar, especially under severe pyrolysis conditions (Yu et al., 2017). The pH value significantly affected the degradation 4-NP due to the synergistic effect exhibited by RAB and  $\text{HO}^\bullet$ . The results agreed with these reported for other pollutants studied previously (Dong et al., 2018a, 2019c; Naghipour et al., 2018). The rate constant,  $k_{obs}$ , was  $3.6 \times 10^{-2}$ ,  $1.4 \times 10^{-2}$ ,  $4.1 \times 10^{-2}$  and  $3.7 \times 10^{-2} \text{ h}^{-1}$  for pH<sub>0</sub> of 3.0, 6.0, 9.0 and 11.0, respectively (Fig. 5b). The results highlighted the crucial role of initial pH in governing the degradation efficiency and rate of 4-NP by SPC over RAB. It was noted that SPC functioned as Fenton-like chemistry over a wide pH range. Further investigation on the relationship between the physicochemical properties and stability and/or reusability of RAB, and the deactivation mechanisms of the



**Fig. 5.** (a) Effect of pH and (b) rate constant of 4-NP degradation. Experimental conditions: sediment = 1.00 g, reaction volume = 40 mL,  $T = 30^\circ\text{C}$ ,  $[\text{RAB}] = 3.0 \text{ g L}^{-1}$ ,  $[\text{SPC}] = 2 \times 10^{-4} \text{ M}$ ,  $\sum[\text{4-NP}]:[\text{SPC}]$  (molar ratio) = 1 : 10.



**Fig. 6.** (a) Proposed degradation mechanism of 4-nonylphenol (4-NP) over RAB catalyst and (b) reaction pathways of 4-NP in the sulfate and hydroxyl radical-based advanced oxidation processes.

fresh and used RAB for the degradation of 4-NP as a function of reaction time is ongoing.

### 3.3. Reaction mechanism of 4-NP degradation

The activation of SPC mediated by RAB was complex, owing to the presence of numeral radicals including HO<sup>•</sup> and O<sub>2</sub><sup>•-</sup> and that the most oxidation reaction was electrophilic addition of HO<sup>•</sup> to aromatic rings (Fu et al., 2015). The presence of Ca<sup>2+</sup> in catalyst implies the formation of oxygen vacancy, which is adsorption site for O<sub>2</sub> to form active chemisorbed oxygen over the calcium-based sorbent surface (Guo et al., 2018). Thus, further experiments must carried out to detect O<sub>2</sub><sup>•-</sup> and HO<sup>•</sup> present the solution surface analysis techniques such by electron paramagnetic resonance spectroscopy (EPR) in the future. Furthermore, a conceptual reaction scheme was proposed to describe the degradation of 4-NP in marine sediments by activation SPC over RAB (Fig. 6a). Reaction of SPC with organic compounds produced harmless compounds, viz. CO<sub>2</sub>, H<sub>2</sub>O and a small amount of CO<sub>3</sub><sup>2-</sup>, which was naturally occurring in the aquatic environment. It is generally recognized that HO<sup>•</sup> is the most active free radical in conventional Fenton system, while O<sub>2</sub><sup>•-</sup> may also contribute to the degradation of contaminant to some less extent (Lin et al., 2017). RAB activated SPC to produce HO<sup>•</sup>. The CaO/CaCO<sub>3</sub> on RAB enabled efficient electron transfer between the HO<sup>•</sup> radical and 4-NP, which further transferred electron to activate SPC and HO<sup>•</sup> production. Further, reaction between HO<sup>•</sup> and H<sub>2</sub>O formed SPC, which was strong oxidation agent. Fig. 6b shows the proposed degradation pathway of 4-NP, based on intermediates identified previously and mechanistic on the interactions between HO<sup>•</sup> and benzene rings by a series of hydroxylation of the benzene ring, cleavage of the ester bond and cleavage of one side chain (Xin et al., 2014; Xu et al., 2016). The HO<sup>•</sup> generated from the activation of SPC attacked the aromatic hydrocarbons by the electrophilic addition on the C=C double bonds of aromatic ring of 4-NP, leading to hydroxylation with the production of 4-tert-octylphenol and 2-

hydroxy-4-nonylphenol. Then 4-tert-octylphenol was attacked by radicals and decomposed to propylbenzene; dealkylation of propylbenzene led to formation of phenol. Finally, phenol was oxidized with subsequent ring-opening to oxalic acid, and then CO<sub>2</sub> and H<sub>2</sub>O. Moreover, 2-hydroxy-4-nonylphenol was attacked by radicals at its aromatic ring and alkyl chain to form dihydroxybenzene. Further attack on dihydroxybenzene by HO<sup>•</sup> formed phenol, which was oxidized to oxalic acid, and finally to CO<sub>2</sub> and H<sub>2</sub>O, a well-reported reaction mechanism stated above. Therefore, further investigation of associated reaction byproducts from RAB/SPC treatment of 4-NP should be explored in order to better understand the health risk in the future.

## 4. Conclusions

RAB was prepared from the red algae raw material for 4-NP degradation in the presence of SPC. The main active mineral phase of CaO provided sufficient catalytic sites with sufficient amount of Ca<sup>2+</sup> ions to facilitate the electron transfer reaction at the RAB surface toward catalytic 4-NP decomposition. Pseudo-first-order kinetics described well 4-NP degradation in the RAB/SPC system. The degradation of 4-NP was pH-dependent, maximum dependent rate at pH 9.0. The degradation mechanism might be dominated by the electrostatic attraction and hydrophobic interactions between 4-NP and OFGs on the RAB surface. Results demonstrated that coupling calcium with algal-derived materials can be a sustainable technology for closed-loop biomass cycling in the decomposition of 4-NP pollutants from marine sediments.

## Declaration of competing interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## CRediT authorship contribution statement

**Chang-Mao Hung:** Conceptualization, Methodology, Investigation, Validation, Formal analysis, Writing - original draft. **C.P. Huang:** Writing - review & editing, Visualization. **Shu-Ling Hsieh:** Resources. **Mei-Ling Tsai:** Resources. **Chiu-Wen Chen:** Resources. **Cheng-Di Dong:** Resources, Supervision.

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