

Effect of Metal Ions on Oxidation of Micropollutants by Ferrate(VI): Enhancing Role of Fe^{IV} Species

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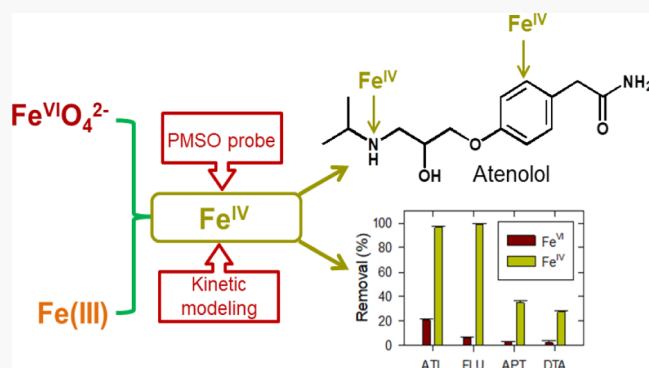


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ABSTRACT: This paper investigated the oxidation of recalcitrant micropollutants [i.e., atenolol (ATL), flumequine, aspartame, and diatrizoic acid] by combining ferrate(VI) ($\text{Fe}^{\text{VI}}\text{O}_4^{2-}$, Fe^{VI}) with a series of metal ions [i.e., Fe(III), Ca(II), Al(III), Sc(III), Co(II), and Ni(II)]. An addition of Fe(III) to Fe^{VI} enhanced the oxidation of micropollutants compared solely to Fe^{VI} . The enhanced oxidation of studied micropollutants increased with increasing $[\text{Fe}(\text{III})]/[\text{Fe}^{\text{VI}}]$ to 2.0. The complete conversion of phenyl methyl sulfoxide (PMSO), as a probe agent, to phenyl methyl sulfone (PMSO_2) by the Fe^{VI} –Fe(III) system suggested that the highly reactive intermediate Fe^{IV} / Fe^{V} species causes the increased oxidation of all four micropollutants. A kinetic modeling of the oxidation of ATL demonstrated that the major species causing the increase in ATL removal was Fe^{IV} , which had an estimated rate constant as $(6.3 \pm 0.2) \times 10^4 \text{ M}^{-1} \text{ s}^{-1}$, much higher than that of Fe^{VI} $[(5.0 \pm 0.4) \times 10^{-1} \text{ M}^{-1} \text{ s}^{-1}]$. Mechanisms of the formed oxidation products of ATL by Fe^{IV} , which included aromatic and/or benzylic oxidation, are delineated. The presence of natural organic matter significantly inhibited the removal of four pollutants by the Fe^{VI} –Fe(III) system. The enhanced effect of the Fe^{VI} –Fe(III) system was also seen in the oxidation of the micropollutants in river water and lake water.



INTRODUCTION

In the past decade, the concerns with water pollution have intensified because of an increase in consumer demand for better water quality. Micropollutants like pharmaceuticals, hormones, and personal care products are generally present in water and are potentially toxic to human health and ecosystems.¹ These micropollutants are indispensable in society, resulting in an increase in their production to several hundred million tons per year.² Researchers continue to develop new technologies to treat micropollutants in water that can be classified as biological, adsorption, membrane, and advanced oxidation processes.^{3–7} Biological treatments usually do not have the oxidizing ability to eliminate micropollutants. Adsorption and membrane processes are physicochemical methods that only transfer micropollutants from one phase to another without degrading them. Among oxidative processes, the use of iron has been regularly proposed to remediate micropollutants. Iron is one of the most abundant metals on earth and its application in treating micropollutants is attractive. The processes of iron-based materials with oxidation states ranging from 0 to +6 have been shown to eliminate micropollutants. This includes zero-valent iron [$\text{Fe}(0)$] technology, Fenton and Fenton-like reactions [e.g., $\text{Fe}(\text{II})/$

$\text{Fe}(\text{III})\text{--H}_2\text{O}_2$], and ferrate(VI) ($\text{Fe}^{\text{VI}}\text{O}_4^{2-}$ or Fe^{VI}) oxidations.^{8–12}

In recent years, research on the applications of Fe^{VI} has been increasing because of its potential in multifunctional water treatment like coagulation, oxidation, and disinfection.^{13–19} Many investigations using Fe^{VI} have been carried out to oxidize micropollutants.^{20–22} Fe^{VI} could oxidize most of the micropollutants at significant rates, but other compounds of interest have shown sluggish reactivity with Fe^{VI} resulting in a much less effective removal.²³ Recent efforts are in progress to activate Fe^{VI} to enhance elimination of recalcitrant micropollutants in water.^{17,24,25} In our laboratory, we have used reducing anions in combination with Fe^{VI} to effectively oxidize pollutants in water.²⁴ The current paper explores the combinations of Fe^{VI} –metal ions to increase the oxidizing ability of Fe^{VI} with an objective to uncover environmental-

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friendly metal ions that achieve efficient oxidation of a wide range of micropollutants.

Limited work has been performed to see the effects of metal ions on oxidation of pollutants by Fe^{VI} . The metal ions studied were only $\text{Fe}(\text{III})$, $\text{Fe}(\text{II})$, and $\text{Mn}(\text{II})$ for water remediation [e.g., removal of diclofenac (DCF)] by Fe^{VI} in water without buffering.^{26–28} An increased removal of DCF was seen when these metal ions were present in a mixed solution of Fe^{VI} –DCF. However, a later study using $\text{Fe}(\text{III})$ in borate buffer solution at pH 8.0 found no influence on the oxidation of DCF and the suggestion was made that the observed increase in oxidation of DCF in former studies was because of decrease in pH as a result of adding $\text{Fe}(\text{III})$ solution into the mixed aqueous solution of Fe^{VI} –DCF.²⁹ Fe^{VI} has shown an increase in oxidation power with a decrease in pH.¹¹ Additionally, a recent study using borate buffer at pH 8.0 reported a higher removal of sulfamethoxazole (SMX) by the Fe^{VI} – $\text{Fe}(\text{III})$ system than only Fe^{VI} .¹³ This study hypothesized the enhanced formation of Fe^{V} and Fe^{IV} by $\text{Fe}(\text{III})$ -catalyzed degradation of Fe^{VI} . The discrepancies in the observed effects of $\text{Fe}(\text{III})$ on the oxidation of the pollutants by Fe^{VI} intrigued us to examine the influence of metal ions on the oxidation of pollutants by Fe^{VI} .

The present paper studied different metal ions [i.e., $\text{Fe}(\text{III})$, $\text{Ca}(\text{II})$, $\text{Al}(\text{III})$, $\text{Sc}(\text{III})$, $\text{Co}(\text{II})$, and $\text{Ni}(\text{II})$] to learn if the type of metal ions has any role in oxidizing pollutants by Fe^{VI} . Salts of $\text{Fe}(\text{III})$ and $\text{Al}(\text{III})$ are commonly used as coagulants and may accelerate the formation of intermediate high-valent iron species from Fe^{VI} . The particles of $\text{Fe}(\text{III})$ have shown to increase the decomposition of Fe^{VI} .^{30,31} Another study has also shown that $\text{Ca}(\text{II})$ could enhance the decomposition of Fe^{VI} by water under alkaline conditions.³² The role of redox-inactive metal ions [i.e., $\text{Ca}(\text{II})$ and $\text{Sc}(\text{III})$] has been investigated in biomimetic oxidation reactions in nonaqueous environment, which showed that these metal ions modulated the reactivity of high-valent iron complexes with increase in oxidizing ability and alternation of mechanism because of the varied coordination environments around the central iron atom.^{33–35} No information of such redox-inactive metal ions on the oxidation power of high-valent iron-oxo species like Fe^{VI} under aqueous environment is currently known. Trace amounts of transition metal ions, such as $\text{Co}(\text{II})$ and $\text{Ni}(\text{II})$, could rapidly decompose Fe^{VI} in water,³⁶ which may produce large amounts of $\text{Fe}^{\text{IV}}/\text{Fe}^{\text{V}}$ species in a short time, before being converted to $\text{Fe}(\text{III})$ leading to an acceleration of oxidations by Fe^{VI} . Formation of $\text{Fe}^{\text{IV}}/\text{Fe}^{\text{V}}$ species has been seen in thermal decomposition of solid salts of Fe^{VI} at 235 °C,^{37,38} and formation of such iron intermediates may also occur under aqueous solution and room-temperature conditions. Furthermore, once the $\text{Fe}^{\text{IV}}/\text{Fe}^{\text{V}}$ species are formed, their structures and properties would vary with the cations (or metal ions) present in solution-like synthesized salts of Fe^{VI} having different metal ions.^{39–41} The current study thus investigated for the first time the varying systems of enhanced oxidation of Fe^{VI} in combination with different metal ions. We also explored whether a $\text{Fe}(\text{III})$ –TAML (TAML = tetra-amide macrocyclic ligand) complex enhances the oxidation of pollutants by Fe^{VI} because of the anticipated formation of $\text{Fe}^{\text{IV}}/\text{Fe}^{\text{V}}$ species, as previously observed in systems of $\text{Fe}(\text{III})$ –TAML with H_2O_2 and hypochlorite, which have shown high ability to oxidize micropollutants.^{42,43}

In this work, we first added $\text{Fe}(\text{III})$ to Fe^{VI} to oxidize four micropollutants [i.e., atenolol (ATL), flumequine (FLU),

aspartame (APT), and diatrizoic acid (DTA)], followed by studying other metal ion additions to the Fe^{VI} -contaminant solution. These micropollutants have varied structures and have shown sluggish reactivity with Fe^{VI} (Table S1). The molecules of these micropollutants possess moieties resilient toward oxidation such as an amide-isopropylamino alcohol, a vinylogous amide/acid, a dipeptide ester, and a bulky triiodoaromatic amide/acid, respectively. Fe^{VI} shows low reactivity with such moieties in molecules.^{20,44} Oxidation experiments using different Fe^{VI} –metal ions could establish the role of each type of metal ion in any potential increase in the removal of the pollutant. Products of the oxidation of phenyl methyl sulfoxide (PMSO) by Fe^{VI} – $\text{Fe}(\text{III})$ showed the participation of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species.¹³ A kinetic modeling of the degradation of the micropollutant was applied to clearly demonstrate that Fe^{IV} species was the dominant oxidant enhancing the oxidation ability of the Fe^{VI} – $\text{Fe}(\text{III})$ system. Oxidized products (OPs) of ATL in the Fe^{VI} – $\text{Fe}(\text{III})$ system were identified, and the proposed mechanisms of their formation in the presence of Fe^{IV} were elucidated. The relevance of the Fe^{VI} – $\text{Fe}(\text{III})$ system in treatment processes was explored by studying the influence of ions (e.g., carbonate and phosphate), pH, and natural organic matter (NOM) on pollutant removal. Finally, removal of the pollutants in surface water samples (i.e., lake water and river water) was examined in the Fe^{VI} – $\text{Fe}(\text{III})$ system.

■ EXPERIMENTAL SECTION

Chemicals and Reagents. Detailed information on the target micropollutants (i.e., ATL, FLU, APT, and DTA), Fe^{VI} solutions, preparation of all metal ions and other reaction solutions, and physicochemical characteristics of surface water samples is given in Text S1.

Removal Experiments. The removal experiments of micropollutants by Fe^{VI} –metal ion systems were conducted in triplicates in 100 mL beakers under a constant stirring rate of 400 rpm at room temperature. The reactions of micropollutants (5.0 μM) and Fe^{VI} (100.0 μM) with and without the addition of $\text{Fe}(\text{III})$ (0–200.0 μM) were initiated by mixing equal solution volumes of 10.0 mL, and the reaction mixtures were maintained at pH 9.0 using 2.0 mM borate buffer. The reaction solutions were quenched at certain reaction times (i.e., 0–20 min) completely using 20.0 μL of 1.0 M hydroxylamine solution. Samples were filtered using 0.45 μm polytetrafluoroethylene syringe filters (Fisherbrand, Fisher Scientific) and transferred into 2.0 mL high-performance liquid chromatography (HPLC) vials for analysis. Additionally, six representative metal ions/complex (i.e., Fe^{III} –TAML, $\text{Fe}(\text{III})$, $\text{Ca}(\text{II})$, $\text{Al}(\text{III})$, $\text{Sc}(\text{III})$, $\text{Co}(\text{II})$, and $\text{Ni}(\text{II})$) were also individually added into Fe^{VI} –ATL solutions to learn their effect on ATL removal. To better evaluate the remediation performance of the $\text{Fe}^{\text{VI}}/\text{Fe}(\text{III})$ system for practical applications, 5–20 mg/L of two typical NOM [i.e., Suwannee River humic acid (SRHA, 52.63% C) and Suwannee River NOM (SRNOM, 50.70% C)], which were obtained from International Humic Substances Society (St. Paul, MN), and carbonate and phosphate at 5.0 mM were individually preadded to study their possible effects. Details of removal experiments of DTA in surface water samples are provided in Text S2.

Analytical Procedures. The concentration changes of target micropollutants during Fe^{VI} –metal ion oxidations were monitored using an Ultimate 3000 ultrahigh-performance liquid chromatography (Thermo Fisher Scientific) with a UV

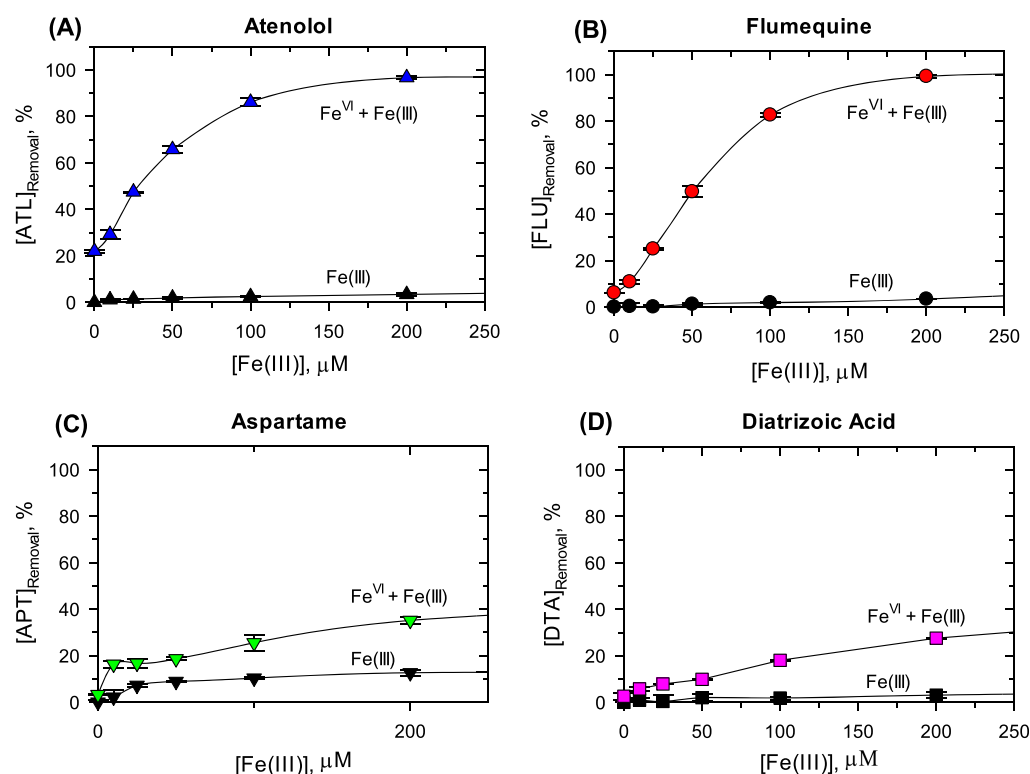


Figure 1. Effect of Fe(III) on removal of ATL, FLU, APT, and DTA by the Fe^{VI}–Fe(III) system. (Experiment conditions: [micropollutant] = 5.0 μM, [Fe(VI)] = 100.0 μM, pH 9.0 ([borate buffer] = 2.0 mM), reaction time = 10 min).

detector. Chromatographic analysis was performed on an ESTEK Ultra C₁₈ analytical column (4.6 mm × 250 mm, particle size 5 μm) at 30 °C. The mobile phase was 0.5% H₃PO₄ in ultrapure water and methanol. The other HPLC information for each micropollutant is provided in Table S1. The identification of the OPs of ATL (5.0 μM) by Fe^{VI} (100.0 μM) with and without Fe(III) at pH 9.0 was performed using the solid-phase extraction-liquid chromatography–high-resolution mass spectrometry technique. The detailed operations are described in our recent paper.¹⁶

Kinetic Modeling. Based on the proposed reactions (discussed later), Simbiology Version 5.7, a kinetic simulation package in MATLAB 2018 (The MathWorks, Inc.), was utilized to estimate the reaction rate constants via the nonlinear least-square regression method. Initially, the “Scan” task was applied to estimate the ranges of *k* for the reactions. The values of *k* were subsequently predicted, and standard errors were refined by using the “Fit Data” task through the least-square nonlinear regression with the constant error model. The confidence level and termination tolerance level on estimated coefficients were set to be default (95% and 1 × 10^{−8}) with maximum iterations to be 1000.

RESULTS AND DISCUSSION

Effect of Fe(III). Initially, we have tested the hypothesis that the addition of Fe(III) to the mixture of Fe^{VI}–micropollutant lowers the solution pH, possibly causing the enhanced oxidation of the target pollutant. As shown in Figure S1, adding small amounts of Fe(III) (0–12.0 μM) into Fe^{VI} solution without buffer (i.e., only in water) lowered the pH from 7.0 to 4.5. This suggests that the possibility of the pH lowering effect leads to an increase in the oxidation of the pollutant and that there is a possibility that the observed

enhanced effect may not be related to Fe(III) chemistry in the mixture of the Fe^{VI}–micropollutant. To address this potential interference, we explored the specific role of Fe(III) by carrying out the experiments using 2.0 mM borate buffer, which maintained the pH at 9.0 with an increase in concentrations of Fe(III) in the mixed solutions of Fe^{VI}–pollutants. Results showed increased removal of pollutants with Fe(III) additions at pH 9.0 (i.e., without effects of lowering of pH) (Figure 1). This indicated the role of Fe(III) in enhancing the oxidation of pollutants by Fe^{VI}.

Of the four tested pollutants, ATL and FLU showed complete removal (≈100%) with increasing Fe(III) dosages (Figure 1a,b), while APT and DTA had maximum removal up to 35% (Figure 1c,d). Comparatively, no significant removal of pollutants was observed in the exclusive presence of Fe(III) (i.e., without any Fe^{VI}). It appears that the molar ratio of ≈2.0 ([Fe(III)]/[Fe^{VI}]) was sufficient to obtain the maximum removal of the pollutants by the Fe^{VI}–Fe(III) system. Furthermore, a molar ratio of Fe(III) to Fe^{VI} has a critical role in determining the enhancing effect of added Fe(III) to the mixture of the Fe^{VI}–pollutant. A study that showed no effect of Fe(III) to oxidize DCF by Fe^{VI} may be related to the use of the much lower molar ratios of Fe(III) to Fe^{VI} (i.e., 0.02–0.10) in the experiments.²⁹ Results of Figure 1 indicate that the oxidizing species generated from Fe^{VI} by Fe(III) are largely responsible for enhancing the removal of pollutants. These oxidizing species may be the intermediate Fe^V/Fe^{IV} species, produced from the decay of Fe^{VI}, which may be catalyzed by Fe(III) at pH 9.0. These intermediate species are much more reactive than Fe^{VI}. This is in agreement with recent results on the oxidation of SMX by the Fe^{VI}–Fe(III) system in borate buffer.¹³ More will be discussed later in the kinetic

modeling interpretation of the enhanced effect of Fe(III) on the oxidation of pollutants by Fe^{VI} .

The results of Figure 1 indicated that the magnitude of the enhanced effect of Fe(III) depended on the type of pollutant. An attempt was made to understand this trend by determining the second-order rate constants of the reaction between Fe^{VI} and pollutants that initially formed the $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species. The obtained rate constants between Fe^{VI} and ATL, FLU, APT, and DTA in 2.0 mM borate buffer at pH 9.0 were $(5.0 \pm 0.4) \times 10^{-1}$, $(3.4 \pm 0.1) \times 10^{-1}$, $(8.2 \pm 1.0) \times 10^{-1}$, and $(5.3 \pm 0.1) \times 10^{-1} \text{ M}^{-1} \text{ s}^{-1}$, respectively. The order of reactivity of Fe^{VI} with the pollutants differed from the trend of removal, as seen in Figure 1, indicating that the nature and reactivity of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species, produced in the Fe^{VI} –Fe(III)–pollutant system, varied with the structure of the pollutant to result in different removal efficiencies by the Fe^{VI} –Fe(III) system.¹² Furthermore, the competitive reactions including self-decomposition of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ and the reactions of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ with pollutants would determine the overall trend of removal of target compound by the Fe^{VI} –Fe(III) system.

Effect of Fe(III)–TAML. In this study, we also tested the possible role of Fe^{IV} –TAML/ Fe^{V} –TAML that may be generated from the reaction of Fe^{VI} and Fe(III)–TAML. The reaction between Fe^{III} –TAML and H_2O_2 in alkaline medium has shown the production of high-valent iron species, complexed with the TAML ligand, to cause the rapid removal of pollutants.^{42,45} In our investigation, we first mixed Fe^{VI} with ATL at pH 9.0 in borate buffer, followed by fast addition of Fe^{III} –TAML. The color of Fe^{VI} instantaneously disappeared. The observed results at a varied amount of Fe^{III} –TAML in mixed solutions are presented in Figure 2A. No enhanced effect on the removal of ATL because of the addition of Fe^{III} –TAML to Fe^{VI} –ATL mixture was seen. At higher concentrations of Fe(III)–TAML, the removal of ATL was lower than when there was no addition of Fe(III)–TAML (Figure 2A). It seems that Fe^{VI} reacted with Fe^{III} –TAML or only TAML, but neither of the reaction resulted in the desired oxidizing species necessary to remove ATL. The results of Figure 2A indicated no role of high-valent intermediate species under our experimental conditions.

Effect of Other Metal Ions. Initially, the effect of $\text{Ca}(\text{II})$ on the removal of ATL by Fe^{VI} was explored. The results of the effects of increasing amounts of $\text{Ca}(\text{II})$, up to 2000 μM , are shown in Figure 2B. The presence of $\text{Ca}(\text{II})$ increased the decay of Fe^{VI} ;⁵⁶ however, no enhancement in ATL removal was observed. It appears that the possible $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species in the system of Fe^{VI} –ATL– $\text{Ca}(\text{II})$ are unable to contribute to the oxidation of ATL. There is a possibility that $\text{Ca}(\text{II})$ also destabilizes the $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species (or increases their self-decays), thereby minimizing their oxidation reaction time with ATL. This is supported by the known instability of the calcium salt of Fe^{VI} (CaFeO_4) in the presence of Fe(III).⁴⁶ Similar to $\text{Ca}(\text{II})$, Al(III) and Sc(III) have no enhancement effect in the removal of ATL by Fe^{VI} (Figure 2C).

Next, the effect of Co(II) on the removal of ATL by Fe^{VI} was tested (Figure 2C). Co(II) has shown an increase in the decay of Fe^{VI} ³⁶ and could produce the intermediate $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species to potentially enhance the removal of ATL. However, the results showed no enhancement by Co(II), similar to Al(III) and Sc(III) under the same conditions. Comparatively, Ni(II) showed enhanced removal of ATL by Fe^{VI} (Figure 2C), although Ni(II) has shown high influence to destabilize the Fe^{VI} even in trace amounts in solution.³⁶ This suggested that

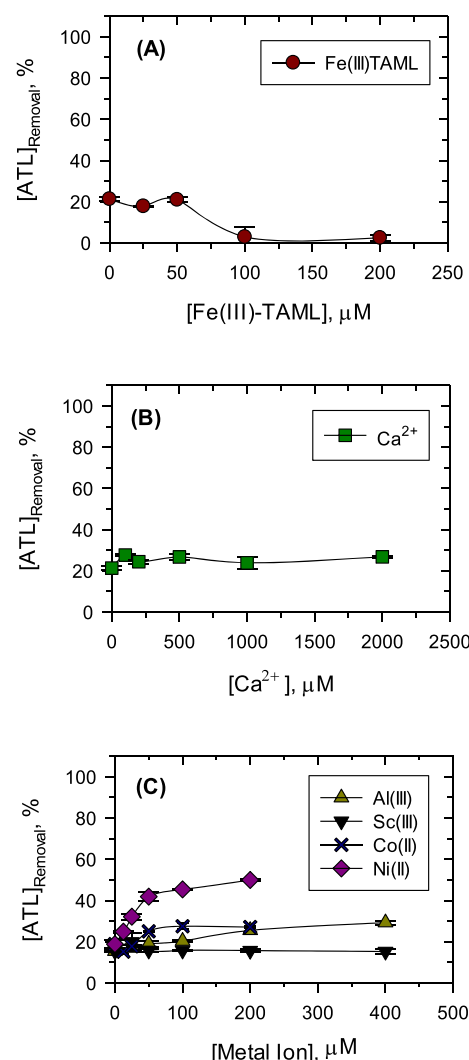


Figure 2. Effect of Fe(III)–TAML and metal ions on degradation of ATL at pH 9.0. (A) Fe(III)–TAML, (B) Ca^{2+} ions, (C) Al(III), Sc(III), Co(II), and Ni(II). (Experiments conditions: $[\text{ATL}] = 5.0 \mu\text{M}$, $[\text{Fe}^{\text{VI}}] = 100.0 \mu\text{M}$, $[\text{borate buffer}] = 2.0 \text{ mM}$, and reaction time = 10 min).

the influence of different metal ions on enhancing pollutant removal is largely determined by the competing rate constants of the self-decay of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ in the presence of metal ions and the reaction of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ with the pollutant.

In further studies of the mechanism and products by the Fe^{VI} –metal ion system, we focused on the Fe(III)–enhanced oxidation of ATL by Fe^{VI} . The Fe^{VI} –Fe(III) system is relatively cleaner and nontoxic⁴⁷ and presents a real possibility for use in remediating pollutants in water.

Mechanisms. Initially, the role of $\text{Fe}^{\text{V}}/\text{Fe}^{\text{IV}}$ species in the oxidation of pollutants by the Fe^{VI} –Fe(III) system was investigated by oxidizing PMSO as a probing compound. High-valent iron species could selectively oxidize PMSO to PMSO_2 .^{13,25} $\text{Fe}^{\text{IV}}/\text{Fe}^{\text{V}}$ species have a much higher reactivity with pollutants than Fe^{VI} does,^{48,49} and therefore, the comparative formation rate of PMSO_2 would demonstrate the formation of $\text{Fe}^{\text{IV}}/\text{Fe}^{\text{V}}$ species in the Fe^{VI} –Fe(III) system. In our experiments, the Fe^{VI} solutions were first mixed with PMSO, followed by the addition of Fe(III) at varying concentrations. The formation of PMSO_2 was seen in 10 min. The conversion of PMSO to PMSO_2 was $\approx 10\%$ by Fe^{VI}

only. However, this conversion increased when Fe(III) was added into Fe^{VI} and became stoichiometric (Figure S2). This suggested that Fe^V/Fe^{IV} species were responsible for enhancing the removal of pollutants by the Fe^{VI}–Fe(III) system (see Figure 1).

A direct evidence of the formation of Fe^{IV}/Fe^V species in the oxidation of pollutants by Fe^{VI} under our experimental conditions was not possible because the formed Fe^{IV}/Fe^V species were short-lived with half-lives ranging from <1 ms to μ s and would also be in low amounts.^{50,51} The use of stopped-flow kinetic trace experiments to characterize Fe^{IV}/Fe^V species spectroscopically⁴⁹ is unsuccessful. This is not surprising because the literature available on the Fe^{IV}/Fe^V–organic complexes under nonaqueous acetonitrile environment suggested their high instability and could be studied only at below freezing temperatures (e.g., $-40\text{ }^{\circ}\text{C}$).^{52,53} Low concentrations of these steady-state high-valent iron intermediates suggested that conventional Mossbauer spectroscopic techniques,⁵⁴ commonly used to identify iron species, will not be appropriate. Overall, the technique to identify directly Fe^{IV}/Fe^V species in the Fe^{VI}–micropollutant systems under aqueous solutions remains elusive. However, the investigation of decomposition of solid Fe^{VI} using Mossbauer spectroscopy has shown Fe^{IV} as the intermediate species.^{37,55} We have therefore applied a kinetic modeling approach to assess which of the two species, that is, Fe^V and Fe^{IV}, caused the enhancement.

Kinetic Modeling. The experimental data on the degradation kinetics of ATL by the Fe^{VI}–Fe(III) system were collected at different concentrations of Fe(III) at pH 9.0 to facilitate developing a kinetic model. The results, as shown in Figure 3, were interpreted using the reactions in Table

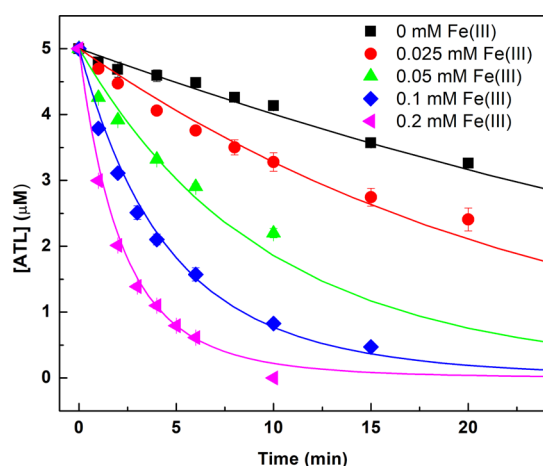


Figure 3. Removal of ATL by the Fe(VI)/Fe(III) system at pH 9.0. (Experimental conditions: [ATL] = $5.0\text{ }\mu\text{M}$, [Fe(VI)] = $100.0\text{ }\mu\text{M}$, [borate buffer] = 2.0 mM , and $n = 2$). Solid lines represent the kinetic modeling.

1.^{50,51,56–61} Reactions 1–10 represent the self-decay of Fe^{VI} by water under alkaline conditions.⁶² These reactions involve Fe^V/Fe^{IV} species and describe the unimolecular decay of Fe^{VI} at pH 9.0 successfully in our previous study.⁶² In the presence of Fe(III), additional reaction with Fe(III) occurs and may be one of the six possible reactions 11a–11f. Equation 11a is the reaction between Fe^{VI} and Fe(III) ion to give Fe^{IV} species. In reaction 11a, it is assumed that the added Fe(III) ion behaves the same as the Fe(III) generated in situ from the Fe^{VI}

reduction (i.e., self-decay of Fe^{VI} by water), and Fe^{VI} is proposed to react with the total amount of these two types of Fe(III). Equations 11b–11f are the reactions between Fe^{VI} and the added Fe(III) ion only [i.e., the Fe^{VI} reacts much more slowly with Fe(III) formed from Fe^{VI} self-decomposition]. Equations 11b and 11c are the proposed reactions between Fe^{VI} and Fe(III) to generate monomeric Fe^{IV} (Fe^{IV}O₃^{2–}) and dimerized Fe^{IV} (Fe₂^{IV}O₆^{4–}) species, respectively. Equation 11d represents the proposed reaction between Fe^{VI} and Fe(III) ions to produce Fe^V. The subsequent reaction of Fe^V with Fe(III) would also generate Fe^{IV} (eq 11e). The reaction of Fe^{VI} with Fe(III) may also form equal proportions of Fe^V and Fe^{IV} at the same time (eq 11f). The results of the decay of Fe^{VI}, as shown in Figure S3, were fitted by applying all reactions from 1 to 10 plus one of the possibilities for reaction 11 in the kinetic modelling.

Of the six possible scenarios (i.e., eqs 11a–f), the best fit of the experimental data in Figure S3 was seen using eq 11b (solid lines of Figures S3 and S4). This indicated that in the Fe^{VI}–Fe(III) system, Fe^{VI} reacted primarily with the added Fe(III) that generated monomeric Fe^{IV} species. This is consistent with a previously reported study on the enhanced decay of Fe^{VI} by freshly added Fe(III) ion.³¹ The obtained rate constant for reaction 11b (k_{11b}) from the kinetic modelling was $(2.7 \pm 0.9) \times 10^4\text{ M}^{-2}\text{ s}^{-1}$, which could successfully simulate the Fe^{VI} self-decay at different levels of Fe(III) in the Fe^{VI}–Fe(III) system. The kinetic modeling also revealed that the reaction rate constant between Fe^{VI} and the generated Fe(III) from self-decay of Fe^{VI} by water must be lower than $1 \times 10^2\text{ M}^{-2}\text{ s}^{-1}$ in order to conform with the observed Fe^{VI} decay and H₂O₂ generation (Figure S5). This further confirms that Fe^{VI} is inherently more reactive toward the added Fe(III) ion compared to produced Fe(III) from the reaction of Fe^{VI} with H₂O. In other words, the reaction of Fe^{VI} with in situ Fe(III) is not significant in the Fe^{VI}–Fe(III) system.

The kinetic modeling of the results demonstrated that the oxidant species to cause enhancement is most likely Fe^{IV} species, which is produced from the reaction of added Fe(III) with Fe^{VI}. Significantly, the evolution profile of the other possible oxidant species, Fe^V, in the Fe^{VI}–Fe(III) system was found to be 2 orders of magnitude lower in concentration compared to that of Fe^{IV} species (see Figure S6). This again supported that Fe^V was a less important oxidant to promote the degradation of substrates in the Fe^{VI}–Fe(III) system, unless Fe^V reactivity toward the substrate was at least 2 orders of magnitude higher than its Fe^{IV} counterpart. Currently, the reactivity trend of Fe^{IV} and Fe^V is scarce in the literature and is limited to cyanide at pH ≥ 10.5 only.^{63,64}

Finally, reactions of Fe^{VI} and Fe^{IV} with ATL (reactions 12 and 13) were added into the kinetic model (Table 1) to predict the results of Figure 3. In the kinetic simulations, the derived k_{12} and k_{13} values could successfully predict the degradation of ATL at varied concentrations of Fe(III) (see the solid lines of Figures 3 and S7). The strong agreement between the model and multiple sets of experimental data supports the reactions used in modeling the Fe^{VI}–Fe(III)–ATL system to be plausible and that Fe^{IV} is the oxidative species to cause the enhanced oxidation of ATL. Additional support could also be seen in the estimated rate constant for the reaction between Fe^{IV} and ATL ($k(\text{Fe}^{\text{IV}} + \text{ATL})$) as $(6.3 \pm 0.2) \times 10^4\text{ M}^{-1}\text{ s}^{-1}$, which is much higher than the rate constant for the oxidation of ATL by Fe^{VI} ($k(\text{Fe}^{\text{VI}} + \text{ATL}) = (5.0 \pm 0.4) \times 10^{-1}\text{ M}^{-1}\text{ s}^{-1}$) (Table 1). The derived rate

Table 1. Possible Reactions in the Fe^{VI}–Fe(III)–ATL System at pH 9.0^a

reactions	k at pH 9.0	references
[1] Fe ^{VI} O ₄ ^{2−} + H ₂ O → Fe ^{IV} O ₃ ^{2−} + H ₂ O ₂	(2.0 ± 0.1) × 10 ^{−5} s ^{−1}	estimated in the Fe(VI) decay system
[2] Fe ^{VI} O ₄ ^{2−} + H ₂ O ₂ → Fe ^{IV} O ₃ ^{2−} + O ₂ + H ₂ O	~0 M ^{−1} s ^{−1}	56
[3] Fe ^{IV} O ₃ ^{2−} + Fe ^{IV} O ₃ ^{2−} → Fe ₂ ^{IV} O ₆ ^{4−}	~10 ⁷ M ^{−1} s ^{−1}	51
[4] Fe ₂ ^{IV} O ₆ ^{4−} + 4H ₂ O + 4H ⁺ → 2Fe ^{III} (OH) ₃ (H ₂ O) + H ₂ O ₂	10 ² s ^{−1}	51
[5] Fe ^{IV} O ₃ ^{2−} + H ₂ O ₂ + 2H ⁺ → Fe ^{II} (OH) ₂ (aq) + O ₂ + 2H ₂ O	3.0 × 10 ³ M ^{−1} s ^{−1}	51,57
[6] Fe ^{IV} O ₃ ^{2−} + Fe ^{II} (OH) ₂ (aq) + 3 H ₂ O → 2Fe ^{III} (OH) ₃ (aq) + 2OH [−]	~10 ⁶ M ^{−1} s ^{−1}	51
[7] Fe ^{VI} O ₄ ^{2−} + Fe ^{II} (OH) ₂ (aq) + H ₂ O → HFe ^V O ₄ ^{2−} + Fe ^{III} (OH) ₃ (aq)	~10 ⁵ M ^{−1} s ^{−1}	58,59
[8] Fe ^{II} (OH) ₂ (aq) + H ₂ O ₂ + 2OH [−] → Fe ^{IV} O ₃ ^{2−} + 3H ₂ O	~10 ³ M ^{−1} s ^{−1}	60
[9a] HFe ^V O ₄ ^{2−} + 2H ⁺ + 4H ₂ O → Fe ^{III} (OH) ₃ (H ₂ O) ₃ + H ₂ O ₂	5.0 s ^{−1}	50
[9b] HFe ^V O ₄ ^{2−} + HFe ^V O ₄ ^{2−} + 4H ₂ O + 4H ⁺ → 2Fe ^{III} (OH) ₃ (H ₂ O) + 2H ₂ O ₂	1.5 × 10 ⁷ M ^{−1} s ^{−1}	61
[10] HFe ^V O ₄ ^{2−} + H ₂ O ₂ + H ₂ O → Fe ^{III} (OH) ₃ (aq) + O ₂ + 2OH [−]	4.0 × 10 ⁵ M ^{−1} s ^{−1}	56
[11a] Fe ^{VI} O ₄ ^{2−} + 2Fe ^{III} (OH) ₃ (aq) [generated from eqs 1–10 and newly added Fe(III) salts] + 4OH [−] → 3Fe ^{IV} O ₃ ^{2−} + 5H ₂ O	n.d.	evaluated in the Fe(VI)–Fe(III) system
[11b] Fe ^{VI} O ₄ ^{2−} + 2Fe ^{III} (OH) ₃ [newly added Fe(III) salts] + 10OH [−] → 3Fe ^{IV} O ₃ ^{2−} + 5H ₂ O	(2.7 ± 0.9) × 10 ⁴ M ^{−2} s ^{−1}	estimated in the Fe(VI)–Fe(III) system
[11c] Fe ^{VI} O ₄ ^{2−} + 2Fe ^{III} (OH) ₃ (aq) [newly added Fe(III) salts] + 4OH [−] → 1.5Fe ₂ ^{IV} O ₆ ^{4−} + 5H ₂ O	n.d.	evaluated in the Fe(VI)–Fe(III) system
[11d] 2Fe ^{VI} O ₄ ^{2−} + Fe ^{III} (OH) ₃ (aq) [newly added Fe(III) salts] + 2OH [−] → 3HFe ^V O ₄ ^{2−} + H ₂ O	n.d.	evaluated in the Fe(VI)–Fe(III) system
[11e] HFe ^V O ₄ ^{2−} + Fe ^{III} (OH) ₃ (aq) [newly added Fe(III) salts] + 2OH [−] → 2Fe ^{IV} O ₃ ^{2−} + 3H ₂ O	n.d.	evaluated in the Fe(VI)–Fe(III) system
[11f] Fe ^{VI} O ₄ ^{2−} + Fe ^{III} (OH) ₃ (aq) [newly added Fe(III) salts] + 2OH [−] → Fe ^{IV} O ₃ ^{2−} + HFe ^V O ₄ ^{2−} + 2H ₂ O	n.d.	evaluated in the Fe(VI)–Fe(III) system
[12] Fe ^{VI} O ₄ ^{2−} + ATL → Fe ^{III} (OH) ₃ + P ₁	(5.0 ± 0.4) × 10 ^{−1} M ^{−1} s ^{−1}	estimated in the Fe(VI)–Fe(III)–ATL system
[13] Fe ^{IV} O ₃ ^{2−} + ATL → Fe ^{III} (OH) ₃ + P ₂	(6.3 ± 0.2) × 10 ⁴ M ^{−1} s ^{−1}	estimated in the Fe(VI)–Fe(III)–ATL system

^a(1) Fe^{IV}O₃^{2−} is the proposed chemical formula of Fe^{IV}, and reactions 3–6 and 8 from the previous studies are modified in this study. (2) The contribution of HFe^VO₄^{2−} was not shown for simplicity as it only accounted for less than 2% of the concentration of Fe^{VI} at pH 9.0. (3) In eqs. 11b–11f, Fe^{III}(OH)₃(aq) was denoted for the added ferric ions, which are not considered as the same Fe(III) species generated from eqs 1–10 in terms of catalytic capability. (4) n.d. = not determined because of unlikelihood of the reaction.

constant of Fe^{IV} with ATL is consistent with the range of rate constants of the Fe^{IV}–pyrophosphate complex with different inorganic molecules at pH 10.0 reported by an earlier study using the pulse radiolysis stopped flow experiments.⁵¹ Compared to the specialized pulse radiolysis techniques, the kinetic modeling approach of our study provides a simple strategy to estimate the rate constants of Fe^{IV} species with micropollutants in water.

OPs of ATL by Fe^{IV}. In this study, the high-resolution liquid chromatography–mass spectrometry (LC–MS) technique was used for structural identification of OPs of ATL by Fe^{VI} with the addition of Fe(III). The high accuracy of this analytical technique for the determination of *m/z* values of unknown OPs gives their molecular composition with small mass errors (<1.5 ppm) (Table S2). A total of nine OPs of ATL were identified based on their significantly increased peak areas as compared to the control sample (i.e., ATL without treatment). They are named as OP-282, OP-240, OP-238, OP-224, OP-222, OP-209, OP-193, OP-167, and OP-151, reflective of their approximate *m/z* value. The detailed information of their MS/MS fragments (Figure S8) facilitated the understanding of the fragmentation patterns of each OP, which provided more structural features. It is noteworthy that some OPs had low MS intensity, and no MS/MS data were therefore available. Together with the reaction pathways of ATL by some other oxidation systems, the molecular structures of all nine OPs of ATL were proposed for the Fe^{VI}–Fe(III) system. Additionally, the OPs of ATL by Fe^{VI} only were also investigated in our study, from which the same OPs were observed, based on the LC–MS analysis.

The possible degradation pathways of ATL by Fe^{VI}–Fe(III) system are presented in Figure 4. As can be noted, two pathways share the following types of oxidative transformations: (1) elimination of the isopropyl group, (2) oxidation of the secondary alcohol, (3) cleavage of the aryl ether, and (4) aromatic and/or benzylic oxidation. Pathway I depicts the first three mentioned transformations, while pathway II is different in that it is preceded by an oxygen addition to ATL, either via aromatic oxidation or benzylic oxidation. Pathway I initiates the oxidative degradation on the secondary amine moiety of ATL, which has been experimentally demonstrated as the reactive site for oxidation.⁶⁵ It has been extensively shown that Fe^{IV} is the operative high valence form of iron that can hydroxylate nonactivated C–H bonds, in both heme-type complexes (e.g., cytochrome P450)⁶⁶ as well as nonheme iron-based enzymes.⁶⁷ While in most of these cases, Fe(II) gets oxidized to Fe(III) in the presence of oxygen gas, followed by the O–O cleavage resulting in subsequent oxidation of Fe(III) to Fe^{IV}; the generation of Fe(IV) in our experiments is a result of the cooperative effect of the Fe^{VI}–Fe(III) combination. Some studies have reflected that the oxidation imposed by Fe^{VI}=O in the hydrogen abstraction of C–H bonds occurs via the diradical character of Fe(III)–O•, also referred to as the oxyl route by which the oxidation is occurring via the oxygen rather than Fe^{IV}.⁶⁸ In some regards, the Fe^{IV} in HFe^VO₃^{2−} receives an electron from the noninnocent oxo ligand, rendering it to be an oxidative radical species. Regardless of which route leads to hydroxylation, the capability of Fe^{IV}=O to initiate a hydrogen abstraction in the hydroxylation, via Fe(III)–OH intermediate,

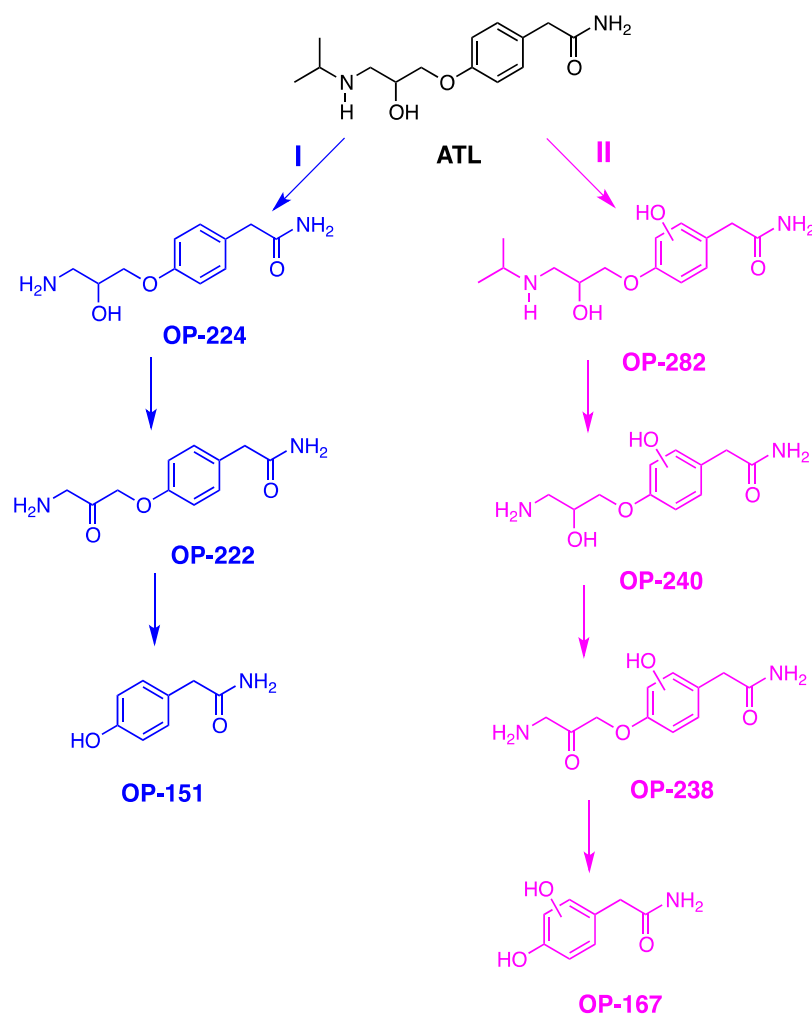


Figure 4. Proposed reaction pathways on the degradation of ATL by the $\text{Fe}^{\text{VI}}\text{--Fe(III)}$ system at pH 9.0. (Experiment conditions: $[\text{ATL}] = 5.0 \mu\text{M}$, $[\text{Fe(VI)}] = 100.0 \mu\text{M}$, $[\text{borate buffer}] = 2.0 \text{ mM}$, and reaction time = 10 min).

is well studied and generally the accepted mechanism.⁶⁹ Enzymatic hydroxylations have the advantage of precise regiocontrol, in part because of their strong binding to their substrate positioning the site of oxidation at proximity to the active site where the iron-oxo of Fe^{IV} resides. Our oxidative pathways do not have such selective regiocontrol, and therefore, the high-valence iron species attacks the most susceptible sites during oxidation.

ATL has four susceptible C–H sites that could lead to stabilized carbon radicals upon hydrogen abstraction by the highly reactive $\text{Fe}^{\text{IV}}\text{=O}$ species. The order of oxidation cannot be easily predicted and may in fact vary as reflected in the two pathways presented in Figure 4. Pathway I shows the abstraction of the secondary C–H of the isopropyl amine group. The detailed mechanism, as shown in Figure 5A, shows an N-stabilized radical, which subsequently receives the local “hydroxyl” radical from $\text{Fe(III)}\text{--OH}$ leading to the unstable aminoalcohol and an Fe(II) species, which will rapidly oxidize to Fe(III) under the highly oxidative conditions of any of the high valence Fe species (i.e., Fe^{IV} , Fe^{V} , or Fe^{VI}). The aminoalcohol readily loses an acetone molecule, releasing the primary amine OP-224. Subsequent oxidation of the hydroxyl group of OP-224 takes place to form OP-222 initiated by a similar C–H abstraction of the alcohol carbon. The detailed mechanism is shown in Figure 5B, in which the corresponding

hydroxylation leads to a gem-diol, which readily loses a water molecule to form OP-222. The cleavage of the phenoxyether evidenced by the observed products in the MS spectrum (Figure S8) occurs via a similar Fe^{IV} C–H abstraction of the α -carbon to both the carbonyl and the phenoxy oxygen. This formed radical (Figure 5C) is stabilized by the carbonyl as well as the oxygen. Subsequent hydroxylation at that position leads to an unstable intermediate that releases the phenol group, OP-151.

Pathway II was initiated by electrophilic attack of Fe^{IV} on the aromatic ring, which can lead to aromatic oxidation, as shown in Figure 5D(a). Similar aromatic oxidations have previously been reported by high-valent metal-oxo species, for example, Fe^{VI} ,²¹ Fe^{V} , and Fe^{IV} .⁷⁰ Alternatively and not possible to rule out using MS data, Fe^{IV} could abstract a hydrogen at the benzylic C–H, resulting in the formation of a hydroxylated ATL (having the same mass to the phenolic product, i.e., both OP-282), as shown in Figure 1D(b). The generation of two initial OPs of ATL, that is, OP-224 and OP-282, was also reported during oxidation of ATL by Fe^{VI} .⁶⁵ Similar to the transformation patterns of ATL in pathway I, OP-282 was sequentially oxidized leading to the formation of OP-240, OP-238, OP-209, and OP-167.

Environmental Relevance. It is well known that water constituents existing in natural waters could affect the removal

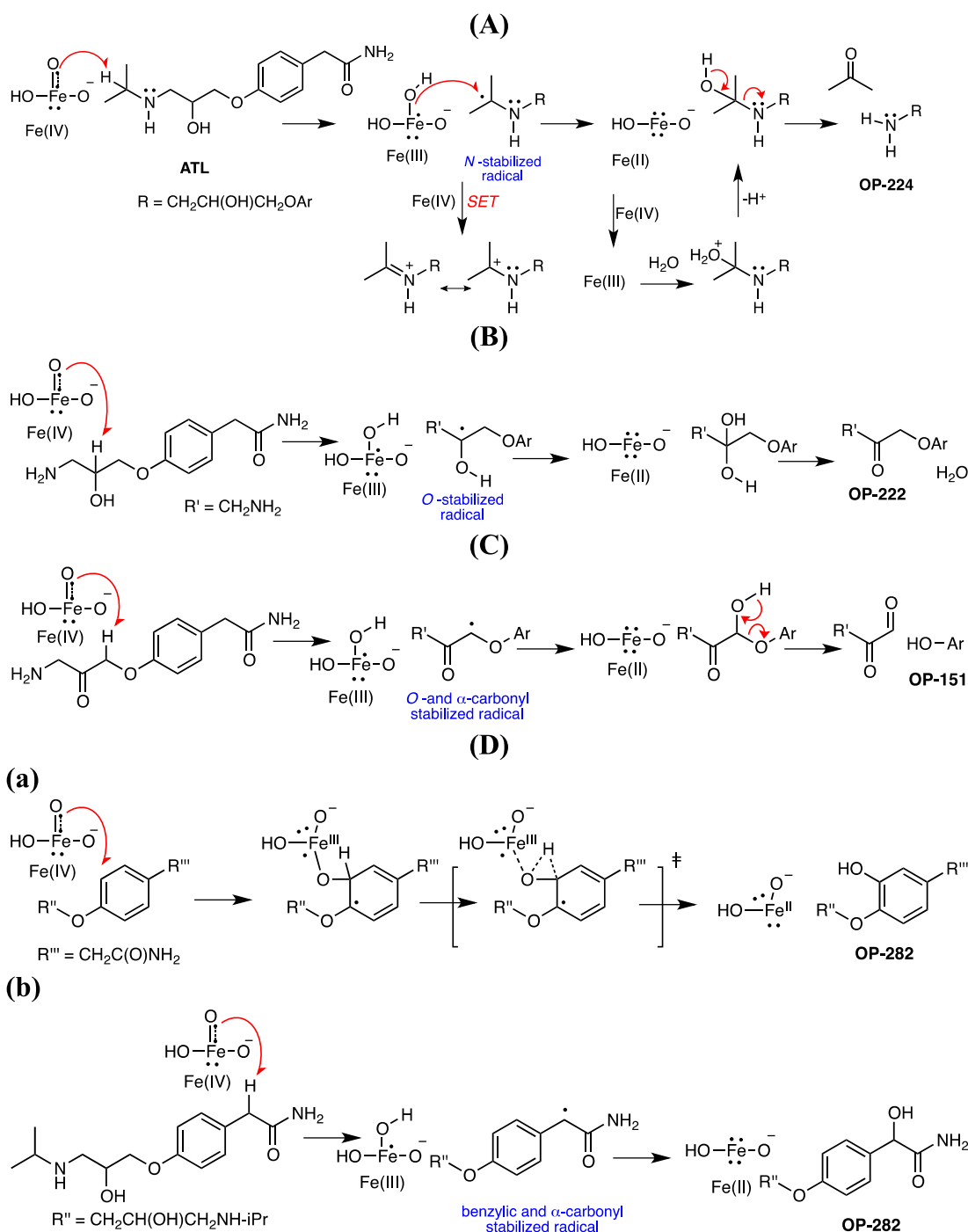


Figure 5. Proposed mechanism by Fe(IV) (A) de-isopropylation of ATL. The lower suggested route is plausible but less probable. The resultant Fe(II) will immediately oxidize back to Fe(III) under the highly oxidative conditions; (B) oxidation of the secondary alcohol via Fe(IV); (C) aryl ether cleavage under Fe(IV); and (D) (a) Fe(IV) electrophilic attack directly on the aromatic ring leading to phenol formation; (b) alternative pathway of benzylic hydroxylation that would lead to oxygen addition to ATL forming an isomer of OP-282 with an identical mass.

efficiency of micropollutants by treatment technologies. In this study, initially, the effect of carbonate and phosphate on the removal of DTA, which is a more recalcitrant pollutant than ATL, was studied independently. When 5.0 mM carbonate was present in solution at pH 9.0, removal of DTA was similar to that without carbonate ($16.2 \pm 2.2\%$ vs $19.7 \pm 1.9\%$). However, the presence of 5.0 mM phosphate lowered the removal of DTA to $5.5 \pm 0.5\%$. The decrease by phosphate ion agrees with previous studies.^{17,29} Next, the effect of SRHA and SRNOM, two representative NOM, was studied for the Fe^{VI}–

Fe(III) system. As shown in Figure S9, the significant inhibitory effect of SRHA and SRNOM (5–20 mg/L) on the elimination of all four selected micropollutants (i.e., ATL, FLU, APT, and DTA) by the Fe^{VI}–Fe(III) system was observed following the increased addition of NOM. In the case of ATL and FLU, the decrease in removal was from 100 to $\approx 20\%$ when the level of NOM and HA increased to 20 mg/L. Under the same conditions, the decrease in removals of APT and DTA was from ≈ 25 to $\approx 10\%$. Generally, no difference in the removal of the micropollutants when adding either

SRNOM or SRHA was found within experimental errors. It has been documented that the competitive consumption of NOM with reactive oxidizing species (e.g., hydroxyl radicals, sulfate radicals, and Fe^{VI}) greatly diminished the remediation performance of water contaminants.^{16,71,72} Similarly, our results may be attributed to the oxidation of NOM by Fe^{IV} , resulting in a lesser amount of Fe^{IV} available for pollutant decomposition.

Finally, the removal of DTA was sought in surface waters (i.e., river water and lake water) by the Fe^{VI} – $\text{Fe}(\text{III})$ system (see Figure 1). First, we found that DTA can be completely eliminated at pH 8.0 after 10 min of oxidation by using increasing doses of Fe^{VI} ($>200.0\ \mu\text{M}$) while maintaining the molar ratio of Fe^{VI} to $\text{Fe}(\text{III})$ as 0.5 (Figure S10). For the surface waters spiked with $5.0\ \mu\text{M}$ DTA, some higher amounts of Fe^{VI} (i.e., $>400.0\ \mu\text{M}$) and $\text{Fe}(\text{III})$ were needed for the complete removal of DTA (Figure S11). In summary, the magnitude of pollutant removal in surface waters will depend on the pH, ions, and the levels and types of NOM. The moieties of pollutants and NOM will also be the factors that influence the degradation of target compounds in water. Some moieties of NOM have acid–base equilibrium (e.g., phenolic),⁷³ and therefore, the reactivity of NOM with Fe^{VI} / Fe^{IV} would vary with pH. The optimization of solution pH, Fe^{VI} concentration, and molar ratio of Fe^{VI} to $\text{Fe}(\text{III})$ may be required to obtain efficient removal of target pollutants in water.

Overall, the findings of our study suggest an important role of $\text{Fe}(\text{III})$ to remove micropollutants in water by Fe^{VI} through generation of relatively high amounts of Fe^{IV} species in a short time. The produced amount of Fe^{IV} can be increased proportionally to the addition of $\text{Fe}(\text{III})$ into Fe^{VI} in water. In other words, lower Fe^{VI} and higher $\text{Fe}(\text{III})$ would give the adequate concentrations of Fe^{IV} species necessary to remove micropollutants rapidly by the Fe^{VI} – $\text{Fe}(\text{III})$ system. Because the cost of $\text{Fe}(\text{III})$ salts is much less than that of the relatively expensive Fe^{VI} solution, the combination of Fe^{VI} and $\text{Fe}(\text{III})$ would make a big stride in the practical use of Fe^{VI} in treatment processes. Furthermore, the applied $\text{Fe}(\text{III})$ in treatment plants is in liquid form, which is acidic. Independent studies have shown that small addition of acids also enhanced the oxidation of micropollutants by Fe^{VI} without greatly affecting the pH of the treated water at nearly neutral conditions.⁷⁴ This phenomenon would add additional advantages of removing pollutants by the Fe^{VI} – $\text{Fe}(\text{III})$ system.

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acs.est.0c04674>.

Information on the chemicals used and stopped-flow measurements; structures and HPLC conditions of four pollutants and the MS/MS data of ATL and its OPs; pH change by adding $\text{Fe}(\text{III})$ without buffering and the PMSO removal by the Fe^{VI} – $\text{Fe}(\text{III})$ system, respectively; kinetic modeling results; mass spectra of ATL and its OPs, and removal of pollutants under different conditions (PDF)

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Notes

The authors declare no competing financial interest.

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