

# Electric Field Manipulation for Improved Rates of Photocatalysis by Mesoporous $\text{TiO}_2$

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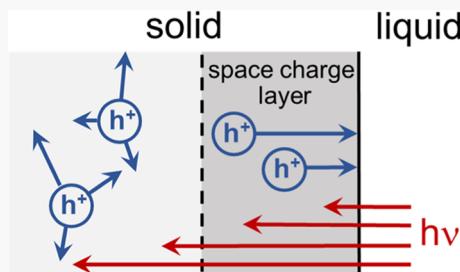
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**ABSTRACT:** This work demonstrates a concept for improving rates of photocatalysis by mesoporous thin films of semiconducting oxide nanoparticles through manipulating the built-in electric field near the nominal free surface. The reaction rate increases via combinations of donor concentration and surface potential that yield wide space charge widths and correspondingly large regions encompassed by the built-in field. The field draws minority carriers generated deep within the film toward the nominal surface where the chemical reactant is most concentrated. In the photo-oxidation of aqueous methylene blue by anatase  $\text{TiO}_2$ , optimization of the parameters increases the rate by nearly a factor of 3. The concept should extend to many photocatalytic materials and reactions.



## INTRODUCTION

Many material properties influence the photocatalytic efficacy of an oxide semiconductor, including the recombination time, absorptivity of light, and rate of carrier transport to the surface. Large bodies of published work describe approaches to improve the first two properties,<sup>1,2</sup> but less attention is focused upon carrier transport rates. In principle, transport driven by drift from electric fields can dwarf that from carrier diffusion. However, little attention has been paid to such effects because in devices such as fuel cells, supercapacitors, and photovoltaic devices that operate within liquid media of high ionic strength, drift-driven transport may be neglected.<sup>3,4</sup> The fluid medium homogenizes the electric potential throughout the solid network and eliminates internal electric fields.

However, such homogenization does not occur in certain important applications of photocatalysts. For example, non-porous polycrystalline films find use in self-cleaning windows and other weather-exposed surfaces<sup>5,6</sup> and in antimicrobial<sup>7</sup> and antifouling coatings.<sup>8</sup> In such films comprising anatase  $\text{TiO}_2$ ,<sup>9</sup> the electric field generally  $\mathcal{E}$  points outward from the solid, encompasses a space charge width  $w$  up to several hundred nanometers, and draws minority carriers toward the surface to increase the reaction rate. Figure S1 in the Supporting Information illustrates the relevant electronic band diagram.

Mesoporous sintered films operating in gases or liquids of low ionic strength should exhibit analogous behavior. Individual particles are too small to support noticeable electric fields across their diameters.<sup>10</sup> However, electrical connectivity within the network enables creation of a field extending over many particle diameters having its principal component directed perpendicular to the nominal film surface. For anatase  $\text{TiO}_2$ , this connectivity occurs under ultraviolet (UV) illumination even for loosely aggregated particulate films

because of an autodoping effect.<sup>11</sup> A field of suitable sign and direction could pull photocarriers toward the nominal surface faster than the fluid reactant diffuses into the porous network. Higher reactant concentrations exist at the nominal surface than within the network, so the overall photoreaction rate should increase. This approach would mitigate some of the fluid diffusion limitations that limit reaction rates, especially in liquids, and also avoids the cost of filtering freely suspended particles<sup>1,2,12–15</sup> from the reactor effluent.

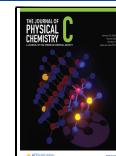
The present work demonstrates the workability of this concept for thin films of porous anatase  $\text{TiO}_2$  that catalyze the photo-oxidation of aqueous methylene blue (MB).  $\mathcal{E}$  is manipulated by methods for defect engineering that vary the donor concentration  $N_d$  and the built-in potential  $V_S$  at the nominal free surface. Indeed, the methods enable considerable decoupling between these two parameters, so their effects may be examined in isolation. The reaction rate varies with  $N_d$  and  $V_S$  in directions and with magnitudes consistent with the predictions of a straightforward photocurrent model. Physical, chemical, and electrical characterization reveals no discernible changes in catalyst properties other than  $N_d$  and  $V_S$ .

**Conceptual Background.** In a semiconductor without internal electric fields, only minority carriers generated within about one diffusion length  $L_p$  of a surface will reach it. However, in thin films, illumination creates photocarriers much deeper in the material, down to roughly the penetration depth

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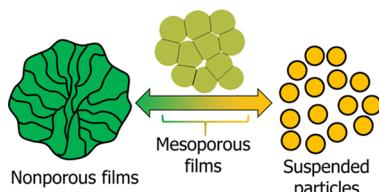
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of light. In anatase, for example,  $L_p$  is about 10 nm,<sup>9,16,17</sup> but the penetration depth at a wavelength of 360 nm is in the order of 1000 nm. To use these minority carriers for reaction, a suitably directed electric field must exist internally to the semiconductor that reaches well beyond  $L_p$ .

Suspended particles are too small to support significant electric fields, but photoreaction still occurs readily because particle radii are in the order of  $L_p$ .<sup>23–27</sup> Such particles have a high specific surface area but require filtration from the reaction effluent. The nonporous polycrystalline material supports internal fields. The specific surface area is rather small, however, and films can be relatively expensive to fabricate. Mesoporous films represent an intermediate case in the continuum from suspended particles to the nonporous polycrystalline material. Figure 1 shows a schematic diagram



**Figure 1.** Conceptual continuum between uniform medium and suspended particles.

representing this idea. Sintered porous films eliminate the need for filtration and offers a high specific surface area and adequate electrical connectivity for electric fields to develop on length scales spanning many particle diameters.

The presence of such electric fields enables manipulation of photocarrier movement by use of layered structures (as in BiOX (X = Cl, Br, and I) nanomaterials<sup>18,19</sup>) and specific forms of defect engineering.<sup>20</sup> Substantial improvements in the photoreaction rate have been demonstrated in nonporous anatase<sup>9,21</sup> by defect engineering to control  $N_d$  and  $V_s$ . The grains within a nonporous polycrystalline semiconductor have a good electrical contact with each other and act as uniform medium to support a built-in space charge region encompassing many crystallites.<sup>9</sup> The width  $w$  of this region varies with  $N_d$  and  $V_s$  according to

$$w = \sqrt{\frac{2\epsilon_s \epsilon_0 V_s}{qN_d}} \quad (1)$$

where  $\epsilon_0$  is the vacuum permittivity;  $\epsilon_s$  is the relative dielectric constant for the solid; and  $q$  is the charge on an electron. In anatase, typical carrier mobilities and lifetimes yield drift distances in the order of 1–10  $\mu\text{m}$ ,<sup>9</sup> far exceeding  $w$ . Thus, nearly all photocarriers generated within a depth  $w$  drift to the surface—a phenomenon that has been noted for various semiconductors including anatase.<sup>9,21,22</sup> A larger value of  $w$  yields an expanded volume from which generated photocarriers can reach the surface for reaction.

Equation 1 indicates that  $w$  increases with the square root of  $V_s$  and inversely with the square root of the donor concentration.  $N_d$  can be manipulated by engineering the concentration of electrically active native and extrinsic defects within the crystallites and at their boundaries.<sup>9</sup>  $V_s$  can be manipulated by defect engineering within the first few nanometers near the surface.<sup>21</sup> For anatase, the engineered values of  $V_s$  appeared to remain robust against shifts<sup>23</sup>

resulting from effects such as light-induced band flattening and adsorption.

If the minority carrier lifetime is sufficiently large in a mesoporous film, a large value of  $w$  may yield benefits through adjustment of  $N_d$  and  $V_s$  akin to nonporous films. In anatase, wherein the minority carriers are typically holes, the lifetime varies widely depending upon the preparation procedure, interfacial charge transfer rates, use of geometries such as nanotubes that promote electron–hole separation,<sup>17</sup> and other factors.<sup>23</sup> However, as a working hypothesis, it is plausible to suppose that the carriers generated within depth  $w$  last long enough to drift to the nominal film surface. The reactant concentration is greater here than deep within the porous structure.

The approach discussed here focuses on minority carriers and therefore differs in important respects from the techniques employed in majority-carrier devices such as solar cells. In such devices, attempts to improve majority-carrier electron transport have focused on approaches such as using one-dimensional nanotubes, nanorods, or nanowires to limit random diffusion within a wide network and to suppress impeded transport at intercrystalline contacts.<sup>28</sup> Internal electric fields have played a smaller role.

## ■ METHODS

**Material Synthesis.** The synthesis method sought to create films of sintered anatase particles on flat substrates of electrically conductive fluorine-doped tin oxide (FTO). This configuration permits electrical characterization of the semiconductor's donor concentration. To this end, FTO-coated glass slides (Sigma-Aldrich, SnO<sub>2</sub>/F, 7  $\Omega/\text{sq}$  surface resistivity, 80–82% transmittance) were coated with a slurry of anatase nanoparticles (Nanostructured & Amorphous Materials, Inc., 10 nm average diameter). The slurry preparation procedure was adapted from the published literature<sup>29</sup> and began with grinding 3 g of anatase in a porcelain mortar/pestle together with 1 mL of deionized water, 0.1 mL of acetylacetone (Sigma-Aldrich), 4 mL of deionized water, and 0.1 mL of Triton X-100 (Sigma-Aldrich) that were added sequentially. The slurry was then applied to the FTO by the doctor blade method, allowed to dry in air for 30 min, and sintered in air for 6 h in a furnace. The sintering temperature of 500 °C avoided the crystalline-phase transformation to rutile.<sup>30,31</sup> The unwanted material was then removed to obtain a coated area of 1 cm × 1 cm.

**Manipulation of the Donor Concentration and Built-In Potential.** Slight chemical reduction of anatase by annealing in H<sub>2</sub> enabled manipulation of the donor concentration  $N_d$ . Annealing was performed in a small (0.2 L) stainless-steel chamber that was evacuated using a mechanical pump. Specimens prepared as described above were heated by affixing them to an electrically conductive back plate cut from an n-type (Sb doped, 0.013  $\Omega/\text{cm}$ ) Si(100) wafer. Bonding was accomplished with a ceramic adhesive (Aremco ULTRA-TEMP 516). The ends of the Si back plate were wrapped with tantalum foil (Sigma-Aldrich, 0.25 mm thick) to improve the contact resistance between the plate and copper support rods that provided electrical current for resistive heating. Annealing was performed at 500 °C for 1 h in partial pressures of H<sub>2</sub> ranging from near zero to 20 mTorr. Temperature was monitored with a chromel–alumel (type K) thermocouple press-fitted to each specimen.

Exposure of the anatase film to a controlled flux of hydrogen ions enabled variation of the built-in potential  $V_s$  at the film's

nominal surface. This exposure was accomplished in an apparatus designed specifically for plasma treatment coupled with *in situ* surface analysis.<sup>32</sup> The main body of the chamber was constructed with stainless steel and was equipped with a load lock, specimen transfer arrangement, and hemispherical analyzer for X-ray photoelectron spectroscopy (XPS). Specimens were mounted at ground potential on a molybdenum holder using double-sided copper tape and a molybdenum clip.

The remote plasma discharge was energized using a 2.45 GHz electron cyclotron resonance source. The deuterium isotope of hydrogen was employed rather than H<sub>2</sub> because D<sub>2</sub> provided a more stable plasma at the operating pressure of  $1.7 \times 10^{-3}$  to  $1.9 \times 10^{-3}$  Torr. Molybdenum grids were placed between the plasma and the specimen. In some cases, voltages were applied to these grids such that ions (mainly D<sub>2</sub><sup>+</sup>) were accelerated to 100 eV before striking the specimen surface. In other cases, the grids were grounded to avoid acceleration. Biased conditions enabled access to higher values of V<sub>S</sub> than unbiased. In both cases, measurement of electrical current through the specimen yielded an incident ion flux of  $1.6 \times 10^{13}$  cm<sup>-2</sup> s<sup>-1</sup>. Simulations employing the TRIM package<sup>33</sup> indicated an ion penetration depth of 2.7 nm under biased grid conditions.

**Material Characterization.** X-ray diffraction patterns were measured using a PANalytical/Philips X'pert Materials Research diffractometer using a Cu K $\alpha_1$  source at 0.154056 nm. The surface area and pore size distribution were, respectively, measured by the Brunauer–Emmett–Teller and Barrett–Joyner–Halenda methods,<sup>34,35</sup> using N<sub>2</sub> as the adsorbing gas in a Quantachrome NOVA 2200e surface area analyzer. The film thickness was measured using a Sloan Dektak 3ST profilometer with 2.5  $\mu\text{m}$ -radius conical-shape stylus (cone angle of 90°). The optical absorption in the UV–near-infrared range was measured with a Cary 5000 spectrophotometer. Absorption spectra were computed by difference between FTO substrates with and without the anatase films.

Electrochemical impedance spectroscopy (EIS) provided values for N<sub>d</sub>. A three-electrode electrochemical cell employed the anatase film as the working electrode, Pt as the counter electrode, and Ag/AgCl as the reference electrode. The aqueous electrolyte was 0.1 M Na<sub>2</sub>SO<sub>4</sub> saturated with Ar gas. A potentiostat (BioLogic Science Instruments model SP150) accomplished the measurement at a frequency of 1 kHz with a modulation amplitude of 10 mV. Calibration of the Ag/AgCl electrode and cleaning of the Pt electrode were performed before each measurement. The cell circuit model assumed Ohmic contacts and components everywhere except for a capacitive Schottky contact at the semiconductor–electrolyte interface. The measured capacitance includes contributions in series from a semiconductor space charge layer (SCL) and a Helmholtz liquid layer, although the semiconductor capacitance dominates at the frequency of measurement.<sup>36</sup> An assumed dielectric constant of 55<sup>37</sup> for anatase then yields N<sub>d</sub> through the Mott–Schottky relation.

XPS measurements for precisely determining the valence band edge in an untreated material were performed using a Kratos Axis Ultra X-ray photoelectron spectrometer (Kratos Analytical, Inc., Manchester, UK) with monochromatic Al K $\alpha$  radiation (1486.6 eV). High-resolution spectra were collected with a pass energy of 20 eV and an energy step of 0.1 eV using a hybrid (electrostatic and magnetic immersion) lens mode. The analyzer specific zero binding energy was set using the

Fermi edge of a gold foil. Although the electron neutralizer was employed to compensate electron loss, specimens were loaded onto copper tape with the FTO surface secured using a copper clip to help reduce the charging effects.

*In situ* XPS measurements were used to gauge the valence band position and chemical composition before and after plasma treatment. A hemispherical analyzer (SPECS 150 EP) was operated with a SPECS XR50 X-ray source. Spectra were collected using Al K $\alpha$  radiation (1486.6 eV) with a pass energy of 50 eV and an energy step of 0.1 eV. Every experiment included a survey encompassing the O 1s, Ti 2p, and C 1s transitions and the valence band edge. Specimen charging effects occurring before plasma treatment were calibrated using the adventitious C 1s peak at 284.8 eV. Plasma treatment distorted this peak, however, so post-treatment calibration employed the Ti 2p<sub>3/2</sub> peak characteristic of anatase with a small shoulder from Ti<sub>2</sub>O<sub>3</sub> added. The movement of the valence band edge was monitored using methods described elsewhere,<sup>21</sup> with details given in the Supporting Information.

**Reaction Rate Measurement.** The apparent first-order reaction rate constants  $k_{\text{app}}$  were measured using the test reaction of MB photo-oxidation, which exhibits well-known pseudo-first-order kinetics. Rates were measured in a small batch reactor, with the specimens illuminated through a quartz window using a solar-simulating light source providing a total broadband intensity of 370 mW/cm<sup>2</sup>. In each experiment, the concentration of MB was monitored as a function of time by continuous UV–visible absorption external to the reactor at 356 nm, with flow through the external tubing driven using a peristaltic pump. Various calibration measurements corrected for the homogeneous reaction of MB, long-term drifts in illumination intensity, and related effects.

Flow within the reactor arising from the external sampling apparatus provided considerable convective mixing to homogenize the reactant concentration. Molecular diffusion also promoted good reactant mixing, as shown by the following estimate. The reaction typically ran for a time  $t$  near 6 h, and the diffusivity of MB in water is  $D = 4 \times 10^{-6}$  cm<sup>2</sup>/s.<sup>38</sup> The corresponding diffusion length  $l$  during the experiment is  $l^2 = 6Dt$ , yielding  $l = 0.58$  cm. This length roughly equaled the internal width of the reactor.

Since adsorption of MB on anatase occurs slowly, 1 h of adsorption equilibration between the MB solution and the TiO<sub>2</sub> was allowed before photocatalytic measurements. The MB absorbance of 665 nm indicated successful establishment of equilibrium within this period, consistent with the published literature for MB and anatase.<sup>39</sup> As discussed in the Supporting Information and observed elsewhere in the literature,<sup>40–43</sup> MB decomposition proceeded according to pseudo-first-order kinetics under the conditions of the experiment. Initial preparation of the reaction mixture provided ample opportunity for equilibration between dissolved O<sub>2</sub> and ambient air, and the reaction apparatus allowed for entry of O<sub>2</sub> during light exposure. Thus, the photobleaching mechanism should be oxidative rather than reductive.<sup>44</sup>

Liquid-phase diffusivities vary inversely with the fluid viscosity according to the Stokes–Einstein relationship. To investigate the effects of such diffusivity variation, experiments were done with a film untreated with hydrogen annealing or plasma, in which polyethylene glycol 2000 (Sigma-Aldrich, molecular weight = 1800 g/mole) was added to the reaction mixture. Varying amounts of thickener were added that sufficed to yield polymer mass fractions up to 0.2, which

decreases the diffusivity by a factor of up to 5. Control experiments indicated that the solution viscosity did not change during photoreaction.

## RESULTS

**Physical and Chemical Characterization.** Figure 2 shows example TEM micrographs of anatase nanoparticles

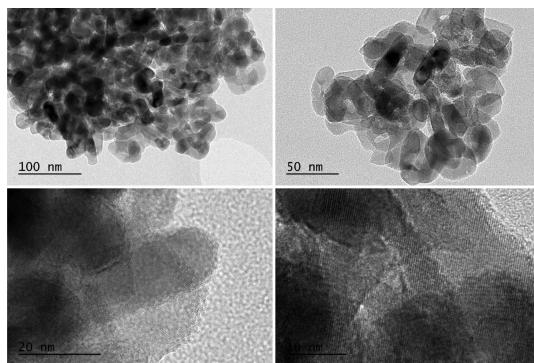


Figure 2. Transmission electron micrograph of suspended  $\text{TiO}_2$  anatase particles at length scales ranging from 100 to 10 nm.

before sintering and confirms an average particle diameter of about 10  $\mu\text{m}$ . Profilometry measurements after film synthesis and sintering reveal a thickness of 13–17  $\mu\text{m}$  as shown in Figure 3. The roughness of 3.1  $\mu\text{m}$  is sizable and accords with plan-view SEM (Figure 4), showing an average grain size near 0.5  $\mu\text{m}$ . A sizable number of grains exhibit diameters above 1  $\mu\text{m}$ .

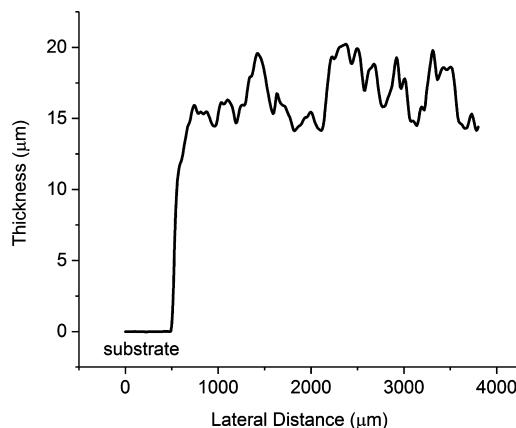


Figure 3. Profile measurement of a typical sintered anatase film.

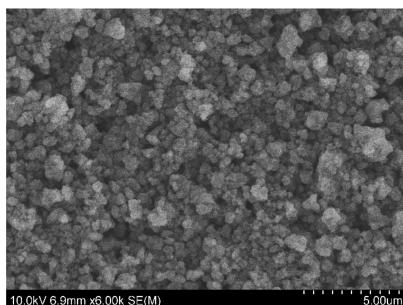


Figure 4. Scanning electron micrograph of a typical sintered anatase film.

Figure 5 shows an example X-ray diffraction pattern for a sintered film. The pattern includes contributions from  $\text{TiO}_2$

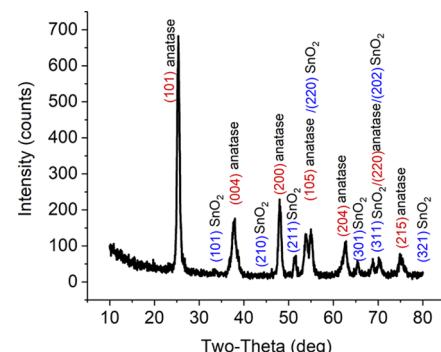


Figure 5. Example X-ray diffraction pattern of a typical sintered anatase film on FTO.

and  $\text{SnO}_2$  in the underlying FTO. No  $\text{TiO}_2$  phases were observed other than anatase, either before or after annealing in  $\text{H}_2$ .  $\text{TiO}_2$  peaks were identified with JCPDS card number 00-021-1272 (tetragonal,  $a = 3.7852$ ,  $c = 9.5139$ ), and  $\text{SnO}_2$  peaks were identified with JCPDS card number 04-003-0649 (tetragonal,  $a = 4.7371$ ,  $c = 3.1851$ ).

Table 1 shows the surface area and pore characteristics from  $\text{N}_2$  adsorption measurements before and after sintering the

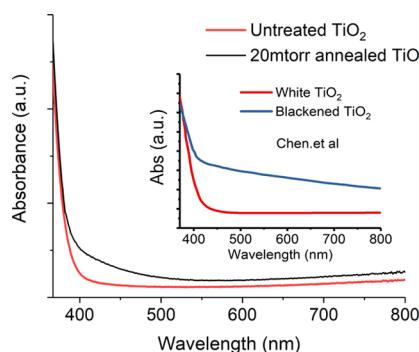
Table 1. Area and Pore Characteristics of Anatase Films

	unsintered	sintered
surface area ( $\text{m}^2/\text{g}$ )	91.1	78.9
pore volume ( $\text{cc/g}$ )	0.36	0.31
porosity (%)	33.8	23.0
pore radius (nm)	4.87	4.88

films. Sintering reduces the surface area by 13%, the pore volume by 14%, and the porosity by nearly one-third. However, the average pore radius remains about constant.

Chemical reduction by hydrogen annealing sought to affect  $N_d$  but not the fundamental atomic structure of the anatase. The procedure increases  $N_d$  because the anatase loses oxygen, which forms native point defects such as Ti interstitials and/or O vacancies that act as donors. However, extensive reduction of anatase leads to additional peaks, its X-ray patterns corresponding to new phases.<sup>45,46</sup> Such new phases were not desired here, and no peaks other than those of anatase were observed in response to the mild hydrogen reduction. Moreover, UV–visible absorption spectra (Figure 6) showed much less perturbation after mild hydrogen reduction than in the literature employing extensive reduction that leads to new phases.

Figure 7a shows the XPS survey scans of the sintered film before and after 0.5 h of plasma treatment. Binding energies were aligned using the C 1s graphitic carbon peak at 284.6 eV. The Ti 2p and O 1s peaks are clearly visible. Figure 7b–d shows the C 1s, O 1s, and Ti 2p peaks in more detail. The C 1s peaks decrease in size upon treatment, presumably due to some volatilization of the C. In addition to the large graphitic peak, there may be two smaller unresolved peaks associated with C–O (286.2 eV) and carbonyl (288.1 eV).<sup>47–50</sup> Treatment induces no new shoulders or other chemical shifts. The O 1s peak has a poorly resolved shoulder above the main peak at 529.7 eV. The shoulder may include contributions



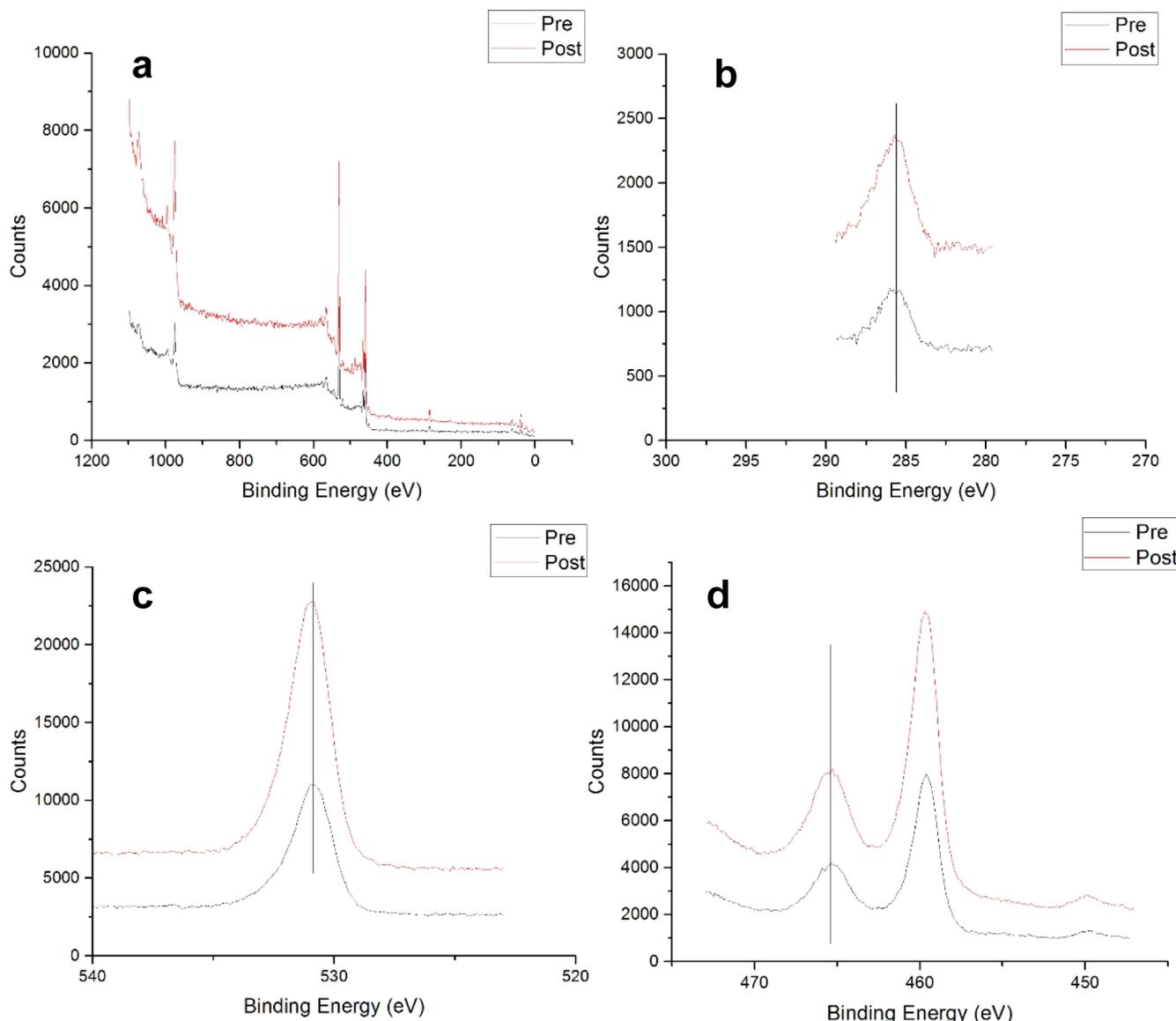
**Figure 6.** UV-visible absorption spectroscopy of a typical sintered anatase film, compared with literature data for strongly reduced anatase shown in the inset (data taken and adapted from ref 46).

from OH groups existing as Ti–OH (533.5 eV) or OH at bridging sites (531.5 eV).<sup>51–54</sup> The O 1s peaks grow slightly in size after treatment, presumably due to loss of partially

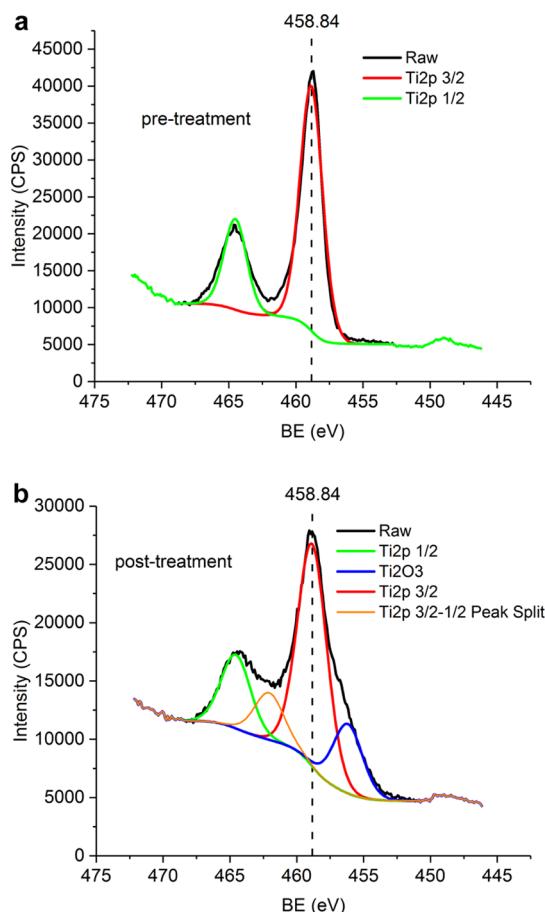
obscuring carbon, but there is no obvious change in the peak shape. The Ti 2p peaks comprising Ti 2p<sub>3/2</sub> and Ti 2p<sub>1/2</sub> are located at 458.6 and 464.4 eV, respectively, with the peak areas in the expected 2:1 ratio. The Ti peak positions indicate an oxidation state of Ti<sup>4+</sup>.<sup>55</sup> The lack of shoulders or asymmetry in the peaks suggests that little or no Ti<sup>3+</sup> is present either before or after treatment. Akin to the behavior of the O 1s peaks, the Ti peaks grow in size after treatment but remain largely unchanged in shape.

In contrast, biased plasma treatment induces extensive chemical changes as shown in Figure 8 for Ti 2p. Two shoulders appear at lower binding energies alongside the two main peaks at 456.5 and 462.2 eV signifying the presence of Ti<sup>3+</sup>,<sup>56,57</sup> indicating that chemical reduction has taken place.

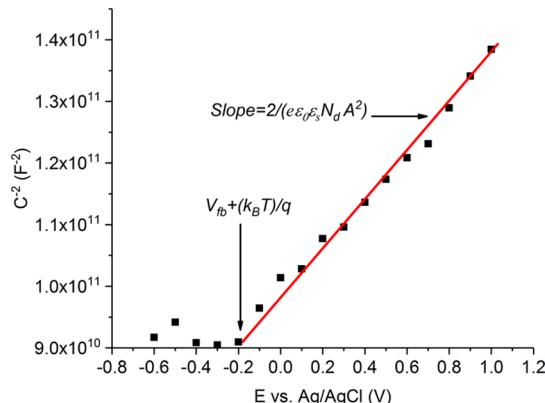
**Electrical Characterization.** Figure 9 shows an example Mott–Schottky plot employed for the determination of  $N_d$ . The curve shape behaves as expected for a depletion layer. Depletion layers are considered as the norm for anatase surfaces,<sup>58</sup> although accumulation layers have been observed



**Figure 7.** XPS shown before and after 0.5 h plasma treatment with no bias, including (a) survey spectra and close-ups of peaks for (b) C 1s, (c) O 1s, and (d) Ti 2p.



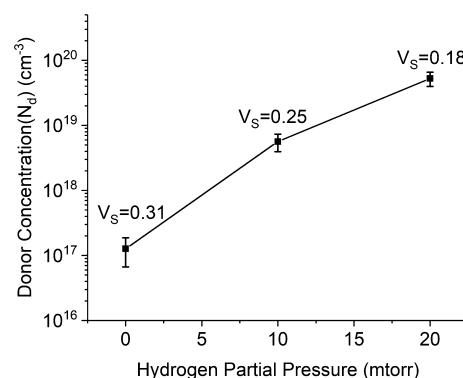
**Figure 8.** XPS Ti 2p peaks shown (a) before and (b) after 1 h of plasma treatment with 100 V bias.



**Figure 9.** Example Mott-Schottky plot for the measurement of  $N_d$  of a sintered anatase film. In this case,  $N_d = 5.3 \times 10^{19} \text{ cm}^{-3}$ .

for anatase single crystals bombarded with 2 keV Ar ions and subsequently annealed in low-pressure  $\text{O}_2$ .<sup>59</sup>

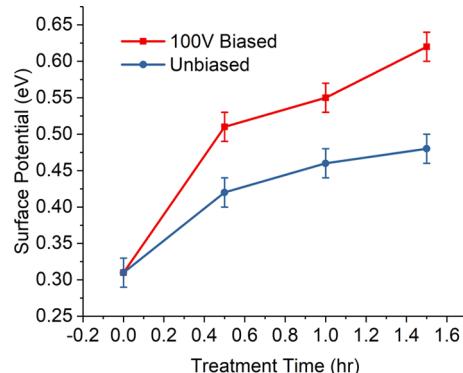
The donor concentration computed from such plots for untreated films is  $1.3 \times 10^{17} \text{ cm}^{-3}$ . Annealing in varying pressures of  $\text{H}_2$  leads to progressively higher values of  $N_d$  up to  $5.3 \times 10^{19} \text{ cm}^{-3}$ . Although this value exceeds that of the untreated material by 2 orders of magnitude,  $N_d$  remains much lower than the reported value for strongly reduced anatase ( $2.1 \times 10^{22} \text{ cm}^{-3}$ ).<sup>45,46</sup> Mild reduction conditions also lead to a decrease in  $V_s$  from 0.31 to 0.18 eV (Figure 10). This decrease results from the increase in  $N_d$  which induces the Fermi



**Figure 10.** Dependence of  $N_d$  on hydrogen annealing pressure.  $V_s$  changes with  $N_d$  because the Fermi level moves within the bulk but remains pinned at the surface.

energy in the bulk to rise by about 0.15 eV assuming that the surface Fermi energy remains constant. In other words, varying  $N_d$  unavoidably leads to modest changes in  $V_s$  as well.

Plasma exposure sought to induce the formation of electrically active point defects within 2–3 nm of the surface in order to move the Fermi energy at the surface without changing  $N_d$  deeper in the bulk. Only the nominal free surface was exposed to H radicals or ions; internal pore surfaces remained unaffected. For the specific surface area reported in Table 1 for sintered films, the internal reactive area in a layer of about 100 nm thickness (typical of the depletion widths used in this work) is larger than the nominal free surface area by roughly a factor of 30. Figure 11 shows that  $V_s$  increases by up

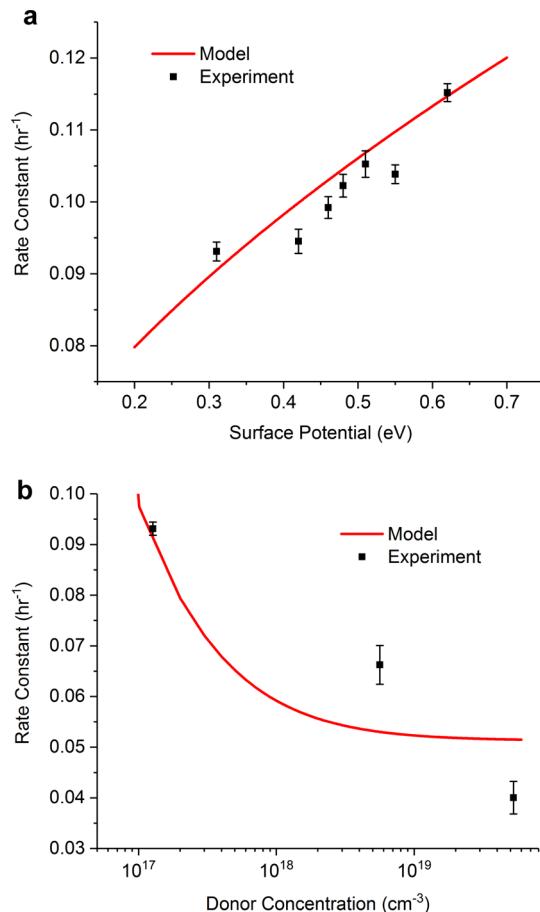


**Figure 11.**  $V_s$  vs plasma treatment time under biased and unbiased conditions. Biasing broadened the range over which  $V_s$  could be varied.

to a factor of about 2 depending upon the treatment time and biasing conditions, from 0.31 to 0.62 eV. The largest change takes place under biased conditions, although the unbiased plasma still induces significant increases.

Hydrogen exists in several forms in anatase.<sup>60,61</sup> Hydrogen atoms present as interstitials or bonded to O vacancies act as shallow donors, while interstitial  $\text{H}_2$  is electrically inactive. Hydrogen donors do not appear to dominate the behavior of  $V_s$  here, as the increasing values signify movement of the surface Fermi energy toward the mid-gap instead of toward the conduction band. However, complexation of hydrogen with oxygen vacancies and extrinsic defects may change their donor properties and give rise to the observed changes.

**Reaction Rate Measurements.** The value of  $k_{app}$  for MB photo-oxidation decreased in response to increases in  $N_d$  by a factor of 2.3, from 0.093 to 0.040  $\text{h}^{-1}$  (Figure 12a). Increasing  $V_s$  caused  $k_{app}$  to rise by about 25% (Figure 12b). It is evident that an increase in  $V_s$  caused  $k_{app}$  to move in the opposite direction from an increase in  $N_d$ .



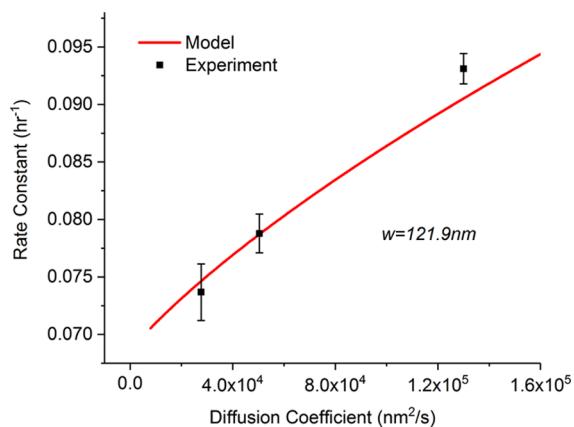
**Figure 12.** Apparent rate constant  $k_{app}$  vs (a)  $V_s$  and (b)  $N_d$ . Data points corresponding to the untreated catalyst are at  $V_s = 0.3$  V in (a) and  $N_d = 1.3 \times 10^{17}$  cm<sup>-3</sup> in (b).

Polyethylene glycol was added to the liquid phase in order to decrease the diffusivity of MB by a factor of up to 5,<sup>62</sup> from  $1.3 \times 10^5$  to  $0.27 \times 10^5$  nm<sup>2</sup>/s. Measurements with a mass fraction of 0.2 showed a decrease in  $k_{app}$  by about 20%, from 0.093 to 0.074 h<sup>-1</sup> (Figure 13). A mass fraction of 0.1 decreased  $k_{app}$  by most of this amount to 0.077 h<sup>-1</sup>.

## DISCUSSION

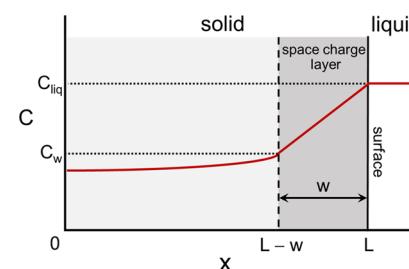
The utility of TiO<sub>2</sub> as a photocatalyst is hampered by limited absorption of the solar spectrum<sup>46,63–66</sup> and fast recombination of charge carriers.<sup>65,67–72</sup> Common methods to improve optical absorption include blackening through hydrogenation<sup>46,73–75</sup> and by doping with foreign elements to shrink the band gap. Methods to lessen recombination include co-doping and placement of metal nanoparticles on the surface.<sup>76,77</sup> The present work uses a different approach that seeks to use photocarriers more efficiently by actively sweeping them toward the surface by building in an electric field.

**Model for Combined Carrier–Reactant Diffusion and Reaction.** The one-dimensional, steady-state treatment



**Figure 13.** Apparent rate constant  $k_{app}$  vs  $D_{pore}$  for the untreated film.

integrates an analytical description of diffusion and reaction in porous catalysts with a photocurrent model for photocatalysis by nonporous films. The following paragraphs describe the model's most important features, with additional details appearing in the *Supporting Information*. We consider steady-state photocatalysis by a porous rectangular slab of thickness  $2L$  with the center line at  $x = 0$ , specific area per unit volume  $A$  (m<sup>2</sup>/m<sup>3</sup>), and nominal film area  $A_{nom}$  on each side of the slab. Figure 14 sketches the reactant concentration versus depth, with the reaction taking place at the film's surface at  $L$  and also within the field-free pores between  $x = 0$  and  $x = L - w$ .



**Figure 14.** Schematic of MB concentration vs depth within the film. The zero is set at the interface between the film and its mechanical support, so that the surface resides at  $x = L$ . The SCL of width  $w$  therefore stretches between the surface at  $L$  and  $L - w$ .

The total reaction rate  $R_{total}$  (moles/s) in the film comprises a drift component  $R_{drift}$  from photocarriers that react at the film surface and a pore component  $R_{pore}$  from photocarriers generated beyond the SCL that diffuse to nearby pore walls. As the *Supporting Information* shows in more detail, the drift contribution to the total rate obeys

$$R_{drift} = kAC_{liq}A_{nom}w \quad (2)$$

where  $k$  denotes the rate constant per unit internal area of pores (s<sup>-1</sup> m<sup>-2</sup>). For the pore component, analytical expressions for the effectiveness factor of heterogeneously catalyzed reactions simplify the computation as shown in the *Supporting Information*. The reactant concentration  $C_w$  at the edge of the SCL becomes

$$C_w = \frac{C_{liq}}{1 + w \sqrt{\frac{kA}{D_{pore}}} \tanh \left[ (L - w) \sqrt{\frac{kA}{D_{pore}}} \right]} \quad (3)$$

A Thiele modulus  $\Phi$  may be defined for the field-free region as

$$\Phi = (L - w) \sqrt{kA/D_{\text{pore}}} \quad (4)$$

with the corresponding effectiveness factor  $\eta$  given by

$$\eta = \frac{\frac{1}{L-w} \int_w^L r(x) dx}{r(C_w)} = \frac{\tanh(\Phi)}{\Phi} \quad (5)$$

In a reactive volume that equals  $A_{\text{nom}}(L - w)$ ,  $R_{\text{pore}}$  becomes

$$R_{\text{pore}} = \eta k A A_{\text{nom}} (L - w) C_w \quad (6)$$

The total reaction rate for comparison with experiment combines the expressions for  $R_{\text{drift}}$  and  $R_{\text{pore}}$

$$R_{\text{total}} = R_{\text{drift}} + R_{\text{pore}} = k A A_{\text{nom}} [C_{\text{liq}} w + \eta C_w (L - w)] \quad (7)$$

The diffusivity  $D_{\text{pore}}$  invariably enters into the overall rate through the combined parameter  $k/D_{\text{pore}}$ . However,  $k$  appears by itself as the leading term in eq 7, enabling  $D_{\text{pore}}$  to be disaggregated from  $k$ . In the asymptotic limit of large  $w$ ,  $R_{\text{drift}}$  dominates  $R_{\text{total}}$  and varies linearly with  $w$ . The effects of  $D_{\text{pore}}$  become negligible. This regime determines a unique value of  $k$ , which permits the determination of  $D_{\text{pore}}$  from  $k/D_{\text{pore}}$  in the asymptotic limit  $w \rightarrow 0$  where pore diffusion dominates.

Fitting of the rate data to obtain  $D_{\text{pore}}$  and  $k$  was performed by minimizing an objective function  $S$  composed of equally weighted squared residuals

$$S = \sum (k_{\text{app}}^{\text{exp}} - k_{\text{app}}^{\text{model}})^2 \quad (8)$$

where  $k_{\text{app}}^{\text{model}}$  denotes the apparent rate constant computed from the model and  $k_{\text{app}}^{\text{exp}}$  denotes the corresponding quantity from experimental rates. The Supporting Information describes the procedures employed to determine confidence intervals for the fitted and derived parameters.

**Comparison of the Model with Rate Data.** The parameters detailed above fall into three categories: known from experimental conditions, fitted from rate data, and derived from the fitted parameters. Known parameters include not only  $N_d$  and  $V_s$  but also others shown in Table 2, such as  $L$

**Table 2. Known Parameters**

parameter	value
$L$	13–17 $\mu\text{m}$
$C_{\text{liq}}$	$1 \times 10^{-5}$ mol/L
$A$	0.146 $\text{nm}^2/\text{nm}^3$
$A_{\text{nom}}$	$1 \text{ cm}^2 = 1 \times 10^{14} \text{ nm}^2$

from profilometry,  $C_{\text{liq}}$  from the MB solution formulation,  $A$  from BET measurements, and  $A_{\text{nom}}$  from the choice of convenience. The model contains only two adjustable parameters to fit from rate data:  $D_{\text{pore}}$  and  $k$ . These two parameters work in concert with the known parameters to control  $k_{\text{app}}$  through the functional forms embodied in eqs 1–7. Since these function forms are rather complicated, the ability of the model to fit variations in  $k_{\text{app}}$  with  $N_d$ ,  $V_s$ , and  $D_{\text{pore}}$  represents a significant test of the underlying physical picture. Parameters derived from  $k$  and  $D_{\text{pore}}$  include  $\Phi$  and  $\eta$ .

Table 3 shows the fitted and derived parameters. The best fit value of  $D_{\text{pore}}$  in water is  $1.3 \times 10^5 \pm 0.3 \text{ nm}^2/\text{s}$ . A similar value of  $4 \times 10^5 \text{ nm}^2/\text{s}$  was obtained for a related type of dye in an

**Table 3. Fitted and Derived Parameters**

parameter	value
$D_{\text{pore}}$	$1.3 \times 10^5 \pm 0.3 \text{ nm}^2/\text{s}$
$k$	$107 \pm 2 \text{ nm/s}$
$\Phi$	141
$\eta$	0.0071

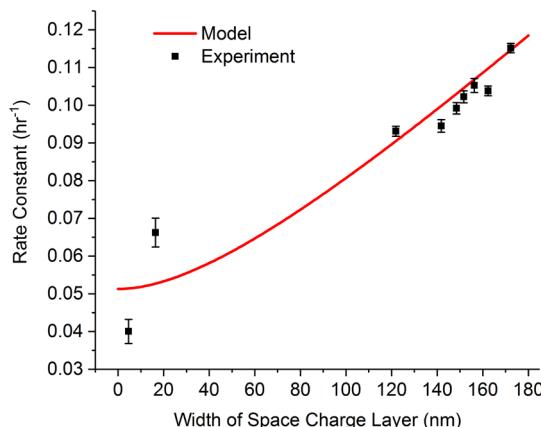
electrode incorporating  $\text{TiO}_2$  particulates.<sup>64</sup> This correspondence provides evidence that the model captures the key physics and chemistry reasonably accurately. As expected for diffusion in confined spaces, both values lie considerably below the normal liquid phase value of  $D = 4 \times 10^{-6} \text{ cm}^2/\text{s} = 4 \times 10^8 \text{ nm}^2/\text{s}$ .<sup>64</sup>

The best-fit value of  $k$  is 107 nm/s under the illumination conditions employed. Variations in synthesis protocols and illumination intensity complicate direct comparison of this number to the literature. Comparison of the measured and modeled magnitude and direction of  $k_{\text{app}}$  with  $N_d$  and  $V_s$  is more instructive. Figure 12a,b shows these comparisons. For  $V_s$ , the model predicts a nearly linear increase in  $k_{\text{app}}$  by about 25% in a range over which  $V_s$  increases by a factor of about 2. The prediction captures both the magnitude and slope of the variation. Confidence intervals on the experimental points are too large to detect the slight curvature in  $k_{\text{app}}$  versus  $V_s$  predicted by the model. For  $N_d$ , the prediction captures the rough magnitude and general direction of the variation—a decrease in  $k_{\text{app}}$  by about a factor of 2 as  $N_d$  increases by a factor of 500. However, the data do not match the significant curvature predicted by the model.

For  $D_{\text{pore}}$  (Figure 13), the model predicts a nearly linear increase in  $k_{\text{app}}$  by about 25% in a range over which  $D_{\text{pore}}$  increases by a factor of about 3. As with  $V_s$ , the prediction for  $D_{\text{pore}}$  captures both the magnitude and slope of the variation, with confidence intervals for the data being too large to assess the slight curvature.

Polymers based on ethylene glycol are known to undergo photocatalytic degradation in the presence of  $\text{TiO}_2$ , yielding shorter glycol chains and a variety of esters and aldehydes.<sup>78,79</sup> Those studies were done at much lower polymer concentrations than employed here, with rates too low to change the solution viscosity in the present work. However, such reactions could conceivably compete with MB decomposition for photogenerated holes and thereby depress the rate constant  $k$ . As mentioned above,  $D_{\text{pore}}$  enters into  $k_{\text{app}}$  through the combined parameter  $k/D_{\text{pore}}$ . Increasing the polymer mass fraction from 0.1 to 0.2 decreases  $D_{\text{pore}}$  by a factor of about 2. Any simultaneous depression of  $k$  would compensate some of this decrease in  $D_{\text{pore}}$  and attenuate the change in  $k_{\text{app}}$  predicted by eqs 1–7. Indeed, if  $k$  decreases in direct proportion to the polymer concentration, the compensation would be complete and  $k_{\text{app}}$  would remain constant. However, Figure 13 shows that  $k_{\text{app}}$  decreases as predicted by eqs 1–7 with constant  $k$ . This result suggests that the polymer photoreaction does not influence the MB rate under the conditions of the experiment.

A fundamental premise of the model is that electric fields within the solid sweep most holes generated to a depth  $w$  toward the nominal free surface. In other words,  $w$  is a physical quantity more fundamental to photocarrier behavior than either  $N_d$  or  $V_s$ . It is therefore instructive to combine the data in Figure 12a,b into a single dataset plotted as a function of  $w$  according to eq 1. Figure 15 shows the experimental and



**Figure 15.** Apparent rate constant  $k_{app}$  vs width  $w$  of SCL. The untreated film corresponds to the data point at 122 nm.

model predictions in this way. As  $w$  increases from 5 to 180 nm,  $k_{app}$  increases by slightly over a factor of 2 for both the experimental data and predictions. Correspondence is best at large values of  $w$  and declines noticeably for small  $w$ . The data points at small  $w$  correspond to the largest values of  $N_d$  in Figure 12b, where deviations are also most pronounced.

**Assessment of Model Assumptions.** The physical picture underlying the model presupposes that the photoreaction by the diffusive motion of holes to particle sidewalls happens only deep within the film beyond the SCL width  $w$ . Holes generated within the SCL react not at the sidewalls but at the nominal surface under the influence of the electric field. A simple computation shows that this picture presupposes that the rate of hole loss by recombination or reaction at the sidewalls must be low enough to enable drift to dominate. The diffusion length  $x_{diff}$  can be estimated from

$$x_{diff} = \sqrt{\frac{k_B T}{\mu q} \tau} \quad (9)$$

where  $k_B$  represents the Boltzmann constant,  $T$  is the temperature,  $\mu$  is the hole mobility, and  $\tau$  is the time of diffusion. The drift length  $x_{drift}$  in an electric field  $\mathcal{E}$  obeys

$$x_{drift} = \mu \mathcal{E} \tau \quad (10)$$

To compare  $x_{diff}$  and  $x_{drift}$  at a single value of  $\tau$ , we can rearrange eqs 9 and 10 to yield

$$x_{drift} = \frac{q \mathcal{E} x_{diff}^2}{k_B T} \quad (11)$$

If we assume a particle radius of 5 nm for  $x_{diff}$  and a typical field strength in the order of 1 V/100 nm =  $10^7$  V/m at room temperature, eq 11 yields  $x_{drift} = 9$  nm. This value is much smaller than the SCL width, so clearly drift cannot sweep holes far enough to reach the nominal surface if the efficiency of hole loss at the sidewall is high.

The efficiency of this loss for anatase particles is a complicated matter that has been reviewed extensively<sup>23,80</sup> and varies over orders of magnitude in colloidal and particulate systems. Loss rates depend upon surface preparation, the presence of electron scavengers, various trapping mechanisms, optical absorptivity, light intensity, and other factors. It is therefore plausible in the present system that surface loss may occur slowly enough for drift to dominate. Furthermore, it is difficult to rationalize the variation in  $k_{app}$  with  $V_s$  without

invoking drift. Plasma treatment affects only the exposed free surface of the film, which as mentioned above comprises only a small percentage of the total reactive surface area. The XPS measurements show changes in the surface chemical composition with plasma treatment under bias with ions accelerated into the surface but not in the absence of bias. However, the data from biased and unbiased treatment all follow an unbroken pattern in Figure 12b—a pattern that furthermore aligns well with the picture embodied in eq 1.

The inability of the model to capture the behavior of  $k_{app}$  in some respects at high values of  $N_d$  deserves discussion. The mild hydrogen reduction employed to reach this regime could have changed some aspects of surface reactivity. Interstitial hydrogen atoms are unstable during long-term storage at room temperature<sup>60</sup> because a low diffusion barrier<sup>81</sup> enables disappearance to form interstitial H<sub>2</sub> or to bond with other intrinsic or extrinsic traps. However, the treatment does affect light absorption as shown in Figure 6, which may propagate into the efficiency of hole loss at the sidewalls. An equally likely explanation relates to the exceptionally small value of  $w$  in this range: only 5–20 nm. Grain sizes are much larger, averaging about 500 nm, with the roughness of the nominal surface near 3  $\mu$ m. Given the mismatch in length scales and the complicated geometry of the nominal surface, it is perhaps notable that the model works modestly well.

**Prospects for Generalizing the Concept.** The concept for influencing the photoreaction rate via  $w$  through defect engineering to control  $N_d$  and  $V_s$  (i.e., via eq 1) has been demonstrated previously for nonporous anatase.<sup>9,21</sup> The present work suggests that these concepts extend to porous anatase and likely to photo-oxidations other than MB, although according to a different quantitative description that includes liquid-phase transport. Defect engineering of nonporous anatase relied upon specialized synthesis methods using amorphous TiO<sub>2</sub> (for  $N_d$ ) and treatment with O<sub>2</sub> plasma (for  $V_s$ ). The effects of synthesis from amorphous TiO<sub>2</sub> are complicated to implement and depend upon film thickness, while O<sub>2</sub> plasma treatment induces a decrease in  $V_s$  rather than an increase. The present work therefore employs different approaches involving hydrogen: thermal annealing (for  $N_d$ ) and treatment with D<sub>2</sub> plasma (for  $V_s$ ). However, thermal annealing in H<sub>2</sub> decreases the rate unhelpfully. Moreover, hydrogen-based methods entail complications that arise from competition between incorporation of hydrogen and formation of interface or bulk defects.<sup>82–84</sup> Under some circumstances, anatase photocatalysts treated with hydrogen exhibit deactivation over time.<sup>84,85</sup> The effects are complex and require further study before practical implementation.<sup>86,87</sup>

In short, for both nonporous and porous anatase, improvements are required in defect engineering methods to stably and simultaneously decrease  $N_d$  and increase  $V_s$ . The plasma method employed here was able to raise  $V_s$  by a few tenths of a volt. Whether other methods could generate larger changes remains a matter of speculation. However, band bending larger than a semiconductor's band gap is very unlikely. Surface Fermi level pinning near the mid-gap is more common, which would limit  $V_s$  for anatase to about 1.6 V. This is a factor of only  $\sim 2.5$  greater than obtained here, leading from eq 1 to a possible rate enhancement of about 1.6. Much larger enhancements would become possible if  $N_d$  could be decreased by 1 or more orders of magnitude. This would require methods for defect engineering capable of neutralizing or compensating the many kinds of donor species in anatase, including native Ti

interstitials, O vacancies, adventitious H, and other foreign impurities. Such attempts have been made,<sup>88,89</sup> although the methods remain far from mainstream.

The model developed here indicates that lower diffusion coefficients inhibit  $R_{\text{pore}}$ , while  $R_{\text{drift}}$  remains unaffected. Thus, tailored electric fields provide the greatest benefit when used for fluid reactions involving small diffusion coefficients. Figure 16 shows predictions for  $k_{\text{app}}$  over a wide range of pore

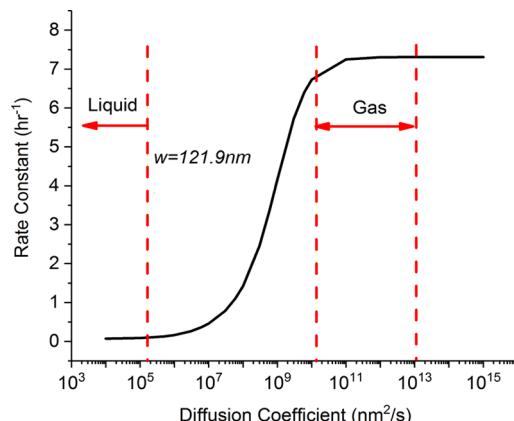


Figure 16. Model prediction for the apparent rate constant vs  $D_{\text{pore}}$ .

diffusivities encompassing both liquids and gases. Gases have much higher diffusivities; in porous media, Knudsen diffusion coefficients typically lie in the range from  $10^{10}$  to  $10^{13}$  nm $^2$ /s.<sup>74,75,90,91</sup> This range is several orders of magnitude higher than for water.<sup>38,62</sup> Maximal reactant concentrations therefore exist throughout the porous network, so the beneficial effects of electric field manipulation largely disappear because they become superfluous. Accordingly, defect engineering to increase  $w$  is likely to be helpful for liquids but not for gases.

Much attention in photocatalysis focuses on separating electrons and holes to preserve the minority holes for useful photoreaction. The field within the SCL does serve in this role; photogenerated holes deep within the semiconductor separate from the majority electrons residing there by sweeping the holes to the surface. However, the approach described here does not address the lateral separation on the nanometer length scale that is crucial for efficient photocatalysis, wherein oxidation and reduction reactions occur in close atomic-scale proximity to each other. Crystal facets, cocatalysts, and localized doping are the most common means to accomplish such separation,<sup>92</sup> although nanotubes are also attracting increasing attention.<sup>17</sup> The present approach implemented in a three-dimensional network sweeps holes in a direction normal to the surface. Upon arrival, they may be separated laterally by other means. This conceptualization in terms of a sequence of discrete transport steps is not precisely accurate in regions very close to the surface, but in three-dimensional networks, it may be useful to view the SCL-mediated transport as lying largely upstream of the lateral separation. In one- or two-dimensional geometries involving nanotubes or two-dimensional BiOX structures, the lateral separation begins much deeper within the solid. However, it is still helpful to view as conceptually distinct the separation that sweeps holes in the normal direction toward the surface.

## CONCLUSIONS

This work provides substantial evidence that photoreaction rates in mesoporous films of semiconducting oxides can be increased through defect engineering that creates combinations of donor concentration and surface potential that yield wider space charge widths. Increased widths sweep more photo-carriers to the nominal free surface where the reactant concentration is highest. Although this work has demonstrated the plausibility of the concept, the defect engineering techniques employed here acted only to increase  $N_d$ , which decreases the space charge width. Given the limited range of values available for varying  $V_s$ , full exploitation of this concept requires defect engineering methods capable of substantially decreasing  $N_d$ .

## ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acs.jpcc.1c09020>.

Method details for determining  $V_s$ ; method details for measuring reaction rates; derivation of the model for combined carrier–reactant diffusion and reaction; and procedure for parameter fitting (PDF)

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### Notes

The authors declare no competing financial interest.

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