

Extending the Kinetic and Thermodynamic Limits of Molecular-Beam Epitaxy Utilizing Suboxide Sources or Metal-Oxide-Catalyzed Epitaxy

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We observe a catalytic mechanism during the growth of III-O and IV-O materials by suboxide molecular-beam epitaxy (*S*-MBE). By supplying the molecular catalysts In_2O and SnO we increase the growth rates of Ga_2O_3 and In_2O_3 . This catalytic action is explained by a metastable adlayer *A*, which increases the reaction probability of the reactants Ga_2O and In_2O with active atomic oxygen, leading to an increase of the growth rates of Ga_2O_3 and In_2O_3 . We derive a model for the growth of binary III-O and IV-O materials by *S*-MBE and apply these findings to a generalized catalytic description for metal-oxide-catalyzed epitaxy (MOCATAXY), applicable to elemental and molecular catalysts. We introduce a mathematical description of *S*-MBE and MOCATAXY, providing a computational framework to set growth parameters in previously inaccessible kinetic and thermodynamic growth regimes when using the aforementioned catalysis. Our results indicate that MOCATAXY takes place with a suboxide catalyst rather than with an elemental catalyst. As a result of the growth regimes achieved, we demonstrate a $\text{Ga}_2\text{O}_3/\text{Al}_2\text{O}_3$ heterostructure with an unrivaled crystalline quality, paving the way for the preparation of oxide device structures with unprecedented perfection.

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I. INTRODUCTION

Molecular-beam epitaxy (MBE) takes place under nonequilibrium conditions and surface kinetics plays a dominant role in the MBE growth process—allowing growth modes to be intentionally manipulated [1–5]. For decades, the single-step reaction mechanism occurring during the MBE growth of III-V (e.g., GaAs, GaN, AlN) [6–8] and II-VI (e.g., ZnSe, ZnO) [9,10] compound semiconductors has defined MBE as a rather simple and straightforward thin-film technique, especially when compared with chemical-vapor-deposition methods [11]. In contrast to the growth of III-V and II-VI materials, the surface kinetics of III-O (e.g., Ga_2O_3 and In_2O_3) [12–18] and IV-O (e.g., SnO_2) [19] compounds is governed by a complex reaction pathway, resulting in a two-step reaction mechanism to form the intended compound. The formation and subsequent desorption of ad molecules, called suboxides (e.g., Ga_2O , In_2O , SnO), define the growth-limiting

step for these classes of materials. The result is a rather narrow growth window within the adsorption-controlled regime [14,15,18–20].

By engineering the MBE processes, two variants of MBE have recently been developed. These variants extend the kinetic and thermodynamic limits within which III-O and IV-O materials may be grown. The first variant, *suboxide* MBE (*S*-MBE) [21], refers to a technique that uses the decomposition of III-VI and IV-VI compounds (i.e., Me_xO_y) by group-III and group-IV elements [13, 17] as well as a special MBE source chemistry [21] to produce suboxide molecular beams that consist almost entirely (typically > 99.9%) of a single suboxide molecular species (i.e., $\text{Me}_x\text{O}_{y-x}$). Stoichiometric coefficients of Me_xO_y and $\text{Me}_x\text{O}_{y-x}$ are $x = 2$ and $y = 3$ for III-O (e.g., Ga_2O_3 , In_2O_3) and $x = 1$ and $y = 2$ for IV-O (e.g., SnO_2) materials.

Using the *S*-MBE approach, the growth-limiting step occurring during the growth of III-O and IV-O materials by conventional MBE is bypassed, enabling the growth of films with excellent structural quality and surface smoothness at growth rates exceeding $1\ \mu\text{m h}^{-1}$

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and a comparatively low growth temperature (T_G) [21]. The second variant is metal-oxide-catalyzed epitaxy (MOCATAXY), a method involving the introduction of a catalyst into oxide growth systems [5,17,18,22]. Using this technique, the growth-limiting step of III-O compounds is bypassed by the catalyst [5]. It has been proposed that MOCATAXY results from metal-exchange catalysis (MEXCAT) [5] and it has been observed on various growth surfaces for the formation of Ga_2O_3 and $(\text{Al}_x\text{Ga}_{1-x})_2\text{O}_3$ [5,18,22–25] as well as during other physical vapor-deposition methods [26]. Nevertheless, the underlying physics leading to the observed catalysis has been explained differently—experimentally [5,22] and theoretically [27]—and thus remains disputable.

In this paper, the combination of *S*-MBE and MOCATAXY is investigated and shown to result in a marked extension of the kinetic and thermodynamic limits of the growth of Ga_2O_3 and In_2O_3 . By supplying suboxide molecular beams of Ga_2O , In_2O , and SnO , a growth-rate (Γ) enhancement of Ga_2O_3 and In_2O_3 is observed. Quantitative models describing this enhanced growth rate during *S*-MBE as well as during the catalyzed *S*-MBE of III-O thin films are derived and applied to the experimental observations to extract model parameters. Through a systematic comparison of experimental Γ data from different growth systems and growth methods (i.e., MOCATAXY during *S*-MBE and conventional MBE), a generalization of the proposed MEXCAT mechanism [5] is developed. This generalized growth mechanism is applicable to the growth of Ga_2O_3 and In_2O_3 by conventional MBE and *S*-MBE.

II. SUBOXIDE-MBE (*S*-MBE) MODEL

We begin by deriving a growth-rate model for the growth of III-VI and IV-VI compounds with general formula Me_xO_y by *S*-MBE and validate it by using Ga_2O_3 and In_2O_3 as examples. Figure 1 shows the growth kinetics of Ga_2O_3 and In_2O_3 as a function of their respective growth parameters. In Figs. 1(a)–1(d), the film growth rate, Γ , is observed to increase linearly with the incident flux of suboxide, $\phi_{\text{Me}_x\text{O}_{y-x}}$ (i.e., $\phi_{\text{Ga}_2\text{O}}$ or $\phi_{\text{In}_2\text{O}}$), in the O-rich regime. This linear increase in Γ reaches a plateau in the adsorption-controlled regime, when $\phi_{\text{Me}_x\text{O}_{y-x}}$ exceeds the flux of active atomic oxygen, ϕ_o . The growth kinetics for the growth of III-O compounds by *S*-MBE are thus the same as those of III-V and II-VI materials when grown by conventional MBE [21].

Figures 1(e) and 1(f) depict Γ as a function of T_G and ϕ_o , respectively. For the same growth conditions, Γ of Ga_2O_3 on $\text{Ga}_2\text{O}_3(010)$ (hollow squares) is larger than that of Ga_2O_3 on $\text{Ga}_2\text{O}_3(\bar{2}01)$ (solid squares) [see Fig. 1(e)]. This result is similar to the growth of Ga_2O_3 by conventional MBE on $\text{Ga}_2\text{O}_3(\bar{2}01)$ versus on $\text{Ga}_2\text{O}_3(010)$ substrates [20,28,29]. A comparison of the growth kinetics of $\text{Ga}_2\text{O}_3(\bar{2}01)$ and $\text{In}_2\text{O}_3(111)$ [e.g., the data in Fig. 1(a)

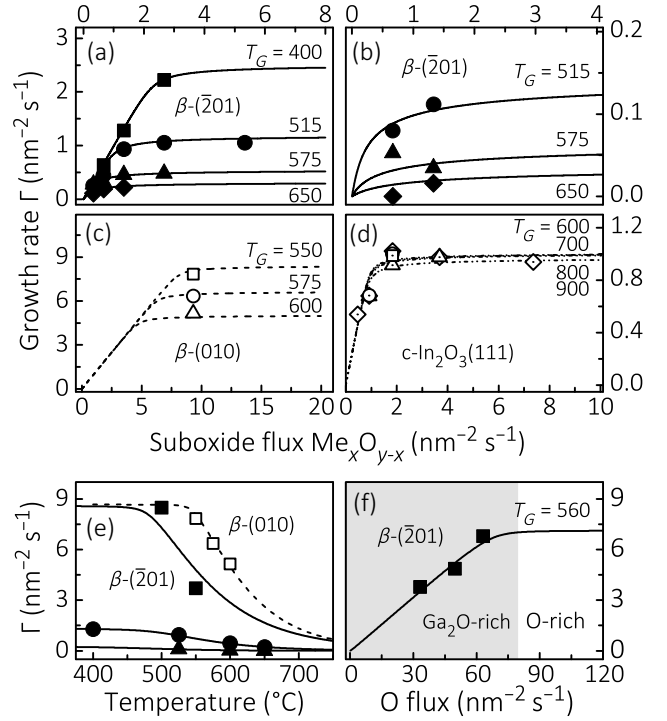
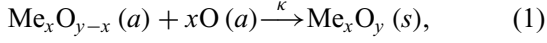


FIG. 1. (a),(b) The dependence of the film growth rate (Γ , in units of the flux of Ga_2O being incorporated into the growing Ga_2O_3 film) of $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ by *S*-MBE on the flux of the suboxide Ga_2O at active atomic oxygen fluxes $\phi_o = 5.7 \text{ nm}^{-2} \text{ s}^{-1}$ and $\phi_o = 0.7 \text{ nm}^{-2} \text{ s}^{-1}$, respectively. (c) The growth rate (Γ) of $\beta\text{-Ga}_2\text{O}_3(010)$ at $\phi_o = 33 \text{ nm}^{-2} \text{ s}^{-1}$ as a function of $\phi_{\text{Ga}_2\text{O}}$. (d) The dependence of Γ of bixbyite $\text{In}_2\text{O}_3(111)$ (in units of the flux of In_2O being incorporated into the growing In_2O_3 film) on the flux of the suboxide In_2O , at $\phi_o = 2.0 \text{ nm}^{-2} \text{ s}^{-1}$. (e) The growth-temperature (T_G) dependence of Γ of $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ and $\beta\text{-Ga}_2\text{O}_3(010)$ at different active atomic oxygen fluxes: $\phi_o = 28.5 \text{ nm}^{-2} \text{ s}^{-1}$ (solid and hollow squares), $\phi_o = 5.7 \text{ nm}^{-2} \text{ s}^{-1}$ (solid circles), and $\phi_o = 0.7 \text{ nm}^{-2} \text{ s}^{-1}$ (solid triangles). The flux of Ga_2O supplied, $\phi_{\text{Ga}_2\text{O}}$, corresponds to the vertical-axis intercepts at low T_G . (f) The growth rate (Γ) of $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ as a function of ϕ_o at a constant value of $\phi_{\text{Ga}_2\text{O}}$ given by the vertical-axis intercept at high ϕ_o . The gray and white areas in (f) indicate the Ga_2O -rich and O-rich flux regimes, respectively. T_G (in $^\circ\text{C}$) is indicated in the figures. The symbols are experimental data and the lines are model predictions according to Eqs. (2)–(7) and the parameters given in Table I for the *S*-MBE growth of $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ (solid symbols and lines), $\beta\text{-Ga}_2\text{O}_3(010)$ (hollow symbols and dashed lines), and bixbyite $\text{In}_2\text{O}_3(111)$ (hollow symbols with a dot in their center and dashed-dotted lines). The data in (a) are taken from Ref. [21].

with the data in Fig. 1(d)] establishes that the range of T_G within which high-quality films of In_2O_3 can be grown at high Γ is larger than that for Ga_2O_3 . This result is also similar to the growth of Ga_2O_3 and In_2O_3 by conventional MBE [13,15,18].

To model the growth of binary oxides (Me_xO_y) from their suboxides ($\text{Me}_x\text{O}_{y-x}$), we take the single-step

reaction kinetics of S -MBE [21] into account. Here, the growth takes place via the reaction



with constant κ describing the Me_xO_y formation rate. Adsorbate and solid phases are denoted as a and s , respectively. Based on the reaction given in Eq. (1), we set up a generalized growth-rate model describing the growth of these materials by S -MBE:

$$\frac{dn_r}{dt} = \phi_r - \kappa n_r n_o^x - \tau_r^{-1} n_r, \quad (2)$$

$$\frac{dn_o}{dt} = \varsigma \phi_o - x \kappa n_r n_o^x - \tau_o^{-1} n_o, \quad (3)$$

$$\frac{dn_p}{dt} = \Gamma = \kappa n_r n_o^x. \quad (4)$$

The surface densities of the adsorbed cationic reactants ($r = \text{Me}_x\text{O}_{y-x}$), O adsorbates, and formed products ($p = \text{Me}_x\text{O}_y$) are denoted as n_r , n_o , and n_p , respectively. Their time derivative is described by the operator d/dt . The surface lifetimes of r and O are given by τ_r and τ_o , respectively. The T_G -, orientation-, and growth-system-dependent sticking probability ς of O can be derived by considering two competing processes: the chemisorption of O and the desorption of O from the given adsorption sites, described by the reaction rates k_c and k_d , respectively,

$$k_i = \nu_i e^{-\frac{\varepsilon_i}{k_B T_G}}, \quad (5)$$

with $i = c, d$, frequency factor ν_i , and the respective energy barrier ε_i . The Boltzmann constant is denoted k_B . Following the Kisliuk model [30], the O sticking probability $0 \leq \varsigma \leq 1$ [31,32] is given by

$$\varsigma = \frac{k_c}{k_c + k_d} = \left(1 + \nu e^{-\frac{\delta\varepsilon}{k_B T_G}}\right)^{-1}, \quad (6)$$

with dimensionless prefactor $\nu = \nu_d/\nu_c$ and activation barrier $\delta\varepsilon = \varepsilon_d - \varepsilon_c$. In the case of a high O desorption barrier or a high O adsorption barrier, the limits of Eq. (6) are (i) $\varepsilon_d \gg \varepsilon_c \Rightarrow \delta\varepsilon \gg 0 \Rightarrow \varsigma \rightarrow 1$ and (ii) $\varepsilon_c \gg \varepsilon_d \Rightarrow \delta\varepsilon \ll 0 \Rightarrow \varsigma \rightarrow 0$, respectively, satisfying our conditions of $0 \leq \varsigma \leq 1$. Figure 2 depicts the model results of Eq. (6) of our model for Ga_2O_3 and In_2O_3 using the parameters given in Table I.

Solving Eqs. (2) and (3) with respect to n_r and n_o and inserting their solutions into Eq. (4) yields an analytical expression for Γ described by three kinetic parameters: κ , τ_r , and τ_o [see Eqs. (A1)–(A7)]. To reduce the complexity of the model, we assume that O adsorbate desorption is negligible and use $\kappa \gg \tau_o^{-1}$ and $\tau_r \ll \tau_o$. Assuming that the observed reaction processes follow a

TABLE I. Parameters ν , $\delta\varepsilon$, P_0 , and $\mathcal{E}$ obtained using an iterative approach of the growth model to the flux dependence of the growth rate (Γ) of Ga_2O_3 (201), Ga_2O_3 (010), and In_2O_3 (111) by S -MBE with Eqs. (2)–(7).

	ν	$\delta\varepsilon$ (eV)	P_0 (nm^2s^{-1})	$\mathcal{E}$ (eV)
$\beta\text{-Ga}_2\text{O}_3$ (201)	$e^{16.1 \pm 1}$	1.07 ± 0.1	$e^{0.15 \pm 0.05}$	0.12 ± 0.01
$\beta\text{-Ga}_2\text{O}_3$ (010)	$e^{16.6 \pm 1}$	1.20 ± 0.2	$e^{0.25 \pm 0.09}$	0.15 ± 0.03
In_2O_3 (111)	$e^{28.4 \pm 1}$	3.21 ± 0.5	$e^{0.90 \pm 0.10}$	0.25 ± 0.02

thermally activated Arrhenius behavior, we further reduce the complexity of our model by forming the product

$$P(T_G) = \tau_r \kappa = P_0 e^{\left(\frac{\mathcal{E}}{k_B T_G}\right)}, \quad (7)$$

with preexponential factor $P_0 = \tau_r^0 \kappa_0$ and activation energy $\mathcal{E} = \varepsilon_{\tau_r} - \varepsilon_{\kappa}$. The latter expression yields a larger κ or a longer τ_r the higher the growth rate Γ of the intended compound. This is in agreement with experiment as shown in Fig. 1.

We apply the solution of this model to the binary growth rate data of Ga_2O_3 and In_2O_3 by S -MBE depicted in Fig. 1 and extract the kinetic parameters summarized in Table I. To extract the parameters, we use an iterative approach. For example, for the growth of Ga_2O_3 by S -MBE, we first establish that the functional form of the equations accurately describes the growth of (201)-oriented $\beta\text{-Ga}_2\text{O}_3$ films, as plotted in Figs. 1(a) and 1(b). Having established that the functional form of the equations [solutions given by Eqs. (A1)–(A7)] accurately describes the growth of (201)-oriented $\beta\text{-Ga}_2\text{O}_3$ films, the model is next expanded to an additional orientation, (010) $\beta\text{-Ga}_2\text{O}_3$ films, using the data in Fig. 1(c).

A. Orientation-dependent growth rate of $\beta\text{-Ga}_2\text{O}_3$

As a quantitative result, we find that the range of T_G that can be used to produce high-quality epitaxial films at

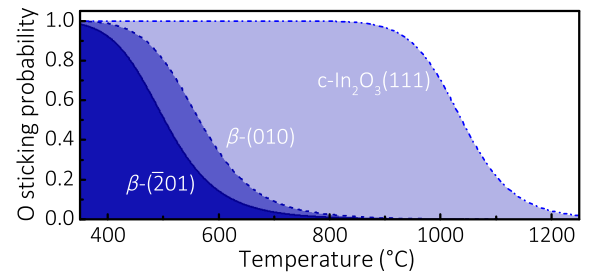


FIG. 2. The O sticking probability ς as a function of the growth temperature T_G . The solid, dashed, and dashed-dotted lines represent ς of $\beta\text{-Ga}_2\text{O}_3$ (201) (the dark-blue area), $\beta\text{-Ga}_2\text{O}_3$ (010) (the blue area), and bixbyite (cubic) $\text{c-In}_2\text{O}_3$ (111) (the pale-blue area), respectively. The lines are modeled by Eq. (6) using the parameters given in Table I for the respective phases and surface orientations.

high Γ (i.e., a growth window) of $\bar{(201)}$ -oriented Ga_2O_3 films is narrower than for the growth of (010) -oriented Ga_2O_3 films, which, in turn, is narrower than the one for the growth of (111) -oriented In_2O_3 films. This is because of the different reaction efficiencies, η , of Ga_2O and In_2O with active O species and resulting O reservoirs, depending on the specific growth surface and the specific growth system (more detailed explanation below in the text). In addition, we explain the different sticking probabilities ζ , e.g., as obtained for $\text{Ga}_2\text{O}_3(\bar{201})$ and $\text{Ga}_2\text{O}_3(010)$, by the activity of surface reactions between Ga_2O and O adsorbates being dependent on the orientation of the surface on which the reaction takes place. In other words, the reservoir of active atomic oxygen for Ga_2O oxidation on $\text{Ga}_2\text{O}_3(010)$ is larger than the one on $\text{Ga}_2\text{O}_3(\bar{201})$. This finding can be transferred to the growth of Ga_2O_3 by conventional MBE, where a similar dependence of Ga_2O_3 growth rate is observed. We propose that this Γ dependence results from an orientation-dependent activity of the oxidation of Ga_2O to Ga_2O_3 [14,20] and that the underlying reason is due to the orientation-dependent vertical and lateral bond strengths between ad-atoms and the substrate surfaces [28,29]. In Refs. [20,28,29], the orientation dependence of the growth rate on the (hkl) plane, $\Gamma_{(hkl)}$, is given for $\beta\text{-Ga}_2\text{O}_3$: $\Gamma_{(010)} > \Gamma_{(001)} > \Gamma_{(\bar{201})} > \Gamma_{(100)}$. We observe this same order of growth rate as a function of surface orientation for the growth of Ga_2O_3 by S -MBE and conclude that the orientation-dependent values of the sticking probability $\zeta_{(010)} > \zeta_{(001)} > \zeta_{(\bar{201})} > \zeta_{(100)}$ can be related to the orientation-dependent reaction activities of adsorbates, underlying the observed order of $\Gamma_{(hkl)}$ for $\beta\text{-Ga}_2\text{O}_3$ (see Fig. 2).

III. MOCATAXY COMBINED WITH S -MBE

We next describe the enhancement of the growth rate of Ga_2O_3 and In_2O_3 due to the presence of the catalysts In_2O and SnO , i.e., the combined effects of S -MBE and MOCATAXY. As depicted in Figs. 3(a)–3(c), we observe a drastic enhancement in Γ of heteroepitaxial $\beta\text{-Ga}_2\text{O}_3(\bar{201})$ grown on $\text{Al}_2\text{O}_3(0001)$ and homoepitaxial $\beta\text{-Ga}_2\text{O}_3(010)$ grown on $\beta\text{-Ga}_2\text{O}_3(010)$ using the suboxides In_2O and SnO as catalysts. The catalytic effect of SnO on the growth rate of Ga_2O_3 is stronger than that of In_2O . It is also stronger for the growth of $\beta\text{-Ga}_2\text{O}_3(\bar{201})$ (solid symbols) than for the growth of $\beta\text{-Ga}_2\text{O}_3(010)$ (hollow symbols). The stronger catalytic effect of SnO compared with In_2O can be explained by their different vapor pressures, i.e., $P_{\text{SnO}} < P_{\text{In}_2\text{O}}$ [33–35]. Thus, under similar growth conditions, the surface lifetime of SnO is longer than that of In_2O . Hence, SnO can be reoxidized more often than In_2O [5,17] and the O reservoir that ultimately ends up oxidizing Ga_2O in the presence of SnO is larger than that for Ga_2O oxidation in the presence of In_2O . Figures 3(d)–3(f)

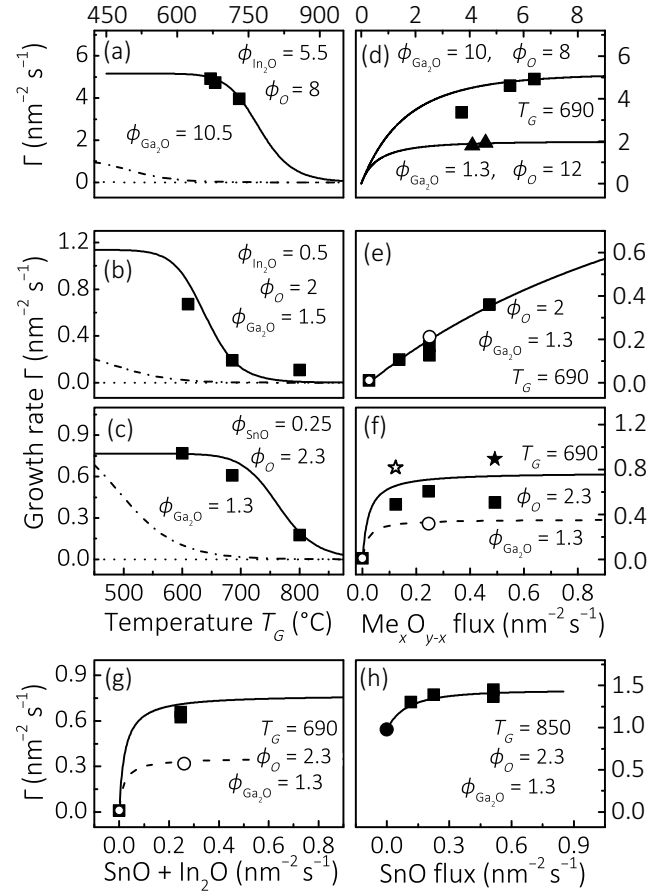


FIG. 3. (a)–(c) The growth rate (Γ) of $\beta\text{-Ga}_2\text{O}_3(\bar{201})$ as a function of T_G in the presence of either the catalyst In_2O or SnO at the steady-state fluxes given. (d)–(g) The growth rate (Γ) of $\beta\text{-Ga}_2\text{O}_3(\bar{201})$ (solid symbols) and $\beta\text{-Ga}_2\text{O}_3(010)$ (hollow symbols) as a function of the In_2O flux as a catalyst [panels (d) and (e)], SnO flux as a catalyst [panel (f)], and their sum $a\text{In}_2\text{O} + (1 - a)\text{SnO}$ as competing catalysts (with $a = 0.5$) [panel (g)]. (h) The growth rate (Γ) of bixbyite $\text{In}_2\text{O}_3(111)$ using SnO as a catalyst. The solid lines are model predictions by the catalytic model, Eqs. (10)–(16). The parameters used for our model predictions are given in Table II. The dashed-dotted and dotted lines depict the model predictions for the growth of $\beta\text{-Ga}_2\text{O}_3$ by S -MBE [Eqs. (2)–(7)] and conventional MBE [36] in the absence of a catalyst, respectively. The units of the fluxes given in the figures are nm⁻² s⁻¹; the temperatures T_G are in °C. The values of ϕ_o correspond to the maximum available active atomic oxygen provided by the catalyst (i.e., In_2O or SnO). Additional characterizations of the sample grown at the conditions depicted by the solid star in (f) are provided in Fig. 4.

depict Γ of Ga_2O_3 as a function of $\phi_{\text{In}_2\text{O}}$ and ϕ_{SnO} , respectively. When SnO is used as a catalyst, it is evident from the data that the catalytic effect on $\text{Ga}_2\text{O}_3(\bar{201})$ is stronger than it is on $\text{Ga}_2\text{O}_3(010)$. As shown below in Eq. (16), the catalytic activity, α , decreases with an increasing O flux. Therefore, the weaker catalytic effect observed on $\beta\text{-Ga}_2\text{O}_3(010)$ compared with the effect on $\beta\text{-Ga}_2\text{O}_3(\bar{201})$

may be explained by the higher surface-dependent sticking probability $\zeta_{(010)} > \zeta_{(\bar{2}01)}$ (values are given in Table I). Further studies on the atomic incorporation and surface segregation of residual Sn and In in the grown thin films, when using SnO and In₂O as catalysts, respectively, need to be performed. Nevertheless, energy-dispersive x-ray spectroscopy (EDXS), secondary-ion mass spectrometry (SIMS), and atomic probe tomography (APT) have already shown that the concentrations of In [5,18,24] and Sn [22] in Ga₂O₃ as well as in (Al_xGa_{1-x})₂O₃ films are below 1%. This is consistent with our x-ray diffraction (XRD) results, showing only diffraction peaks from Ga₂O₃ in the thin films, an example of which is shown in Fig. 4.

A comparison of Figs. 3(f) and 3(g) reveals that the growth rates Γ of β -Ga₂O₃($\bar{2}01$) and β -Ga₂O₃(010) using solely SnO and SnO + In₂O as catalysts are very similar (under otherwise identical growth conditions). We thus conclude that SnO suppresses In₂O as a catalyst, i.e., the catalytic effects are not additive: the presence of SnO inhibits (or isolates) the catalytic activity of In₂O in the SnO—In₂O—Ga₂O—O system. We predict the same effect for MOCATAXY by conventional MBE, i.e., when using the elemental catalysts In [5] and Sn [22] in combination for the growth of Ga₂O₃ in the Sn—In—Ga—O system.

Figure 3(h) shows the catalytic effect of SnO on Γ of In₂O₃(111) grown on Al₂O₃(0001) substrates. The solid circle in Fig. 3(h) corresponds to the growth rate of In₂O₃ determined by x-ray reflectivity (XRR) in the absence of SnO. In the presence of SnO, the growth rate of In₂O₃ (again measured by XRR) is seen to increase by a factor of approximately 1.4, i.e., far larger than the effect caused by additional SnO incorporation into In₂O₃. SIMS [37] and x-ray fluorescence (XRF) [37] are used to quantify the Sn content present in the In₂O₃ films grown with the SnO catalyst. A value of approximately 3% Sn in In₂O₃ is observed by SIMS and XRF independent of the SnO fluxes in the (0.2–0.5) nm⁻² s⁻¹ range.

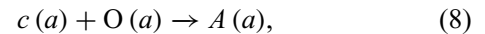
This result indicates that SnO increases the available O reservoir for the oxidation of In₂O to In₂O₃ by a factor of approximately 1.4 (at these growth conditions). This finding is in line with the data plotted in Figs. 3(f) and 3(g), i.e., that SnO has a higher reactivity with O than In₂O. We explain the catalytic action of SnO on In₂O by their different vapor pressures $P_{\text{SnO}} < P_{\text{In}_2\text{O}}$ [33–35]. Thus, SnO provides a larger O reservoir for In₂O oxidation than is available in the absence of SnO. The In₂O—SnO—O system is the first catalytic system observed for MBE growth beyond Ga₂O₃-based systems [5,18,22–25]. The discovery of MOCATAXY during *S*-MBE and its extension to In₂O₃ suggests its universality for the MBE growth of a multitude of oxide compounds (during *S*-MBE as well as conventional MBE).

We explain the observed catalysis during the growth of Ga₂O₃ and In₂O₃ by *S*-MBE by the formation of a

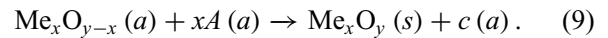
metastable adlayer *A* between the catalyst *c* and O, e.g., *A* = In₂O—O or *A* = SnO—O. As experimentally and mathematically shown by Fig. 1, Table I, and Eqs. (2)–(6), In₂O possesses a higher surface reactivity with active O than does Ga₂O, leading to a higher growth rate of In₂O₃ compared with Ga₂O₃ at comparable growth conditions. This behavior is similar to the growth of Ga₂O₃ and In₂O₃ by conventional MBE [13,16], which has been explained by the different oxidation efficiencies η of the elements Sn, In, and Ga following the order $\eta_{\text{Sn}} \approx 1.1$ $\eta_{\text{In}} \approx 3.1$ η_{Ga} [5,13,17]. Taking the ratio of maximum available O for Ga₂O and In₂O oxidation [data plotted in Figs. 1(b) and 1(d) and flux conversions given in Eqs. (A11)] from mixtures of O₂ and 10% O₃ [38] at a background pressure of 1×10^{-6} Torr, we obtain $\eta_{\text{In}_2\text{O}} \approx 2.8$ $\eta_{\text{Ga}_2\text{O}}$. This result is very similar to $\eta_{\text{In}} \approx 2.8$ η_{Ga} [5,13,17] observed during conventional MBE growth. We surmise, following Ref. [17], that the same value of η observed during MOCATAXY in conventional MBE and *S*-MBE arises from what is the second reaction step of conventional MBE and the sole reaction step of *S*-MBE, where the suboxide reacts with O to complete the formation of the intended oxide (e.g., Ga₂O → Ga₂O₃) [18] and *not* to the suboxide-formation step (e.g., Ga → Ga₂O) [18]. Thus, for the discussion and analysis that follow, we use $\eta_{\text{SnO}} \approx 1.1$ $\eta_{\text{In}_2\text{O}} \approx 3.1$ $\eta_{\text{Ga}_2\text{O}}$ during *S*-MBE. These oxidation efficiencies follow the same order in η as has been observed for growth by conventional MBE [5,17].

A. Generalized metal-exchange catalytic model

We propose that the role of the catalyst *c* (e.g., In₂O, SnO, In [5], or Sn [22]) is to increase the O adsorbate reservoir of the reactant *r* (e.g., Ga₂O or Ga) by forming *A* through the reaction



with examples of *A* being In₂O—O, In—O, SnO—O, or Sn—O. In the presence of *r*, *A* is unstable and catalyzes the incorporation of *r* into the intended product *p* (e.g., Ga₂O₃), while decreasing the reaction barrier of *r* with O. Thus, the reaction given in Eq. (8) is subsequently followed by the reaction



Equation (9) describes the consumption of *A* while forming the product (*p* = Me_xO_y) and releasing *c* on the growth surface. The catalyst *c* may be reoxidized [5], leading to an increase in the available O reservoir for the reactant (*r* = Me_xO_{y-x}) and thus to an extension of the kinetic and thermodynamic limits to the formation of *p*.

An adlayer formed by In has also been observed during the formation of GaN using In as a surface active agent (surfactant) [3]. Here, the In adlayer enables an enhanced

diffusion channel for the Ga and N adsorbates. Moreover, a surface instability of In—O bonds in the presence of Fe [39] and Ga [5] has been observed during conventional MBE. We emphasize, however, that the catalytic effect we are describing must not be confused with effects resulting from surfactants during the growth of III-V compounds by conventional MBE [2–4].

In order to describe MOCATAXY for elemental (e.g., In [5] and Sn [22]) and molecular catalysts (e.g., In₂O and SnO) as well as for different materials (e.g., Ga₂O₃ and In₂O₃) mathematically, we would have to take into account the surface populations of c , r , and atomic O together with the surface density of the p that forms following the Langmuir-Hinshelwood mechanism [40]. We may reduce the complexity of the model significantly by only taking into account the most likely reactions involved in the formation of p , following the Eley-Rideal formalism [41]. The resulting set of coupled differential equations reads as follows:

$$\frac{dn_c}{dt} = \phi_c - \sigma n_c(1 - \theta_A)\phi_o + \alpha\phi_r\theta_A - \gamma_c n_c, \quad (10)$$

$$\frac{d\theta_A}{dt} = \sigma n_c(1 - \theta_A)\phi_o - \alpha\phi_r\theta_A, \quad (11)$$

$$\frac{dn_p}{dt} \equiv \Gamma = \alpha\phi_r\theta_A, \quad (12)$$

with the adatom density n_c and desorption-rate constant γ_c of the catalyst c , as well as the surface coverage θ_A of A . The second and third terms in Eq. (10) refer to the formation rates of A and p , respectively, and the factor $(1 - \theta_A)$ assures that A constitutes a surface phase. The last term in Eq. (10) accounts for the desorption of c from the growth surface and σ (with the dimension of nm²) represents the cross section of colliding c with O [5]. The impinging fluxes of c and r are denoted as ϕ_c and ϕ_r , respectively. We note that the structure of the model introduced here is similar to the MEXCAT model given in Ref. [5]. The improvement of the model given in this work and its generalization to elemental and molecular catalysts arises by taking a cationiclike, metastable adlayer A into account. This allows MOCATAXY to be described for the growth of ternary systems involving molecular catalysts [e.g., In₂O (Fig. 3) and SnO (Fig. 3)] as well as elemental catalysts [e.g., In (Fig. 5) and Sn (Fig. 5)].

B. Suboxide catalysts

Our results thus indicate that MOCATAXY takes place with a suboxide catalyst (e.g., for A being In₂O—O or SnO—O) and *not* with an elemental catalyst (e.g., for A being In—O or Sn—O). For conventional MBE, i.e., when using elemental source materials, we assume that the reaction of the metal to form the suboxide (e.g., $2\text{Ga} + \text{O} \rightarrow \text{Ga}_2\text{O} = r$) occurs very rapidly [36] and, thus, the catalysis takes place between the suboxide reactant r and A ,

satisfying the reactions given in Eqs. (8) and (9). Should the reaction of $2\text{Ga} + \text{O} \rightarrow \text{Ga}_2\text{O}$ not occur very rapidly, we would see Ga desorption (at least a fraction of it), and a plateau in Γ in the adsorption-controlled regime during the growth of Ga₂O₃ by conventional MBE; similar to the Γ plateau observed, e.g., during the growth of GaN by conventional MBE [8]. The subsequent desorption of the rapidly formed Ga₂O is the growth-rate-limiting step in conventional MBE, as it removes active O from the growth front (by forming Ga₂O), leading to the decrease in Γ in the adsorption-controlled regime as well as at elevated T_G [12,17,36]. In S -MBE, the formation of Ga₂O (through $2\text{Ga} + \text{O} \rightarrow \text{Ga}_2\text{O}$) is bypassed since Ga₂O is directly provided from the source. Therefore, the O-consuming step is now avoided and a plateau in Γ of Ga₂O₃ in the adsorption-controlled regime occurs [21]. The assumption that MOCATAXY takes place with a suboxide catalyst is further supported by our finding in this work that the oxidation efficiency η for In₂O and Ga₂O during MOCATAXY by S -MBE follows the same order in η as for Ga and In during conventional MBE, i.e., $\eta_{\text{In}_2\text{O}} = 2.8\eta_{\text{Ga}_2\text{O}}$ for S -MBE (this work) versus $\eta_{\text{In}} = 2.8\eta_{\text{Ga}}$ for conventional MBE [5,17]. Nevertheless, we emphasize that the microscopic origin and reaction pathways of MOCATAXY during S -MBE and conventional MBE require further investigation to fully understand which species are indeed involved, leading to the observed catalysis given in this work and presented in Refs. [5,17,18,22–27].

The solution of Eqs. (10) and (11) with respect to n_c and θ_A yields $\phi_c = \gamma_c n_c$, consistent with our observation of negligible incorporation (approximately 3%) of c into the grown thin films for the data plotted in Fig. 3. Insertion of the solution for θ_A into Eq. (12) yields the following expression:

$$\Gamma = \frac{\alpha\phi_c\phi_r\phi_o}{\alpha J\phi_r + \phi_c\phi_o}. \quad (13)$$

The free parameters are the pseudoflux

$$J = \frac{\gamma_c}{\sigma} = J_0 \exp\left(-\frac{\Delta}{k_B T_G}\right), \quad (14)$$

with $J_0 = 1 \times 10^{14} \text{ nm}^{-2} \text{ s}^{-1}$ (assumed for all species as a first approximation [31]) and energy Δ . The value of Δ depends linearly on ϕ_c (e.g., $\phi_{\text{In}_2\text{O}}$ and ϕ_{SnO}),

$$\Delta(\phi_c) = \Delta_0 + \delta\phi_c, \quad (15)$$

with Δ_0 denoting the evaporation enthalpy, e.g., of In₂O and SnO, and δ describing its increase with increasing ϕ_c . The other free parameter is the catalytic activity coefficient, α . For α (ranging from 1 to 0), we use a linear

TABLE II. The values of Δ_0 , δ , and b used in Eqs. (15) and (16) for different catalytic systems and growth surfaces.

	Δ_0 (eV)	δ (meV nm ² s)	b (nm ² s)
β -Ga ₂ O ₃ ($\bar{2}01$):In ₂ O	2.6 ± 0.05 [34]	30 ± 2	0.07 ± 0.01
β -Ga ₂ O ₃ (010):In ₂ O	2.6 ± 0.05 [34]	30 ± 2	0.07 ± 0.01
β -Ga ₂ O ₃ ($\bar{2}01$):SnO	2.9 ± 0.05 [33]	50 ± 4	0.20 ± 0.03
β -Ga ₂ O ₃ (010):SnO	2.9 ± 0.05 [33]	10 ± 1	0.33 ± 0.05
In ₂ O ₃ (111):SnO	3.2 ± 0.05	400 ± 10	0.33 ± 0.05

approximation depending on impinging ϕ_o , i.e.,

$$\alpha(\phi_o) = 1 - b\phi_o, \quad (16)$$

with b describing the decrease of α with ϕ_o . By an iterative approach of our model to the experimental growth-rate data, the values obtained of Δ_0 , δ , and b for In₂O and SnO are given in Table II.

The evaporation enthalpies Δ_0 of In₂O and SnO on Ga₂O₃ surfaces correspond to the values given in the literature, as noted in Table II. Only the value of Δ_0 for SnO on the In₂O₃(111) surface is slightly above the literature value, indicating an additional energy term caused by vertical and lateral interactions between adsorbed species and the In₂O₃(111) surface. The increase in Δ with ϕ_c , described by the parameter δ , indicates an increase in the lateral adsorbate binding energy with increasing $\phi_c \propto n_c$. An analogous behavior has also been observed for the desorption kinetics of In on Ga₂O₃ [5] and Ga on GaN [42]. We explain the linear decrease of α with ϕ_o by a linear increase of O adsorbates with ϕ_o , i.e., $\phi_o \propto n_o$. It has been shown that an increase in ϕ_o promotes the incorporation of In during the growth of (In_xGa_{1-x})₂O₃ by conventional MBE; this decreases the catalytic strength of In for the formation of Ga₂O₃ [5,16,17,29]. We therefore explain the decrease in α with increasing $\phi_o \propto n_o$ by a decreasing diffusion length of c and r and, thus, a decrease in the probability of the reaction given in Eq. (9) occurring.

C. Elemental catalysts

We apply the above model to the data published in Refs. [5] and [22] for MOCATAXY during conventional MBE growth of Ga₂O₃, i.e., using elemental In and Sn as catalysts (see the Appendix). For the former, our model and the parameters given in this paper can describe the data published in Ref. [5] with the same accuracy. For the latter, we introduce a mathematical description of a catalytic system involving the element Sn (see the Appendix). These results, and the comparison among different MBE variants (i.e., S -MBE and conventional MBE), confirm the accuracy of our refined and generalized MEXCAT model, describing MOCATAXY for elemental and molecular catalysts.

D. Obtained “pseudo” β -Ga₂O₃/Al₂O₃

As a result of combining S -MBE with MOCATAXY, in Figs. 4(a)–4(d), we demonstrate an previously unknown “pseudo” β -Ga₂O₃($\bar{2}01$)/Al₂O₃(0001) heterostructure with unparalleled crystalline perfection. Figure 4(a) shows θ - 2θ XRD scans of a 90-nm-thick SnO-catalyzed Ga₂O₃ film (black trace) and a 40-nm-thick noncatalyzed Ga₂O₃ film grown by S -MBE under similar growth conditions ($T_G = 500^\circ\text{C}$, $\phi_{\text{Ga}_2\text{O}} = 0.9 \text{ nm}^{-2} \text{ s}^{-1}$, and $\phi_o = 2.3 \text{ nm}^{-2} \text{ s}^{-1}$). The SnO-catalyzed Ga₂O₃ film is the same film that is plotted in Fig. 3(f) as a solid-black star. It is grown at $T_G = 690^\circ\text{C}$, $\phi_{\text{Ga}_2\text{O}} = 1.3 \text{ nm}^{-2} \text{ s}^{-1}$, and $\phi_o = 2.3 \text{ nm}^{-2} \text{ s}^{-1}$. The reflections of the noncatalyzed Ga₂O₃ thin film coincide with the β -Ga₂O₃($\bar{2}01$) phase grown with its ($\bar{2}01$) plane parallel to the (0001) plane of the Al₂O₃ substrate. In contrast, the XRD scan of the SnO-catalyzed Ga₂O₃ film shows only the even reflections of the β -Ga₂O₃ phase grown with its ($\bar{2}01$) plane parallel to the (0001) plane of the Al₂O₃ substrate. We speculate that the “pseudo” β -Ga₂O₃($\bar{2}01$)/Al₂O₃(0001) contains an aperiodic occurrence of low-energy stacking faults, parallel to the ($\bar{2}01$) plane of the Ga₂O₃ film, that reduce the number of the observed XRD diffraction peaks of the “pseudo” β -Ga₂O₃($\bar{2}01$) phase. This hypothesis is consistent with calculations showing that the stacking fault energy in β -Ga₂O₃ is low [43,44], experimental observation of high densities of stacking faults in β -Ga₂O₃ films [45], and the scanning transmission electron microscopy (STEM) image depicted in Fig. 4(b). The epilayer shows a single-crystalline structure with an abrupt interface to the Al₂O₃(0001) substrate at the bottom of the image. Figure 4(c) shows a transverse scan (rocking curve) across the symmetric 402 reflection of the same “pseudo” β -Ga₂O₃($\bar{2}01$) film. The measured full width at half maximum (FWHM) is just $\Delta\omega \approx 10$ arcsec; this is a measure of the out-of-plane mosaic spread of the thin film. Figure 4(d) depicts an atomic force microscope (AFM) image of the surface morphology of the same SnO-catalyzed Ga₂O₃ film; it has a root-mean-square (rms) roughness of 2.5 Å. The obtained rocking curve of $\Delta\omega \approx 10$ arcsec and smooth surface morphology of rms = 2.5 Å provide the best results obtained for any Ga₂O₃ thin film grown on Al₂O₃(0001) by any method [14,46–49]. We point out that optimizations utilizing the unprecedented growth regimes—becoming accessible by the combination

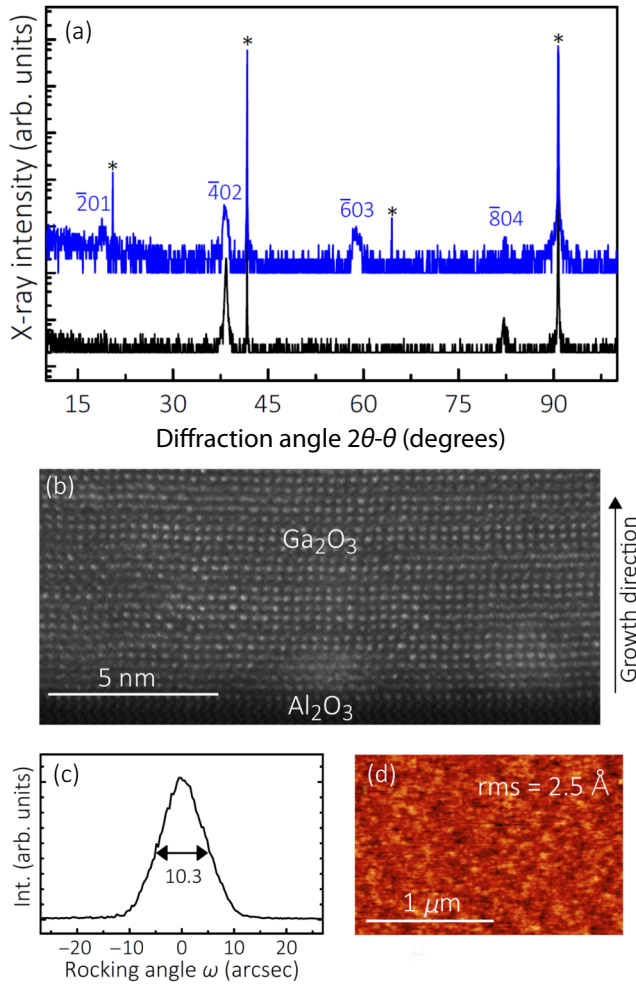


FIG. 4. (a) Longitudinal XRD scans recorded from an SnO-catalyzed Ga_2O_3 film (black trace) and a noncatalyzed $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ film (blue trace) grown by *S*-MBE on $\text{Al}_2\text{O}_3(0001)$ substrates. Reflections labeled by an asterisk originate from the substrate. The reflections from the Ga_2O_3 films are marked in the figure. (b) A STEM image along the $[100]$ -zone axis of the Ga_2O_3 thin film. (c) A transverse XRD scan across the $\bar{4}02$ peak of the same SnO-catalyzed Ga_2O_3 film [black trace in (a)], with its full width at half maximum indicated in the figure. (d) The surface morphology of the same SnO-catalyzed Ga_2O_3 film; it has a rms roughness of $2.5 \text{ \AA}$. The data depicted in (a) [black trace], (b), (c), and (d) are taken from the same Ga_2O_3 film plotted by the solid star in Fig. 3(f). Int., intensity.

of *S*-MBE with MOCATAXY—still need to be performed to further improve the crystalline perfection of the grown Ga_2O_3 -based heterostructures.

We note that in the absence of a catalyst, Ga_2O_3 does not form at this high T_G of 690°C . In addition, at a lower catalyst flux of SnO [depicted as the open star in Fig. 3(f)] compared with the sample grown at a higher SnO flux [depicted as the solid star in Figs. 3(f) and 4], we do not measure the “pseudo” $\beta\text{-Ga}_2\text{O}_3(201)$ phase, but instead see the “conventional” $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ peaks by XRD (data not shown

in this work). We therefore conclude that extending the kinetic (e.g., higher possible T_G) and thermodynamic limits (e.g., different surface chemical potential) by combining *S*-MBE with MOCATAXY benefits the formation of the “pseudo” $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)/\text{Al}_2\text{O}_3(0001)$ heterostructure that has unparalleled crystalline perfection.

IV. CONCLUSION

As we demonstrate, the nature of the model derived to describe MOCATAXY using elemental and molecular catalysts does *not* depend on the specific growth surface. We note, however, that the growth surface may change the kinetic parameters used in our model, as shown for the examples of $\beta\text{-Ga}_2\text{O}_3(\bar{2}01)$ and $\beta\text{-Ga}_2\text{O}_3(010)$ using In_2O or SnO as catalysts in this work.

Finally, the increase in the growth rates of Ga_2O_3 and In_2O_3 by *S*-MBE that occurs when using the catalysts SnO and In_2O demonstrates MOCATAXY as a potentially inherent feature in conventional MBE growth [5, 18, 22–25] as well as in *S*-MBE growth. Furthermore, our results provide deeper insight into this catalysis, indicating that MOCATAXY occurs through a suboxide catalyst rather than with an elemental catalyst. This more broad applicability of MOCATAXY opens an unprecedented path for the epitaxial synthesis of thin films by intentionally extending the kinetic and thermodynamic limits during their growth processes. If successful, this could enable the growth of (yet) unknown crystal phases and unprecedented functional electronic materials.

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TABLE III. The values of Δ_0 and δ used in Eq. (14) (main text) for the catalytic model when using In and Sn as catalysts.

	Δ_0 (eV)	δ (meV nm ² s)
Ga ₂ O ₃ :In	2.42 ± 0.05 [50]	41 ± 2
Ga ₂ O ₃ :Sn	2.91 ± 0.07 [33]	10 ± 2

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APPENDIX

We apply the generalized MOCATAXY model, Eqs. (10)–(16), to published catalytic data using elemental In [5] and elemental Sn [22] as catalysts for the growth of Ga₂O₃ by MBE. The parameters used in Eqs. (15) for In and Sn are collected in Table III. Within experimental uncertainty, the obtained Δ_0 corresponds to the vaporization enthalpies of elemental In [50] and Sn [33] as given in the literature; the values are given in Table III. Moreover, for our model, we use $\alpha = 1$ (the catalytic activity), the same value of α as used in Ref. [5].

Figures 5(a) and 5(b) show our results for the growth of Ga₂O₃ by MBE when supplying In and Sn as elemental catalysts, respectively. Our model drawn in Fig. 5(a) (solid lines) describes the data published in Ref. [5] with the same accuracy as the previously established MEXCAT model [5]. Figure 5(b) plots the catalyzed growth rate data of Ga₂O₃ taken from Ref. [22]. Our model applied to this data is drawn as the solid line. It precisely describes the Sn-catalyzed growth of Ga₂O₃ by MBE and it provides a quantitative description of MOCATAXY using Sn as a catalyst. To model the Sn-catalyzed data, we linearly

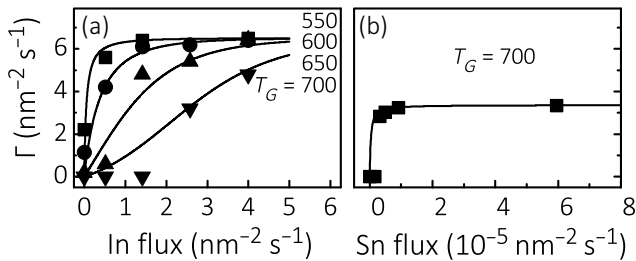


FIG. 5. (a) The growth rate (Γ) of Ga₂O₃ as a function of the In flux at different growth temperatures T_G and an active atomic oxygen flux $\phi_o = 19.2 \text{ nm}^{-2} \text{ s}^{-1}$. The data are taken from Ref. [5]. (b) The Γ of Ga₂O₃ as a function of the Sn flux, with $\phi_o = 7.5 \text{ nm}^{-2} \text{ s}^{-1}$ used for the model. The data are taken from Ref. [22]. Model predictions by Eqs. (10)–(16) are drawn as solid lines using the kinetic parameters given in Table III. The unit of the T_G values given is °C.

extrapolate the value of ϕ_o^{Sn} given in Eq. (A13) while using the O flux conditions published in Ref. [22].

To conclude, our model introduced in the main text is able to describe the growth of Ga₂O₃ and In₂O₃ by *S*-MBE as well as conventional MBE when using elemental and molecular catalysts. This is achieved by introducing a cationiclike, catalytic adlayer *A*.

1. Detailed model of the growth of III-VI materials by *S*-MBE

The analytical solution of the growth rate, Γ , of Eqs. (2)–(4) for III-VI compound materials is as follows:

$$\Gamma = \left[\zeta_-^2 P^2 + \xi_-^{\frac{2}{3}} - P \left(3 - 2\zeta_+ \xi_-^{\frac{1}{3}} \right) \right] \times \left[\zeta_-^2 P^2 + \xi_-^{\frac{2}{3}} - P \left(3 - \zeta_- \xi_-^{\frac{1}{3}} \right) \right] \times \left(-54P\xi_+ \right)^{-1}, \quad (\text{A1})$$

with

$$\zeta_+ = 2\phi_r - \varsigma\phi_o, \quad (\text{A2})$$

$$\zeta_- = -2\phi_r + \varsigma\phi_o, \quad (\text{A3})$$

$$\xi_+ = \left(\zeta_+ P - 9P\psi - \sqrt{27\Psi} \right)^3, \quad (\text{A4})$$

$$\xi_- = - \left(\zeta_- P + 9P\psi + \sqrt{27\Psi} \right)^3, \quad (\text{A5})$$

$$\psi = \phi_r + \varsigma\phi_o, \quad (\text{A6})$$

and

$$\Psi = P^3 \left[1 + \zeta_-^3 P^2 \varsigma\phi_o + P \times \left(-\phi_r^2 + 10\varsigma\phi_r\phi_o + 2\varsigma^2\phi_o^2 \right) \right]. \quad (\text{A7})$$

The growth rates of Ga₂O₃ and In₂O₃ as presented in Fig. 1 are explicitly modeled with Eqs. (A1)–(A7).

2. Detailed model of the growth IV-VI materials by *S*-MBE

The analytical solution for Γ of Eqs. (2)–(4) for IV-VI compound materials is as follows:

$$\Gamma = \frac{1 + P\psi_+ - \sqrt{1 + 2P\psi_+ + P^2\psi_-^2}}{2P}, \quad (\text{A8})$$

with

$$\psi_{\pm} = \phi_r \pm \varsigma\phi_o. \quad (\text{A9})$$

We predict that the Γ of IV-VI materials (e.g., SnO₂)—obtained by *S*-MBE—may be modeled by Eqs.

(A8) and (A9) with the same accuracy as the Γ modeled for III-VI materials (e.g., Ga_2O_3 and In_2O_3) by Eqs. (A1)–(A7); this is demonstrated in the main text.

3. Conversion factors for ϕ_r and ϕ_o

The model uses reactant fluxes, ϕ_r (e.g., Ga_2O , In_2O , SnO , Ga, In, Sn) and active atomic oxygen fluxes, ϕ_o (from active O_3 or O species), in $\text{nm}^{-2} \text{s}^{-1}$.

The conversion factors for S -MBE used in an ozone MBE system are as follows:

$$\begin{aligned}\phi_{\text{Ga}_2\text{O}}^{\text{QCM}} &= 1 \text{ Å s}^{-1} \rightarrow \phi_{\text{Ga}_2\text{O}} = 0.38 \text{ nm}^{-2} \text{ s}^{-1}, \\ \phi_{\text{In}_2\text{O}}^{\text{QCM}} &= 1 \text{ Å s}^{-1} \rightarrow \phi_{\text{In}_2\text{O}} = 0.25 \text{ nm}^{-2} \text{ s}^{-1}, \\ \phi_{\text{SnO}}^{\text{QCM}} &= 1 \text{ Å s}^{-1} \rightarrow \phi_{\text{SnO}} = 0.45 \text{ nm}^{-2} \text{ s}^{-1},\end{aligned}\quad (\text{A10})$$

$$\begin{aligned}P_{\text{O}}^{\text{Ga}_2\text{O}} &= 1 \times 10^{-6} \text{ Torr} \rightarrow \phi_{\text{O}}^{\text{Ga}_2\text{O}} = 0.73 \text{ nm}^{-2} \text{ s}^{-1}, \\ P_{\text{O}}^{\text{In}_2\text{O}} &= 1 \times 10^{-6} \text{ Torr} \rightarrow \phi_{\text{O}}^{\text{In}_2\text{O}} = 2.05 \text{ nm}^{-2} \text{ s}^{-1}, \\ P_{\text{O}}^{\text{SnO}} &= 1 \times 10^{-6} \text{ Torr} \rightarrow \phi_{\text{O}}^{\text{SnO}} = 2.25 \text{ nm}^{-2} \text{ s}^{-1}.\end{aligned}\quad (\text{A11})$$

The reactant fluxes, ϕ_r^{QCM} , are measured prior to growth by a quartz-crystal microbalance (QCM) in Å s^{-1} , with the density of the QCM set to 1 g cm^{-3} . These QCM readings are readily converted to absolute fluxes using the known masses of the Ga_2O , In_2O , and SnO molecules that condense onto the QCM. The active atomic oxygen fluxes given result from an oxidant, P_{O}^r , with mixtures of O_2 and approximately 10% O_3 in the oxygen molecular beam [38]. The different oxidation efficiencies are taken from Ref. [17] while using the results obtained for S -MBE.

The conversion factors for conventional MBE used in an oxygen-plasma-assisted MBE system are as follows:

$$\begin{aligned}P_{\text{Ga}}^{\text{BEP}} &= 1 \times 10^{-7} \text{ Torr} \rightarrow \phi_{\text{Ga}} = 1.2 \text{ nm}^{-2} \text{ s}^{-1}, \\ P_{\text{In}}^{\text{BEP}} &= 1 \times 10^{-7} \text{ Torr} \rightarrow \phi_{\text{In}} = 0.6 \text{ nm}^{-2} \text{ s}^{-1}, \\ P_{\text{Sn}}^{\text{BEP}} &= 1 \times 10^{-7} \text{ Torr} \rightarrow \phi_{\text{Sn}} = 1.5 \text{ nm}^{-2} \text{ s}^{-1},\end{aligned}\quad (\text{A12})$$

$$\begin{aligned}\phi_{\text{O}}^{\text{Ga}} &= 1 \text{ SCCM} \rightarrow \phi_{\text{O}}^{\text{Ga}} = 9.8 \text{ nm}^{-2} \text{ s}^{-1}, \\ \phi_{\text{O}}^{\text{In}} &= 1 \text{ SCCM} \rightarrow \phi_{\text{O}}^{\text{In}} = 27.4 \text{ nm}^{-2} \text{ s}^{-1}, \\ \phi_{\text{O}}^{\text{Sn}} &= 1 \text{ SCCM} \rightarrow \phi_{\text{O}}^{\text{Sn}} = 30.1 \text{ nm}^{-2} \text{ s}^{-1}.\end{aligned}\quad (\text{A13})$$

The beam-equivalent pressure (BEP), P_r^{BEP} , of the reactant fluxes is measured prior to growth by an ion gauge in 10^{-7} Torr . P_r^{BEP} is converted from a pressure into a flux using the kinetic theory of gases [51]. The oxygen flux, ϕ_{O}^r , is measured in standard cubic centimeters per minute (SCCM) and a radio-frequency plasma power of 300 W is

applied. The conversion factors are taken from Ref. [17] and applied to the data given in Ref. [22]. We note that the conversion factors [17] and data [22] are obtained in different MBE systems. Thus, the actual conversion may differ slightly due to the different geometries of the MBE systems used. Nevertheless, the use of the same conversion factors for different MBE systems is a practical and reasonable approach.

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