

## Original Research Article

# Comparative functional genomics identifies an iron-limited bottleneck in a *Saccharomyces cerevisiae* strain with a cytosolic-localized isobutanol pathway



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## ABSTRACT

Metabolic engineering strategies have been successfully implemented to improve the production of isobutanol, a next-generation biofuel, in *Saccharomyces cerevisiae*. Here, we explore how two of these strategies, pathway re-localization and redox cofactor-balancing, affect the performance and physiology of isobutanol producing strains. We equipped yeast with isobutanol cassettes which had either a mitochondrial or cytosolic localized isobutanol pathway and used either a redox-imbalanced (NADPH-dependent) or redox-balanced (NADH-dependent) ketol-acid reductoisomerase enzyme. We then conducted transcriptomic, proteomic and metabolomic analyses to elucidate molecular differences between the engineered strains. Pathway localization had a large effect on isobutanol production with the strain expressing the mitochondrial-localized enzymes producing 3.8-fold more isobutanol than strains expressing the cytosolic enzymes. Cofactor-balancing did not improve isobutanol titers and instead the strain with the redox-imbalanced pathway produced 1.5-fold more isobutanol than the balanced version, albeit at low overall pathway flux. Functional genomic analyses suggested that the poor performances of the cytosolic pathway strains were in part due to a shortage in cytosolic Fe-S clusters, which are required cofactors for the dihydroxyacid dehydratase enzyme. We then demonstrated that this cofactor limitation may be partially recovered by disrupting iron homeostasis with a *fra2* mutation, thereby increasing cellular iron levels. The resulting isobutanol titer of the *fra2* null strain harboring a cytosolic-localized isobutanol pathway outperformed the strain with the mitochondrial-localized pathway by 1.3-fold, demonstrating that both localizations can support flux to isobutanol.

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## 1. Introduction

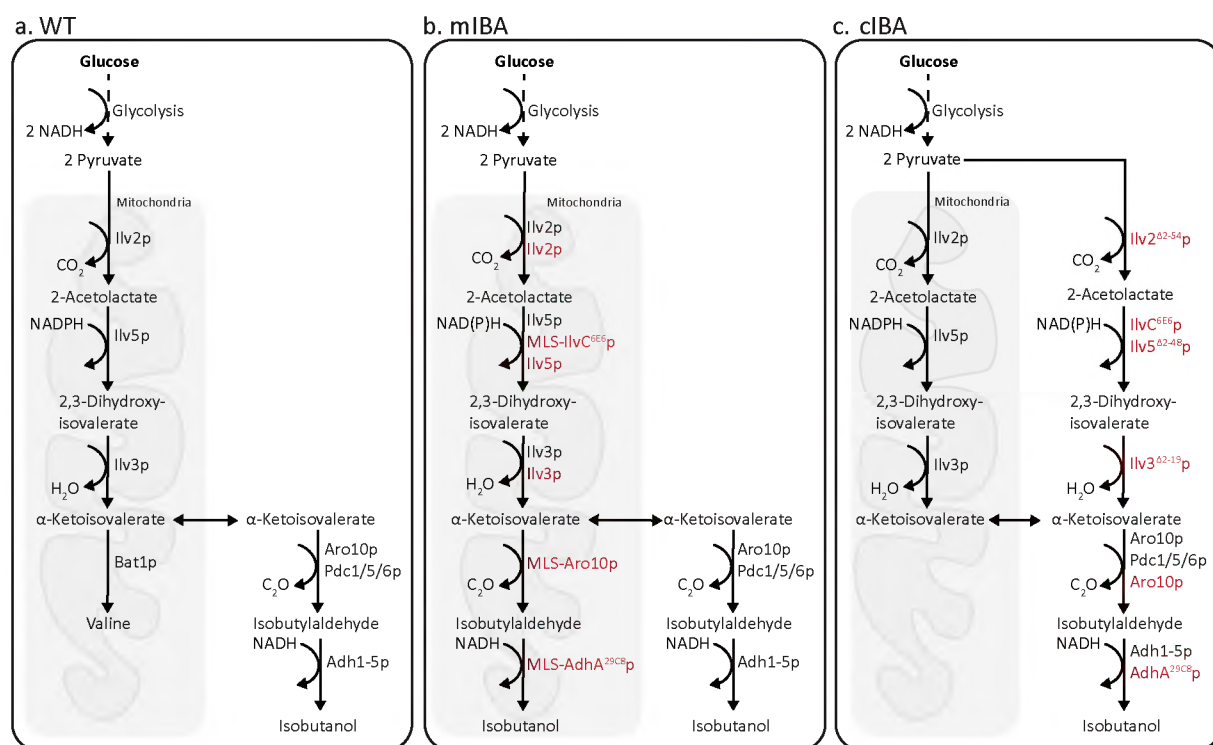
Isobutanol is a branched four-carbon alcohol targeted by many as a biofuel for light-duty engines and as a precursor to jet and diesel fuels via catalytic upgrading [1]. Relative to ethanol, isobutanol has a higher energy density, a lower vapor pressure, and a higher flash point, making it a better option for spark-ignition engines. Isobutanol is also less corrosive and less hygroscopic, making it a better biofuel for current piping infrastructure [2]. Isobutanol biosynthesis is redox balanced with glycolysis and can therefore be made via fermentation. *Saccharomyces cerevisiae*, the workhorse for industrial fermentations, is therefore a suitable host for its production. While yeast have a natural ability to synthesize isobutanol, there are many barriers to making isobutanol the primary fermentation product at high rates [3].

*S. cerevisiae* synthesizes isobutanol from pyruvate via enzymes involved in valine biosynthesis and the Ehrlich pathway. The first half of the pathway converts pyruvate to  $\alpha$ -ketoisovalerate (KIV) by mitochondria-localized *ILV* enzymes: acetolactate synthase (ALS, encoded by *ILV2*), a NADPH-dependent ketol-acid reductoisomerase (KARI, encoded by *ILV5*), and a 2Fe–2S cluster-requiring dihydroxyacid dehydratase (DHAD, encoded by *ILV3*). The second part of the pathway, the Ehrlich pathway, converts KIV to isobutanol by promiscuous cytosolic enzymes:  $\alpha$ -ketoacid decarboxylase (KDC, encoded by pyruvate decarboxylases, *PDC1* *PDC5* or *PDC6*, or phenylpyruvate decarboxylase, *ARO10*) and a NADH-dependent alcohol dehydrogenase (ADH, encoded by *ADH1-5*) (Fig. 1a). *S. cerevisiae*'s native isobutanol production is low (<1% of the theoretical maximum yield), so substantial work is needed to make isobutanol the primary fermentation product [4–6].

The spatial segregation of the native pathway enzymes, split between

the mitochondria and the cytosol, may be a limiting factor for synthesizing isobutanol at high levels. The segregation can be overcome by localizing the five-step pathway into a single compartment: mitochondrial localization is achieved by adding a mitochondrial localization sequence (MLS) to the genes in the Ehrlich pathway (*PDC1/5/6* or *ARO10* and *ADH1-5*), and cytosolic localization is achieved by removing the MLS sequence from the genes in the valine biosynthesis pathway (*ILV2*, *ILV5*, and *ILV3*) [5,6]. However, the role that localization plays in isobutanol production is obscured by conflicting reports in the literature as both pathway localizations have achieved similar isobutanol titers and yields (Table 1). It has been shown that a strain with mitochondrial-localization benefits from having a higher local concentration of enzyme and pathway intermediates [5]. On the other hand, it has been proposed that cytosolic localization would be preferable in the context of industrially relevant conditions such as high glucose concentrations or anaerobic growth. This is in part because the mitochondria are known to enter a minimal energy-requirement mode under those conditions [7,8].

A second limitation in the isobutanol pathway is the redox cofactor imbalance that exists between glycolysis and isobutanol fermentation; glycolysis produces two NADH per molecule of glucose, while isobutanol fermentation consumes one NADPH by *ILV5* and one NADH by *ADH*. This results in an NADPH shortage and NADH excess. One strategy to resolve this imbalance is to use a heterologous NADH-dependent KARI, such as the *E. coli* KARI variant, *ilvC<sup>6E6</sup>*, that was previously engineered with improved specificity towards NADH [9,10]. Another strategy is to increase the supply of NADPH by introducing a transhydrogenase-like shunt ( $\text{NADH} + \text{NADP}^+ \rightarrow \text{NAD}^+ + \text{NADPH}$ ) into *S. cerevisiae* [11]. Both strategies have been successful in improving



**Fig. 1. Native and engineered *S. cerevisiae* isobutanol pathways.** a) Shows the endogenous isobutanol synthesis pathway from pyruvate. The first half of the pathway converts pyruvate to  $\alpha$ -ketoisovalerate (KIV) by the mitochondria-localized valine biosynthesis enzymes *ilv2p*, *ilv5p*, and *ilv3p*. The second part of the pathway, the Ehrlich pathway, converts KIV to isobutanol by promiscuous cytosolic-localized decarboxylase enzymes *Pdc1/5/6p* or *Aro10p* and *Adh1-5p*. b) Mitochondrial-localized isobutanol pathway (mIBA) consists of codon-optimized variants of *S. cerevisiae* *ilv2p*, *S. cerevisiae* *ilv3p*, mitochondria targeted *S. cerevisiae* *Aro10p*, mitochondria targeted *L. lactis* *AdhA<sup>29CB</sup>*, and either *S. cerevisiae* *ilv5p* or mitochondria targeted *E. coli* *ilvC<sup>6E6</sup>* for the redox cofactor imbalanced and balanced pathways respectively (red enzymes). c) Cytosolic-localized isobutanol pathway (cIBA) consists of codon-optimized variants of *S. cerevisiae* *ilv2<sup>Δ2-54</sup>p*, *S. cerevisiae* *ilv3<sup>Δ2-19</sup>p*, *S. cerevisiae* *Aro10p*, *L. lactis* *AdhA<sup>29CB</sup>*, and either *S. cerevisiae* *ilv5<sup>Δ2-48</sup>p* or *E. coli* *ilvC<sup>6E6</sup>* for the redox cofactor imbalanced and balanced pathways respectively (red enzymes). For both the mIBA and cIBA pathways, the endogenous/native enzymes (*ilv2p*, *ilv5p*, *ilv3p*, *Aro10p*, *Pdc1/5/6p*, *Adh1-5p*, and *Bat1p*) in black remain in each strain. (For interpretation of the references to colour in this figure legend, the reader is referred to the Web version of this article.)

**Table 1**Highlight report of engineered *S. cerevisiae* strains for isobutanol production.

Pathway localization	NAD <sup>+</sup> regeneration	Overexpress isobutanol genes	Block competing pathway	Metabolic control of ethanol production	Isobutanol titer (mg/L)	Isobutanol yield (mg/g carbon source)	Conditions (carbon source, condition, vessel)	Refs	Year
Mito		✓			635±23	6.4±0.2	Glucose, semi-aerobic, batch	[5]	2013
Cyto		✓	✓		630.27±14.18	14.86±0.55	Glucose, aerobic, batch	[6]	2012
Cyto and mito	✓	✓	✓		1620±110	16.0±1.0	Glucose, semi-aerobic, batch	[11]	2013
Mito		✓	✓		1245±33	12.45	Glucose, aerobic, batch	[12]	2017
Cyto and mito	✓	✓	✓		224±5	12.04±0.23	Glucose, semi-aerobic, batch	[13]	2015
Cyto and mito		✓	✓		330.9	16.55	Glucose, aerobic, batch	[14]	2016
Cyto		✓	✓		2090	59.55	Glucose, aerobic, batch	[4]	2019
Cyto		✓	✓		263.2	13.16	Glucose, semi-aerobic, batch	[15]	2019
Mito		✓	✓	✓	8494.6±305.3	53.5±8.4	Glucose, micro-aerobic, batch and fed batch	[16]	2018
Cyto	✓	✓	✓		148±24	7.4± 1.2	Glucose, micro-aerobic, batch	[9]	2016
Mito		✓			2600	26	Xylose, aerobic, fed-batch	[17]	2019
Mito		✓			3100 ± 180	38.8 ± 2.4	Xylose, semi-aerobic, fed-batch	[18]	2019
Mito		✓		✓	167.2	3.4	Glucose, semi-aerobic, batch	[19]	2016
Cyto and mito		✓	✓		283 ± 13	11.46	Glucose, aerobic, batch	[20]	2017
Cyto and mito		✓			85.2	2.13	Glucose, anaerobic, batch	[21]	2011

Cyto = cytosolic-localization.

Mito = mitochondrial-localization.

isobutanol titers, demonstrating the importance of having a redox cofactor-balanced pathway (Table 1).

In this work, we aimed to provide insight into how pathway localization and redox cofactor-balancing affect the performance and physiology of isobutanol producing strains. We conducted a functional genomics analysis to elucidate differences between *S. cerevisiae* strains equipped with DNA cassettes that localized isobutanol biosynthesis to specific compartments, *i.e.* mitochondria vs. cytosol, and included either a NADPH-dependent (cofactor-imbalanced) or NADH-dependent (cofactor-balanced) KARI enzyme. Here, we report that pathway localization had a greater effect on isobutanol production than redox-balancing; the strain harboring the mitochondrial-localized isobutanol pathway outperformed the cytosolic version by 3.8-fold. The main limitation in the cytosolic-localization is the supply of the 2Fe–2S cluster cofactor for the DHAD enzyme; however, we found that this limitation may be partially overcome by increasing the availability of iron in the cell by perturbing iron homeostasis. Our findings contribute towards improving the metabolic engineering designs for building further improved isobutanol producing strains.

## 2. Materials and methods

### 2.1. Yeast media

Complex lab media for culturing, YP, consisted of 10 g/L yeast extract, 20 g/L peptone, and 20 g/L dextrose (YPD). 200 µg/mL Geneticin (US Biological, Swampscott, MA), 200 µg/mL Hygromycin B (US Biological, Swampscott, MA), 100 µg/mL Nourseothricin (Jena Bioscience, Jena, Germany), or 200 µg/mL Zeocin (Thermo Fisher Scientific, Waltham, MA) were added for maintenance of expression constructs where needed. Defined minimal medium contained 6.7 g/L yeast

nitrogen base (YNB) without amino acids with ammonium sulfate, 19.5 g/L MES, 100 g/L dextrose, 4 mL/L 250X tween/ergosterol stock (62.5 mL Tween80 + 625 mg Ergosterol in 187 mL 95% EtOH) and pH adjusted to 5.5. Defined synthetic complete media contained 6.7 g/L yeast nitrogen base (YNB) without amino acids with ammonium sulfate, 1 g/L drop-out mix without yeast nitrogen base, and 20 g/L dextrose.

### 2.2. Cloning and yeast strain engineering

*S. cerevisiae* strains used in this study are described in Table S1. The parental WT strain [22] <https://paperpile.com/c/CNM88o/8W7t> was generated by transforming [23] a polymerase chain reaction (PCR) product containing the *URA3* open reading frame (ORF), 225 bp of the 5' UTR and 173 bp of the 3' UTR from the GLBRCY22-3 strain ([24], G3) into the CEN.PK113-5D strain and plating on SC minus uracil plates. Transformants were confirmed for growth on auxotrophic medium without uracil and Sanger-sequenced. To generate strains expressing the isobutanol pathway genes, DNA containing codon-optimized versions of *ILV2*, *ILV3*, *ILV5* and *ARO10* from *S. cerevisiae*, and *adhA*<sup>29C8</sup> from *Lactobacillus lactis* [25] were synthesized (Life Technologies) and cloned between various yeast promoters and terminators (together called the “isobutanol pathway cassette”). Specifically, expression was driven by the following promoter and terminator pairs: *P<sub>ADH1</sub>-ILV2-T<sub>CYC1</sub>*; *P<sub>PGK1</sub>-ILV3-T<sub>TEF2</sub>*; *P<sub>TEF2</sub>-adhA*<sup>29C8</sup>-*T<sub>TDH3</sub>*; *P<sub>TDH3</sub>-ARO10-T<sub>TEF1</sub>*; *P<sub>TEF1</sub>-ILV5-T<sub>TUB1</sub>*. The *P<sub>ADH1</sub>* consisted of 408 bp upstream of the *ScADH1* protein-coding sequence, *T<sub>CYC1</sub>* consisted of 251 bp downstream of *ScCYC1* protein-coding sequence, *P<sub>PGK1</sub>* consisted of 998 bp upstream of the *ScPGK1* protein-coding sequence, *T<sub>TEF2</sub>* consisted of 293 bp downstream of the *ScTEF2* protein-coding sequence, *P<sub>TEF2</sub>* consisted of 402 bp upstream of the *ScTEF2* protein-coding sequence, *T<sub>TDH3</sub>* consisted of 514 bp downstream of the *ScTDH3* protein-coding sequence, *P<sub>TDH3</sub>* consisted

of 672 bp upstream of the *ScTDH3* protein-coding sequence, *T<sub>TEF1</sub>* consisted of 350 bp downstream of the *ScTEF1* protein-coding sequence, *P<sub>TEF1</sub>* consisted of 577 bp upstream of the *ScTEF1* protein-coding sequence, *T<sub>TUB</sub>* consisted of 380 bp downstream of the *ScTUB1* protein-coding sequence. The transcriptional units (promoter-gene-terminator pairs) for the five genes were then cloned in the above order into the *SacI-KpnI* polylinker sites of a modified pRS426 plasmid containing *HygMX4* as the selection marker in place of *URA3* [26]. Homology arms to the *HO* locus (*HO-L* and *HO-R*) were inserted 5' and 3' of the isobutanol pathway cassette to facilitate genome insertion by homologous recombination [27]. The *HO-R* homology arm also included the *LoxP-KanMX-LoxP* selection marker, which was inserted 3' of *ScTUB1* protein-coding sequence [28]. For expressing *ARO10* and *adhA*<sup>29C8</sup> in the mitochondria, coding sequence for the *COX4* MLS was synthesized in-frame at the 5' ends of codon-optimized *ARO10* and *adhA*<sup>29C8</sup>. The full length isobutanol pathway cassette containing mitochondrial-localized enzymes and flanking *HO* arms (GenBank: MZ541859) was excised from the plasmid by digestion with *SacI*-HF and *KpnI*-HF, purified and transformed into the WT strain. After selection on YPD + Geneticin plates, PCR and Sanger sequencing were used to confirm the insertion of the isobutanol pathway cassette into the *HO* locus. The *LoxP-KanMX-LoxP* selection marker was then excised by Cre recombinase to generate the final mIBA<sup>ILV5</sup> strain [28]. The inserted isobutanol pathway cassette was amplified by PCR with multiple primer sets from mIBA<sup>ILV5</sup> genomic DNA (gDNA) and confirmed for complete insertion by Sanger-sequencing (Fig. S1a). To generate the cIBA<sup>ILV5</sup> strain, CRISPR/Cas9 was used to delete the MLSs at the N-terminus of the engineered isobutanol pathway enzymes in mIBA<sup>ILV5</sup> (Fig. S1b). In brief, an sgRNA sequence targeting the MLS of each synthetic isobutanol pathway enzyme were identified by CRISpy-pop [29] and cloned into the pXIPHOS plasmid as described previously [30]. sgRNA targeting sequences are as follows: *ILV2*, CTTAATAGCGAAGTCTTCA; *ILV3*, AGTAGTAGAGAATTGTCTAG; *ILV5*, GCAGATCAATCTAGCAGCTT; *MLS-adhA*<sup>29C8</sup> and *MLS-ARO10*, AAATCTGATGGACTGTCTCA. Each mitochondrial-localized gene in the synthetic isobutanol pathway was sequentially replaced by transforming the pXIPHOS plasmid containing a single sgRNA to one gene along with the appropriate PCR repair template of the gene lacking the MLS in the following order: *ILV5* - > *ilvC*<sup>6E6</sup>, *MLS-ARO10* and *MLS-adhA*<sup>29C8</sup> simultaneously - > *ARO10* and *adhA*<sup>29C8</sup>, *ILV3* - > *ILV3*<sup>Δ2-19</sup>, *ILV2* - > *ILV2*<sup>Δ2-54</sup>. To generate repair templates with the cytosol-localized isobutanol pathway enzymes, individual genes were first cloned into the TOPO vector and then the appropriate MLS was removed (*ILV2*<sup>Δ2-54</sup>, *ILV3*<sup>Δ2-19</sup>, and *ILV5*<sup>Δ2-48</sup>, *ARO10*<sup>ΔMLS</sup>, and *adhA*<sup>29C8</sup>, <sup>Δ2-MLS</sup> [6]) by restriction digestion/PCR-aided Gibson assembly and confirmed with Sanger-sequencing. These vectors were then used as the PCR repair template which contained part of the promoter and part of the gene lacking the MLS. The repair template for replacing *ILV5* with *ilvC*<sup>6E6</sup> was generated by amplifying the *E. coli* *ilvC*<sup>6E6</sup> CDS from pIBA1 [31] and cloning it in place of the *ILV5*<sup>Δ2-48</sup> CDS in the TOPO vector; this vector was Sanger-sequenced and used for the PCR repair template in the same manner as described earlier. To generate the cIBA<sup>ILV5</sup> strain, the cIBA<sup>ILV5</sup> strain was transformed with the pXIPHOS plasmid containing an sgRNA to *ilvC*<sup>6E6</sup> (AGTTTAAATTACAACCGGTA) and a PCR repair template containing *ILV5*<sup>Δ2-48</sup> (Fig. S1c). To generate the mIBA<sup>ILV5</sup> strain, the mIBA<sup>ILV5</sup> strain was transformed with the pXIPHOS plasmid containing an sgRNA to codon-optimized *ILV5* (GCA-GATCAATCTAGCAGCTT) and a PCR repair template containing *MLS-ilvC*<sup>6E6</sup> (Fig. S1d). For the cIBA<sup>ILV5</sup>, cIBA<sup>ILV5</sup> and mIBA<sup>ILV5</sup> strains, DNA sequence changes where CRISPR/Cas9 editing occurred were confirmed by Sanger-sequencing. Deletions of codon-optimized *ILV3*, native *ILV3* and/or native *FRA2* from the cIBA<sup>ILV5</sup>, mIBA<sup>ILV5</sup>, and cIBA<sup>ILV5</sup> strains were performed by integration of PCR products generated from *LoxP-KanMX-LoxP* (pUG6) or *LoxP-HphMX-LoxP* (pUG75) plasmid templates and primers containing 40–60 bp of homology flanking the targeted genes [32]. PCR products were purified

and transformed into the appropriate strains and selected for growth on the appropriate antibiotic. Gene deletions were confirmed by PCR of gDNA and Sanger-sequencing.

### 2.3. Fermentation growth conditions and sample collection

For aerobic growth, starter cultures were grown in a shaking incubator at 30 °C. For anaerobic growth, media was allowed to degas in a 30 °C Coy anaerobic chamber (10% H<sub>2</sub>, 10% CO<sub>2</sub>, and 80% N<sub>2</sub>) for >12 h prior to use and cultures were grown with stir bars on a magnetic stir plate to prevent flocculation. Fermentations for multi-omic sampling were performed in biological triplicate. Yeast cells were grown aerobically in YPD until stationary phase ~12 h. The cultures were then shifted to minimal medium and anaerobic conditions by diluting the culture to OD<sub>600</sub> 0.3 in minimal medium and allowed to reach exponential phase ~8.5 h. Working cultures, which were used for sampling, were then inoculated from the shifted culture to OD<sub>600</sub> 0.2 in minimal medium and allowed to grow anaerobically for 48 h. Cell growth was monitored by taking OD<sub>600</sub> measurements with the Beckman DU720 spectrophotometer. Samples for end-product analysis were taken by collecting 2 mL of culture supernatant. Samples for protein isolation were obtained by collecting and flash freezing ~1 × 10<sup>11</sup>/1 × 10<sup>12</sup> cells. Similarly, samples for RNA isolation were obtained by collecting and flash freezing the equivalent of 25 mL of cells at an OD<sub>600</sub> of 1. Samples for intracellular metabolite quantification were collected inside the anaerobic chamber by vacuum filtrations of culture through 0.45 μm hydrophilic nylon filters. Filters with the retained cells were immediately placed cell-side down in 1.5 mL of extraction solvent (40 vol% acetonitrile, 40 vol% methanol, 20 vol% water) kept on dry ice to quench metabolism and extract metabolites.

### 2.4. End-product analysis

#### 2.4.1. Determination of isobutanol concentration by automated headspace GC/MS

The equipment used included the following: an Agilent 7890A GC system (Agilent Technologies, Inc. Palo Alto, CA); a LPAL3 autosampler and sample preparation system equipped with a heated agitator/stirrer and heated headspace sampling syringe (Agilent Technologies, Inc. Palo Alto, CA); and a Pegasus 4D ToF-MS (Leco Corp., Saint Joseph, Michigan). Typical analysis range is 0.065 mM–8.4 mM isobutanol and uses an aliquot volume of 500 μL and 2-Methylpropyl-d<sub>9</sub> alcohol (as internal standard). Instrument run control and conditions are set by the Chromatof (®Leco Corp.) software (version 4.72.0.0) provided with the Pegasus 4D GCxGC ToF MS system. Samples were incubated at 70 °C for 5 min in the heated agitator set to 350 rpm. 0.5 mL of the headspace is then sampled by the autosampler with a 2.5 mL gastight syringe heated to 75 °C and injected into the GC system. The sample was withdrawn at 100 mL/s and injected into the GC at 1000 mL/s. The syringe was purged with nitrogen gas for 0.5 min prior to the next injection. The analytical capillary GC column was a Stabilwax-DA® (Restek, Inc. Bellefonte, PA) length 30 m, 0.25 mm ID, 0.25 mm film thickness. Helium was used as a carrier gas with a pressure corrected constant flow rate of 1 mL/min. The GC inlet was fitted with a 4 mm deactivated glass liner and held at 250 °C throughout the run. The inlet split ratio was set to 50:1. The GC oven was initially set to 50 °C and held for 1 min then increased to 200 °C at 40 °C/min and held at 200 °C for 5 min. The filaments of the mass spectrometer were turned on 42.5 s after injection and 10 spectra/sec were recorded from *m/z* 10 to *m/z* 250. The MS source temp was 200 °C, electron energy set to 70 eV, and the detector voltage was adjusted to approximately 50 V above the minimum voltage determined by the instrument tune check procedure. The peak area of isobutanol was measured using the extracted ion chromatogram of *m/z* 43 and the peak area of 2-Methylpropyl-d<sub>9</sub> alcohol was measured from the extracted ion chromatogram of *m/z* 46. An unpaired *t*-test was performed to determine statistical significance.



#### 2.4.2. Analysis of fermentation supernatants by HPLC-RID

End-product analytes (glucose, ethanol, glycerol, lactate, and acetate) were measured with an analytical system consisting of an Agilent 1260 Infinity HPLC system (Agilent Technologies, Inc., Palo Alto, CA) with a quaternary pump, chilled (4 °C) autosampler, vacuum degasser, refractive index detector, and a Aminex HPX-87H column with a Cation-H guard column (BioRad, Inc. Hercules, CA; 300 × 7.8 mm, cat# 125-0140). Operating parameters were as follows: 0.02 N H<sub>2</sub>SO<sub>4</sub> mobile phase, 0.500 mL/min flow rate, 50 °C column temperature, 50 °C detector temperature, 28 min run time, and a 50 µL injection volume. Instrument control, data collection and analysis/calculation are done using Chem Station V. B04.03 software (Agilent Technologies, Inc., Palo Alto, CA). An unpaired *t*-test was performed to determine statistical significance.

#### 2.5. Intra- and extra-cellular metabolomics preparation, quantification, and analysis

After collecting all samples at a given time point, the filter disks in extraction solvent were removed from the anaerobic chamber and the cells were washed off the filter into the solvent. The entire suspension was transferred into a centrifuge tube and centrifuged for 5 min at 16,000×g at 4 °C to remove cellular debris. The supernatant was collected in another centrifuge tube and immediately prepped for quantification.

The extraction solvent containing intracellular metabolites was dried under N<sub>2</sub> and the metabolites were resuspended in Solvent A (97:3H<sub>2</sub>O: methanol with 10 mM tributylamine adjusted to pH 8.2 by addition of 10 mM acetic acid). Samples were analyzed by LC-MS as described previously [33,34]. Data analysis was performed using MAVEN software [35,36] and compounds were identified by retention time (matched to pure standards). “Peak Area Top” values were extracted and normalized by OD<sub>600</sub> equivalent of sample injected into the LC-MS. Extracellular metabolite samples for LC-MS analysis were diluted to appropriate concentration, then analyzed using the above method. An unpaired *t*-test was performed to determine statistical significance.

#### 2.6. Transcriptomic sample preparation, library construction, sequencing, and analysis

Total RNA was extracted with hot phenol lysis [37], DNA was digested with Turbo-DNase (Life Technologies, Carlsbad, CA) for 30 min at 37 °C, and RNA was precipitated with 2.5 M LiCl for 30 min at 20 °C. In brief, RNA-Seq libraries were generated using the Illumina TruSeq® Stranded mRNA HT kit, AMPure XP bead for PCR purification (Beckman Coulter, Indianapolis, IN), and SuperScriptII reverse transcriptase (Invitrogen, Carlsbad, CA) as described in the Illumina kit. Single-end 50-bp reads were generated using an Illumina NovaSeq 6000 at the University of Wisconsin-Madison Biotechnology Center. Reads were processed with Trimmomatic version 0.3 [38] and mapped to the S288C genome (with foreign mutant sequences added) using Bowtie 2 version 2.2.2 with default settings [39]. Read counts were calculated using HTseq version 0.6.0 [40]. edgeR version 3.6.8 [41] was used to perform differential gene analysis, taking a Benjamini and Hochberg false discovery rate (FDR) of <0.05 as significant [42]. Raw sequencing counts were normalized using Trimmed Means of M-values (TMM). Samples were clustered using Cluster 3.0 [43] and visualized in Java TreeView [44], and functional GO term enrichment was performed using SetRank [45] with an FDR set to < 0.05 for significance.

#### 2.7. Label-free quantitative proteomics preparation, quantification, and analysis

Yeast pellets were resuspended in 150 µL of 6 M guanidine, 100 mM Tris (pH 8) and boiled for 5 min at 100 °C. Methanol was then added to 90% to precipitate proteins, and the samples were centrifuged for 5 min

at 9,000 G. The supernatant was discarded, and the protein pellet was resuspended in lysis buffer (8 M urea, 100 mM Tris pH 8, 20 mM TCEP, 80 mM Chloroacetamide). LysC was added to an estimated 50:1 protein to enzyme ratio and incubated for 4 h at room temperature. The samples were diluted with 100 mM Tris to a urea concentration of 1.5 M. Trypsin was added to an estimated 50:1 protein to enzyme ratio and incubated overnight at room temperature. Samples were desalted with Strata C18 solid phase extraction cartridges and dried in a vacuum centrifuge. Peptide concentration was then determined from a NanoDrop One spectrophotometer before re-suspending in 0.2% formic acid and injecting onto the mass spectrometer.

Samples were analyzed using an LC-MS/MS instrument comprising an Orbitrap Eclipse Tribrid mass spectrometer and UltiMate 3000 RSLCnano liquid chromatography system (Thermo Fisher Scientific). Mobile phase A consisted of 0.2% formic acid in water and mobile phase B consisted of 0.2% formic acid in 80% acetonitrile. Peptides were loaded in 0% B and separated at a flow rate of 310 nL/min over a 120 min gradient of increasing % B. Peptides were injected onto a 1.7 µm C18 column (75 µm i.d.) packed in-house to a length of 30 cm [46] and heated to 50 °C. Survey scans of peptide precursors were collected every second from 300 to 1350 Th with an AGC target of 1,000,000 and a resolution of 240,000 in the orbitrap. Precursors were isolated from a 0.5 Th window in the quadrupole and HCD MS/MS scans at 35% collision energy were collected in the ion trap with an AGC target of 35,000 from 150 to 1350 Th.

The resulting LC-MS/MS proteomics data were processed using MaxQuant [47] software version 1.5.2.8 and searched against a *Saccharomyces cerevisiae* database (with foreign mutant proteins added) downloaded from Uniprot. The digestion enzyme was set to Trypsin/P with up to two missed cleavages, and oxidation of methionine and protein N-terminal acetylation were set as variable modifications. Cysteine carbamidomethylation was set as a fixed modification. Label-free quantification was enabled with a minimum ratio count of 1, and the match between runs feature was utilized to decrease missing data values within the dataset. Peptides were filtered to a 1% FDR and combined to protein groups based on the rules of parsimony. Differential protein analysis was done taking a Benjamini and Hochberg false discovery rate (FDR) of <0.05 as significant [42]. Functional enrichment was assessed using the FunSpec database [48].

#### 2.8. Petite frequency

To assess the propensity of different strains to form petite colonies due to loss of respiratory competence each strain was revived on YPD media and streaked for single colonies on YPG (2% glycerol) media to ensure all starting cells could respire. Single colonies were used to inoculate 3 independent 5 mL YPD cultures, which were grown rolling overnight at 30 °C. Each culture was plated for single colonies on YPDG (0.1% dextrose, 3% glycerol) media to differentiate petite and respiring colonies and colonies were counted after 3 days of growth at 30 °C.

### 3. Results and discussion

#### 3.1. Engineered isobutanol producing strains

In order to evaluate the effects of pathway localization and redox cofactor-balancing on isobutanol production, we constructed four engineered strains: a mitochondrial-localized isobutanol pathway with a NADPH-dependent Ilv5p KARI, mIBA<sup>Ilv5</sup>; a mitochondrial-localized isobutanol pathway with a NADH-dependent IlvC<sup>6E6</sup>p KARI, mIBA<sup>IlvC6E6</sup>; a cytosolic-localized isobutanol pathway with a NADPH-dependent Ilv5p KARI, cIBA<sup>Ilv5</sup>; and a cytosolic-localized isobutanol pathway with a NADH-dependent IlvC<sup>6E6</sup>p KARI, cIBA<sup>IlvC6E6</sup> (Fig. 1b and c, Table S1/ Fig. S1, Materials and methods 2.2). DNA cassettes for expressing each pathway were assembled from genes previously tested [5], including those encoding an alcohol dehydrogenase (*adhA*<sup>29C8</sup>, from

*Lactococcus lactis* [25]), an acetolactate synthase (*ILV2*, from *S. cerevisiae*), a dihydroxyacid dehydratase (*ILV3*, from *S. cerevisiae*), a  $\alpha$ -ketoacid decarboxylase (*ARO10*, from *S. cerevisiae*), and a ketol-acid reductoisomerase (*ILV5*, from *S. cerevisiae* or *ilvC<sup>6E6</sup>*, from *E. coli* [31]). Each open reading frame was codon-optimized, synthesized commercially, and cloned in frame with promoters (P) and terminators (T) resulting in the following pairs: *P<sub>ADHI</sub>-ILV2-T<sub>CYCI</sub>*; *P<sub>PGK1</sub>-ILV3-T<sub>TEF2</sub>*; *P<sub>TEF2</sub>-adhA<sup>29C8</sup>-T<sub>TDH3</sub>*; *P<sub>TDH3</sub>-ARO10-T<sub>TEF1</sub>*; *P<sub>TEF1</sub>-ILV5-T<sub>TUB1</sub>*; *P<sub>TEF1</sub>-ilvC<sup>6E6</sup>-T<sub>TUB1</sub>* (Materials and methods 2.2). Mitochondrial localization was achieved by adding DNA encoding the previously characterized Cox4p N-terminal MLS [5] to the N-terminus of genes which natively localized to the cytosol (*MLS-ARO10*, *MLS-adhA<sup>29C8</sup>*, and *MLS-ilvC<sup>6E6</sup>*). Conversely, cytosol targeting was achieved by removing sequences encoding previously identified MLS from genes which natively localized to the mitochondria (*ILV2<sup>Δ2-54</sup>*, *ILV3<sup>Δ2-19</sup>*, and *ILV5<sup>Δ2-48</sup>*) [6]. DNA cassettes containing each of the five genes were assembled and integrated into the *S. cerevisiae* genome at the *HO* locus via homologous recombination. When constructing the mIBA<sup>ilvC6E6</sup> strain we uncovered an unexpected petite phenotype. The frequency at which the petite colonies arose in the mIBA<sup>ilvC6E6</sup> strain was 166-fold that of the wild-type (WT) strain (Table S2). All other engineered strains had a low petite frequency consistent with natural *S. cerevisiae* isolates [49,50]. The mIBA<sup>ilvC6E6</sup> strain was not included in further studies due to this irreversible fitness defect.

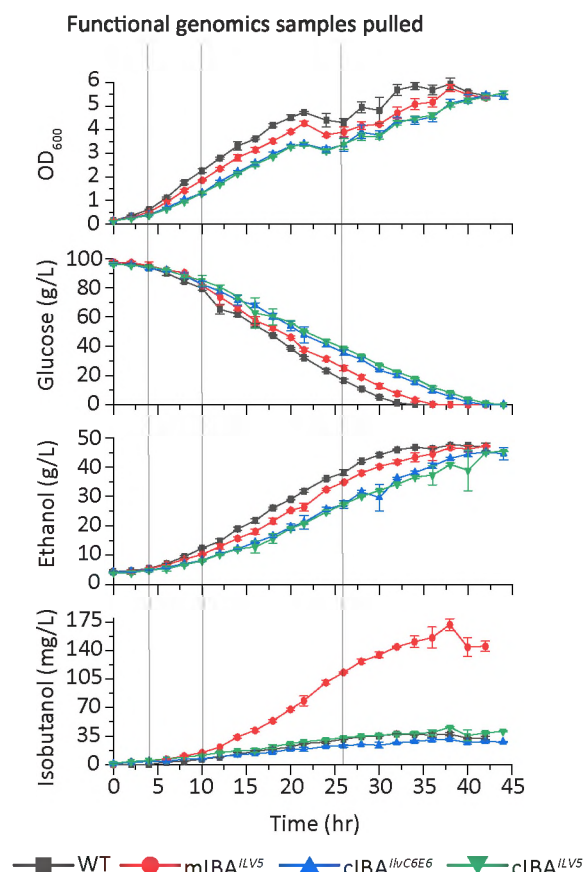
### 3.2. Engineered strains produce varied amounts of isobutanol

A fermentation experiment was performed to evaluate and compare the physiological and molecular phenotypes of the engineered strains and WT. Each strain was cultivated anaerobically at 30 °C in minimal medium containing 100 g/L glucose. We collected samples every 2 h to monitor growth, glucose consumption, isobutanol production, and ethanol production. Samples for functional genomics analyses (transcriptomic, proteomic and metabolomic) were collected at 4, 10, and 26 h post inoculation to represent the different phases of cell growth: early-exponential phase, mid-exponential phase, and early-stationary phase (Fig. 2). The three engineered strains grew slower than the WT strain (Fig. 2); doubling times during the exponential phase of the mIBA<sup>ilvC6E6</sup>, cIBA<sup>ilvC6E6</sup> and cIBA<sup>ilvC6E6</sup> strains were 1.1, 1.3, and 1.3-fold larger than the WT strain, respectively. All strains completely consumed the glucose provided and reached similar final OD<sub>600</sub> (5.3–5.6) values by the end of the 48 h fermentation. All strains produced ethanol titers of 45–47 g/L by 44 h of the fermentation corresponding to yields over 90% of the theoretical maximum (Fig. 2). These metrics indicate that ethanol remains the dominant fermentation product and that pathway localization and cofactor-balance alone were not the limiting factor in isobutanol fermentation.

Isobutanol production varied significantly among the engineered strains. The cIBA<sup>ilvC6E6</sup> and cIBA<sup>ilvC6E6</sup> strains produced isobutanol at levels less than or equal to WT; at 38 h, the isobutanol titers were 37, 46, and 31 mg/L in the WT, cIBA<sup>ilvC6E6</sup>, and cIBA<sup>ilvC6E6</sup> strains, respectively. The cIBA<sup>ilvC6E6</sup> strain produced 1.5-fold ( $P < 5E-5$ ) more isobutanol than the cIBA<sup>ilvC6E6</sup> strain indicating that redox cofactor-balancing is not a limiting factor for driving flux to isobutanol synthesis in these strains and NAD<sup>+</sup> is preferentially regenerated through ethanol fermentation. The highest isobutanol titer was achieved by the mIBA<sup>ilvC6E6</sup> strain, which produced 170 mg/L at 38 h, corresponding to a yield of 1.8 mg isobutanol/g glucose. This metric is similar to other isobutanol over-producing strains grown under anaerobic conditions [21]. In summary, the mIBA<sup>ilvC6E6</sup> strain outperforms the other engineered strains and had a 3.8-fold ( $P < 5E-6$ ) higher isobutanol titers than the cIBA<sup>ilvC6E6</sup> strain.

### 3.3. Strains with cytosolic-localized isobutanol pathway have an altered transcriptome and proteome

We next assessed the molecular phenotypes of the engineered strains

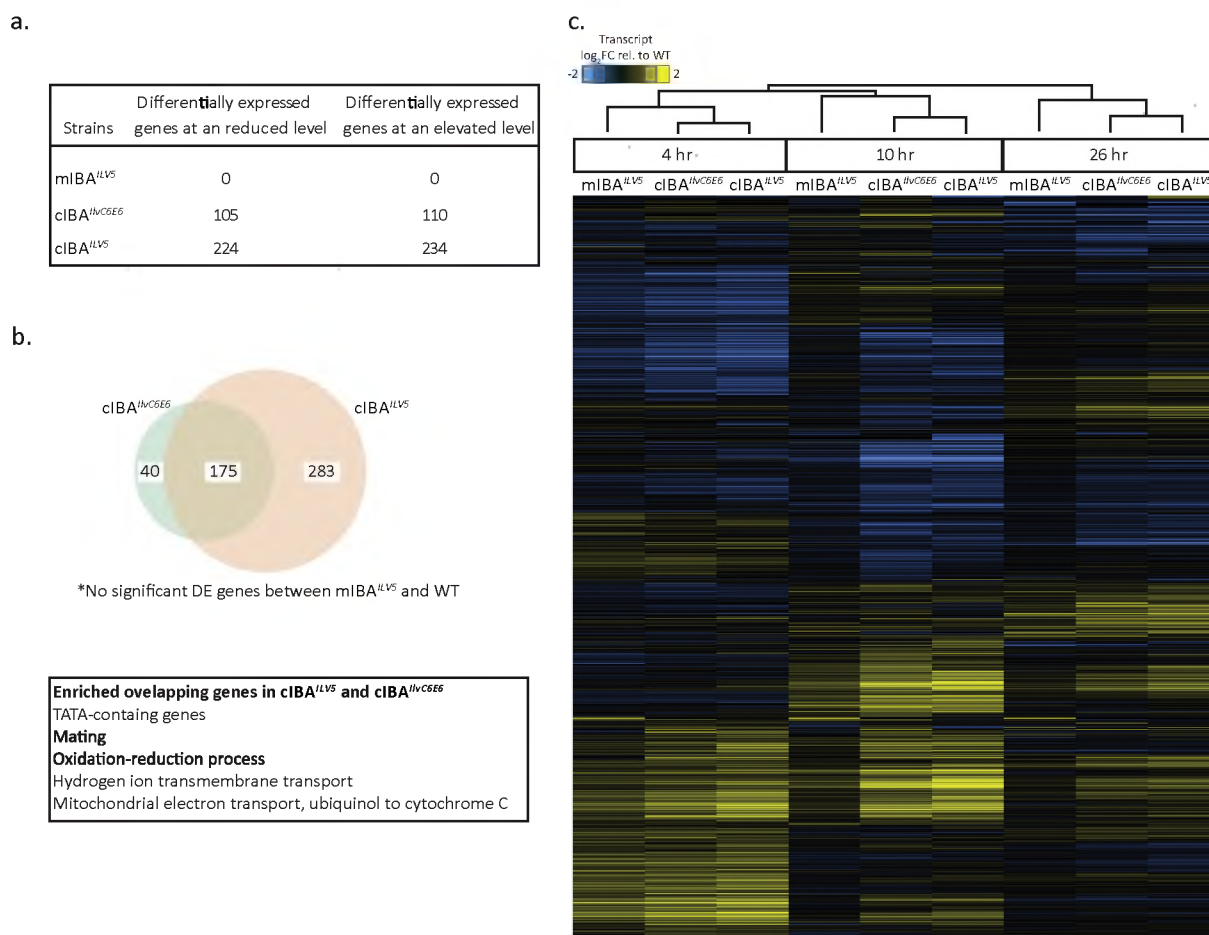


**Fig. 2. Mitochondrial-localized isobutanol pathway is sufficient for increasing isobutanol titers.** Fermentation was performed on the isobutanol producing *S. cerevisiae* strains under anaerobic conditions in minimal medium for 48 h. Cell growth (OD<sub>600</sub>), glucose, ethanol and isobutanol production were measured. Error bars represent the standard deviation of three biological replicates. Samples for functional genomics analysis (proteomics, transcriptomics, and metabolomics) were pulled at 4, 10, and 26 h indicated by vertical gray lines.

and WT using the functional genomics samples collected during the above-mentioned fermentation experiment. We identified and collected data for 59 intracellular metabolites using LC-MS, 34 extracellular metabolites (28 LC-MS and 6 HPLC/GC), 4339 proteins by LC-MS/MS proteomics, and 6434 genes by RNA-seq (File S1–S4, Data availability).

The transcriptome and proteome data collected from our top isobutanol producer, mIBA<sup>ilvC6E6</sup>, was more similar to WT than the cIBA<sup>ilvC6E6</sup> and cIBA<sup>ilvC6E6</sup> strains which both displayed a larger number of differentially expressed RNA and proteins (Fig. 3a, Table S3). The cIBA<sup>ilvC6E6</sup> and cIBA<sup>ilvC6E6</sup> strains shared 175 of the same differentially expressed genes, which were enriched for oxidation-reduction processes, mitochondrial respiration, and TATA-containing genes (Fig. 3b). Hierarchical clustering of the data was also performed, and the strains clustered together in a distinct clade within each timepoint (Fig. 3c). Taken together, we concluded that the cIBA<sup>ilvC6E6</sup> and cIBA<sup>ilvC6E6</sup> strains have functionally similar transcriptomes and that a cytosolic-localized isobutanol pathway induces gene expression changes in specific biological processes.

The metabolite dataset showed that all engineered strains had significantly altered levels of aromatic amino acid biogenesis intermediates (Fig. S2 and Fig. S3). We suspect this was due to over-expression of the synthetic KDC enzyme, Aro10p, in our engineered strains enhancing aromatic amino acid degradation flux (Fig. S3). The depletion of phenylalanine (Phe) and tyrosine (Tyr) did not cause any unexpected changes in cell growth as supplementation with 0.1% (w/v)



**Fig. 3. Transcriptomics overview of the engineered isobutanol strains.** **a)** Number of differentially expressed genes at an elevated or reduced level in the engineered strains relative to WT **b)** Venn Diagram showing the number of overlapping differentially expressed genes in the cIBA<sup>ILV5</sup> and cIBA<sup>ILV5</sup> strains and the GO terms enrichment results (Bonferroni adjusted  $P < 1E-05$ ). **c)** Heatmap shows the average relative Log<sub>2</sub> fold change of genes (rows) for each strain/time point (columns) relative to WT. The three sampling times were early-exponential phase (4 h), mid-exponential phase (10 h), and early-stationary phase (26 h) for strains mIBA<sup>ILV5</sup>, cIBA<sup>ILV5</sup>, and cIBA<sup>ILV5</sup> grown in minimal medium anaerobically. Yellow denotes induced expression, blue denotes repressed expression, and black denotes unchanged values according to the key. Hierarchical clustering was performed with Cluster 3.0 and visualized in Java TreeView (Materials and methods 2.6). The transcriptome of the cIBA<sup>ILV5</sup> and cIBA<sup>ILV5</sup> strains were more similar than the mIBA<sup>ILV5</sup> strain. (For interpretation of the references to colour in this figure legend, the reader is referred to the Web version of this article.)

Phe and Tyr yielded no improvement in growth rate (Fig. S4). Metabolites in the IBA pathway were also dramatically altered but more so in the cIBA<sup>ILV5</sup> and cIBA<sup>ILV5</sup> strains when compared to WT (Fig. S2). The remainder of the manuscript will discuss conclusions we drew after integrating specific aspects of the functional genomics data.

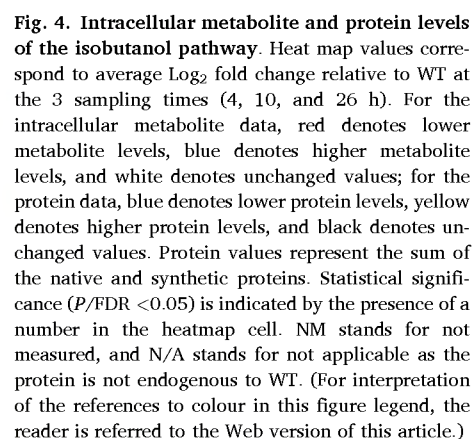
### 3.4. Cytosolic-localized isobutanol pathway has a bottleneck at *Ilv3p*

We first examined data related to enzymes in the isobutanol pathway. To judge if each of our synthetic enzyme variants was expressed, the mRNA counts and protein abundance data were investigated. Normalized counts (RPKM) for all synthetic codon-optimized isobutanol genes (*ILV2*, *ILV2*<sup>Δ2-54</sup>, *ILV5*, *ILV5*<sup>Δ2-48</sup>, *ilvC*<sup>6E6</sup>, *ILV3*, *ILV3*<sup>Δ2-19</sup>, *MLS-adhA*<sup>29C8</sup>, *adhA*<sup>29C8</sup>, *MLS-ARO10*, and *ARO10*) were successfully detected in the transcriptomes of the engineered strains (Table S4). In general, the amount of RNA detected for each transcript correlated with the predicted promoter strengths of each gene ( $P_{THD3-ARO10} > P_{PGK1-ILV3} > P_{TEF1-ILV5/ilvC}^{6E6} > P_{TEF2-adhA}^{29C8} > P_{ADHI-ILV2}$ ) (Table S4) [51,52]. The transcript levels of the native *ILV2*, *ILV5*, *ILV3*, and *ARO10* genes were also investigated, and as expected, the mRNA abundances of the native genes were not statistically significantly altered in any of the engineered strains compared to the WT strain (File S1). The protein levels of the isobutanol enzymes (*Ilv2p*, *Ilv3p*, *Ilv5p*,

and *Aro10p*) were elevated across all the engineered strains when compared to WT (Fig. 4). This elevated protein abundance in our engineered strains can be a result of our synthetic variants being successfully translated and contributing to the protein pool. Overall, neither the mRNA counts nor the protein abundance data yielded an explanation for the differences in isobutanol production we observed between the engineered strains. We contribute the higher isobutanol production in the mIBA<sup>ILV5</sup> strain to be the result of added activity from the mitochondrial pathway localization.

Next, we looked at the intracellular levels of the isobutanol pathway intermediates in our engineered strains and saw that 2-acetolactate (AL), 2,3-dihydroxyisovalerate (DHIV), and  $\alpha$ -ketoisovalerate (KIV) were significantly altered compared to the WT strain. At 4 h, the cIBA<sup>ILV5</sup> strain had a 23-fold ( $P < 5.0E-4$ ), 16-fold ( $P < 5.0E-5$ ), and 4.1-fold ( $P < 0.005$ ) increase in intracellular AL, DHIV, and KIV, respectively when compared to WT. Similarly, at 4 h, the cIBA<sup>ILV5</sup> strain had a 22-fold ( $P < 5e-6$ ), 8.6-fold ( $P < 0.0005$ ), and 2.5-fold ( $P < 5E-4$ ) increase in intracellular AL, DHIV, and KIV, respectively when compared to WT (Fig. 5). This trend of elevated intracellular AL, DHIV, and KIV in the cIBA<sup>ILV5</sup> and cIBA<sup>ILV5</sup> strains was also seen at the other timepoints, 10 and 26 h, but to a lesser extent. The significant accumulation of AL and DHIV in these strains indicates that *ILV3* is a rate-limiting step. This finding was also in agreement with a previous study where additional



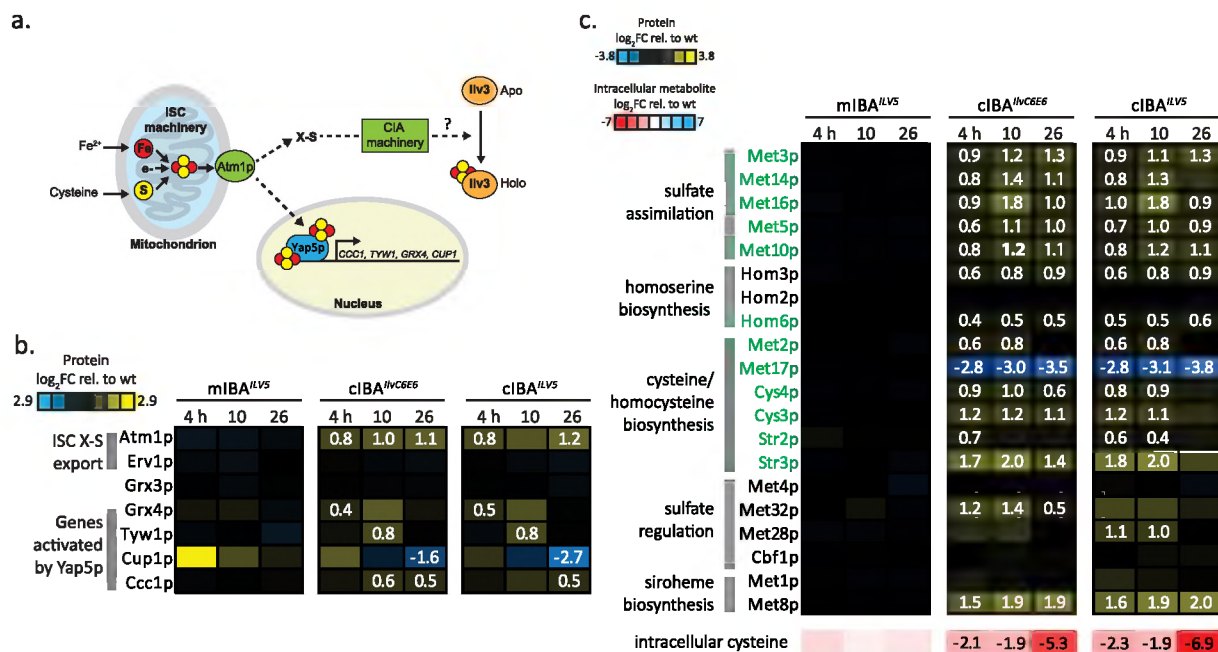


We hypothesized that the mitochondrial-localized *Ilv3p* is not a rate-limiting step in the *mIBA<sup>ILV5</sup>* strain because the required cofactor for the enzyme, a 2Fe–2S cluster, is more accessible in the mitochondria where its biogenesis begins. This is not the case for the *cIBA<sup>Ihvc6E6</sup>* and *cIBA<sup>ILV5</sup>* strains since the synthesis and delivery of the required 2Fe–2S cluster into the cytosolic-localized *Ilv3p* requires Fe–S cluster biogenesis machinery that spans multiple compartments (both the mitochondria and cytosol). Specifically, the mitochondrial iron sulfur cluster (ISC) machinery is responsible for generating the sulfur-containing intermediate (X–S), which is then exported to the cytosol via the ABC transporter *Atm1p* [53]. In the cytosol, the X–S intermediate is matured into a cluster and loaded onto the cytosolic-localized apoprotein by the cytosolic iron sulfur cluster assembly (CIA) machinery (Fig. 5a). We hypothesized that the *Ilv3p* step is rate-limiting in the *cIBA<sup>Ihvc6E6</sup>* and *cIBA<sup>ILV5</sup>* strains due to this added complexity of the cross-compartmental assembly of the required cofactor. To confirm that our cytosolic-localized *Ilv3p* was functional, we deleted the endogenous mitochondrial-localized *ILV3* in the *cIBA<sup>Ihvc6E6</sup>* strain and performed a

### 3.5. Proteomics analysis revealed a cytosolic-localized isobutanol pathway results in altered sulfur metabolism

To further explore our hypothesis that the Fe-S cluster requiring enzyme was the rate-limiting step in the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains, we took a closer look at genes involved in Fe-S cluster synthesis. The protein levels of enzymes in the ISC and CIA machinery between the engineered strains and WT were relatively unchanged, with the exception of *Atm1p*, the mitochondrial X-S intermediate transporter (Table S5). *Atm1p* was upregulated approximately 2.0-fold in the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains at all time points when compared to WT (Fig. 5b). *Atm1p* overexpression is predicted to increase the number of available clusters in the cytosol by increasing the abundance of the X-S intermediate used by the CIA machinery for generating cytosolic Fe-S clusters [53]. In the cytosol, excess Fe-S clusters are sensed by the iron responsive transcription factor, *Yap5p*. *Yap5p* can stably bind to 2Fe-2S





**Fig. 5. Proteomics response of sulfur-related pathways in the engineered strains** a) Model for cytosolic 2Fe–2S cluster biogenesis, delivery, and sensing. Fe–S cluster biogenesis begins with the mitochondrial iron sulfur cluster (ISC) machinery where a sulfur containing compound (X–S) is made and exported to the cytosol via the ABC transporter, Atm1p. Through a yet unknown mechanism, the X–S intermediate is matured into a 2Fe–2S cluster and loaded into the cytosolically localized DHAD/Ilv3p apoprotein to form the holo form; we hypothesize that this process is facilitated by the cytosolic iron sulfur cluster assembly (CIA) machinery. High cytosolic iron conditions are sensed by the transcription factor Yap5p via binding two 2Fe–2S clusters; once clusters are bound, Yap5p undergoes a conformational change and activates transcription of genes in the nucleus including *CCC1*, *TWY1*, *GRX4*, and *CUP1*. b) Heat map shows the protein levels of such genes in model a. c) Heat map shows the protein levels of genes in sulfur-related pathways and the intracellular level of cysteine. Genes that are transcriptionally activated by Met4p under cysteine-depleted conditions are indicated in green. For all heatmaps, values correspond to average  $\log_2$  fold change relative to WT at the 3 timepoints (4, 10, and 26 h). For the protein data, blue denotes lower protein levels, yellow denotes higher protein levels, and black denotes unchanged values. For the intracellular metabolite data, red denotes lower metabolite levels, blue denotes higher metabolite levels, and white denotes unchanged values. Statistical significance ( $P/FDR < 0.05$ ) is indicated by the presence of a number in the heatmap cell. (For interpretation of the references to colour in this figure legend, the reader is referred to the Web version of this article.)

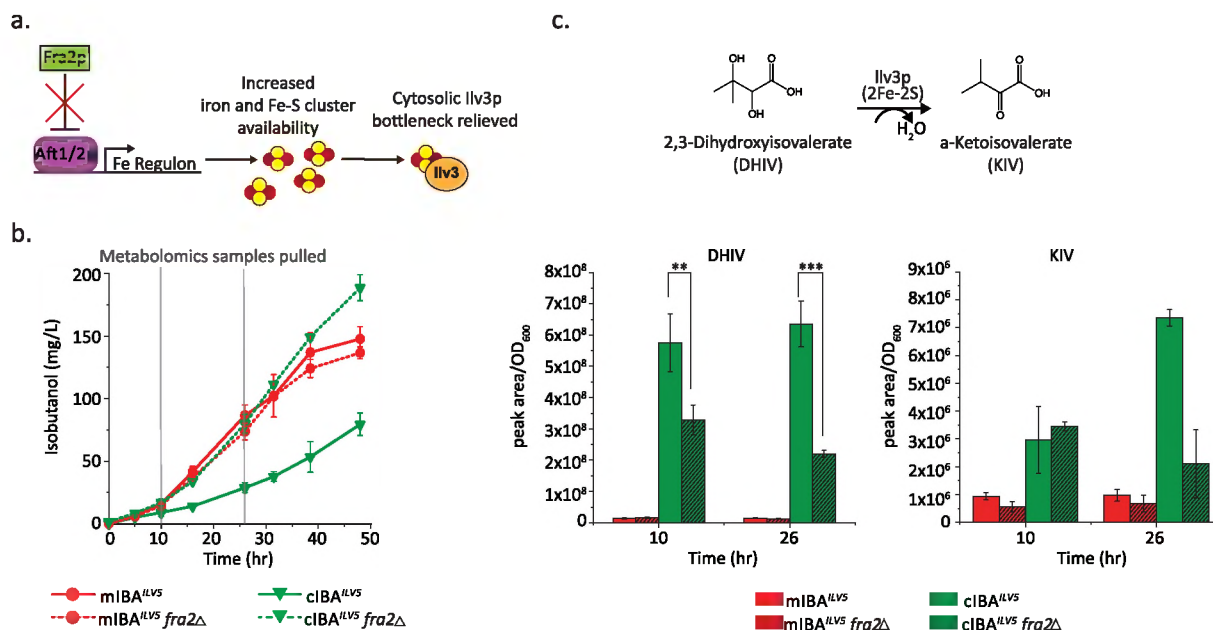
clusters, inducing a conformational change that activates the transcription of genes to help regulate iron storage including *CCC1*, *TWY1*, *GRX4*, and *CUP1* (Fig. 5a). Indeed, protein levels of Ccc1p, Tyw1p, and Grx4p were elevated in the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains for at least one of the time points with Tyw1p having the highest fold change of 1.7 at 10 h when compared to WT (Fig. 5b). This increase in Yap5p responsive genes indicated there was an increased number of 2Fe–2S clusters in the cytosol of the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains compared to WT, which was expected with the increased level of Atm1p.

We next asked if the different isobutanol pathways could affect other aspects of the strain's proteome. Pathway enrichment analysis using Funspec [48] was performed on the statistically significant protein hits from the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains to identify any enriched patterns. Proteins at a higher abundance compared to WT were enriched ( $P < 5E-5$ ) for sulfur-related pathways (methionine biosynthesis [GO:0009086], cysteine biosynthesis [GO:0019344], and sulfate assimilation [GO:0000103]) (File S5). The protein abundance of enzymes in sulfate assimilation, sulfate regulation, homoserine biosynthesis, cysteine biosynthesis, and siroheme biosynthesis pathways were elevated in the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains compared to WT (Fig. 5c). This response was largely due to the depletion of intracellular cysteine since *MET* gene expression is induced by Met4p under cysteine-limited conditions [54]; in fact, the intracellular cysteine levels were depleted in all engineered strains but more significantly in the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains (Fig. 5c). Cysteine is used as the sulfur donor for synthesizing Fe–S clusters, and we hypothesized the altered sulfur metabolism was related to the 2Fe–2S cluster requirement of the rate-limiting enzyme, Ilv3p. The elevated levels of Atm1p in conjunction with the elevated sulfur metabolism suggests that the strains with the cytosolic

pathway are trying to overcome a limitation in the quantity of cytosolic Fe–S clusters. We hypothesize that the insufficient availability of cytosolic Fe–S clusters causes the Ilv3p to be the bottleneck in the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains.

### 3.6. Increasing iron availability boosts production with a cytosolic-localized pathway

We next sought to determine if the *cIBA<sup>IlvC6E6</sup>* and *cIBA<sup>ILV5</sup>* strains' performance would benefit from increased Fe–S cluster biogenesis in the cell. This strategy was successful in increasing the activity of a different cytosolic-localized Fe–S cluster requiring enzyme, xylonate dehydratase, in *S. cerevisiae* [55,56]. This can be accomplished by increasing the availability of iron in the cell through deregulation of the iron regulon genes. To test our hypothesis, we disrupted iron homeostasis by deleting the transcriptional repressor Fra2p (also referred to its standard name Bol2p) of the iron regulon transcriptional activator, Aft1/2p, in the *cIBA<sup>ILV5</sup>* and *mIBA<sup>ILV5</sup>* strains (Fig. 6a) [53,57]. We then performed a time-course experiment where extracellular isobutanol production was monitored periodically and intracellular isobutanol metabolites were measured during mid-exponential phase (10 h) and early-stationary phase (26 h) (Fig. 6b and c). We observed that the deletion of *FRA2* significantly altered the isobutanol titer in the *cIBA<sup>ILV5</sup>* background strain, but not in the *mIBA<sup>ILV5</sup>* strain; the *cIBA<sup>ILV5</sup> fra2Δ* strain produced 190 mg/L isobutanol at 48 h which is 2.4-fold more than the *cIBA<sup>ILV5</sup>* strain ( $P < 5E-5$ ) (Fig. 6b). Furthermore, the titer achieved by the *cIBA<sup>ILV5</sup> fra2Δ* strain surpassed the isobutanol titer in our previous best producer, *mIBA<sup>ILV5</sup>*, by 1.3-fold ( $P < 5E-5$ ) indicating a high titer with a cytosolic isobutanol pathway localization can be achieved. We



**Fig. 6.** Increasing iron availability improves isobutanol production with cytosolic-localized pathway **a)** Schematic demonstrating how Ilv3p activity may be enhanced by altering iron homeostasis. The transcriptional activator, Aft1/2p, is negatively regulated by Fra2p. **b)** Isobutanol titer of engineered isobutanol producing strains with and without *FRA2* deletion. **c)** Normalized peak area (peak area/OD<sub>600</sub>) of Ilv3p's metabolites (reactant DHIV and product KIV) observed by LC-MS. Samples for metabolomics were pulled at 10 and 26 h post inoculation. Fermentation was performed under anaerobic conditions in minimal medium. Error bars represent the standard deviation of three biological replicates. Asterisks denote statistically significant differences by pairwise *t*-test (\*,  $P < 0.05$ ; \*\*,  $P < 0.005$ ; \*\*\*,  $P < 0.0005$ ).

hypothesize the *fra2* deletion had no effect on isobutanol titer in the mIBA<sup>ILV5</sup> strain because the cofactor availability for the mitochondrial-localized Ilv3p was not limited.

We next tested if the deletion of *FRA2* specifically benefited Ilv3p by looking at the intracellular metabolite levels of the enzyme's reactant, DHIV, and product, KIV (Fig. 6c). Indeed, the cIBA<sup>ILV5</sup> *fra2*Δ strain had lower levels of DHIV compared to the cIBA<sup>ILV5</sup> strain indicating the Ilv3p bottleneck was partially relieved; the normalized peak area (peak area/OD<sub>600</sub>) of DHIV was 1.7-fold ( $P < 0.05$ ) and 2.9-fold ( $P < 0.005$ ) lower in cIBA<sup>ILV5</sup> *fra2*Δ compared to cIBA<sup>ILV5</sup> at 10 and 26 h, respectively. The KIV level was also measured, but we did not observe an increased level of KIV in the cIBA<sup>ILV5</sup> *fra2*Δ strain compared to the cIBA<sup>ILV5</sup> strain as one might expect from relieving the bottleneck at Ilv3p. Instead, the KIV level between the engineered strains was not significantly altered, except at 26 h where the cIBA<sup>ILV5</sup> strain had a 3.5-fold increase in KIV compared to the cIBA<sup>ILV5</sup> *fra2*Δ strain ( $P < 0.05$ ). We suspect an accumulation of KIV was not seen because KIV is readily consumed in the subsequent step. Taken together, the *fra2* mutation in the cIBA<sup>ILV5</sup> strain resulted in an increase in isobutanol titer, potentially by partially overcoming the 2Fe–2S cluster cofactor limitation for cytosolic Ilv3p.

#### 4. Conclusions

Here, we combined transcriptomic, proteomic, and metabolomic analyses to generate a wealth of data on how enzyme pathway localization and redox cofactor-balancing affect isobutanol biosynthesis and physiology in genetically engineered *S. cerevisiae*. Localizing isobutanol pathway enzymes to the mitochondria resulted in higher titers, while cytosolic localization resulted in much lower titers. Metabolomic analysis uncovered a potential limitation in cytosolic Fe–S cluster biogenesis. This limitation could be overcome by increasing Fe uptake through deletion of *FRA2*. This strategy of increasing the availability of iron in the cell was also successful in increasing the activity of another Fe–S cluster requiring enzyme xylonate dehydratase; however, this strategy may not be effective for all Fe–S cluster requiring enzymes as this strategy had no effect on 6-phosphogluconate dehydratase activity [55,

58]. While we did not observe a beneficial effect in having a redox cofactor-balanced isobutanol pathway, we hypothesize that the cofactor imbalance will have to be resolved for the capacity of the isobutanol pathway to be enhanced. Furthermore, any problems caused by an imbalance will be exacerbated when ethanol flux is displaced to enhance the rate of isobutanol synthesis. Future functional genomics studies with engineered strains disabled for ethanol production should uncover new genetic targets for achieving greater isobutanol titers and yields.

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#### Data availability

The mass spectrometry proteomics data have been deposited to the MassIVE database with the identifier MSV000088169. The transcriptomics data discussed in this publication has been deposited in

NCBI's Gene Expression Omnibus [59] and is accessible through GEO Series accession number GSE186126 (<https://www.ncbi.nlm.nih.gov/geo/query/acc.cgi?acc=GSE186126>). Intracellular metabolomics data is available on GitHub (<https://github.com/AmadorNoguezLab/compartimentalized-isobutanol-pathways-in-S-cerevisiae>). The full isobutanol pathway cassette sequence containing mitochondrial-localized enzymes and flanking *HO* arms is available on GenBank with the identifier MZ541859 (Materials and methods 2.2).

### Credit authorship statement

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### Declaration of competing interests

JJC is a consultant for Thermo Fisher Scientific.

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### Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.synbio.2022.02.007>.

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