

Published in *Journal of the Electrochemical Society* on April 30, 2021

Too much of a good thing? Assessing performance tradeoffs of two-electron compounds for redox flow batteries

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Abstract

Engineering redox-active compounds to support stable multi-electron transfer is an emerging strategy for enhancing the energy density and reducing the cost of redox flow batteries (RFBs). However, when sequential electron transfers occur at disparate redox potentials, increases in electrolyte capacity are accompanied by decreases in voltaic efficiency, restricting the viable design space. To understand these performance tradeoffs for two-electron compounds specifically, we apply theoretical models to investigate the influence of the electron transfer mechanism and redox-active species properties on galvanostatic processes. First, we model chronopotentiometry at a planar electrode to understand how the electrochemical response and associated concentration distributions depend on thermodynamic and mass transport factors. Second, using a zero-dimensional galvanostatic charge / discharge model, we assess the effects of these key descriptors on performance (i.e., electrode polarization and voltaic efficiency) for a single half-cell. Finally, we extend the galvanostatic model to include two-electron compounds in both half-cells, demonstrating compounding voltage losses for a full cell. These results show that multi-electron compounds with disparate redox potentials are less attractive than those with concerted electron transfer—as such, we suggest new directions for molecular and systems engineering to improve the prospects of these materials for RFBs.

Keywords: Redox flow battery, Multi-electron transfer, Electrochemical engineering, Zero-dimensional modeling, Galvanostatic cycling, Chronopotentiometry

Introduction

The development of low-cost redox couples and associated electrolytes is a promising cost-reduction pathway for redox flow batteries (RFBs).^{1,2} To this end, organic molecules and metal-coordination complexes are emerging as alternative charge storage species to compete with more traditional inorganic salts. These candidate materials are especially compelling for meeting production demands, as many can be derived from abundant, widely accessible sources and synthesized at-scale using existing process knowledge and infrastructure.³ Further, their chemical structures can be functionalized to refine key properties, such as the redox potential, electrochemical reversibility, solubility, and stability.^{4–6} Of particular note is the possibility for these materials to support multiple electron transfers, which, in principle, may facilitate marked increases in capacity and concomitant decreases in energy-specific electrolyte cost.⁷ However, multi-valent redox couples are often chemically irreversible due to the increasing instability and/or decreasing solubility of the charged species.⁸ Recent research efforts have led to the advancement of several multi-electron transfer molecular platforms, which have been tuned to mitigate major decomposition pathways and promote solubility across different oxidation states in relevant electrolytes, furthering their viability in practical embodiments.^{9–12} Despite this progress, the overall impact of the multi-electron approach on cell performance has not been widely explored beyond proof-of-concept demonstrations.⁷

While many molecular engineering challenges (e.g., stability, solubility, etc.) are universal to the design of redox electrolytes, the unique electron transfer mechanisms (sequential vs. concerted) of multi-electron compounds present a characteristic feature that may constrain their design. For example, many redox-active organic molecules that undergo multi-electron transfer in aqueous electrolytes (e.g., phenazines,¹³ phenothiazines,¹⁴ and quinones^{15–17}) typically exhibit multiple

redox reactions occurring at similar potentials due to hydrogen bonding interactions present in these environments.¹⁸ Conversely, similar molecules used in nonaqueous electrolytes (e.g., bipyrimidines,¹⁹ bispyridinylidenes,²⁰ phenazines,²¹ phenothiazines,^{9,10} quinones,²² and viologens^{23,24}), some used in aqueous electrolytes (e.g., viologens^{25–28}), and metal-coordination complexes containing non-innocent ligands^{11,29–31} often feature sequential electron transfer events with disparate and easily discernable redox potentials, ranging from 200 – 800 mV. Compared to the concerted mechanism, which presents minimal voltage losses (*vide infra*), the sequential mechanism imposes significant losses, increasing with the potential difference between redox events. Indeed, prior experimental work has shown that, during galvanostatic cell cycling, there is an asymmetry between voltage-time plateaus during charge and discharge: during the charging step, more time is spent at the higher cell voltage, while during the discharging step, more time is spent at the lower cell voltage.^{9–12} This augments the difference between the average charge and discharge voltages, lowering both the voltaic and energy efficiencies of the cell. To assess the efficacy of multi-electron compounds, it is necessary to understand the magnitude of these losses, which, in turn, requires a deeper understanding of the extent to which the molecular properties and cell operating conditions contribute to RFB performance.

Low-dimensional reaction-transport models hold utility for uncovering the sources of performance loss and quantifying their contributions in electrochemical cells. Specifically, zero-dimensional models, which are the central focus of this work, consider only time-dependent behavior, foregoing spatial variation and geometric constraints in the electrochemical and fluid dynamic properties to provide theoretically concise and computationally light modeling frameworks.³² Importantly, these simple analytical treatments—based on fundamental electrochemical engineering principles—enable the determination of tradeoffs in device

performance for redox electrolytes prior to embarking on intensive cell cycling and modeling studies to understand complex behavior in geometrically-accurate domains. Such models have previously been used to assess crossover effects and various operating conditions in vanadium RFBs^{33–36} and are beginning to be used to evaluate other candidate RFB platforms.³⁷

In this work, we develop three electrochemical models (**Figure 1**) to understand the effect of two-electron compounds on cell cycling and assess their performance tradeoffs in RFBs. To gain initial insight into the underlying physics driving multi-electron transfer, we begin by analyzing the chronopotentiometric response of a one-dimensional planar electrode (**Figure 1a**), highlighting the influence of thermodynamic and mass transport factors on electrode polarization. Subsequently, using a single half-cell (**Figure 1b**) to simulate galvanostatic charge / discharge cycling, we show that voltaic efficiency is significantly affected by both the average redox potential and the potential difference between the redox events. To a lesser extent, different mass transfer rates between species, along with comproportionation reaction rates, further alter the cycling behavior. Finally, using a full cell galvanostatic cycling model (**Figure 1c**), we consider the impact of utilizing two-electron compounds in both half-cells, which results in compounding inefficiencies due to additional voltage losses and charge imbalance. By connecting molecular properties to cell performance, we are able to propose design criteria for more efficient high-capacity redox electrolytes—specifically, lowering the potential difference between redox events through molecular engineering and integrating multi-electron compounds into long-duration applications will greatly improve their viability. More broadly, this approach provides a framework for evaluating the impact of material properties on cell performance, which can be extended to investigate additional sources of inefficiency (e.g., activation and ohmic

overpotentials) and other characteristic failure modes (e.g., molecular decomposition, crossover, etc.) for candidate systems.

Theoretical Framework

The theoretical framework presented here describes concerted and sequential two-electron transfer processes by quantifying the voltage-time relationship typical of galvanostatic processes. Specifically, the sequential two-electron transfer for species A is described by **Equations (1) and (2)**.



In addition to heterogeneous electron transfer on the electrode surface, homogeneous comproportionation and disproportionation (**Equation (3)**) in the bulk must be considered when the redox potential of **Equation (2)** is more positive than that of **Equation (1)**:



In contrast to **Equations (1)-(3)**, species A may undergo a concerted two-electron transfer in which the oxidation of A proceeds directly to A^{2+} according to **Equation (4)**.



The following sections discuss the role of thermodynamics, kinetics, and mass transport effects on the reactions in **Equations (1)–(4)**, and subsequently describe model nondimensionalization and execution.

Thermodynamics and reaction kinetics

To simplify the reaction kinetics and the overall theoretical analysis, all electrode reactions are assumed to be electrochemically reversible such that reactive species at the electrode surface are in equilibrium and their concentrations are governed by the Nernst Equation (**Equations (5) and (6)** for the first and second oxidation, respectively). We note this assumption is in agreement with prior experimental literature for many of the organic molecules and metal-coordination complexes under consideration for use in RFBs.^{2,5,7}

$$E = E_1^{(A)} + \frac{RT}{F} \ln \left(\frac{C_{A^+}^s}{C_A^s} \right) \quad (5)$$

$$E = E_2^{(A)} + \frac{RT}{F} \ln \left(\frac{C_{A^{2+}}^s}{C_{A^+}^s} \right) \quad (6)$$

In **Equations (5) and (6)**, E (V) is the potential at the electrode surface, $E_1^{(A)}$ (V) is the formal redox potential of the first oxidation (**Equation (1)**), $E_2^{(A)}$ (V) is the formal redox potential of the second oxidation (**Equation (2)**), R ($8.314 \text{ J mol}^{-1} \text{ K}^{-1}$) is the universal gas constant, T (K) is the absolute temperature (here, $T = 298 \text{ K}$), F (96485 C mol^{-1}) is the Faraday constant, and C_j^s (mol m^{-3}) is the concentration of species j at the electrode surface. It is also convenient to introduce $E_{avg}^{(A)}$ as the arithmetic mean of $E_1^{(A)}$ and $E_2^{(A)}$. Note that throughout this work, all potentials are defined relative to an arbitrary reference electrode.

The rate of bulk comproportionation, r_p ($\text{mol m}^{-3} \text{ s}^{-1}$), and bulk disproportionation, r_d ($\text{mol m}^{-3} \text{ s}^{-1}$) are given by **Equations (7) and (8)**, respectively:

$$r_p = k_p C_A^\infty C_{A^{2+}}^\infty \quad (7)$$

$$r_d = k_d \left(C_{A^+}^\infty \right)^2 \quad (8)$$

Where C_j^∞ (mol m^{-3}) is the concentration of species j in the bulk solution and k_p and k_d ($\text{m}^3 \text{mol}^{-1} \text{s}^{-1}$) are the comproportionation and disproportionation rate constants, respectively. These rate constants are related by the difference in formal redox potentials, $\Delta E^{(A)} = E_2^{(A)} - E_1^{(A)}$, according to **Equation (9)**:

$$k_p = k_d \exp\left(\frac{F}{RT} \Delta E^{(A)}\right) \quad (9)$$

For a concerted two-electron transfer (**Equation (4)**), equilibrium concentrations at the electrode surface are again described by the Nernst equation as shown in **Equation (10)**.

$$E = E_{\text{avg}}^{(A)} + \frac{RT}{2F} \ln\left(\frac{C_{A^{2+}}^s}{C_A^s}\right) \quad (10)$$

Because the concerted step does not proceed through an intermediate, comproportionation and disproportionation are assumed to be negligible.

Chronopotentiometry at a planar electrode

To analyze the time-dependent potential response for sequential two-electron transfer at a planar electrode (**Figure 1a**), a one-dimensional model can be derived from the mass conservation equation in the absence of convection and migration (**Equation (11)**):

$$\frac{\partial C_j}{\partial t} = -D \nabla^2 C_j = -D \frac{\partial^2 C_j}{\partial x^2} \quad (11)$$

Subject to the following initial and boundary conditions:

$$C_j(t=0, x) = C_j^\infty \quad (12)$$

$$-D \frac{\partial C_j(t, x=0)}{\partial x} = N_j \quad (13)$$

$$C_j(t, x=\infty) = C_j^\infty \quad (14)$$

Where t (s) is the time, x (m) is the axial position perpendicular to the planar electrode surface, D ($\text{m}^2 \text{s}^{-1}$) is the diffusivity, which is assumed to be the same for all species, C_j (mol m^{-3}) is the local concentration of species j , and N_j ($\text{mol m}^{-2} \text{s}^{-1}$) is the molar flux of species j to the electrode surface. The solution to **Equations (11)-(14)** for the time-dependent concentration of species j is given by **Equation (15)**.³⁸

$$C_j(x,t) = C_j^\infty - \frac{1}{(\pi D)^{1/2}} \int_0^t \frac{-N_j(\eta)}{(t-\eta)^{1/2}} \exp\left(\frac{-x^2}{4D(t-\eta)}\right) d\eta \quad (15)$$

Note that η is an integration variable. To derive the electrode potential as a function of time, **Equation (16)** relates the applied current, I (A), to the partial currents, I_1 and I_2 (A), for the reactions given in **Equations (1) and (2)**, respectively:

$$I = I_1 + I_2 \quad (16)$$

The partial currents are equivalent to the surface fluxes according to **Equations (17)-(19)**:

$$N_A = -\frac{I_1}{FS} \quad (17)$$

$$N_{A^+} = \frac{I_1}{FS} - \frac{I_2}{FS} \quad (18)$$

$$N_{A^{2+}} = \frac{I_2}{FS} \quad (19)$$

Here, S (m^2) is the electrode surface area. **Equation (15)** can be combined with **Equations (16)–(19)** for each species to determine the electrode potential as a function of time using **Equations (5) and (6)**. These coupled, nonlinear equations can then be solved implicitly, as discussed below.

Galvanostatic cell cycling

To describe the effects of sequential two-electron transfers on galvanostatic charge / discharge, a zero-dimensional model is derived (**Figure 1b**). Similar to the planar electrode case, the model applies a constant charging current (**Equation (16)**), which is the sum of the partial currents. Electrode kinetics are again described by **Equations (5)** and **(6)**, and the relationship between the bulk and surface concentrations of each species can be described by convective mass transfer (**Equations (20)** and **(21)**) and the flux balance (**Equation (22)**):

$$I_1 = FSk_{m,A} (C_A^\infty - C_A^s) \quad (20)$$

$$I_2 = -FSk_{m,A^{2+}} (C_{A^{2+}}^\infty - C_{A^{2+}}^s) \quad (21)$$

$$I_1 - I_2 = -FSk_{m,A^+} (C_{A^+}^\infty - C_{A^+}^s) \quad (22)$$

Here, $k_{m,j}$ (m s^{-1}) is the mass transfer coefficient of species j . **Equations (20)–(22)** can be combined with the equilibrium expressions in **Equations (5)** and **(6)** to arrive at an expression for the surface concentration of A^+ ($C_{A^+}^s$):

$$C_{A^+}^s = \frac{k_{m,A} C_A^\infty + k_{m,A^+} C_{A^+}^\infty + k_{m,A^{2+}} C_{A^{2+}}^\infty}{k_{m,A} \exp\left(\frac{F}{RT}(E_1^{(A)} - E)\right) + k_{m,A^+} + k_{m,A^{2+}} \exp\left(\frac{F}{RT}(E - E_2^{(A)})\right)} \quad (23)$$

The surface concentration is then substituted into **Equation (16)** to solve for the electrode potential as a function of the time-dependent bulk concentrations (**Equation (24)**). Again, the coupled nonlinear algebraic equations (**Equations (23)** and **(24)**) can be solved implicitly (vide infra).

$$I = FSk_{m,A} \left[C_A^\infty - C_{A^+}^s \exp\left(\frac{F}{RT}(E_1^{(A)} - E)\right) \right] - FSk_{m,A^{2+}} \left[C_{A^{2+}}^\infty - C_{A^+}^s \exp\left(\frac{F}{RT}(E - E_2^{(A)})\right) \right] \quad (24)$$

Finally, to track changes in the bulk concentration, the system is assumed to be well-mixed such that the total current is uniformly distributed throughout the entire volume. Note that the model

treats the electrode half-cell, reservoir, and connecting tubing as a single continuous domain. For this treatment, the mass balances on the reactor volume for each species are a system of ordinary differential equations as shown by **Equations (25)–(28)**,

$$V \frac{dC_A^\infty}{dt} = -\frac{I_1}{F} - V k_p C_A^\infty C_{A^{2+}}^\infty + V k_d (C_{A^+}^\infty)^2 \quad (25)$$

$$V \frac{dC_{A^+}^\infty}{dt} = \frac{I_1}{F} - \frac{I_2}{F} + 2V k_p C_A^\infty C_{A^{2+}}^\infty - 2V k_d (C_{A^+}^\infty)^2 \quad (26)$$

$$V \frac{dC_{A^{2+}}^\infty}{dt} = \frac{I_2}{F} - V k_p C_A^\infty C_{A^{2+}}^\infty + V k_d (C_{A^+}^\infty)^2 \quad (27)$$

which are subject to the initial conditions:

$$C_j^\infty(t=0) = C_j^o \quad (28)$$

V (m³) is the total electrolyte volume and C_j^o (mol m⁻³) is the initial bulk concentration. These coupled ordinary differential equations can be numerically solved to yield changes in bulk concentrations as a function of time, which can be further used to implicitly solve for the electrode potential (**Equations (23) and (24)**).

For concerted electron transfer in the absence of comproportionation, the mass balances can be solved analytically, yielding time-dependent bulk concentrations and the subsequent electrode potential according to **Equations (29)–(31)**:

$$C_A^\infty = C_A^o - \frac{It}{2FV} \quad (29)$$

$$C_{A^{2+}}^\infty = C_{A^{2+}}^o + \frac{It}{2FV} \quad (30)$$

$$E = E_{avg}^{(A)} + \frac{RT}{2F} \ln \left(\frac{C_{A^{2+}}^{\infty} + \frac{I}{2FSk_{m,A^{2+}}}}{C_A^{\infty} - \frac{I}{2FSk_{m,A}}} \right) \quad (31)$$

Dimensionless variables and analysis

To reduce the total number of independent model parameters, dimensionless variables are introduced. **Equation (32)** defines the dimensionless concentration, θ_j^m , which describes the concentration in state z ($z \in \{s, \infty, o\}$) normalized by the total bulk concentration, C_T^{∞} (mol m⁻³), which remains constant:

$$\theta_j^z = \frac{C_j^z}{C_A^{\infty} + C_{A^+}^{\infty} + C_{A^{2+}}^{\infty}} = \frac{C_j^z}{C_T^{\infty}} \quad (32)$$

Equation (33) defines the dimensionless charging current, Ψ , which is derived by normalizing the total charging current by the mass transfer limiting current for the oxidation of A :

$$\Psi = \frac{I}{Fk_{m,A}SC_T^{\infty}} \quad (33)$$

Similarly, **Equation (34)** defines a dimensionless time, τ , which normalizes the cycle time by the theoretical charging time for one electron:

$$\tau = \frac{tI}{FVC_T^{\infty}} \quad (34)$$

The mass transfer coefficients are normalized by that of species A according to **Equation (35)** to yield dimensionless mass transfer coefficients, γ_j :

$$\gamma_j = \frac{k_{m,j}}{k_{m,A}} \quad (35)$$

Finally, **Equation (36)** scales the rate of comproportionation by the charging current to give a dimensionless rate constant, κ :

$$\kappa = \frac{Vk_p (C_T^\infty)^2 F}{I} \quad (36)$$

Note that for the discharging step, the current reverses sign, resulting in negative values for Ψ , τ , and κ . To ensure the solutions comprise a consistent time domain ($\tau \in [0, 2]$), the sign of τ is reversed. The complete dimensionless equations are provided in the **Supplementary Information (SI)**.

In this analysis, the coupled ODEs (**Equations (25)–(28)**) were solved using the *ode15s* function in MATLAB® R2018a, while nonlinear algebraic equations were solved implicitly using the *fsolve* function in the same program. The software code used to simulate charge / discharge cycling is included in **Sections S.4 and S.5** of the **SI**. Simulations were performed on a Dell Latitude 7290 laptop computer with an Intel® Core™ i7-8650U processor (quad-core, 1.90 GHz) and random-access memory of 16 GB. Solving each charge / discharge cycle took approximately 20 – 30 seconds. To allow for capacity stabilization during cycling, a total of five complete charge / discharge cycles were simulated (**Figures S1 and S2**) and results for the fifth cycle are reported, unless stated otherwise.

Results and Discussion

Chronopotentiometry at a planar electrode

To gain insight into the underlying physics of electron transfer in two-electron compounds, we first model this process for a one-dimensional planar electrode (**Figure 1a**). Chronopotentiometry is a constant-current technique that measures potential at the electrode surface arising from surface

redox reactions coupled with boundary layer diffusion, as opposed to galvanostatic cycling, where transport primarily takes place via the convection of bulk species whose concentrations change over time. Although the modes of transport are different, chronopotentiometry displays analogous behavior to galvanostatic cycling and can therefore serve as a basis for interpreting the underlying physics present in both systems. For brevity, we examine only the oxidation of A to A^{2+} via sequential electron transfers, assuming that all species have equal diffusion coefficients and comproportionation reaction rates are negligible. When a constant current is applied to a planar electrode, the reactant species concentration at the surface decreases until inevitably approaching zero, which results in a sharp increase in potential. The time required for this process is commonly referred to as Sand's time,³⁹ $t_{sand}^{(n)}$ (s), as shown in **Equation (37)**:

$$t_{sand}^{(n)} = \frac{(nFSC_j^\infty)^2 \pi D_j}{4I^2} \quad (37)$$

n is the number of electrons transferred per redox reaction (here, $n = 1$). **Figure 2a** shows the time-dependent potential response for a constant current applied to a planar electrode for a two-electron donating species, A , with an exemplary value of $\Delta E^{(A)} = 0.6$ V. The first plateau, corresponding to the oxidation of A to A^+ (**Equation (1)**), is equivalent to a traditional Sand's time measurement for a one-electron transfer. Then, as A^+ continues to be oxidized to A^{2+} (**Equation (2)**), a much longer second plateau can be observed until eventually reaching another sharp increase in potential. Note that the time required to reach this second asymptote is equivalent to that for a concerted two-electron transfer (**Equation (37)**); however, similar to galvanostatic cycling, the time spent at each plateau is unequal.^{9–12}

Although initially dissimilar plateau durations may seem unintuitive, a closer look at the temporal evolution of the concentration and current distributions reveals this to be a sensible

outcome (**Figures 2b** and **2c**). Consistent with conventional Sand's time, the concentration of species A reaches zero at $t = t_{sand}^{(1)}$. However, as current continues to flow, A does not stop diffusing from the bulk; rather, the oxidation of A continues contributing significantly to the current, resulting in an elongation of its concentration profile. Correspondingly, the concentration of A^+ at the surface (**Figure 2c**) increases sharply as $t \rightarrow t_{sand}^{(1)}$ but decreases more gradually because the partial current (I_2) of the second oxidation remains low as A^+ freely diffuses away from the electrode. Thus, despite the higher potential plateau corresponding to the second oxidation, the first oxidation continues to supply a significant fraction of current (I_1), extending the duration of the second plateau as compared to the first. Although analytically simpler, this illustration of chronopotentiometric reaction-diffusion at a planar electrode is analogous to the physics present during galvanostatic charge / discharge and underpins the combined effects of thermodynamics, kinetics, and mass transfer on two-electron transfer compounds.

Two-electron galvanostatic half-cell cycling

With a foundational understanding of the combined factors influencing electrode polarization, we extended our analysis to galvanostatic charging / discharging of two-electron compounds to interrogate their cycling performance. Here, we consider only a single half-cell (**Figure 1b**), assuming the other half-cell remains at a fixed reference potential of 0 V, and apply a constant, dimensionless charging rate for both charge and discharge (Ψ), which is defined as the applied current relative to the mass transfer limiting current. The resulting potential is a measure of the kinetic and mass transport losses in the half-cell, but note that this model neglects ohmic losses. While these are generally a dominant source of voltage loss in RFBs,⁴⁰ they are mostly independent of redox-active material properties, which are the focus of this work. To aid comparison, we

initially assume all species have equal mass transfer coefficients ($\gamma_{A^+} = \gamma_{A^{2+}} = 1$) and that comproportionation reaction rates are negligible ($\kappa = 0$); these complicating factors will be introduced subsequently and sequentially to explore their individual effects.

Figure 3a shows a typical charge / discharge profile for a two-electron transfer process at an intermediate dimensionless current ($\Psi = 0.25$), comparing the response of a concerted electron transfer to that of the more commonly observed sequential electron transfer both with and without a potential difference ($\Delta E^{(A)} = 0.6$ V and $\Delta E^{(A)} = 0$ V, respectively). Because τ is non-dimensionalized by the charging capacity for a one-electron transfer, the theoretical capacity for the two-electron system is, by definition, $\tau = 2$. The accessed capacity (i.e., the maximum value of τ) is directly related to the applied current—in the case of equal mass transfer coefficients, the accessed capacity equals $2(1 - \Psi)$. This means that, in the case of $\Psi = 0.25$, the electrolyte undergoes a state of charge (SOC) swing between 12.5% and 87.5% and accesses 75% of the theoretical capacity, as discussed in **Section S.2** of the SI. Comparing the electrochemical responses, we initially observe a non-negligible difference between the concerted and sequential ($\Delta E^{(A)} = 0$ V) electron transfer mechanisms. Specifically, there is a slightly larger difference between average charging and discharging potentials calculated for the sequential mechanism (31.3 mV) compared to the concerted mechanism (19.2 mV), which can be understood by considering that the sequential reaction proceeds through an intermediate, imposing additional mass transfer losses (and thus overpotential).

When a potential difference is applied between the redox events, we observe the formation of two separate plateaus during cycling—during charging, the lower plateau corresponds to the oxidation of A to A^+ (**Equations (1)**) and the higher plateau corresponds to the oxidation of A^+ to A^{2+} (**Equation (2)**). For very small currents ($\Psi \approx 0.001$), the plateaus are nearly symmetric (i.e.,

each plateau accounts for almost the same dimensionless time), and the theoretical capacity is accessed. However, increasing currents result in reduced accessible capacity and significant plateau asymmetry (**Figure 3b**), as demonstrated in earlier bulk electrolysis and cell cycling experiments.^{9–12} Like the planar electrode case (**Figure 2**), species A is not consumed entirely once the second plateau is reached and continues contributing to the current, resulting in a slower consumption of A^+ than if no A remained. At dimensionless currents above $\Psi = 0.5$, the charging profile displays a disappearance in the first plateau—at this point, the oxidation of A on charge and the reduction of A^{2+} on discharge are mass transfer limiting (zero surface concentration) at all points during cycling, meaning the electrode polarization is driven entirely by the second reaction step. Also, because the mass transfer coefficients are assumed to be equal, the resulting charge and discharge curves are symmetric; however, this changes under varying values of γ_{A^+} and $\gamma_{A^{2+}}$ (vide infra), as mass transfer overpotentials contribute unequally to charge and discharge.

While there are several means by which the effects of asymmetry may be quantified, its most significant influence is on voltaic efficiency, which can be expressed as the ratio of the average discharge voltage to the average charge voltage. For reference, under typical cycling conditions, the coulombic efficiency is near unity, thus the voltaic efficiency is a reasonable approximation of the energy efficiency, defined as the product of the coulombic and voltaic efficiencies. In general, the voltaic efficiency decreases with increasing current as the effects of ohmic, kinetic, and mass transport losses become more pronounced, although as mentioned above, we neglect ohmic losses in this study. Additionally, we consider losses from only one half-cell with reversible kinetics, and therefore, these values should be considered as upper bounds for the voltaic efficiency under the specified conditions. Considering these constraints, the results obtained from this model cannot be quantitatively compared to the performance of experimental flow cells; however, we aim not to

describe specific systems but rather investigate the phenomenology of multi-electron transfer, which is independent of more complex design features.

Figure 4 shows the combined effect of dimensionless charging current, potential difference, and average redox potential on the half-cell voltaic efficiency. Ranges chosen for the average redox potential and potential differences reflect values for experimentally reported redox species in aqueous and nonaqueous electrolytes. The curves are characterized by two distinct regions—at low currents, the voltaic efficiency drops rapidly with increasing current due to an imbalance between the two plateaus; at higher currents, where the first plateau disappears completely, the voltaic efficiency slope parallels that of the case where $\Delta E^{(A)} = 0$ V with an offset in magnitude. Importantly, the presence of a potential difference between redox events drastically reduces voltaic efficiency under all conditions, though especially at increasing currents and lower average redox potentials, which are particularly relevant for aqueous chemistries.⁴¹ In general, voltage losses can be compensated with higher average redox potentials, but the half-cell voltaic efficiency for sequential processes may still suffer a 10 – 20% decrease at moderate currents and high cell voltages compared to the concerted process, which represents the maximum voltaic efficiency. These losses in voltaic efficiency are substantial, especially considering they only account for one electrochemically reversible half-cell—additional kinetic (e.g., quasireversible and irreversible behavior,⁴² low electrochemically active surface area⁴³) and ohmic losses (e.g., electrolyte and membrane resistance⁴⁰) will further reduce overall efficiency.

Additional mass transfer losses can be evaluated by relaxing the assumption that all species have equal mass transfer coefficients; to simplify our analysis, we will consider cases where the mass transfer rates of A^+ and A^{2+} are equal ($\gamma_{A^+} = \gamma_{A^{2+}}$) but differ from A . The values used here ($\gamma_{A^+} = 0.8, 1.2$) were estimated based on previously reported Sherwood number correlations for

RFBS⁴⁴ for typical changes in diffusivity for soluble two-electron redox species in differing oxidation states.^{9,11} Although the variations in mass transfer are relatively small, the effects can be readily observed from the respective charge / discharge profiles (**Figure 5a**); specifically, the charging and discharging curves become asymmetric, as differing mass transfer rates affect the relative fluxes and, consequently, the surface concentrations of each species. Similar to the asymmetry between plateaus described already (see **Figure 4**), this additional asymmetry impacts the half-cell voltaic efficiency (**Figure 5b**). First, we observe the appearance of an additional change in slope at intermediate dimensionless currents corresponding to the disappearance of a single charge / discharge plateau. For example, when $\gamma_{A^+} = 0.8$, the first plateau on the discharging curve will disappear while the first plateau on the charging curve persists. Second, as expected, slower mass transfer rates (e.g., reduced flow rates, higher electrolyte viscosity, larger redox-active molecules) correspond to lower voltaic efficiencies at all current values.

Given the inclusion of variable mass transfer coefficients, the differences between individual species thus necessitates the treatment of comproportionation reactions. When considering sequential electrode reactions of identical kinetic and mass transport conditions, comproportionation does not play a distinguishable role in determining the electrode potential as the species identity does not influence boundary layer fluxes.^{45,46} Comproportionation yields a shift in the time-dependent bulk concentrations toward the formation of A^+ (**Figure 6a**), and with varying mass transport coefficients, this causes charge / discharge curves to become increasingly asymmetric, thus accentuating voltaic efficiency losses that arise from differences in mass transfer (**Figure 6b**). However, for comproportionation to proceed, both A and A^{2+} must be present in solution concurrently—therefore, this effect only occurs where mass transfer limitations lead to simultaneous oxidation of A and A^+ (charging) or reduction of A^{2+} and A^+ (discharging). These

simultaneous reactions only constitute a fraction of the total charging time, which increases with increasing current, meaning that its influence on voltaic efficiency only becomes discernable at dimensionless currents above $\Psi \approx 0.5$. Operation under such low accessible capacity regimes is likely to be impractical and inefficient, and as such, we tentatively conclude that comproportionation for two-electron transfer is negligible under typical galvanostatic conditions. Note that in this treatment, comproportionation and disproportionation reactions are assumed to occur only in the bulk as opposed to the mass transfer boundary layer. This assumption ignores the expected non-linear boundary layer concentrations, although even if the concentrations were to change in the boundary layer, the system is still beholden to the fact that comproportionation reactions only occur alongside the simultaneous oxidation / reduction of both species, so any significant effects will still be restricted to higher currents. As a result, we expect this will have only minor effects on the overall voltaic efficiency and, consequently, the conclusions drawn here are expected to remain valid.

Full cell analysis with two-electron compounds at both electrodes

To this point, we have only considered two-electron compounds in a half-cell, holding the counter half-cell at a constant reference potential (0 V). However, the presence of two-electron reactions in both half-cells presents additional voltage losses. Here, we introduce a second redox-active species, B , which undergoes analogous two-electron transfer according to **Equations (38)** and **(39) (Figure 1c)**:



Species B is subject to the same governing equations as species A , which are detailed in the SI. For simplicity, we once again neglect ohmic losses and assume that mass transfer rates for all species are equal, the latter of which implies comproportionation / disproportionation reactions can also be ignored. In addition, we impose $\Delta E^{(A)} = \Delta E^{(B)} = 0.6 \text{ V}$ and $E_{avg}^{(B)} = 0 \text{ V}$ for all analyses presented here. Note that half-cell reactions proceed in opposite directions—a positive, oxidizing current applied to species A corresponds to a negative, reducing current applied to species B , and vice versa.

While one would correctly expect voltage losses to double in the case of a full cell if A and B were symmetric (i.e., equal concentrations, volumes, states of charge, transport properties, cell features), there are additional factors when this symmetry deviates that further hinder performance. In particular, we study charge imbalance (i.e., where the half-cells exist at different states of charge), which may result from self-discharge reactions occurring in the bulk or undesired side reactions (e.g., solvent or supporting salt decomposition, crossover-induced self-discharge, redox species decay). For one-electron compounds, this primarily impacts the accessible capacity because one half-cell becomes capacity-limiting during charge while the other is capacity-limiting during discharge.⁴⁷ For two-electron compounds, the effects of charge imbalance become more pronounced, significantly impacting the shape of the charge / discharge curves and the subsequent voltaic efficiency.¹⁰ To quantify charge imbalance between the two half-cells, we vary the initial dimensionless concentration of A (θ_A^o), assuming the initial dimensionless concentration of B^{2+} is 1.

Figure 7a shows representative cycling profiles for the full cell potential at varying degrees of charge imbalance. Most notably, because each compound features a potential difference ($\Delta E^{(j)}$), the difference between plateaus is doubled for the full cell. In the presence of charge imbalance,

an intermediate plateau appears, corresponding to the disappearance of the first potential plateau for one half-cell. For example, during the charging step, species A will be fully oxidized to A^+ before species B^{2+} can be fully reduced to B^+ , resulting in the intermediate plateau, which extends with increasing degrees of charge imbalance. **Figure 7b** shows the resultant effect of these behaviors on voltaic efficiency. Compared to the single half-cell examined in **Figure 4**, the inclusion of both half-cells doubles the associated losses and further diminishes the voltaic efficiency. Like the case of different mass transfer rates, charge imbalance leads to a characteristic region corresponding to the sequential disappearance of charge / discharge plateaus at increasing dimensionless currents. However, despite the reduction in dimensionless capacity shown in **Figure 7a**, charge imbalance causes only minor losses in voltaic efficiency at low to moderate currents ($0.2 < \Psi < 0.5$). Overall, the combined effects of two-electron compounds at both electrodes and charge imbalance result in heightened voltaic efficiency losses compared to the single half-cell.

Design strategies for multi-electron RFBs

The models explored here provide initial evidence that the multi-electron approach, while promising, has significant limitations if operating conditions and molecular design are not carefully considered. Even under optimistic conditions (i.e., losses at one electrode, reversible kinetics, no ohmic losses), we observe 10 – 20% losses in voltaic efficiency at moderate dimensionless currents ($\Psi \approx 0.2$), and these losses grow as the average redox potential decreases and potential difference increases (ca. 30 – 40% losses). Therefore, the advantages of increased charge storage capacity in multi-electron transfer must be weighed against the drawbacks in flow battery performance for a given redox chemistry.

In particular, the losses observed here for two-electron materials are driven primarily by mass

transfer, requiring current densities well below the mass transfer limit and / or considerably high mass transfer coefficients to maintain high voltaic efficiency. Such conditions present a complex design tradeoff, where additional stack costs due to increasing cell area and pumping costs due to improving mass transfer rates compete with concomitant advancements in electrochemical performance. This may restrict the viable operating space to applications where costs are less dependent on energy efficiency, as the ability to tolerate voltage losses is closely tied to technoeconomics and system specifications. For example, long-duration and/or low current energy storage applications may be comparatively more tolerant of low voltaic efficiencies if other related capital costs are sufficiently low.^{48,49} Alternatively, higher cell voltages, enabled by nonaqueous electrolytes⁸ and certain aqueous electrolytes,⁵⁰ can at least partially offset the increased overpotentials of multi-electron transfer (**Figure 4**).

To reduce the losses associated with sequential multi-electron transfer, molecular engineering efforts should aim to minimize the potential difference between electron transfer events without sacrificing cell voltage, solubility, or stability. Independently tuning the properties of individual redox events (e.g., potential inversion⁵¹) is a significant challenge, but future molecular engineering campaigns can build upon previously established examples and strategies, presenting new opportunities for research in this area.^{19,20,52–55} For example, Kini et al. demonstrated that nonaqueous anthraquinone derivatives may undergo potential inversion by virtue of successive benzo substitution. Upon functionalization from the tetracyano naphthaquinone to the analogous anthraquinone derivative, a shift is observed from sequential one-electron transfer events to a concerted two-electron transfer due to the distorted, non-planar molecular structure of the anthraquinone.^{52,55} Similarly, engineering the supporting electrolyte (i.e., solvent and supporting salt) may serve as an additional handle to modulate the properties of multi-electron redox

couples.^{56–58} These examples highlight the need for a more holistic conceptualization of the combined steric and electronic character of such molecules that influence their electrochemical nature, which should serve to advance fundamental knowledge in molecular electrochemistry and lead to improved nonaqueous RFB chemistries. Conversely, many aqueous organic compounds that undergo proton-coupled electron transfer already exhibit multi-electron reactions with a minimal potential difference,^{13–15} but these electron transfer reactions should be carefully scrutinized to elucidate gaps between their redox potentials,⁵⁹ as the low cell voltages of these systems make them more susceptible to performance losses.

Conclusions

The emergence of charge storage materials that support the reversible transfer of multiple electrons provides new pathways toward high energy density, low-cost charge storage. However, depending on the electrochemical and transport properties of the redox electrolyte, these multi-electron compounds face inherent design tradeoffs between improved storage capacity and diminished voltaic efficiency. Here, we have explored various electrochemical models to describe the underlying phenomenology of two-electron transfer in RFBs and to estimate upper bounds for these performance tradeoffs, focusing on the redox electrolyte properties and foregoing more complex geometric constraints. These results reveal that the charging rate (Ψ), average redox potential ($E_{avg}^{(j)}$), and potential difference between redox events ($\Delta E^{(j)}$) primarily drive voltaic efficiency losses, with relative mass transfer rates (γ_j) and comproportionation rates (κ) playing more nuanced roles. Considering the possible limitations, synthetic chemists and material scientists may seek new strategies to tune independent redox events, such as introducing concepts of potential inversion for nonaqueous electrolytes or leveraging existing knowledge of proton-

coupled electron transfer for aqueous electrolytes. This low-dimensional modeling approach can further serve as a framework to bound performance for novel charge storage materials, including those with more complex electron transfer mechanisms, and to predict performance prior to embarking on complicated and time-consuming cell cycling studies.

CRedit authorship contribution statement

Bertrand J. Neyhouse: Conceptualization, Methodology, Software, Validation, Investigation, Data curation, Visualization, Writing – original draft, Writing – review and editing. **Alexis M. Fenton Jr.:** Validation, Visualization, Writing – original draft, Writing – review and editing. **Fikile R. Brushett:** Conceptualization, Project administration, Supervision, Writing – original draft, Writing – review and editing.

Acknowledgements

This work was funded by the National Science Foundation (NSF) under Award Number 1805566. B.J.N. gratefully acknowledges the NSF Graduate Research Fellowship Program under Grant Number 1122374. Any opinion, findings, and conclusions or recommendations expressed in this material are those of the authors and do not necessarily reflect the views of the NSF. The authors also thank Katharine Greco, Dr. Jeffrey Kowalski, Kara Rodby, and Kevin Tenny of the Brushett Research Group for insightful discussion.

List of variables and constants

C_j^z	Concentration of species j in state z (mol m ⁻³)
C_T^∞	Total bulk species concentration (mol m ⁻³)
D	Diffusion coefficient (m ² s ⁻¹)
E	Electrode potential (V)
$E_1^{(j)}$	Formal redox potential for the first oxidation of species j (V)
$E_2^{(j)}$	Formal redox potential for the second oxidation of species j (V)
$E_{avg}^{(j)}$	Average redox potential of species j (V)
$\Delta E^{(j)}$	Difference in formal redox potentials of species j (V)
F	Faraday's constant (96485 C mol ⁻¹)
I	Galvanostatic charging current (A)
I_1	Partial current for the first oxidation (A)
I_2	Partial current for the second oxidation (A)
k_d	Disproportionation rate constant (m ³ mol ⁻¹ s ⁻¹)
$k_{m,j}$	Convective mass transfer coefficient of species j (m s ⁻¹)
k_p	Comproportionation rate constant (m ³ mol ⁻¹ s ⁻¹)
n	Number of electrons transferred per redox reaction
N_j	Molar flux of species j (mol m ⁻² s ⁻¹)
r_d	Bulk disproportionation rate (mol m ⁻³ s ⁻¹)
r_p	Bulk comproportionation rate (mol m ⁻³ s ⁻¹)
R	Universal gas constant (8.314 J mol ⁻¹ K ⁻¹)
S	Electrode surface area (m ²)
t	Time (s)
$t_{sand}^{(n)}$	Sand's time for a redox reaction with n electrons (s)
T	Temperature (K)
V	Electrolyte volume (m ³)
x	Axial position perpendicular to the planar electrode surface (m)

Greek symbols

γ_j	Dimensionless mass transfer coefficient of species j
η	Integration variable (s)
θ_j^z	Dimensionless concentration of species j in state z
κ	Dimensionless comproportionation rate
τ	Dimensionless charging time
Ψ	Dimensionless charging current

Superscripts

s	Surface
∞	Bulk solution
o	Initial state

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Figures

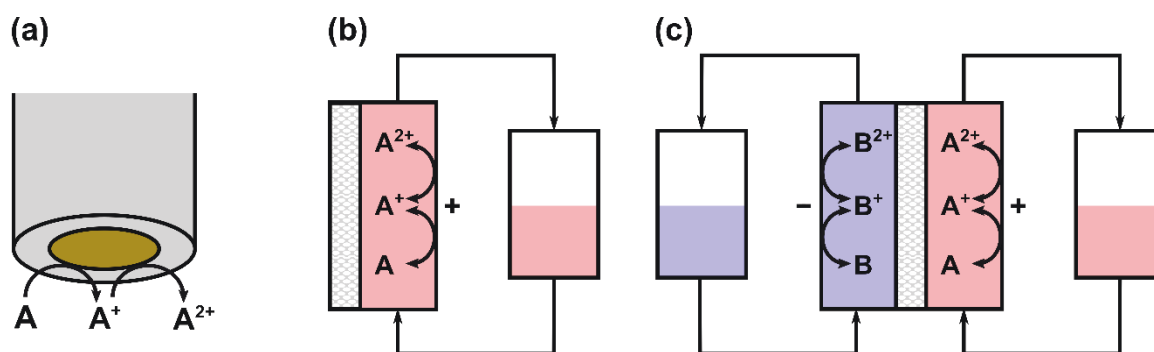


Figure 1. Schematic of modeling domains for (a) chronopotentiometry at a planar electrode, (b) galvanostatic charging / discharging for a single half-cell with a two-electron compound A , and (c) galvanostatic charging / discharging of a full cell with the two-electron compounds A and B .

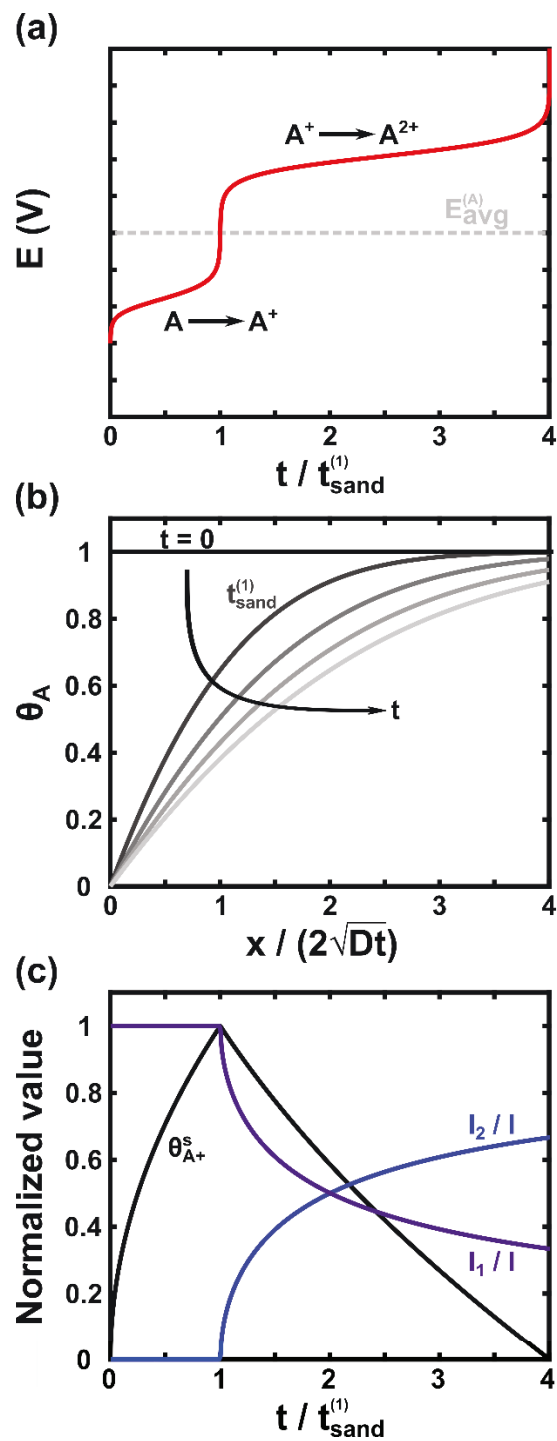


Figure 2. (a) Chronopotentiometry at a planar electrode for a generic $E_{\text{avg}}^{(A)}$ and $\Delta E^{(A)}$; the response is independent of the applied current. (b) Temporal evolution of the dimensionless concentration profile for species A . (c) Temporal evolution of the dimensionless surface concentration of species A^+ and the normalized partial currents.

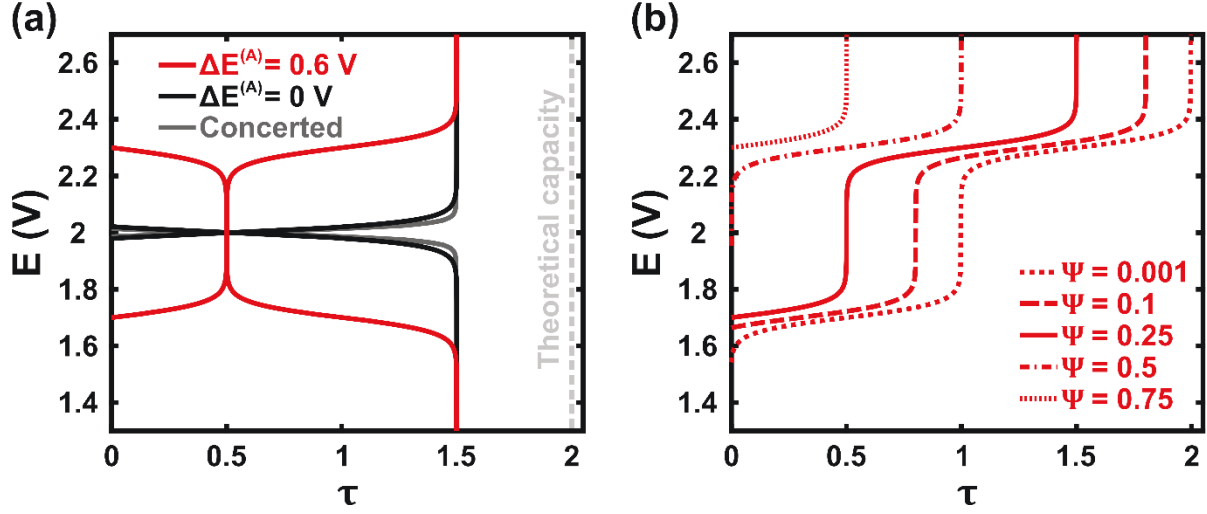


Figure 3. (a) Charge / discharge profiles shown for $\Psi = 0.25$ and different values of the potential difference (sequential mechanism) compared to the concerted mechanism, and (b) charge profiles for increasing values of dimensionless charging current ($\Delta E^{(A)} = 0.6$ V). Results shown for $E_{avg}^{(A)} = 2$ V, $\gamma_{A^+} = \gamma_{A^{2+}} = 1$, and $\kappa = 0$.

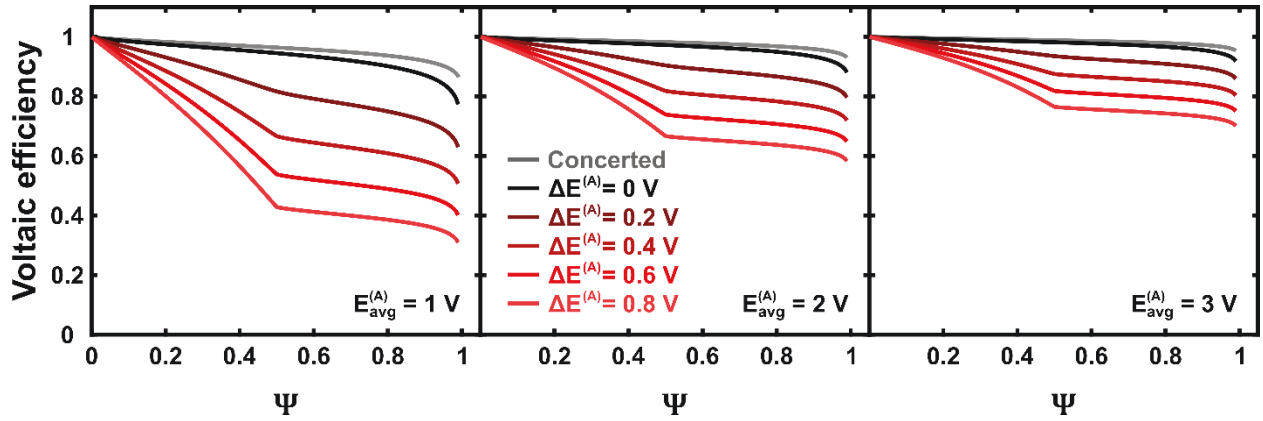


Figure 4. Half-cell voltaic efficiency as a function of dimensionless charging current, comparing a concerted two-electron transfer to a sequential two-electron transfer with varied $\Delta E^{(A)}$ for increasing values of $E_{avg}^{(A)}$. Results shown for $\gamma_{A^+} = \gamma_{A^{2+}} = 1$ and $\kappa = 0$.

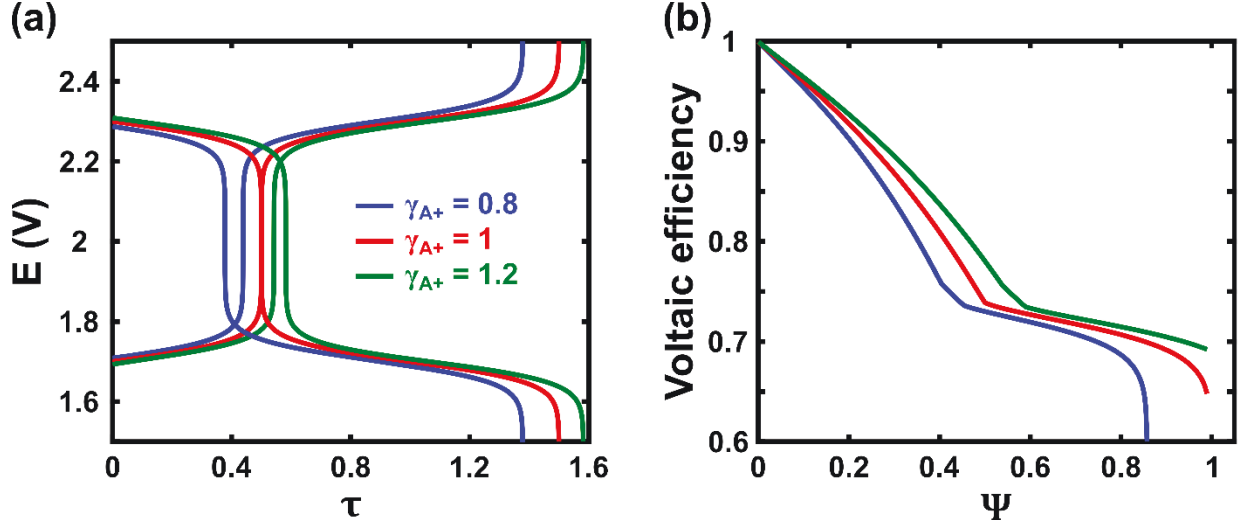


Figure 5. (a) Charge / discharge profiles shown for $\Psi = 0.25$ and (b) half-cell voltaic efficiency as a function of dimensionless current for varying mass transfer coefficients ($\gamma_{A^+} = \gamma_{A^{2+}}$). Results shown for $E_{avg}^{(A)} = 2$ V, $\Delta E^{(A)} = 0.6$ V, and $\kappa = 0$.

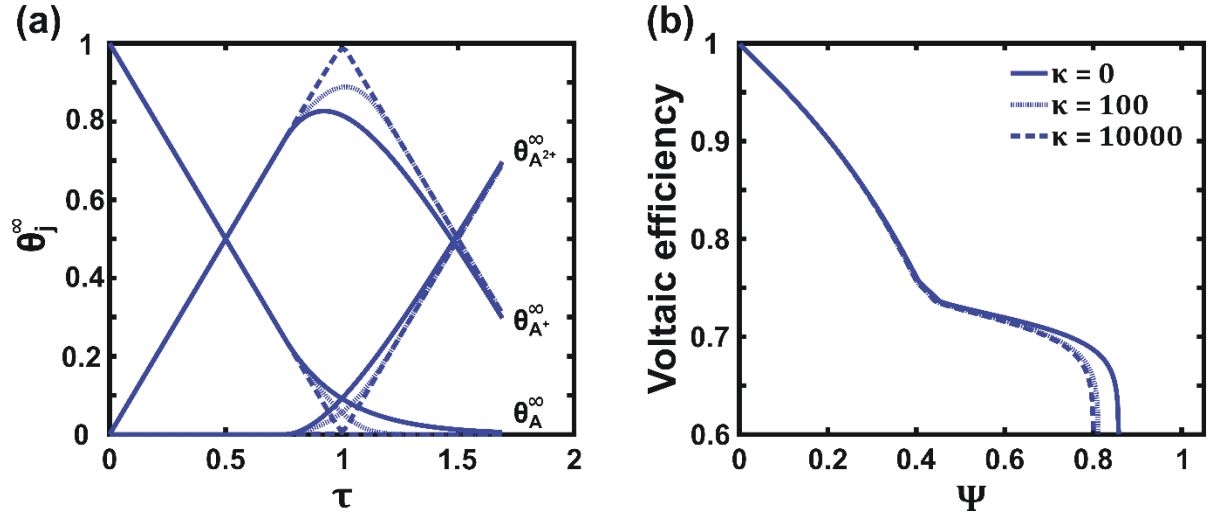


Figure 6. (a) Dimensionless concentration profiles as a function of dimensionless time (τ), shown for the first charging step ($\Psi = 0.25$) and (b) half-cell voltaic efficiency as a function of dimensionless charging current (Ψ) for varying values of the dimensionless comproportionation rate constant: $\kappa = 0$, $\kappa = 100$, and $\kappa = 10000$. Results shown for $\gamma_{A^+} = \gamma_{A^{2+}} = 0.8$, $E_{avg}^{(A)} = 2$ V, and $\Delta E^{(A)} = 0.6$ V.

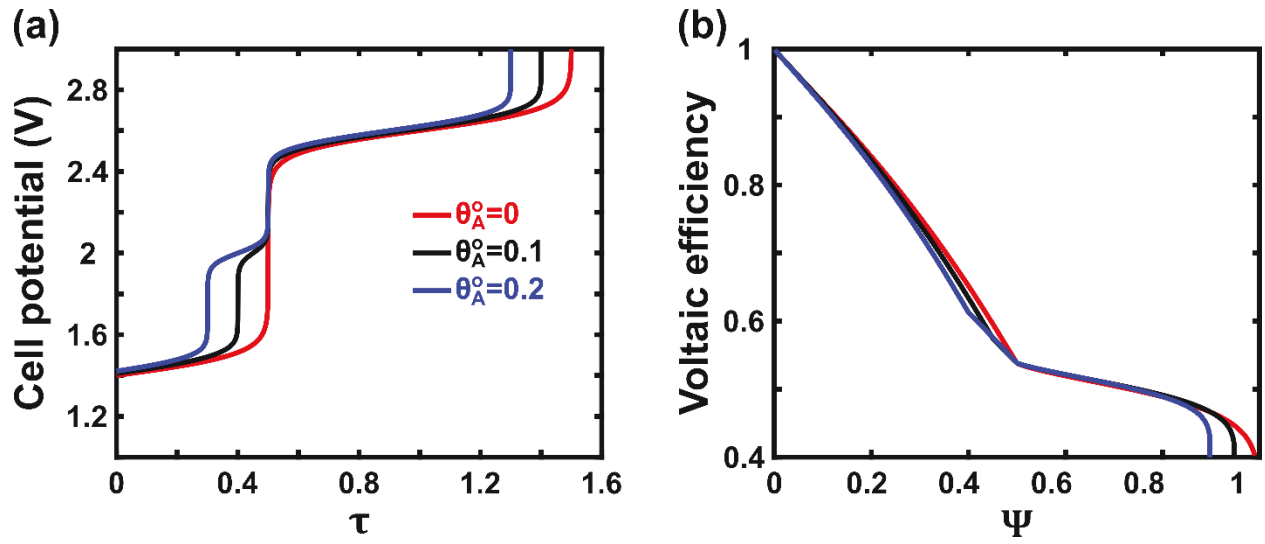


Figure 7. (a) Charge / discharge profiles shown for $\Psi = 0.25$ and (b) full cell voltaic efficiency as a function of dimensionless current for varying extents of charge imbalance. Results shown for $E_{avg}^{(A)} = 2 \text{ V}$, $E_{avg}^{(B)} = 0 \text{ V}$, $\Delta E^{(A)} = \Delta E^{(B)} = 0.6 \text{ V}$, $\gamma_j = 1$, and $\kappa = 0$.