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Droplet microfluidics for studying surfactant-rich interfaces found in aerosols, emulsions and foams

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Droplet microfluidics for studying surfactant-rich interfaces found in aerosols, emulsions and foams

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### Abstract

The presence of droplets suspended in a liquid or gas is known to play an essential role in fields ranging from materials to atmospheric science. Often, the dispersed phase is stabilized by surface active compounds and surfactants, resulting in complex chemical composition and material properties at the fluid-fluid interface. In this talk, recent advancements in use of microscale flow fields will be highlighted for measuring properties of aqueous multiphase, interface-rich systems. Systems studied will include atmospheric aerosol droplets and liquid-liquid emulsions. Microfluidic contractions, traps, and wells are used to measure surface-bulk partitioning and temperature-dependent liquid-liquid phase separation of aqueous droplets, towards better understanding of suspensions of aerosol droplets in our atmosphere. Advanced measurements of droplet shape deformations and coalescence will also be presented for both water-in-fuel and oil-in-water emulsions, for improved treatment and separation of emulsions. Dynamic interfacial tensions measurements were performed using a microfluidic tensiometer, demonstrating a dependence on if the surfactant approaches the interface from inside (dispersed) versus outside (continuous), implying phase-dependent surfactant transport to curved interfaces at the microscale. Droplet coalescence and film drainage experiments are also performed in a microfluidic Stokes trap across a range of viscosity ratios and surfactant concentrations. Results are used to explore the influence of interfacial mobility and Marangoni stresses on film stability with soluble surfactants.

### Keywords

Droplet microphysics, Phase separation, Surfactant transport, Dynamic interfacial tension, Interfacial rheology, Droplet coalescence

### Figures and tables

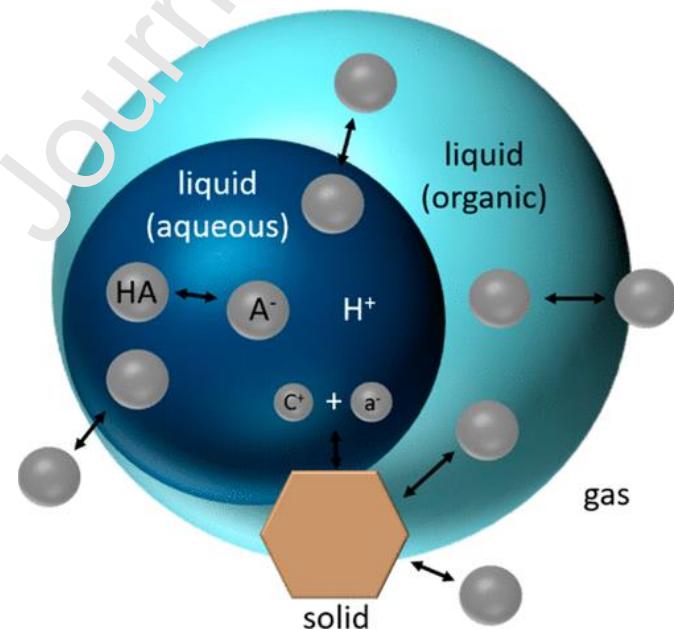


Figure 1. Schematic of possible aerosol particle chemical phase partitioning (not to scale), including liquid-liquid phase-separation (LLPS) into water-rich (aqueous) and water-poor

(organic) phases. Adapted with permission from [1]. Copyright 2017 American Chemical Society.

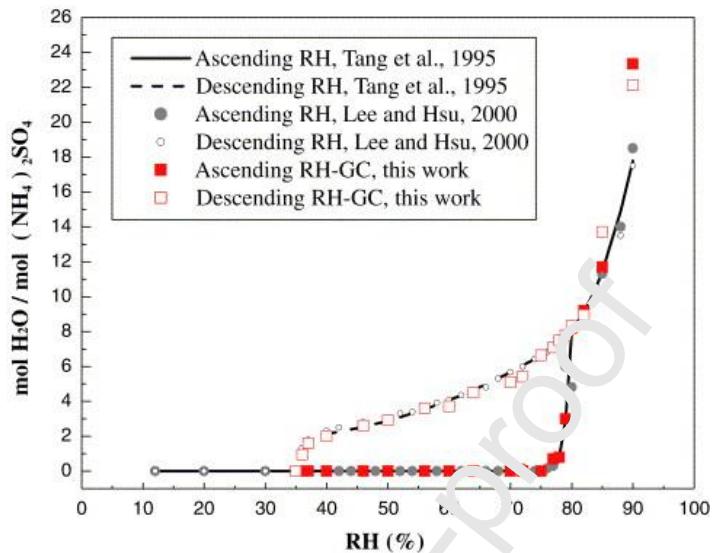


Figure 2. Hysteresis of deliquescence/efflorescence curves for ammonium sulfate salt. Deliquescence (water uptake) follows the lower curve, and occurs during relative humidity (RH) changes from a low RH to a high RH value. Efflorescence (water loss) follows the upper curve, and occurs during RH changes from high RH to low RH, and. Figure reprinted from [2], with permission from Elsevier; this work refers to that from Tsai and Kuo [2].

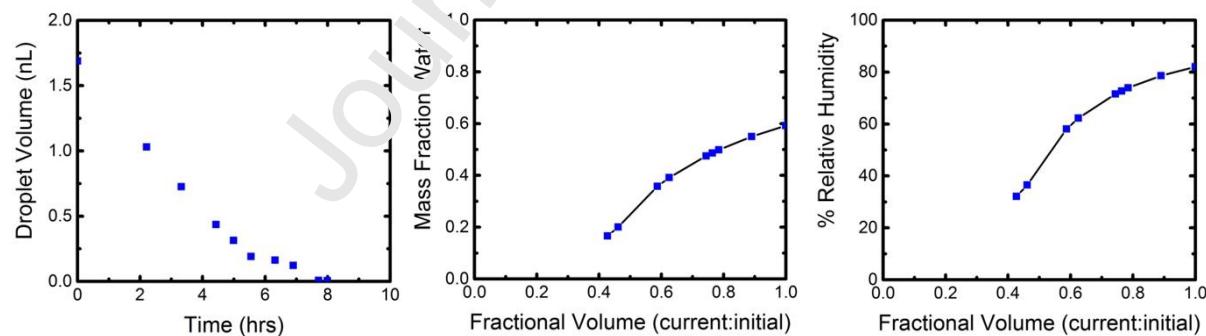


Figure 3. (left) Change in droplet volume of ammonium sulfate solution with time. (middle, right) Change in mass fraction of water and % RH, corresponding to the water activity within the droplet phase, as a function of fractional droplet volume during drying. Adapted with permission from [3]. Copyright 2018 American Chemical Society.

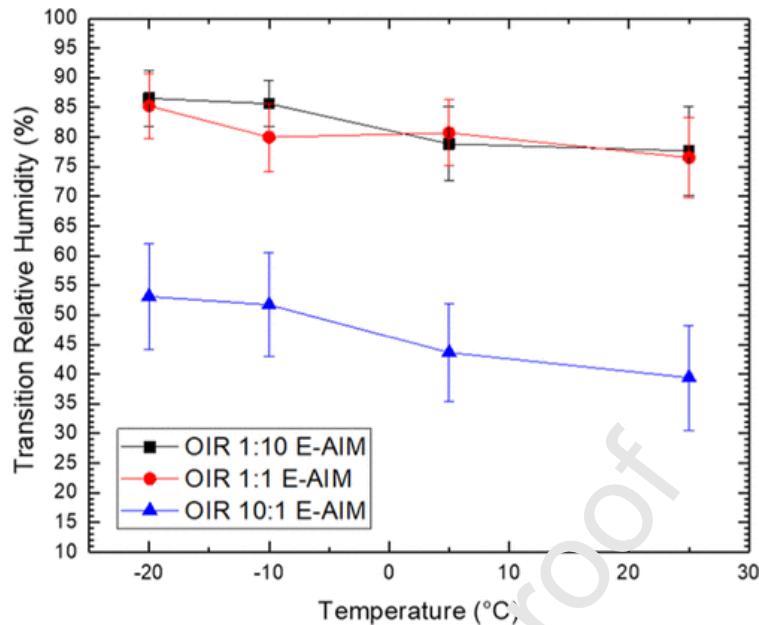


Figure 4. RH of phase transitions at different organic to inorganic ratios and at different temperatures for ammonium sulfate + 3-methylglutaric acid aqueous droplets. The phase transition refers is LLPS for OIR 1:10 and 1:1 and e<sup>+</sup>llorecence for OIR 10:1. Reprinted with permission from [4]. Copyright 2020 American Chemical Society.

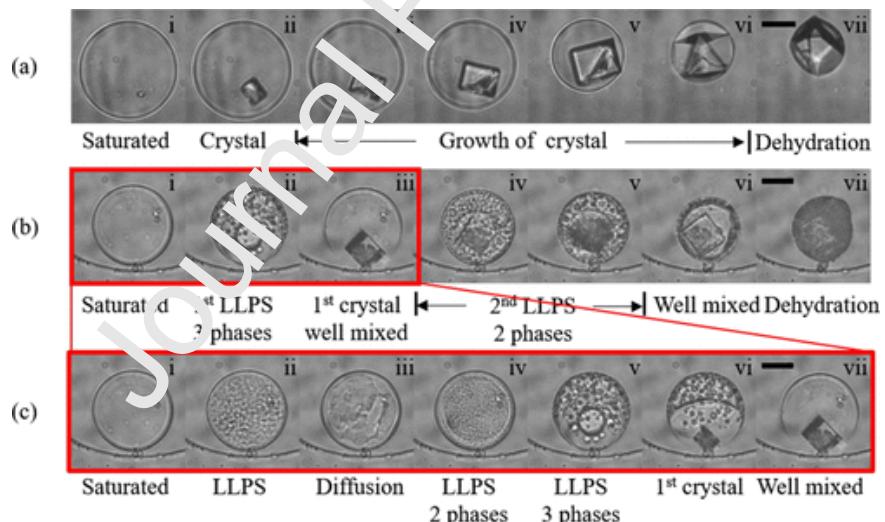


Figure 5. Microscopy images of phase transitions in time observed for (a)  $\text{NaCl} + \text{MgCl}_2 + \text{Na}_2\text{SO}_4$  aqueous droplet, and (b, c) in 3-methylglutaric acid +  $\text{NaCl} + \text{MgCl}_2 + \text{Na}_2\text{SO}_4$  aqueous droplet. Scale bar is 50  $\mu\text{m}$ . Reprinted with permission from [5]. Copyright 2019 American Chemical Society.

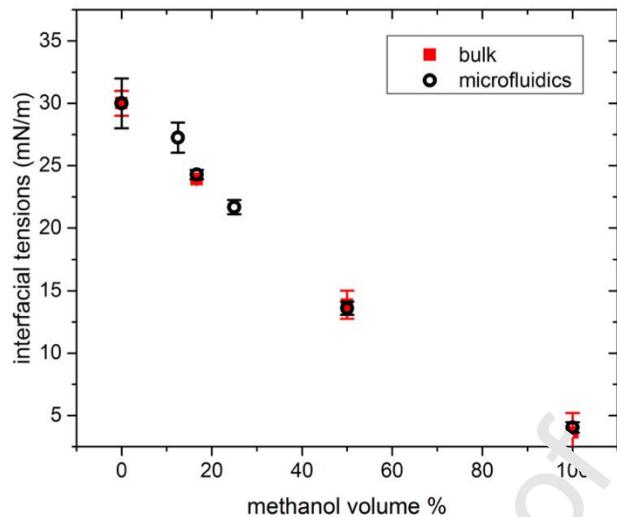


Figure 6. Example of interfacial tension between an oil and aqueous methanol solutions, measured using pendant drop ("bulk") and microfluidic method, showing good agreement between the two methods for simple surfactant-free mixtures. For more information, see ref [6].

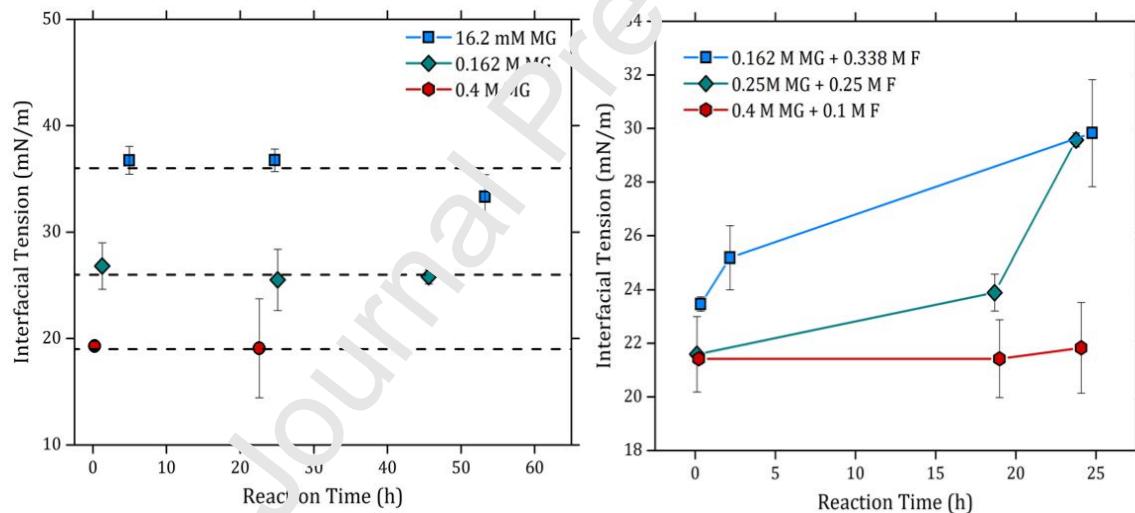


Figure 7. Microfluidic measurements of interfacial tensions of aqueous ammonium sulfate and (left) methylglyoxal (MG) and (right) methylglyoxal (MG) + formaldehyde (F) solutions. Adapted with permission from ref [7]. Copyright 2016, American Chemical Society.

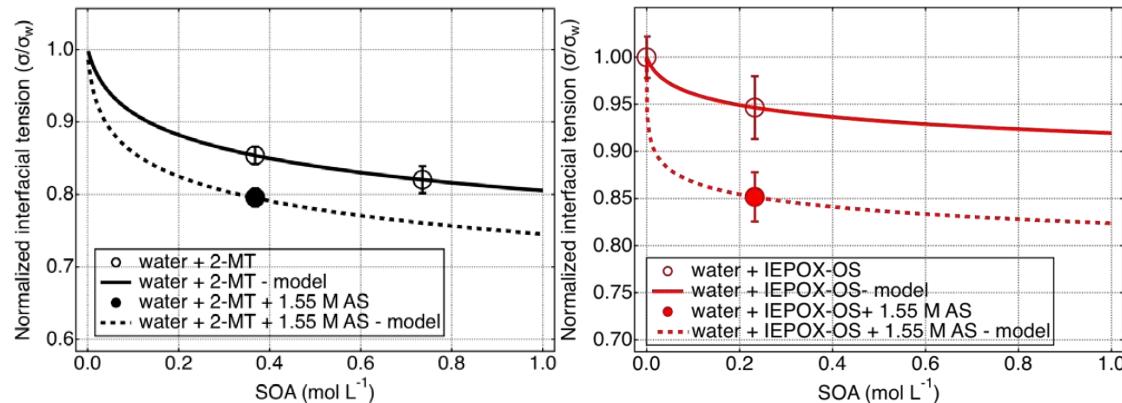


Figure 8. Microfluidic measurements and modeled values of interfacial tensions of (left) 2-methyltetrols and (right) IEPOX-OS, without and with ammonium sulfate (AS). Reprinted with permission from ref [8]. Copyright 2019, American Chemical Society.

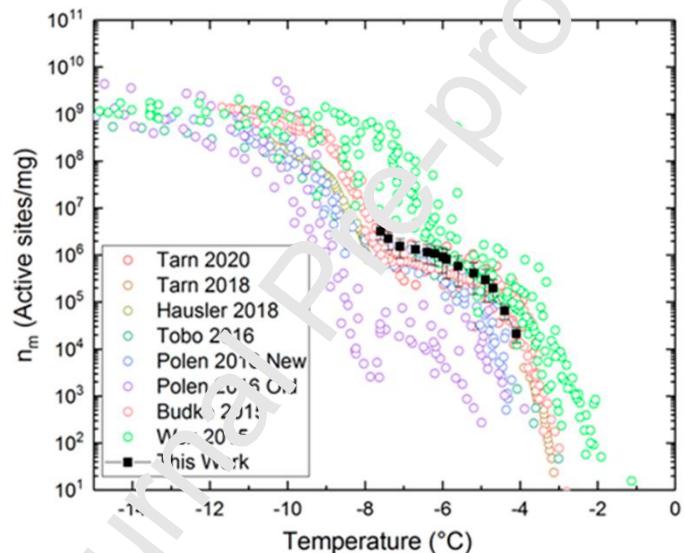


Figure 9. Ice nucleation site density per unit mass of Snomax® in aqueous droplets using a microfluidic platform ("This Work"), along with comparison to literature data obtained from others (see ref [9] for more information). Reprinted with permission from ref [9], open access Creative Commons CC BY license.

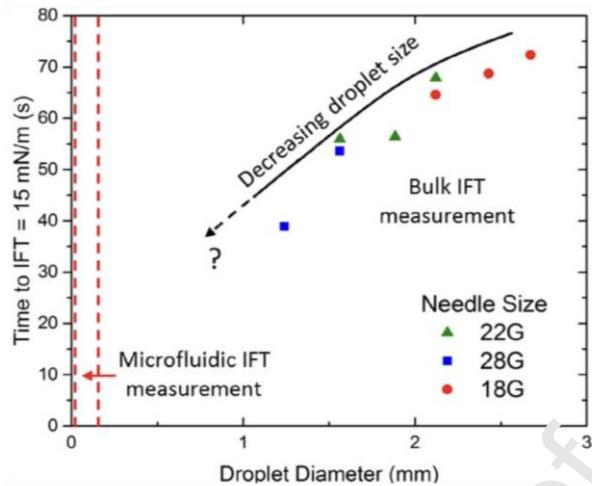


Figure 10. Time required to reach a dynamic interfacial tension (IFT) value of 15 mN/m millimeter-sized water droplet in surfactant-containing fuel as a function of droplet size, using a pendant drop method. For the same chemical composition, less time is needed as the droplet size decreases. Adapted with permission from ref [10]. Copyright 2018 American Chemical Society.

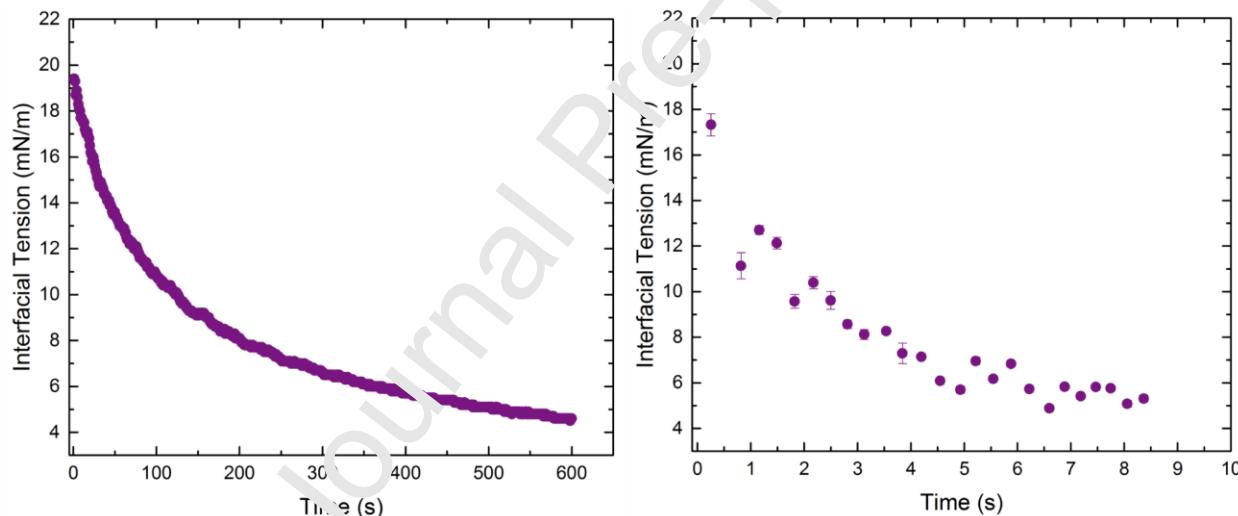
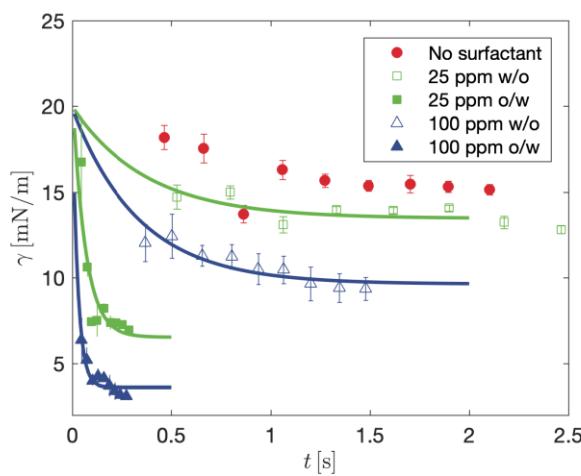


Figure 11. Dynamic interfacial tension measurements using (left) pendant drop and (right) microfluidic for water – fuel interface, in the presence of a fuel-phase surfactant. Droplet size dependent kinetics are evident, with the microfluidic approach reaching an IFT of 5 mN/m much faster than the pendant drop method for the same chemical system. Adapted with permission from ref [10]. Copyright 2018 American Chemical Society.



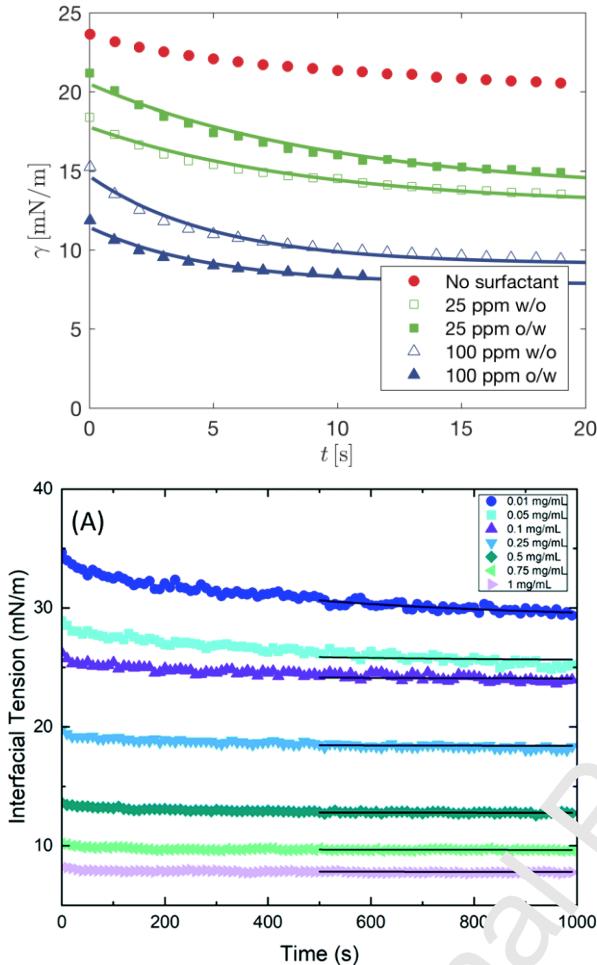


Figure 12. Dynamic interfacial tension of both water-in-oil (w/o) and oil-in-water (o/w) droplets using (left) pendant drop and (right) microfluidic platform. Note that some surface-active additives are already present in the complex oil mix used here, and “No surfactant” simply refers to a case where no additional surfactant was added. Figure adapted from Refs. [11] and [12], with permission from the Royal Society of Chemistry.

Figure 13. Dynamic interfacial tension using pendant drop tensiometry for water – fuel systems contain (A) mono-olein and (B)  $\text{PIB-Cl}$  surfactants. Solid black lines are fits to either the (A) late or (B) early time solutions to the Ward and Tordai equation [43]. Panel (A) uses results from Ref. [10]. Reproduced from Ref. [13] with permission from the Royal Society of Chemistry.

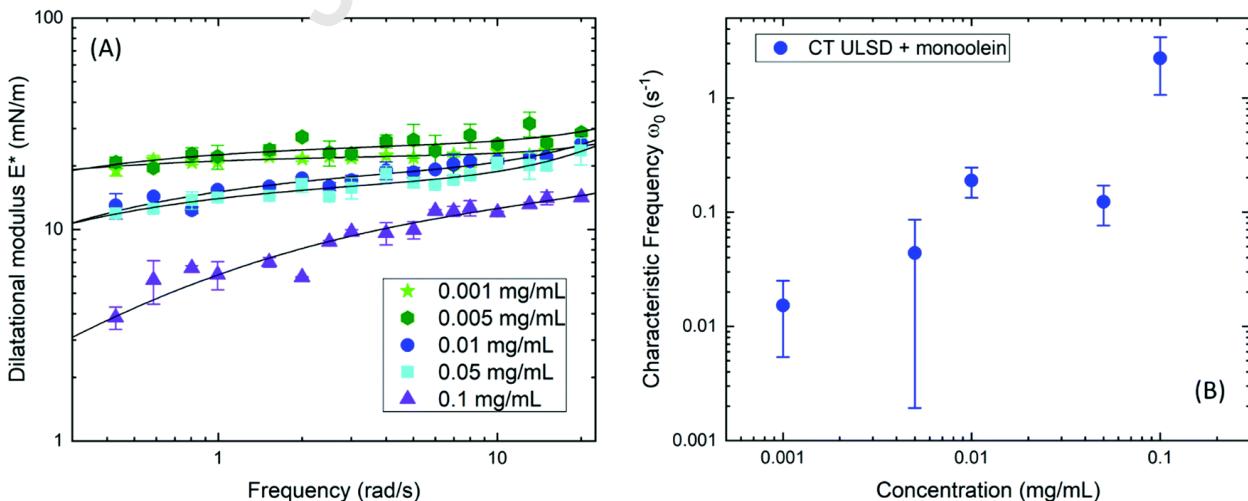


Figure 14. (A) Magnitude of the interfacial dilatational modulus for water – fuel interface, at varied fuel phase surfactant concentrations, as a function of frequency. (B) Characteristic frequency of surfactant exchange with the subphase obtained from the fits to the data in (A), as a function of surfactant concentration. Reproduced from Ref. [13] with permission from the Royal Society of Chemistry.

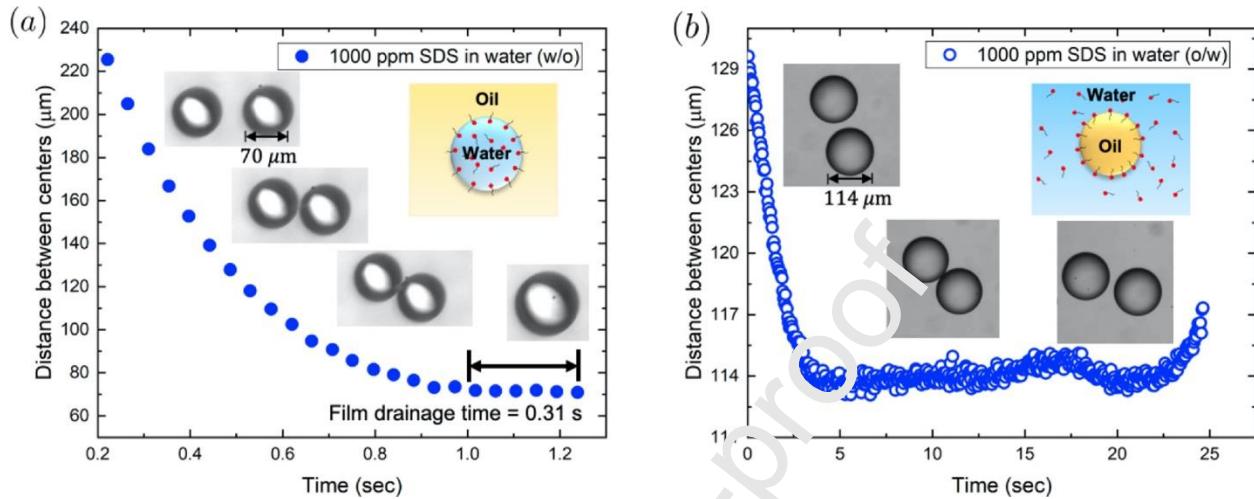


Figure 15. (a) Distance between the two approaching droplets for (a) water in light mineral oil (w/o) and (b) light mineral oil in water (o/w), with a water-soluble surfactant. For the same chemical system, the film drainage time is less than a second for the w/o and did not coalesce for the o/w. In general, the dynamics after droplet impact depend on a range of factors, including droplet size, viscosity ratio, surfactant type, concentration, and phase, and velocities and angles of impact. Reprinted from Ref. [14].

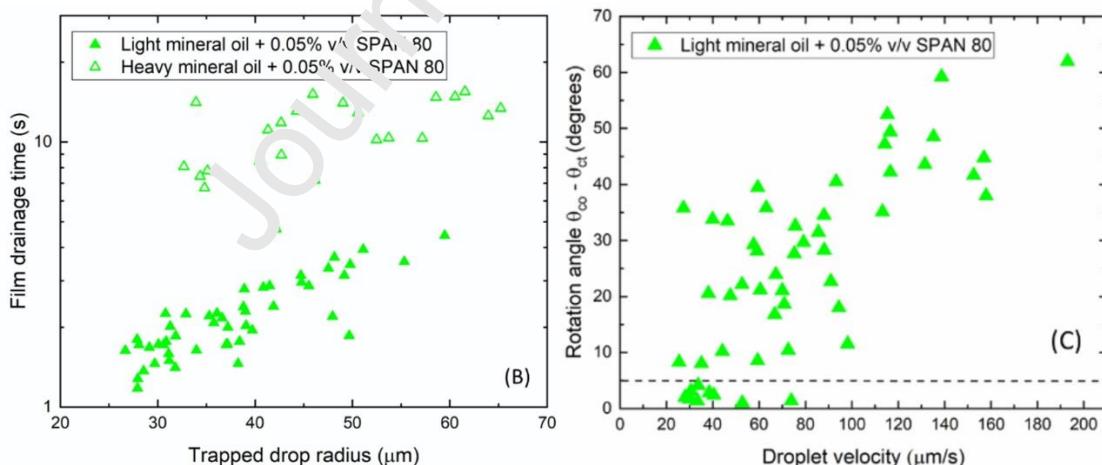


Figure 16. (left) Film drainage time during water droplet coalescence in a microfluidic platform, as a function of trapped droplet radius, for continuous phases of light mineral oil (closed triangles) and heavy mineral oil (open triangles) with an oil phase SPAN 80 surfactant. (right) Degree of droplet rotation (equal to angle of coalescence minus angle of impact) as a function of the velocity of the incoming droplet. Reproduced with permission from ref [15]. Copyright 2020 American Chemical Society.

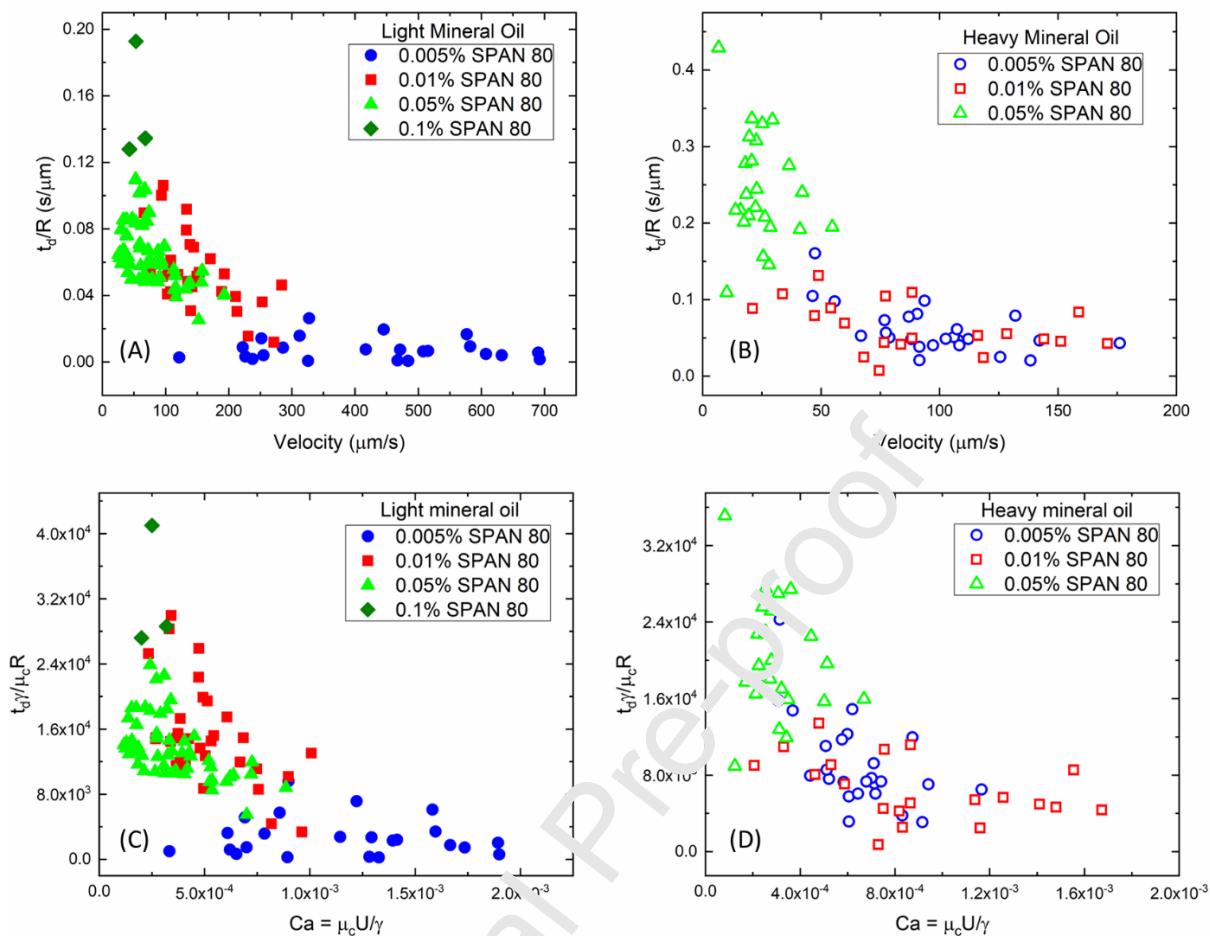


Figure 17. Characterization of film drainage times for two coalescing water droplets in light or heavy mineral oil. (A, B) Film drainage time normalized by mean radius, as a function of droplet velocity at various concentrations of SPAN 80 in (A) light and (B) heavy mineral oil. (C,D) Dimensionless film drainage time as a function of capillary number at various concentrations of SPAN 80 in (C) light and (D, heavy mineral oil. Reproduced with permission from refs [15] and [16]. Copyright 2020 and 2022 American Chemical Society.

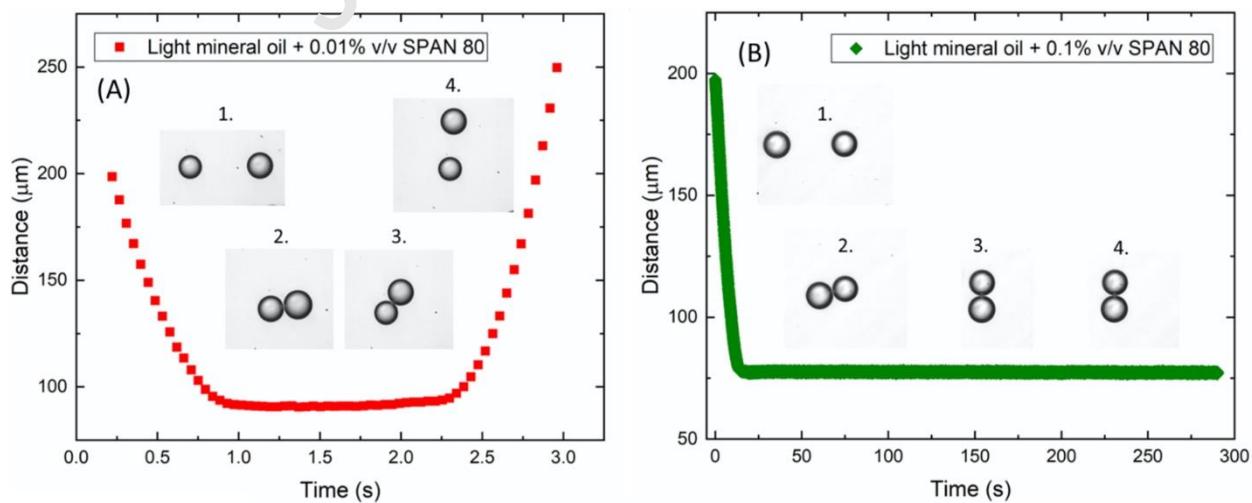


Figure 18. Beyond coalescence, droplets can also experience other dynamics, such as (A) bounce-off or (B) flocculation, depending on factors such as impact velocity and surfactant concentration. Here the center-to-center distance between water droplets as a function of time in light mineral oil + SPAN 80 systems demonstrate of two non-coalescing events. Reproduced with permission from ref [15]. Copyright 2020 American Chemical Society.

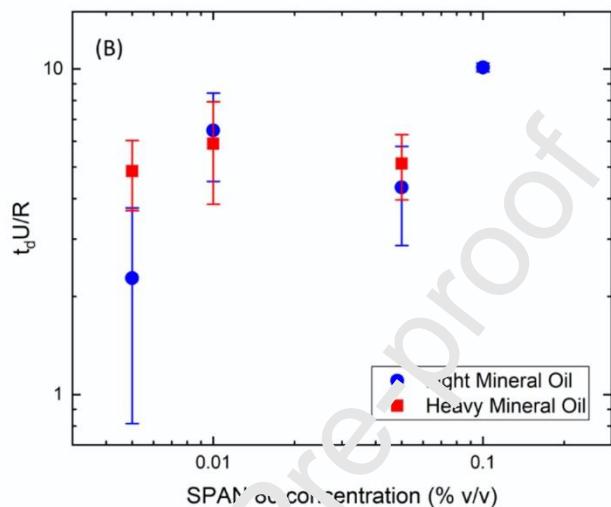


Figure 19. Film drainage time between two water droplets scaled by velocity and mean drop radius as a function of oil phase SPAN 80 concentration with light (blue circles) and heavy (red squares) mineral oils in the continuous phase. Adapted with permission from ref [15]. Copyright 2020 American Chemical Society.

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**Declaration of interests**

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The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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