

Ultrasensitive electrode-free and co-catalyst-free detection of nanomoles per hour hydrogen evolution for the discovery of new photocatalysts

Cite as: Rev. Sci. Instrum. 93, 025002 (2022); doi: 10.1063/5.0077650

Submitted: 4 November 2021 • Accepted: 26 January 2022 •

Published Online: 8 February 2022



View Online



Export Citation



CrossMark

Huaiyu(Hugo) Wang,¹ Rowan R. Katzbaer,² Julian Fanghanel,¹ Raymond E. Schaak,² and Venkatraman Gopalan^{1,a)}

AFFILIATIONS

¹ Department of Material Science and Engineering, The Pennsylvania State University, University Park, Pennsylvania 16802, USA

² Department of Chemistry, The Pennsylvania State University, University Park, Pennsylvania 16802, USA

^a) Author to whom correspondence should be addressed: vxg8@psu.edu

ABSTRACT

High throughput theoretical methods are increasingly used to identify promising photocatalytic materials for hydrogen generation from water as a clean source of energy. While most promising water splitting candidates require co-catalyst loading and electrical biasing, computational costs to predict them *a priori* become large. It is, therefore, important to identify bare, bias-free semiconductor photocatalysts with small initial hydrogen production rates, often in the range of tens of nanomoles per hour, as these can become highly efficient with further co-catalyst loading and biasing. Here, we report a sensitive hydrogen detection system suitable for screening new photocatalysts. The hydrogen evolution rate of the prototypical rutile TiO₂ loaded with 0.3 wt. % Pt is detected to be $78.0 \pm 0.8 \text{ } \mu\text{mol/h/0.04 g}$, comparable with the rates reported in the literature. In contrast, sensitivity to an ultralow evolution rate of $11.4 \pm 0.3 \text{ } \text{nmol/h/0.04 g}$ is demonstrated for bare polycrystalline TiO₂ without electrical bias. Two candidate photocatalysts, ZnFe₂O₄ ($18.1 \pm 0.2 \text{ } \text{nmol/h/0.04 g}$) and Ca₂PbO₄ ($35.6 \pm 0.5 \text{ } \text{nmol/h/0.04 g}$) without electrical bias or co-catalyst loading, are demonstrated to be potentially superior to bare TiO₂. This work expands the techniques available for sensitive detection of photocatalytic processes toward much faster screening of new candidate photocatalytic materials in their bare state.

Published under an exclusive license by AIP Publishing. <https://doi.org/10.1063/5.0077650>

I. INTRODUCTION

Efficient and clean energy production promises to reduce or reverse the detrimental effects of anthropogenic global warming by reducing carbon emission^{1–3} and meet the increasing energy consumption needs worldwide.⁴ Replacement of fossil fuels with various sources of renewable energy requires a cost-efficient method of sustainable production without carbon emission,⁵ a reliable and low-cost method of energy storage and distribution,⁶ and a large production volume that can satisfy the increasing market needs. Hydrogen is a prime candidate as a renewable fuel^{7,8} and is an efficient energy carrier with an energy density that is three times that of gasoline.⁹ While conventional methods to produce hydrogen mostly involve steam reforming, a process that releases carbon dioxide,¹⁰ photocatalysis offers a potential solution for carbon-neutral generation of hydrogen by electrochemically cleaving water.¹¹ Given

that the earth receives $3 \times 10^{-24} \text{ J}$ of solar energy annually,¹² solar production of hydrogen can potentially contribute significantly to the realization of a totally renewable energy supply that can largely satisfy the primary energy consumption needs of the world.

Direct photoelectrochemical water-splitting was first shown by Fujishima and Honda in 1972.¹³ This work has been followed by decades of intense research into photocatalytic water-splitting systems involving various co-catalysis and sacrificial agents.¹⁴ Despite these efforts, the photocatalytic production of hydrogen has been limited by the lack of stable and inexpensive materials with solar-to-hydrogen conversion efficiency exceeding the threshold of 10% for practical commercial applications.¹⁵ Data driven prediction of new photocatalytic materials provides new opportunities for expediting the discovery and development of efficient photocatalysis.¹⁶ Most of the reported photocatalysts require co-catalysts, sensitizers, or support materials to reach above $0.1 \text{ } \mu\text{mol/h}$ hydrogen

production rate.¹⁴ This is due to the fact that the photoexcited carriers recombine in the bulk before migrating to the surface reaction sites, and loading different materials can help mitigate this process. However, co-catalyst choices and loading condition combinations can increase exponentially when it comes to materials screening. Thus, for efficient screening of candidate materials, it is crucial to be able to test a potential new photocatalytic material as-is, without any co-catalyst loadings or electrical bias. This motivates our present work in building an ultrasensitive tool for detecting small rates of hydrogen generation. Using this tool, we study the hydrogen evolution rates of two recently identified photocatalyst materials.¹⁶

Producing large amounts of novel but untested catalyst candidates for rapid screening can be challenging and expensive. It has, therefore, become important to investigate the photoactivity of these materials requiring small quantities (i.e., mg) of the catalysts, thus motivating the development of a photo-reactor with a small volume that can detect very low quantities of product gas. This, in turn, requires efficient collection and detection of small amounts of hydrogen over a long period of time with minimal leakage loss. Most of the current photochemical water-splitting instruments or systems involve glass containers with rubber O-ring compression fittings and/or plastic tubing fittings.^{11,17,18} These setups work fine with efficient hydrogen evolution processes that have production rates of above 0.1 $\mu\text{mol}/\text{h}$ but are not sensitive enough for reactions with hydrogen production rates of 10 nmol/h, which is an order of magnitude lower. In addition, these systems still have relatively large reactor volumes that require larger amounts of photocatalysts to be tested. Recently, a new design involving gas-phase water-splitting systems with a small volume and a sensitive detection using mass spectrometer (MS) demonstrated sensitive detection of small volumes of hydrogen gas with an error bar of ± 25 nmol and a hydrogen evolution rate of 50 nmol/h/0.003 g.¹⁹ The apparatus design requires precise control of gas transfer and sensitive gas detection, which can be expensive. Furthermore, the detection rate is still not sensitive enough to detect a few nmol/h of hydrogen evolution.

In order to investigate the capability of hydrogen production from bare semiconductor compounds without any co-catalyst loading, we have developed a new experimental apparatus for ultrasensitive detection of sub-nanomole per hour hydrogen production rates. The reactor requires minimal volume of liquid (5–10 ml) and mg quantities of catalyst suspended in the solution. The setup does not require high-cost components, and the detection end is monitored by a gas chromatograph (GC) installed with a thermal conductivity detector (TCD), which costs less than a MS. The results from a pair of standard photocatalysts, namely, 0.3 wt. % Pt loaded TiO₂ rutile phase and bare TiO₂ rutile phase are presented to demonstrate the working principles of the setup. Furthermore, the detection of hydrogen from three recently discovered candidates, Ca₂PbO₄, ZnFe₂O₄, and MgSb₂O₆,¹⁶ is presented to showcase the application in fast screening of predicted samples from first-principle calculation without co-catalyst or electrode. While the photocatalytic activity of ZnFe₂O₄ has recently been investigated and optimized,^{20–22} our literature search did not reveal previous experimental evidence of the photocatalytic activity of Ca₂PbO₄. Of the three candidates, Ca₂PbO₄ and ZnFe₂O₄ are confirmed to be active photocatalysts, while MgSb₂O₆ is shown to be inactive and acts as a control sample for baseline detection sensitivity. To compare the new candidates

with standard photocatalysts directly, the bare polycrystalline TiO₂ rutile phase is tested and shown to have a smaller hydrogen production rate as compared with bare Ca₂PbO₄ and ZnFe₂O₄. The results motivate further studies of these two photocatalysts, including the development of appropriate co-catalysts.

II. MATERIALS AND METHODS

A. Materials synthesis and preparation

Rutile TiO₂ powder (Alfa Aesar, 99.9%) is mixed with 0.3 wt. % Pt reduced from 1.0 mM of H₂PtCl₆ (Sigma-Aldrich) and stirred for 2 h at room temperature. A rotary evaporator with a water bath at 323 K was employed to remove the water. The resulting paste was dried at 383 K for 12 h to yield a yellow powder. This powder was calcined at 773 K in air for 3 h to yield the PtO_x/TiO₂ catalyst precursor, which was reduced in flowing hydrogen at a rate of 30 ml min⁻¹ at 423 K for 3 h to yield a dark-gray TiO₂/Pt photocatalysts. All samples were synthesized by finely grinding and pelletizing a mixture of powders using an agate mortar and pestle in the molar ratios described below. The samples were added to an alumina boat and heated in air in a Lindberg/Blue M tube furnace. The samples were heated at 5 °C/min and held at 400 and 800 °C for 2 h prior to heating to the final temperature indicated for each sample, unless other parameters are explicitly mentioned. The samples were then cooled to room temperature inside the furnace.

Synthesis of Ca₂PbO₄ powder: CaCO₃ powder (Alfa Aesar, 99.99%) and PbO powder (Alfa Aesar, 99.999%) were combined in a 2:1 molar ratio of CaCO₃:PbO and heated to 800 °C for 26 h in a Lindberg/Blue M tube furnace. Note that the PbO used to produce Ca₂PbO₄ had an orange color, likely due to Pb₂O₃ impurities; Pb₂O₃ was necessary for this phase to form in high yield. However, using x-ray diffraction, the impurity phase is undetected/below the detection limit. *Synthesis of ZnFe₂O₄ powder:* ZnO powder (Sigma-Aldrich, ≥99.0%) and Fe₂O₃ powder (Aldrich, catalyst grade) were combined in a 1:1 molar ratio and heated to 900 °C for 72 h in a Lindberg/Blue M tube furnace. *Synthesis of MgSb₂O₆ powder:* MgO powder (Alfa Aesar, 99.99%) and Sb₂O₃ powder (Aldrich, ≥99.9%) were combined in a 1:1 molar ratio, pelletized, and heated at 5 °C/min and held at 400 and 800 °C for 2 h prior to heating to the final temperature of 1300 °C for 48 h in a Mullite tube furnace.

B. Materials characterization

X-ray diffraction: Powder x-ray diffraction (XRD) was performed on a Malvern PANalytical Empyrean (3rd gen.) x-ray diffractometer for 2θ in the range of 20°–80°. The pellets of each material were ground to powders prior to analysis. Reference XRD patterns were generated from the Powder Diffraction File (PDF) card numbers: Ca₂PbO₄: PDF 04-008-2917; ZnFe₂O₄: PDF 04-002-2708; and MgSb₂O₆: PDF 01-080-4590.

Field Emission Scanning Electron Microscope: Field Emission Scanning Electron Microscope (FESEM) was performed on an Apreo 2 S SEM using a backscattered electron (BSE) sensitive T1 detector under the opti-plan mode with a voltage of 7 KV and a current of 50 pA. The prepared sample is in powder form on top of a carbon tape prior to analysis.

C. High throughput screening processes

The instrument is used in a recent high throughput study of new photocatalytic candidates for hydrogen generation.¹⁶ Here, we propose a general strategy in the high throughput candidate screening process, as presented in a decision tree chart in Fig. S5, showcasing the unique functionality of the instrument. First, the bandgap and band edges of the material candidates are calculated from the DFT + U method and compared to water splitting redox potentials. Second, the material candidates predicted to show hydrogen evolution under illumination under sunlight are synthesized in powder form and phase pure state. The synthesized samples undergo Mott–Schottky measurements and UV-Visible spectroscopy (see Ref. 16) to experimentally probe band edges and bandgaps in order to compare with theoretical calculations. Third, the synthesized candidates without any co-catalyst are tested in the *continuous-flow mode*: if there is any hydrogen production detected, then we conclude that the sample is hydrogen production active. If there is no hydrogen, the sample is further tested in the *gas-accumulation mode*, since the hydrogen production rate could be below the detection limit of the *continuous-flow mode*, which is around 1 $\mu\text{mol}/\text{h}$. Finally, the instrument in the *gas-accumulation mode* monitors the generated gas for up to 4 days at 12 h intervals; often during the process, one may observe that the hydrogen production rate changes potentially due to new phases formed under light illumination. As shown in the two examples in Fig. 3(b), we can identify the time at which the hydrogen production rate is no longer linear and identify the new phases through XRD characterization of the catalysis compounds or inductively coupled plasma mass spectroscopy (ICP-MS) characterization of the trace elements in the liquid.

D. Gas chromatograph (GC) calibration

The GC needs to be calibrated to an accurate volume of the hydrogen gas produced for accurate recording of quantitative analysis of gas products. The calibration process includes extracting known amount of 5% hydrogen balanced with argon samples from a tank using precise microliter gas tight syringes (Hamilton 80956 used in this paper). A plot of the gas volume vs the GC peak area is fitted to a linear or quadratic equation (in the case when the injected gas amount is small, the calibration curve is no longer linear). The GC peak area from the tested new photocatalysts is converted to the gas volume following the calibration curve equation. The Limit of Detection (LOD) for hydrogen for the TCD detector is 1 ppm V/V using Ar carrier gas, and the smallest amount of hydrogen detected in this study is 25 ppm V/V, which is above the LOD.

E. Data analysis and error bar calculation

There are two modes presented in this work, which are described in detail in Sec. IV. For the *continuous-flow mode*, the volume of hydrogen is calculated in the following equation:

$$V_{H_2} = \frac{V_{H_2-GC} \times R_{flow} \times t}{V_{sampling}}, \quad (1)$$

where V_{H_2} is the actual hydrogen volume generated over the time interval period (30 minutes in this paper); V_{H_2-GC} is the detected hydrogen volume from the GC sampling tube in μL ; $V_{sampling}$ is the

volume of the sampling tube, which is calculated to be 0.02 inch³ (or 0.328 ml); R_{flow} is the flow rate reading from the flow meter in mL/min; and t is the time interval in minutes. The volume in the sampling tube is calculated from the calibration curve of the gas volume vs the GC peak area. The main error comes from the flow meter reading, which has an accuracy of 1 ml/min with an error range of ± 0.5 ml/min. The error bar is calculated considering the accuracy of the flow rate and the standard error of GC readings of ten samplings, which is presented in the TiO_2/Pt data in Fig. 1(b). The error bar of hydrogen evolution rate is calculated from the standard error in linear regression fitting.

For *gas-accumulation mode*, the volume of hydrogen is calculated in the following equation:

$$V_{H_2} = \frac{V_{H_2-GC} \times (V_{chamber} + V_{circulation})}{V_{sampling}} \times f_{correction}, \quad (2)$$

where V_{H_2} is the actual hydrogen volume generated up after some time (every 12 h in this paper); V_{H_2-GC} is the detected hydrogen volume from the GC sampling tube in μL ; $V_{sampling}$ is the volume of the sampling tube; $V_{chamber}$ is the volume of the reaction chamber, which is calculated to be 10 inch³ or 164 ml; $V_{circulation}$ is the volume of the circulation tubing, which is calculated to be 0.9 inch³ or 15 ml; $f_{correction}$ is the correction factor accounting for gas sample loss at each detection step due to the purging of the circulation tubing, which is

$$\frac{(V_{chamber} + V_{circulation})}{V_{chamber}} = 1.09. \quad (3)$$

The error of the detection from this mode is mainly from the sampling gas not completely evenly mixed in the argon gas. The error bar of detected hydrogen volume is determined from the standard error of 10 samplings at each time stamp, which is presented in Fig. 3(b). The error bar of hydrogen evolution rate is calculated from the standard error in linear regression fitting.

III. DESCRIPTION OF THE APPARATUS AND REFERENCE PHOTOCATALYST TESTING

As illustrated in the block diagram shown in Figs. 1(a)–1(c), the apparatus is a closed cycle system designed with a leakage rate of 3.10×10^{-5} Pa \times m³/s (Fig. S1). Stainless steel (SS) and copper gaskets have been used in all constructions in order to allow the system to operate with minimal leakage. SS tubing is connected by Swagelok compression fittings in most parts except the reaction cell, where a ConFlat (CF) fitting is used, and the six-way valve (SWV) of the gas chromatography (GC), where a Valco compression fitting is used. The reaction cell is a low-cost (a few hundred dollars), low volume (164 ml), commercially available high vacuum four-way reducer cross from Kurt J. Lesker (C-0275-133) with a fused silica viewport (VPZL-275Q) installed on the top, a CF flange (DN35CF-DN40CF) on the bottom, and CF to a Swagelok adaptor (F0133X4SWG) installed on both sides. The reactor requires only milligrams of catalyst suspended in 5–10 ml of solution. The light source is a 300 W xenon arc lamp (6258) from Newport. The circulation pump is from IWAKI air pumps (APN-30GD2-W), which required sealing with Torr Seal epoxy (110516) to reduce the leakage

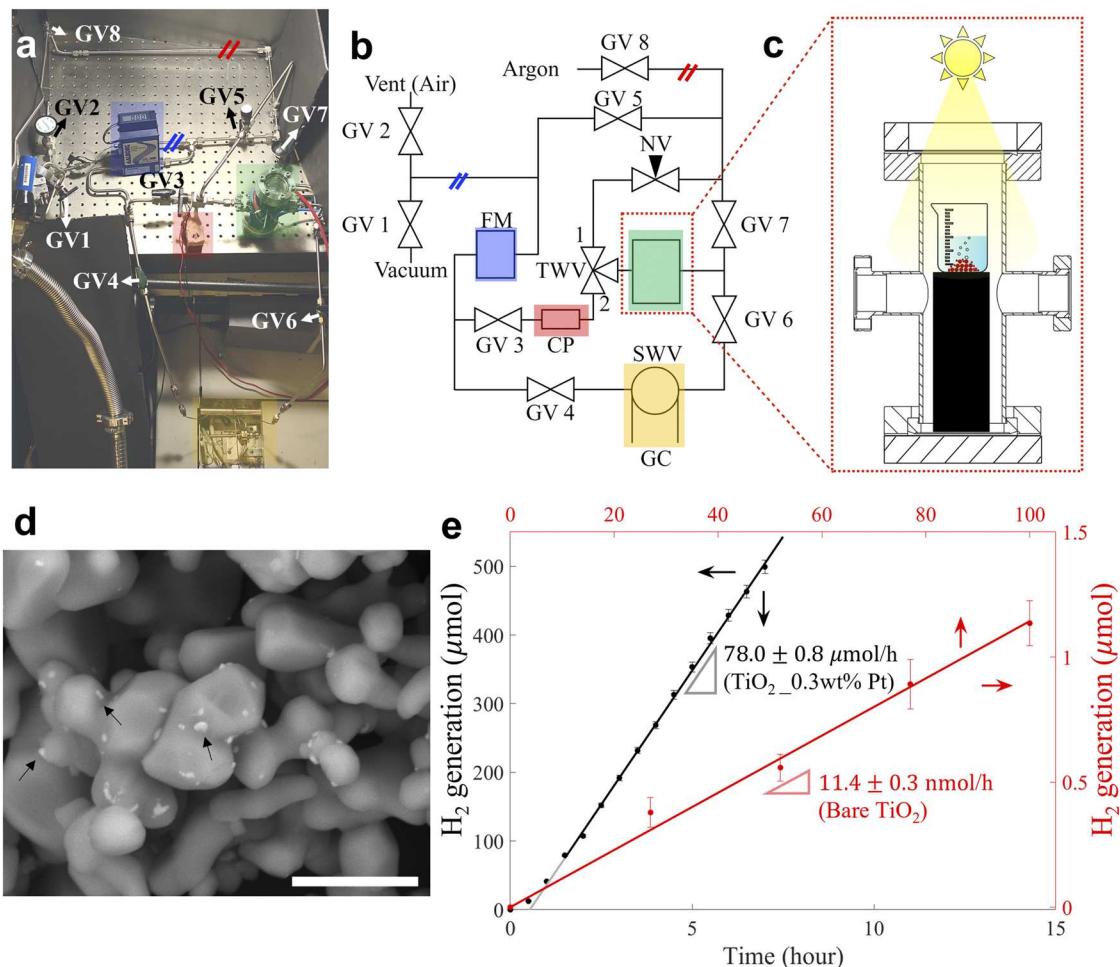


FIG. 1. (a) Photograph of the experimental setup. The highlighted region indicates key components and connections in the setup corresponding to the illustration in panel (b). (b) Illustration of the closed-cycle electrode-free gas chromatography photochemical cell setup. GV: general valve; TWV: three-way valve; FM: flow meter; CP: circulation pump; SWV: six-way valve; GC: gas chromatography. (c) Detailed illustration of the reaction chamber. The liquid is mixed with the catalyst in the beaker and is raised by a piston. A viewport is installed on the top. (d) The FESEM BSE image of TiO₂ loaded with Pt used as a reference photocatalyst. The liquid highlight the Pt islands shown with Z contrast. The scale bar is 1 μm. (e) Comparison between rutile TiO₂ loaded with 0.3 wt. % Pt co-catalyst and bare TiO₂. 40 mg of rutile phase TiO₂ loaded with and without 0.3 wt. % Pt were immersed in 10 ml of 15 V% methanol in water, which was used as an electron donor sacrificial agent.

(see the [supplementary material](#)). The flow meter is from AALBORG (GFM17). All needle valves, three-way valves, and general valves are from Swagelok. Gas Chromatography (GC) analyses were carried out with the 5890II instrument (Hewlett Packard) with the thermal conductivity detector (TCD). The GC column was a stainless-steel molecular sieve 5 Å packed column with the 80/100 mesh using argon as the carrier gas. The initial oven temperature was 50 °C, followed by heating to the inlet temperature at 120 °C, and finally the detector was kept at 150 °C. The solar simulator has a 300 W Xe lamp and an AM 1.5 global filter (81094) from Newport. The output power is measured to be 114 mW/cm², close to 1 sun intensity for simulated solar conditions.

To benchmark the performance of our home-built instrument, we chose a popular and standard semiconductor used in

photocatalysis, titanium dioxide (TiO₂).²³ Early work involving TiO₂ photoelectrochemical hydrogen production using a Pt metal electrode as a cathode and a TiO₂ irradiated with the UV light was reported by Fujishima and Honda.¹³ In 1977, Schrauzer and Guth reported the photocatalytic decomposition of H₂O on powdered TiO₂ photocatalysts loaded with small amounts of Pt or Rh metal particles.²⁴ This led to the development of the mechanism that on such TiO₂/Pt photocatalysts, the photo-induced electrons move to the Pt metal island on the surface where they induce reduction reactions, while photo-induced holes migrate to the TiO₂ surface where they induce oxidation reactions.²⁵ The rate of photocatalysis is determined mainly by the competitive rates of recombination of electron-hole pairs and the charge separation and harvest of electron and holes. The band-structure alignment of semiconductors

with water decomposition into the hydrogen and oxygen reaction potential is a prerequisite for water-splitting reactions, but the kinetics often limits the rate of photocatalysis, which means that the most promising water splitting catalysts require co-catalysts for efficient hydrogen production.¹⁴ Here, we chose the rutile phase of TiO_2 to be our reference photocatalyst, since the rutile phase was reported to split water into hydrogen and oxygen, while the anatase phase was reported to only evolve hydrogen,²⁶ which leads to surface deactivation overtime in the anatase TiO_2 phase. For efficient hydrogen production, the *continuous-flow mode* (to be described in greater detail later) is used where argon gas continuously flows through the chamber and is measured by a flow meter. An example experiment shown with rutile phase TiO_2 loaded with 0.3 wt. % Pt and a sacrificial agent of 15 vol. % of methanol in water is used to improve the hydrogen production rate. The choice of Pt loading amount is based on a previous optimization study²⁷ of Pt loading, and the optimal loading range of Pt on TiO_2 P25 is reported to be around 0.25 wt. %. The loading process described in the Materials and Methods section is followed. The FESEM image of rutile TiO_2 after loading with Pt, as shown in Fig. 1(d), indicates uniform distribution of Pt islands on TiO_2 grains. The powder solution mix is exposed to illumination from a mercury arc lamp, providing an effective light beam diameter of 25 mm with an averaged intensity of 114 mW/cm², which is close to 1 sun intensity (100 mW/cm²). As shown in Fig. 1(e), the hydrogen production rate in the steady state region is measured to be $78.0 \pm 0.8 \mu\text{mol}/\text{h}/0.04 \text{ g}$ of the catalyst. This number is comparable to the surface area optimized TiO_2 based photocatalyst experiments ($136.2 \mu\text{mol}/\text{h}/0.1 \text{ g}$) and is close to the performance of pristine TiO_2 ($76.6 \mu\text{mol}/\text{h}/0.1 \text{ g}$) reported under similar sacrificial agent conditions.²⁸ After testing platinized TiO_2 , we focus on detecting hydrogen produced from a photocatalyst with very slow kinetics, namely, bare rutile TiO_2 . Here, we showcase the second mode of this instrument, the *gas-accumulation mode* (to be described in greater detail later), for ultrasensitive hydrogen detection rates as low as several nmol/h. The *gas-accumulation mode* operates with the evolved hydrogen gas closed cycled within the reaction chamber so that it builds up for up to several days before being detected by the GC. As shown in Fig. 1(e), the bare rutile phase TiO_2 shows a hydrogen production rate of $11.4 \pm 0.3 \text{ nmol}/\text{h}/0.04 \text{ g}$ with no change in the hydrogen production rate after 100 h. Only a couple of studies^{29,30} have reported a hydrogen evolution rate for polycrystalline TiO_2 (not P25 TiO_2 nanoparticles), which is often below the standard instrument detection limit. For example, one study reported the rate of hydrogen production on bare TiO_2 to be zero within an experimental error bar of $\pm 20 \mu\text{mol}/\text{h}/\text{g}$.²⁹ In contrast, the instrument in Fig. 1(a) has an estimated error bar of $\pm 7.5 \text{ nmol}/\text{h}/\text{g}$, which is three orders of magnitude more sensitive.

IV. CONTINUOUS-FLOW AND GAS-ACCUMULATION MODES

Before discussing the testing of new photocatalysts, we first discuss the approach that is taken when measuring an unknown candidate material. There are two modes of operation: the *continuous-flow mode* and the *gas-accumulation mode*. A flowchart of the procedures for operating the experimental apparatus is shown in Fig. 2(a). After cleaning the chamber with methanol and then loading the sample in the reaction chamber, the top view portal is attached and the

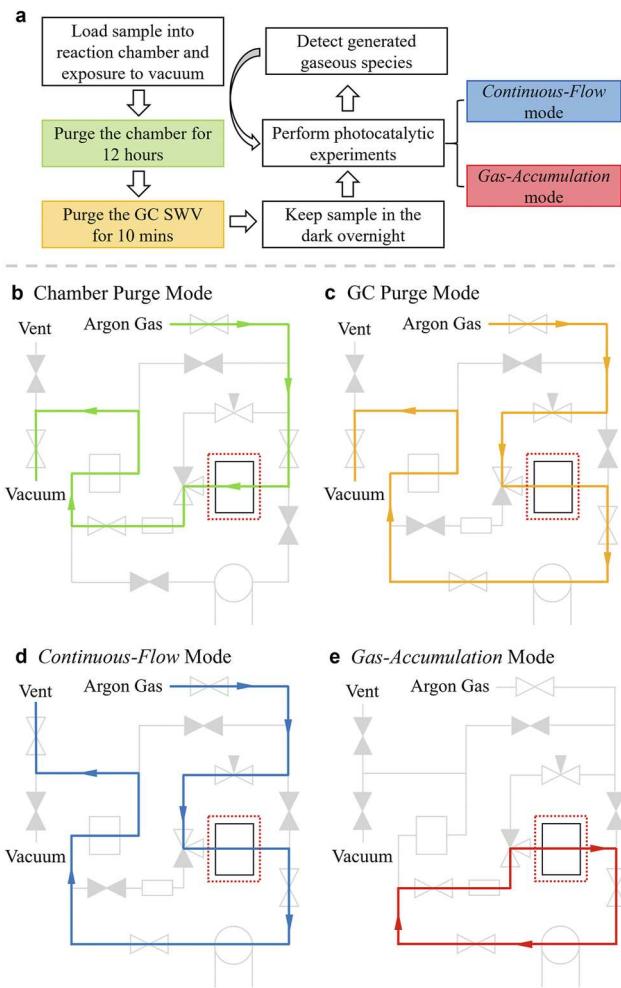


FIG. 2. (a) Flowchart of operational procedures. The color codes correspond to setup illustrations in (b) to (e). Illustration of the operation modes during (b) purging the chamber, (c) purging the GC SWV, (d) *continuous-flow mode*, and (e) *gas-accumulation mode*. The colored lines and arrows indicate the flow of argon gas during the operation modes. The gray-filled valve symbols indicate that the valve is closed, while the unfilled valve symbol indicates that the valve is open.

standard procedure used to tighten all ConFlat flanges is followed, including wearing nitrile gloves and appropriate cleaning. Next, all the air is purged from the chamber and the detection lines so that the sample is under pure argon. For this, one must start pumping the reaction chamber to create vacuum for a short period of time until one notices the liquid vapor pressure in the sample beaker exceeds the vacuum level and the liquid starts to boil. In order to expel the air completely from the chamber, we use the purging method shown in Fig. 2(b) where the argon gas flows through the chamber continuously for 12 h. Following this purging, we purge the GC SWV for 10 min using a valve configuration shown in Fig. 2(c). Using this configuration to purge GC lines, one can detect through GC if there is any trace amount of nitrogen and oxygen from air left in the chamber. To exclude the possibility that hydrogen is produced

from the corrosion of the sample materials without light, one should check the gas inside the chamber after the sample is kept in the dark overnight. If there is no corrosion in the dark, the setup is ready for the water-splitting measurement of the sample of interest.

One can choose between the *continuous-flow mode* and the *gas-accumulation mode* depending on the efficiency of the water splitting process. For the *continuous-flow mode*, the sample is under a constant flow of argon gas. The configuration of valves for the *continuous-flow Mode* is shown in Fig. 2(d). During measurement, we found that the vent should be at ambient pressure instead of vacuum in order to keep a constant flow rate for oxygen and hydrogen. As shown in Fig. S2, the correct molar ratio between oxygen and hydrogen from water electrolysis is achieved when the sink is at ambient pressure, and a specialized tubing is installed to purge gas right above the liquid level. Once there is a stable flow of argon, gas detection is achieved by switching the GC SWV and collecting the GC spectrum. The speed of the flow is detected using a flow meter and can be controlled either by changing the gas pressure using the gas cylinder valve or adjusting the needle valve. The flow rate should be moderate (approximately above 5 ml/min) in order to ensure a steady flow of purge gas. The error bar of the measurement, as shown in the TiO_2/Pt data in Fig. 1(e), is mainly from the flow meter, since its accuracy is 1 ml/min. For the *gas-accumulation mode*, the photocatalytic water splitting takes place when the chamber is sealed with all valves closed (GV 6,7 and TWV closed) to isolate the circulation pump from the chamber (see the discussion in S3). This process is needed to ensure minimum leakage of the gas product during the accumulation time. The configuration of the valves for detection in the *gas-accumulation mode* is shown in Fig. 2(e). During detection, the circulation pump is turned on to mix the product gas with the argon gas inside the six-valve sampling tubes. After 2–3 min, the circulation pump is turned off. The circulation flow of gas can be monitored by a flow meter to ensure that the gas stops flowing and the pressures in the sampling tube and the chamber are the same before the detection. GC SWV is used to switch the collected gas sample from the sampling tube to flow toward the TCD. This detection process is repeated 10 times to obtain error bar ranges, as shown in the pure TiO_2 data in Fig. 1(e). After each detection step, one must close GV 6 and 7 and TWV (to make sure that the reaction chamber is sealed) and turn on GV1 to keep the circulation tubing and the SWV under vacuum. This step is to ensure minimum leakage during the photocatalytic process. Right before the next detection step, the circulation tubing and the SWV need to be purged by first pulling vacuum followed by injecting argon gas by turning GV5,8 on and GV1 off. The purging process is repeated 3 times and no air is detected from the GC spectra.

V. PROMISING NEW PHOTOCATALYSTS

The two operational modes available in this instrument have been demonstrated with bare TiO_2 and TiO_2/Pt [Fig. 1(e)] and showcase the setup sensitive detection of the hydrogen generation rate down to several nmol/h and, at the same time, capable of characterizing the efficient hydrogen generation process. In this section, we will demonstrate how the setup is capable of screening new materials from theoretical prediction without co-catalyst or electrical biasing following a procedure described in Fig. S5. Three new photocatalyst candidates are predicted through high

throughput density functional theory (DFT) calculations¹⁶ and tested with this instrument. The computational screening process is described in detail elsewhere.¹⁶ Powder samples of the three compounds were synthesized via solid-state reactions involving the mixing of precursors and calcinating these at high temperatures for a given amount of time, as described in the Materials and Methods section. Figure 3(a) shows the normalized experimental x-ray diffraction (XRD) pattern, which closely match the reference patterns in all cases, confirming the synthesis of the expected single phase. We then proceed to the photocatalytic activity characterization of these compounds.

To characterize the photocatalytic activity during the water-splitting reaction, we implemented the *gas-accumulation mode* to measure hydrogen photo-generation. In analyzing these measurements, it must be taken into account that the oxygen evolution reaction is much more sluggish than the hydrogen reduction reaction and often requires loading a co-catalyst to proceed.³¹ Although understanding the influence of co-catalysts on the photoactivity is of practical interest for optimizing solar-to-hydrogen conversion, this objective is beyond the scope of the present assessment whose goal is to screen the computationally predicted candidates for solar production of hydrogen. We, thus, restricted this analysis to the hydrogen reduction half-reaction by introducing sacrificial redox couples to circumvent the slow kinetics of oxygen evolution. The

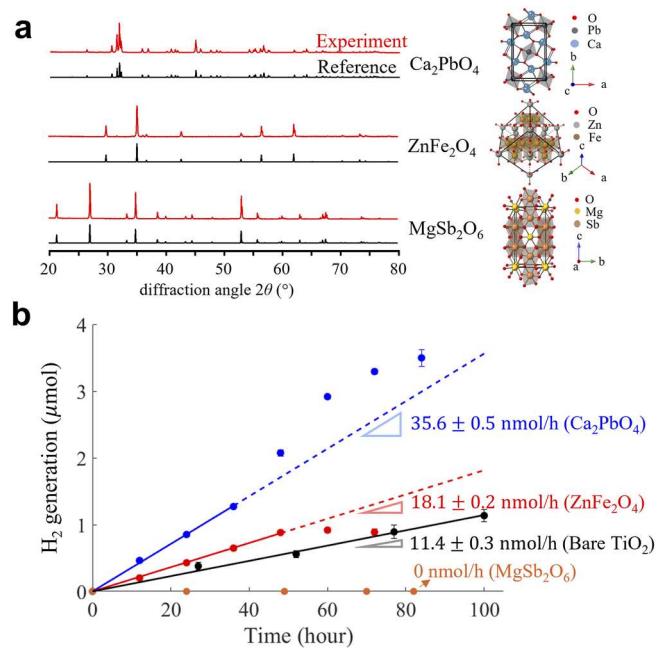


FIG. 3. (a) Comparison of the reference and measured XRD patterns for the three compounds that were synthesized and tested. The plane indexing of the peaks is shown in Fig. S3. (b) Hydrogen evolution test using the *gas-accumulation mode*. 40 mg of Ca_2PbO_4 , MgSb_2O_6 , and TiO_2 were tested in 10 ml 15 vol. % methanol in water, and 40 mg of ZnFe_2O_4 was tested in 10 ml 0.05M oxalic acid. Closed dots are experimental data and solid lines are the linear fitting results. The dotted line is an extrapolation of the model that deviates from experimental data indicating corrosion. The error bar calculation is explained in the Materials and Methods section.

main results expected from the photoactivity tests are two-fold: (1) confirm the location of conduction bands aligned with hydrogen reduction half-reaction and (2) study the corrosion mechanism and how photoactivity is affected by the corrosion process.

Each compound is tested with electron donor agents: (i) acidic pH, with the addition of 0.1M of oxalic acid, which not only tends to favor the generation of H₂ (by increasing the activity of the protons) but may also cause the premature dissolution of the sample; (ii) neutral pH, corresponding to volume fractions of 15% of methanol and 85% of water. The powder solution mix is exposed to illumination from a mercury arc lamp, providing an effective light beam diameter of 25 mm with an averaged intensity of 114 mW/cm², which is close to 1 sun intensity (100 mW/cm²). From the hydrogen evolution plot shown in Fig. 3(b), we can conclude that Ca₂PbO₄ shows an initial hydrogen production rate of 35.6 ± 0.5 nmol/h with a higher hydrogen production rate after 36 h. Similarly, ZnFe₂O₄ shows a hydrogen production rate of 18.1 ± 0.2 nmol/h but becomes inactive after 48 h. MgSb₂O₆ shows no hydrogen production and serves as a control test for null detection. In comparison, the bare rutile phase TiO₂ shows a hydrogen production rate of 11.4 ± 0.3 nmol/h with no change in hydrogen production rate after 100 h. It is noted that although TiO₂/Pt is a successful and well-studied photocatalyst system,²⁸ the bare TiO₂ sample with sluggish oxidation pathway performs worse than the two new candidates shown here in terms of hydrogen production. On the other hand, TiO₂ evolves hydrogen steadily over 100 h, indicating no corrosion of TiO₂ happened in the pH = 7 condition under illumination for 100 h.

To further explore the corrosion process during the photocatalytic reaction, samples during different hydrogen generation rate periods are characterized with XRD to probe the phases. The goal here is to correlate chemical composition of the tested compounds to photoactivity tested over time. As shown in XRD phase analysis in Fig. S4(a), ZnFe₂O₄ after 24 and 72 h of photoactivity tests indicate that the compound decomposes to Fe(C₂O₄) (H₂O)₂ in 0.1M oxalic acid under illumination overtime. Combining the XRD characterization with the GC test, we can conclude that the corroded compound of ZnFe₂O₄ is no longer capable of generating hydrogen. On the other hand, the XRD structure characterization of the tested Ca₂PbO₄ catalyst shown in Fig. S4(b) indicates that Pb₃O₄ and CaPbO₃ form after 85 h of photocatalytic reaction and they are not present after 24 h. This suggests that the formation of Pb₃O₄ and CaPbO₃ are related to the higher hydrogen production measured from Ca₂PbO₄ after 36 h.

To benchmark the performance of our sensitive hydrogen detection system, we choose two parameters that are important for high throughput screening of photocatalytic materials: (1) sensitive detection of a small hydrogen generation rate and (2) small catalyst mass required for the test to expand the material candidates to those with small quantity that are hard to scale up in the synthesis process. As shown in Fig. 4, after extracting reported literature values on photoactivity tests with the hydrogen production rate of 1 μ mol/h or lower, it is noted that most of literature values cluster above 0.1 μ mol/h and above 0.1 g. The detection setup designs reported in the literature are a combination of a closed container equipped with a rubber septum,^{36,38} a closed cycle system with a Pyrex glass container linked to GC^{34,35,37} or MS,³² or a closed container with water vapor reduction.³³ A closed container with a rubber septum combined with syringe sampling can achieve a sensitive detection

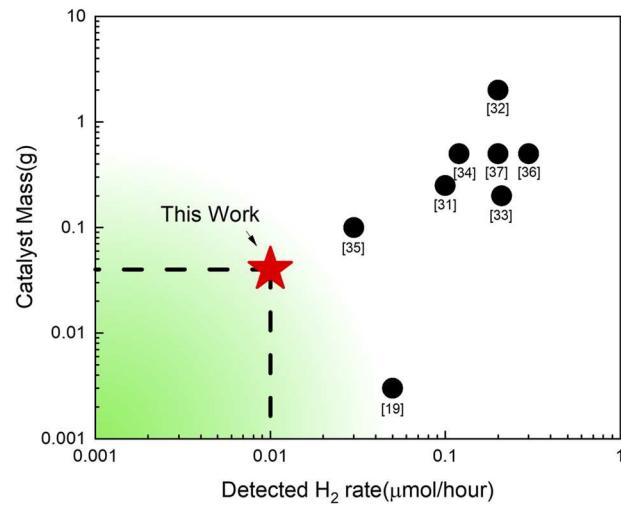


FIG. 4. Comparison of reported lowest hydrogen detection rate and catalyst mass used from photoactivity measurement setups in literature to this work.^{19,32–38} The green region indicating high sensitivity low mass detection desired for photoactivity screening of co-catalyst-free and electrode-free materials.

level;³⁶ however, the reported hydrogen evolution curve is nonlinear due to a change of partial pressure in the reaction cell after each sampling. Recently reported new design involving gas-phase water-splitting systems requires a few mg of samples and can achieve a sensitive detection of 50 nmol/h/0.003 g using MS;¹⁹ however, the apparatus design requires precise control of gas transfer, sensitive gas detection, and specialized sample preparation. Overall, our design of a closed-cycle online hydrogen generation detection system shows superior performance as compared to the above-mentioned sensitive setups from the literature.

VI. CONCLUSION

We demonstrate a specially designed closed cycle experimental setup for the ultrasensitive detection of gaseous products from photocatalysis covering the reaction rate over 4 order of magnitude from hundreds of μ mol/h down to tens of nmol/h and catalyst mass as small as 0.04 g. We demonstrate its utility by studying two photocatalysts, Ca₂PbO₄ and ZnFe₂O₄, that were recently predicted and experimentally validated, both of which exhibit superior performance to TiO₂ in their bare, co-catalyst-free, bias-free state. However, ZnFe₂O₄ decomposes to Fe(C₂O₄) (H₂O)₂ in 0.1M oxalic acid under illumination and terminates the hydrogen generation after 48 h. Ca₂PbO₄ decomposes to Pb₃O₄ and CaPbO₃ and enhanced the hydrogen generation after 36 h. Future studies on corrosion mechanisms of the two compounds under photoillumination might be able to shed lights on pathways to enhance the stability of two studied compounds. These sensitive experimental measurements are made feasible by the low leakage rate of the instrument combined with a small volume size of the reaction chamber, which allows three orders of magnitude higher detection sensitivity for hydrogen evolution than a conventional gas chromatograph system, while still maintaining high sensitivity to trace products. The small volume of the reactor enables the use of small quantities of a catalytic material, thus

avoiding large volumes of expensive catalyst preparation. With further improvement in the vacuum and replacing GC detection with a MS, an order of magnitude improvement in both the detected H₂ rate and catalyst mass is required. High detection sensitivity can thus fast-track experimental screening of new computationally identified photocatalysts for hydrogen production (see the experimental methods for a procedure) as well as a variety of quantitative catalytic studies across a wide range of conditions.

SUPPLEMENTARY MATERIAL

See the [supplementary material](#) for the leakage rate of the apparatus, purging condition test, circulation pump sealing, degradation analysis, and a description of the high throughput screening process.

ACKNOWLEDGMENTS

This work was supported by the DMREF and INFEWS programs of the National Science Foundation under Grant No. DMREF-1729338. The authors are deeply thankful to I. Dabo for fruitful discussions.

AUTHOR DECLARATIONS

Conflict of Interest

The authors have no conflicts to disclose.

Author Contributions

H.W. and V.G. conceived the idea and designed the experiments. H.W. wrote the main manuscript text. R.K. and J.F. synthesized the compounds used in the experiments. H.W. and R.K. conducted characterization and analysis of photochemical stability of the compounds. All the authors reviewed and revised the manuscript. V.G. and R.E.S. supervised the work.

DATA AVAILABILITY

The data that support the findings of this study are available from the corresponding author upon reasonable request.

REFERENCES

1. J. Cook, N. Oreskes, P. T. Doran, W. R. L. Anderegg, B. Verheggen, E. W. Maibach, J. S. Carlton, S. Lewandowsky, A. G. Skuce, S. A. Green, D. Nuccitelli, P. Jacobs, M. Richardson, B. Winkler, R. Painting, and K. Rice, "Consensus on consensus: A synthesis of consensus estimates on human-caused global warming," *Environ. Res. Lett.* **11**, 048002 (2016).
2. W. R. L. Anderegg, J. W. Prall, J. Harold, and S. H. Schneider, "Expert credibility in climate change," *Proc. Natl. Acad. Sci. U. S. A.* **107**, 12107–12109 (2010).
3. N. Oreskes, "Beyond the ivory tower. The scientific consensus on climate change," *Science* **306**, 1686 (2004).
4. Annual energy outlook, 2021.
5. D. Connolly, B. V. Mathiesen, and I. Ridjan, "A comparison between renewable transport fuels that can supplement or replace biofuels in a 100% renewable energy system," *Energy* **73**, 110–125 (2014).
6. D. Gielen, F. Boshell, D. Saygin, M. D. Bazilian, N. Wagner, and R. Gorini, "The role of renewable energy in the global energy transformation," *Energy Strategy Rev.* **24**, 38–50 (2019).
7. Y. Tachibana, L. Vayssières, and J. R. Durrant, "Artificial photosynthesis for solar water-splitting," *Nat. Photonics* **6**, 511–518 (2012).
8. J. H. Montoya, L. C. Seitz, P. Chakhranont, A. Vojvodic, T. F. Jaramillo, and J. K. Nørskov, "Materials for solar fuels and chemicals," *Nat. Mater.* **16**, 70–81 (2017).
9. A. Züttel, A. Remhof, A. Borgschulte, and O. Friedrichs, "Hydrogen: The future energy carrier," *Philos. Trans. R. Soc., A* **368**, 3329–3342 (2010).
10. P. L. Spath and M. K. Mann, "Life cycle assessment of hydrogen production via natural gas steam reforming," No. NREL/TP-570-27637 (NREL, 2001); available at <https://www.nrel.gov/docs/fy01osti/27637.pdf>.
11. T. Takata and K. Domen, "Particulate photocatalysts for water splitting: Recent advances and future prospects," *ACS Energy Lett.* **4**, 542–549 (2019).
12. M. Grätzel, "Photoelectrochemical cells," *Nature* **414**, 338–344 (2001).
13. A. Fujishima and K. Honda, "Electrochemical photolysis of water at a semiconductor electrode," *Nature* **238**, 37 (1972).
14. F. E. Osterloh, "Inorganic materials as catalysts for photochemical splitting of water," *Chem. Mater.* **20**, 35–54 (2008).
15. B. A. Pinaud, J. D. Benck, L. C. Seitz, A. J. Forman, Z. Chen, T. G. Deutsch, B. D. James, K. N. Baum, G. N. Baum, S. Ardo, H. Wang, E. Miller, and T. F. Jaramillo, "Technical and economic feasibility of centralized facilities for solar hydrogen production via photocatalysis and photoelectrochemistry," *Energy Environ. Sci.* **6**, 1983–2002 (2013).
16. Y. Xiong, Q. T. Campbell, J. Fanganel, C. K. Badding, H. Wang, N. E. Kirchner-Hall, M. J. Theibault, I. Timrov, J. S. Mondschein, K. Seth, R. Katz, A. M. Villarino, B. Pamuk, M. E. Penrod, M. M. Khan, T. Rivera, N. C. Smith, X. Quintana, P. Orbe, C. J. Fennie, S. Asem-Hiablie, J. L. Young, T. G. Deutsch, M. Cococcioni, V. Gopalan, H. D. Abruña, R. E. Schaak, and I. Dabo, "Optimizing accuracy and efficacy in data-driven materials discovery for the solar production of hydrogen," *Energy Environ. Sci.* **14**, 2335–2348 (2021).
17. M.-Y. Xie, K.-Y. Su, X.-Y. Peng, R.-J. Wu, M. Chavali, and W.-C. Chang, "Hydrogen production by photocatalytic water-splitting on Pt-doped TiO₂–ZnO under visible light," *J. Taiwan Inst. Chem. Eng.* **70**, 161–167 (2017).
18. Y.-H. Pai and S.-Y. Fang, "Preparation and characterization of porous Nb₂O₅ photocatalysts with CuO, NiO and Pt cocatalyst for hydrogen production by light-induced water splitting," *J. Power Sources* **230**, 321–326 (2013).
19. J. F. Alvino, T. Bennett, R. Kler, R. J. Hudson, J. Aupoil, T. Nann, V. B. Golovko, G. G. Andersson, and G. F. Metha, "Apparatus for the investigation of high-temperature, high-pressure gas-phase heterogeneous catalytic and photo-catalytic materials," *Rev. Sci. Instrum.* **88**, 054101 (2017).
20. J. H. Kim, J. H. Kim, J.-W. Jang, J. Y. Kim, S. H. Choi, G. Magesh, J. Lee, and J. S. Lee, "Awakening solar water-splitting activity of ZnFe₂O₄ nanorods by hybrid microwave annealing," *Adv. Energy Mater.* **5**, 1401933 (2015).
21. R. Dom, R. Subasri, K. Radha, and P. H. Borse, "Synthesis of solar active nanocrystalline ferrite, MFe₂O₄ (M: Ca, Zn, Mg) photocatalyst by microwave irradiation," *Solid State Commun.* **151**, 470–473 (2011).
22. R. Dom, R. Subasri, N. Y. Hebalkar, A. S. Chary, and P. H. Borse, "Synthesis of a hydrogen producing nanocrystalline ZnFe₂O₄ visible light photocatalyst using a rapid microwave irradiation method," *RSC Adv.* **2**, 12782–12791 (2012).
23. J. Schneider, M. Matsuoka, M. Takeuchi, J. Zhang, Y. Horiechi, M. Anpo, and D. W. Bahnemann, "Understanding TiO₂ photocatalysis: Mechanisms and materials," *Chem. Rev.* **114**, 9919–9986 (2014).
24. G. N. Schrauzer and T. D. Guth, "Photolysis of water and photoreduction of nitrogen on titanium-dioxide," *J. Am. Chem. Soc.* **99**, 7189–7193 (1977).
25. D. Hufschmidt, D. Bahnemann, J. J. Testa, C. A. Emilio, and M. I. Litter, "Enhancement of the photocatalytic activity of various TiO₂ materials by platinisation," *J. Photochem. Photobiol., A* **148**, 223–231 (2002).
26. R. Li, Y. Weng, X. Zhou, X. Wang, Y. Mi, R. Chong, H. Han, and C. Li, "Achieving overall water splitting using titanium dioxide-based photocatalysts of different phases," *Energy Environ. Sci.* **8**, 2377–2382 (2015).
27. F. G. Santomauro, S. Ahmadi, H. Rensmo, D. L. Fernandes, and J. Sá, "Enhancement of UV photo-catalytic activity in greenly modified nano-TiO₂," *Chem. Mater. Eng.* **4**, 1 (2016).
28. W. Zhou, W. Li, J.-Q. Wang, Y. Qu, Y. Yang, Y. Xie, K. Zhang, L. Wang, H. Fu, and D. Zhao, "Ordered mesoporous black TiO₂ as highly efficient hydrogen evolution photocatalyst," *J. Am. Chem. Soc.* **136**, 9280–9283 (2014).
29. A. S. Hainer, J. S. Hodgins, V. Sandre, M. Vallières, A. E. Lanterna, and J. C. Sciano, "Photocatalytic hydrogen generation using metal-decorated TiO₂: Sacrificial donors vs true water splitting," *ACS Energy Lett.* **3**, 542–545 (2018).

³⁰X. Li, K. Peng, H. Chen, and Z. Wang, “TiO₂ nanoparticles assembled on kaolinites with different morphologies for efficient photocatalytic performance,” *Sci. Rep.* **8**, 11663 (2018).

³¹J. Yang, D. Wang, H. Han, and C. Li, “Roles of cocatalysts in photocatalysis and photoelectrocatalysis,” *Acc. Chem. Res.* **46**, 1900–1909 (2013).

³²S. Sato and J. M. White, “Photodecomposition of water over Pt/TiO₂ catalysts,” *Chem. Phys. Lett.* **72**, 83–86 (1980).

³³K. Domen, S. Naito, M. Soma, T. Onishi, and K. Tamaru, “Photocatalytic decomposition of water vapour on an NiO/SrTiO₃ catalyst,” *J. Chem. Soc., Chem. Commun.* **1980**, 543–544.

³⁴K. Sayama, K. Mukasa, R. Abe, Y. Abe, and H. Arakawa, “Stoichiometric water splitting into H₂ and O₂ using a mixture of two different photocatalysts and an IO₃[−]/I[−] shuttle redox mediator under visible light irradiation,” *Chem. Commun.* **2001**, 2416–2417.

³⁵M. P. Kapoor, S. Inagaki, and H. Yoshida, “Novel zirconium- titanium phosphates mesoporous materials for hydrogen production by photoinduced water splitting,” *J. Phys. Chem. B* **109**, 9231–9238 (2005).

³⁶Y. I. Kim, S. J. Atherton, E. S. Brigham, and T. E. Mallouk, “Sensitized layered metal oxide semiconductor particles for photochemical hydrogen evolution from nonsacrificial electron donors,” *J. Phys. Chem.* **97**, 11802–11810 (1993).

³⁷D. Wang, Z. Zou, and J. Ye, “Photocatalytic water splitting with the Cr-doped Ba₂In₂O₅/In₂O₃ composite oxide semiconductors,” *Chem. Mater.* **17**, 3255–3261 (2005).

³⁸K. Kobayakawa, A. Teranishi, T. Tsurumaki, Y. Sato, and A. Fujishima, “Photocatalytic activity of CuInS₂ and CuIn₅S₈,” *Electrochim. Acta* **37**, 465–467 (1992).