

## PAPER

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11, 6832Revisiting trends in the exchange current for  
hydrogen evolution†Timothy T. Yang,<sup>a</sup> Rituja B. Patil, <sup>b</sup> James R. McKone <sup>b</sup> and Wissam A. Saidi <sup>\*a</sup>

Nørskov and collaborators proposed a simple kinetic model to explain the volcano relation for the hydrogen evolution reaction on transition metal surfaces such that  $j_0 = k_0 f(\Delta G_H)$  where  $j_0$  is the exchange current density,  $f(\Delta G_H)$  is a function of the hydrogen adsorption free energy  $\Delta G_H$  as computed from density functional theory, and  $k_0$  is a universal rate constant. Herein, focusing on the hydrogen evolution reaction in acidic medium, we revisit the original experimental data and find that the fidelity of this kinetic model can be significantly improved by invoking metal-dependence on  $k_0$  such that the logarithm of  $k_0$  linearly depends on the absolute value of  $\Delta G_H$ . We further confirm this relationship using additional experimental data points obtained from a critical review of the available literature. Our analyses show that the new model decreases the discrepancy between calculated and experimental exchange current density values by up to four orders of magnitude. Furthermore, we show the model can be further improved using machine learning and statistical inference methods that integrate additional material properties.

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Hydrogen is a powerful energy carrier that can be generated through the hydrogen evolution reaction (HER) – the critical cathodic reaction of electrochemical water-splitting. Not surprisingly, the HER is still a topic of great fundamental interest for electrochemical energy conversion.<sup>1–9</sup> To understand the HER activity, Bockris,<sup>10</sup> Conway and Bockris,<sup>11</sup> Petrenko,<sup>12</sup> Kita<sup>13</sup> and Trasatti<sup>14–16</sup> correlated experimental HER reaction rates with physicochemical descriptors such as atomic number, work function, d-band center, the heat of hydrogen adsorption, and Pauling electronegativities. Motivated by Sabatier's principle that the maximum catalytic rate is achieved when the interaction between the reactants and catalyst is neither too strong nor too weak,<sup>17</sup> Parsons and Gerischer independently proposed the free energy of hydrogen adsorption,  $\Delta g^0$ , as an HER descriptor such that the maximum rate corresponds to a minimum in the magnitude of  $\Delta g^0$  under equilibrium conditions.<sup>18,19</sup> To link the theoretical  $\Delta g^0$  with experimental measurements, early attempts were made by Trasatti.<sup>15</sup> Later, Krishtalik<sup>20</sup> and Trasatti<sup>15</sup> used a compilation of experimental data to validate the Parsons volcano relationship using the metal-hydrogen interaction strength based on the Eley–Stevenson method.<sup>21,22</sup> However, this approach had limited

success because the maximum exchange current was not associated with  $\Delta g^0 = 0$ , as proposed by Parsons.

In a seminal study, Nørskov and collaborators introduced the hydrogen adsorption free energy  $\Delta G_H$  computed from density functional theory (DFT) as an accurate estimate of Parsons'  $\Delta g^0$ . Further, this study built a connection with electrochemical exchange currents using a simple kinetic model based on systematic investigations on transition metal surfaces.<sup>23</sup> We will refer to this model as the Nørskov model hereafter. The Nørskov model confirms the theoretical volcano trend proposed by Parsons where  $\Delta G_H \approx 0$  at the maximum exchange current density of the HER. Further, this model also demonstrated that a computational framework based on an easy-to-compute descriptor  $\Delta G_H$  can provide a rational approach to catalyst design, which improved on approaches to materials design based on trial-and-error or chemical heuristics that have historically been the norm for experimental catalysis research.

Although the Nørskov model for the HER has been widely accepted by the electrochemistry community (*e.g.*, see recent studies<sup>24–27</sup>), several studies highlighted caveats in this model. For example, the Nørskov model is applied to pristine metallic surfaces to compute  $\Delta G_H$  while under electrochemical conditions, many metals are likely to be oxidized or exhibit amorphous surface structure.<sup>28–30</sup> Further, it was argued that the electrostatic effects from metal–water interfaces and the effects from the adsorption of water and oxygen, as well as kinetic factors and d-band characteristics, are not adequately accounted for in the Nørskov model.<sup>28–30</sup> In addition, it has been recently argued that Pt is not a

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thermoneutral catalyst with  $\Delta G_{\text{H}}$  that deviates from zero.<sup>31–33</sup> Several studies proposed HER models based on microkinetic analysis.<sup>34,35</sup> However, these models are generally complex with many parameters that are obtained by some approximation for by fitting to experimental data. *These caveats notwithstanding, the Nørskov model remains a leading framework for the design of HER catalysts and heterogeneous electrocatalysts in general.*<sup>1–5</sup>

Herein we revisit the Nørskov model and show that the calculated exchange current densities deviate from the corresponding experimental values by up to six orders of magnitude.<sup>23</sup> While differences between experimental and DFT-computed rates are not uncommon, we show that the discrepancy can be substantially reduced by considering that the rate constant is material-dependent rather than universal, as assumed in the original Nørskov model.<sup>23</sup> Specifically, we present evidence that the kinetic pre-factor  $k_0$  also depends on the absolute value of  $\Delta G_{\text{H}}$ . We further validate the findings based on reliable data obtained from a critical review of experimental exchange current densities on transition metal surfaces from the available research literature.

In the Nørskov model, the exchange current density  $j_0$ , which describes the magnitude of the forward and reverse reaction rates at equilibrium, is defined as

$$j_0 = \begin{cases} ek_0 \exp(-\Delta G_{\text{H}}/k_{\text{B}}T) C_{\text{tot}}(1 - \theta) & \text{for } \Delta G_{\text{H}} > 0 \\ ek_0 C_{\text{tot}}(1 - \theta) & \text{for } \Delta G_{\text{H}} < 0 \end{cases} \quad (1)$$

where  $e$  is the charge of an electron and  $C_{\text{tot}}$  is the areal concentration of adsorption sites. Note that while the Nørskov model was presented in terms of the exchange current (e.g., amps), eqn (1) is defined in terms of the exchange current density (e.g., amps per square cm), which necessitates the inclusion of an area-normalized  $C_{\text{tot}}$ . The model is derived from the basic relation that the current is linearly proportional to the concentration of reactants  $\text{H}^+$  ( $\text{H}^*$ ) for  $\Delta G_{\text{H}} > 0$  ( $\Delta G_{\text{H}} < 0$ ). Further,  $k_0$  encompasses several factors such as additional concentration factors due to applied and formal potentials, reaction rates for all elementary steps, and the effects from transfer coefficients in microkinetic models.<sup>34–36</sup> Based on *ab initio* thermodynamic analysis,<sup>37,75</sup> we assume that the hydrogen coverage is at the lowest limit for metal surfaces that repel hydrogen (i.e., with  $\Delta G_{\text{H}} > 0$ ), and attains a full monolayer coverage for surfaces that are attractive to hydrogen (i.e., with  $\Delta G_{\text{H}} < 0$ ). At a given temperature  $T$ , the fraction of surface occupied sites by hydrogen follows the Langmuir model such that  $\theta = K/(1 + K)$  with  $K = \exp(-\Delta G_{\text{H}}/k_{\text{B}}T)$ .  $k_0$  is the rate constant that is assumed to have a universal value for all metals, which is taken as  $k_0 = 200 \text{ s}^{-1} \text{ site}^{-1}$  by linearly fitting exchange currents to experimental data.<sup>23</sup> In a previous study we have shown that  $k_0$  assumes a different value for  $\beta\text{-Mo}_2\text{C}$  nanoparticles by fitting to experimental results.<sup>38</sup>

The hydrogen adsorption free energy  $\Delta G_{\text{H}}$  is obtained from the free energy difference between the hydrogen in gas phase and in adsorbed phase, which can be computed as,

$$\Delta G_{\text{H}} = \Delta E_{\text{ads}} + \Delta E_{\text{ZPE}} - T\Delta S, \quad (2)$$

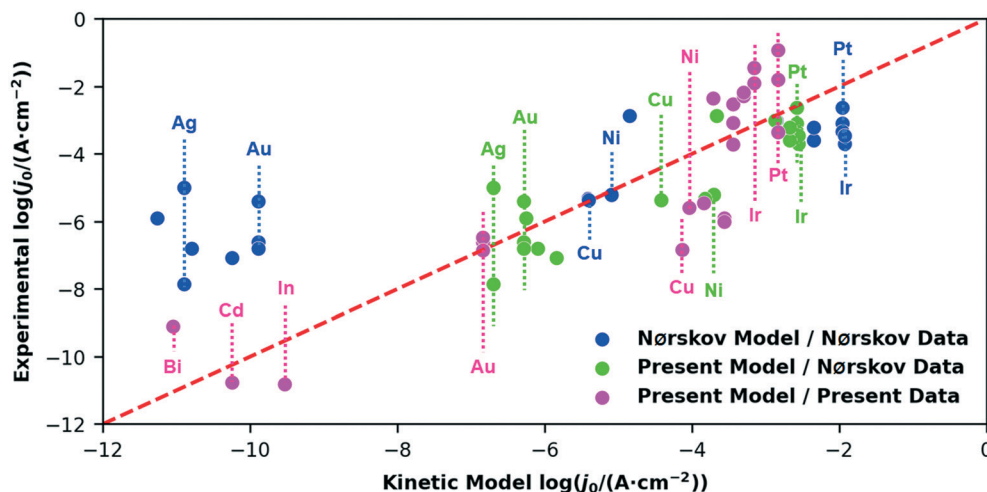
where  $\Delta E_{\text{ZPE}}$  is the zero-point energy that is found to be less than 0.05 eV for all metals, consistent with prior results.<sup>23</sup>  $\Delta S$  is the entropy between the hydrogen adsorbed state and the gas state. It can be approximated as  $-\frac{1}{2}S_{\text{H}_2}^0$  where  $S_{\text{H}_2}^0 = 1.35 \times 10^{-3} \text{ eV K}^{-1}$  is the entropy of hydrogen in the gas phase at room temperature, as obtained from experimental measurements.<sup>39</sup> The hydrogen adsorption energy  $\Delta E_{\text{ads}}$  is defined as,

$$\Delta E_{\text{ads}} = \frac{1}{n} \left( E_{\text{slab}/n\text{H}^*} - E_{\text{slab}} - \frac{n}{2} E_{\text{H}_2} \right), \quad (3)$$

where  $n$  is the number of adsorbed hydrogen atoms,  $E_{\text{slab}/n\text{H}^*}$  and  $E_{\text{slab}}$  are the energies of the slab with  $n$  adsorbed hydrogen atoms ( $\text{H}^*$ ) and of a clean slab respectively, and  $E_{\text{H}_2}$  is the energy of  $\text{H}_2$  in gas phase. All terms in eqn (3) are directly computed from DFT. The Nørskov model of eqn (1) shows that the maximum catalytic activity is at  $\Delta G_{\text{H}} = 0$  and the activity decreases when  $\Delta G_{\text{H}}$  moves away from zero, thus reproducing the volcano relationship for exchange current and adsorption free energy  $\Delta G_{\text{H}}$ .

The data labeled “Nørskov Model/Nørskov Data” in Fig. 1 shows the experimental exchange current densities  $j_0$  obtained from the original report vs. the computed values based on the Nørskov model. For consistency, we use the same  $\Delta G_{\text{H}}$  values as in the original report to compute  $j_0$  from eqn (1). As seen in Fig. 1, the Nørskov model qualitatively captures the experimental trend for the currents among the different metals. However, the model underestimates the experimental exchange currents by 3–6 orders of magnitude for the metal surfaces with low HER activity such as W, Nb, Au, and Ag, while it is in better agreement (within two orders of magnitude) for the highly catalytic surfaces of Pt, Pd, Ir, and Rh. We further confirm that the underestimation of exchange currents on low activity surfaces is not due to experimental errors. For example, for Bi, In and Cd, the experimental values are  $\sim 10^{-10} \text{ A cm}^{-2}$  that we have carefully examined from available literature (see Table S5†). In contrast, the corresponding exchange currents obtained from Nørskov model are  $\sim 10^{-21}$ ,  $\sim 10^{-17}$  and  $\sim 10^{-19} \text{ A cm}^{-2}$ , respectively. The large discrepancy between experimental and theoretical predictions, in addition to the systematic variation in the discrepancy, strongly suggests that the model does not capture one or more relevant physical parameters.

In the Nørskov model, the rate constant  $k_0$  is assumed to be constant for all metals, which was justified considering that  $k_0$  includes mainly effects of solvent reorganization during proton transfer to electrode surfaces. However, this approximation is too simplistic given the significant differences in the HER kinetics between highly efficient

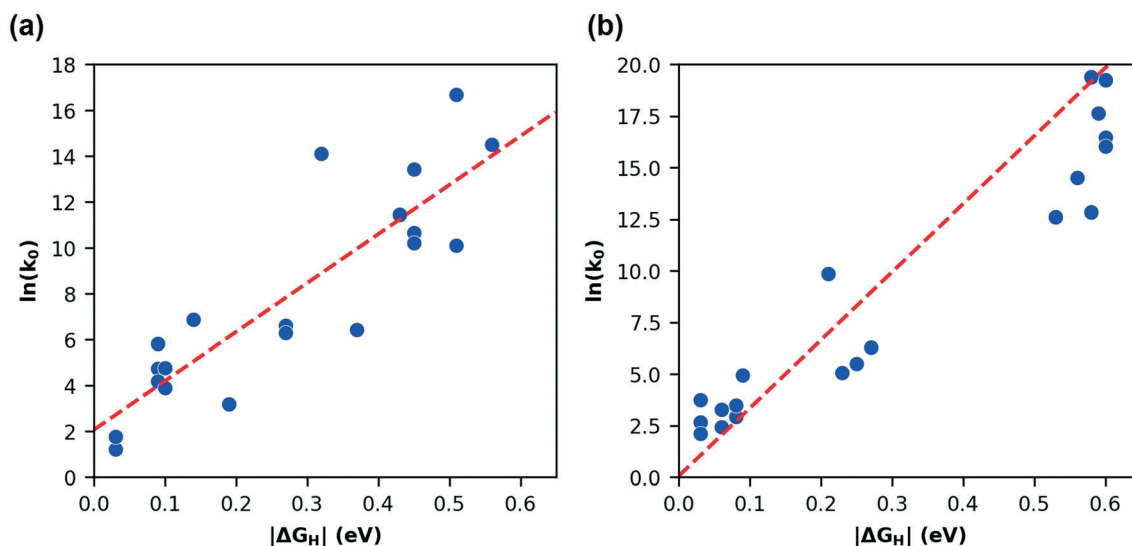


**Fig. 1** Comparison of experimental and calculated exchange current densities. We use the experimental data provided from the original work of ref. 23 (Nørskov data) and our database of Table 1 (present data). The models from the original work (Nørskov model) and our modified model (present model) are used for the calculation of  $j_0$ . To avoid clutter, we only labeled few elements belonging to three categories that are excellent (Pt and Ir), moderate (Ni and Cu) and poor (Ag, Au, Bi, In and Cd) HER catalysts. All data are shown in Table S3.†

surfaces such as Pt and Ir, and surfaces with lower HER activity such as W and Ag. For example, a very weak H-binding surface is likely to have a transition state that is similar in nature to a surface-bound hydrogen (the Volmer reaction as the rate-determining step), whereas a strong H-binding surface is likely to have a transition state that resembles  $H^+$  in the electrolyte or a weakly bound  $H_2$  (the Heyrovsky or the Tafel reaction is rate-determining). Thus, outer-sphere effects that can be rationalized as the reorganization of solvents<sup>40</sup> may be more significant for strong H-binding surfaces than weak H-binding surfaces.<sup>41</sup> Further, other factors contribute to different HER dynamics between metal surfaces, such as the solution pH and the composition and structure of the double layer, particularly

for inefficient catalysts that require very large overpotentials (and commensurately large electric fields across the double layer) to drive the HER.<sup>42</sup>

Re-examining the data provided in the original report,<sup>23</sup> our analyses clearly show that a universal  $k_0$  value is not justified. Fig. 2 presents implied  $k_0$  values obtained from linear regression analysis of eqn (1) using experimental  $j_0$  values and the DFT computed  $\Delta G_H$ . This approach amounts to testing the hypothesis that deviations between the experimental and DFT-predicted  $j_0$  using the Nørskov model can be attributed to a metal-dependent value of  $k_0$ . As seen in the figure, for both low and high coverage limits,  $k_0$  varies systematically with  $\Delta G_H$  over several orders of magnitude, where metals that weakly interact with hydrogen have low  $k_0$



**Fig. 2** The correlation of  $\ln(k_0)$  vs. absolute value for the hydrogen adsorption free energy  $|\Delta G_H|$  calculated from DFT for (a) low- and (b) high-coverage limits. All data including experimental currents and computed  $\Delta G_H$  are from ref. 23.

values and those that strongly interact with hydrogen, either repulsive or attractive, have larger  $k_0$  values. Further, as shown in Fig. 2, we find a strong linear correlation between  $\ln(k_0)$  and  $|\Delta G_H|$ . Indeed, invoking this linear relationship is found to substantially decrease the inconsistency between the kinetic model and the experimental values, as shown in Fig. 1 for the data labeled “Present Model/Nørskov Data”. We conclude from the analysis based on data in ref. 23 that  $k_0$  is not universal but is material-specific, at least to the extent that efficient *versus* inefficient metals should exhibit characteristically different  $k_0$  values. Notably, when restricted to a model that only incorporates metals with a similar range of H-binding energies, this effect is diminished – hence the fit is relatively good near the peak of the volcano only.

Recently, the Brønsted–Evans–Polanyi (BEP) relation, a linear relation between a reaction's free energy and its activation energy  $E_a$ , is confirmed for the HER on pure metal surfaces<sup>43</sup> using a computational approach that corrects for finite-size effects in periodic supercell simulations. For example, for the metals with  $\Delta G_H < 0$  ( $\Delta G_H > 0$ ), the activation barrier of the rate-limiting Heyrovsky (Volmer) reaction decreases with increasing (decreasing)  $\Delta G_H$ . The BEP relation on HER is also confirmed experimentally on precious metals of Pt, Ir, Pd and Rh.<sup>44</sup> If we assume that  $k_0$  of the Nørskov model is the HER reaction rate constant which follows the Arrhenius relation that  $\ln(k_0)$  is linearly proportional to activation energy  $E_a$ , and is in conjunction with the BEP relationship, we can infer the linear dependence between  $\ln(k_0)$  and  $|\Delta G_H|$  that is obtained using our data-driven approach. Further, the enthalpy–entropy compensation where  $E_a$  (or  $\Delta G_H$ ) has a linear relationship with entropy<sup>45</sup> suggests that  $\ln(k_0)$  includes effects from activation entropy that is metal-dependent,<sup>46</sup> which also supports our findings. However, we believe that a careful derivation is needed to formally derive the dependence between  $k_0$  and  $E_a$ .

To further examine the metal-dependence of  $k_0$ , we have compiled an additional set of experimental  $j_0$  values from a thorough literature search in Table 1 (see comments and references in Table S5†) and re-analyzed  $\Delta G_H$  using different DFT functionals (see Table S2†). The comparison between the experimental values and the values computed from the present model are shown in Fig. 1 under “Present Model/Present Data”. Fig. 3(a) shows the correlation between  $\ln(k_0)$  and  $|\Delta G_H|$  and Fig. 3(b) shows the volcano relationship corresponding to the new data. The DFT calculations are carried out using the Vienna *ab initio* simulation package (VASP).<sup>47–49</sup> More details about the DFT computational framework are provided in the ESI.† We employ the conventional<sup>50</sup> (PBE) and revised<sup>51</sup> (RPBE) Perdew–Burke–Ernzerhof exchange–correlational functional with and without van der Waals (vdW) corrections<sup>52,53</sup> to assess the variability of the results with the computational framework. The results shown in Fig. 1 and 3 are based on RPBE + vdW; however, the findings are found not to be sensitive to the functional (see Table S2†).

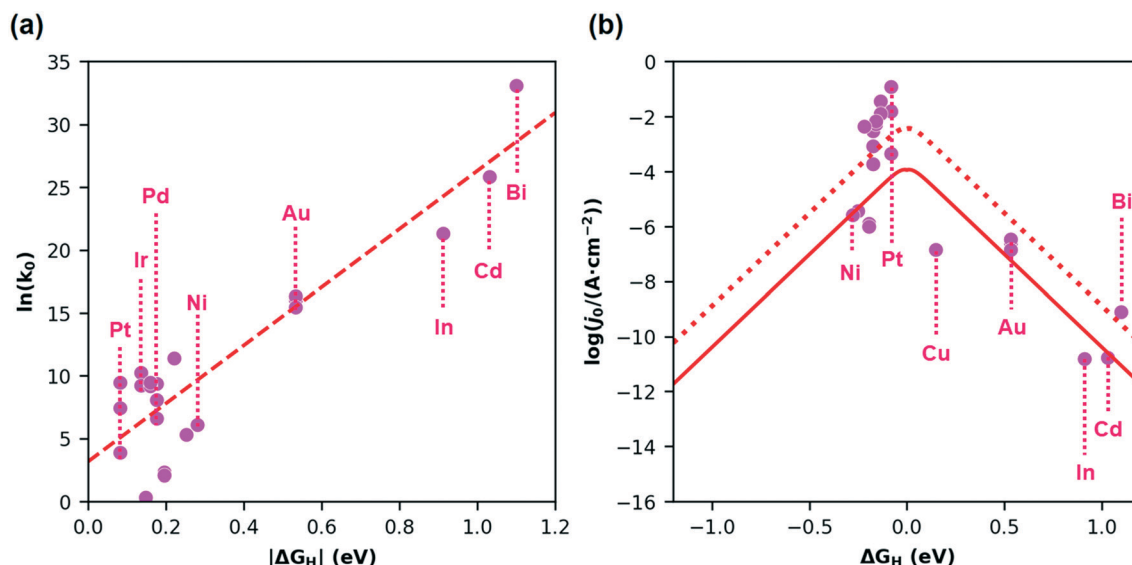
**Table 1** The collected exchange current densities from experiments

Electrode	Reported $j_0$ (A cm <sup>-2</sup> )	Electrolyte	Temperature	Ref.
Pt (111)	$4.5 \times 10^{-4}$	0.05 M H <sub>2</sub> SO <sub>4</sub>	303 K	54
Pt (100)	$6.0 \times 10^{-4}$			
Pt (110)	$9.8 \times 10^{-4}$			
Pt/C	$1.6 \times 10^{-2}$	0.2 M H <sub>3</sub> PO <sub>4</sub>	293 K	55
Pt/C	$1.2 \times 10^{-1}$	0.1 M HClO <sub>4</sub>	313 K	56
Ir/C	$3.6 \times 10^{-2}$	0.1 M HClO <sub>4</sub>	313 K	56
Ir/C	$1.28 \times 10^{-2}$	0.2 M H <sub>2</sub> SO <sub>4</sub>	293 K	55
Pd	$1.9 \times 10^{-4}$	0.5 M H <sub>2</sub> SO <sub>4</sub>	Not mentioned	57
Pd/C	$3.0 \times 10^{-3}$	0.1 M HClO <sub>4</sub>	313 K	56
Pd/C	$8.4 \times 10^{-4}$	0.1 M HClO <sub>4</sub>	293 K	55
Rh/C	$5.2 \times 10^{-3}$	0.1 M HClO <sub>4</sub>	313 K	56
Rh/C	$6.7 \times 10^{-3}$	0.1 M HClO <sub>4</sub>	293 K	55
Ru	$4.5 \times 10^{-3}$	1 M HCl + NaCl	298 K	58
Cu	$1.45 \times 10^{-7}$	0.1 N HCl	Not mentioned	59
Co	$3.6 \times 10^{-6}$	1 M H <sub>2</sub> SO <sub>4</sub>	293 K	60
Ni	$2.6 \times 10^{-6}$	0.5 M H <sub>2</sub> SO <sub>4</sub>	295 K	61
Au (111)	$2.5 \times 10^{-7}$	0.1 M HClO <sub>4</sub>	Not mentioned	62
Au (100)	$0.5 \times 10^{-7}$			
Au (110)	$0.3 \times 10^{-7}$			
Au (111)	$3.38 \times 10^{-7}$	0.5 M H <sub>2</sub> SO <sub>4</sub>	Not mentioned	63
Poly Au	$1.40 \times 10^{-7}$	0.1 M HClO <sub>4</sub>	Not mentioned	62
Re	$1.25 \times 10^{-6}$	0.5 M H <sub>2</sub> SO <sub>4</sub>	298 K	64
Re	$1 \times 10^{-6}$	0.5 M H <sub>2</sub> SO <sub>4</sub>	298 K	65
Cd	$1.7 \times 10^{-11}$	0.5 N H <sub>2</sub> SO <sub>4</sub>	Not mentioned	66
Bi	$8 \times 10^{-10}$	4.8 M H <sub>2</sub> SO <sub>4</sub>	Not mentioned	67
In	$1.51 \times 10^{-11}$	0.1 M HClO <sub>4</sub>	303 K	68

The library of experimental exchange current densities<sup>54–68</sup> labeled as “Present Data” in Fig. 1 and used in Fig. 3 was collected from a larger set of prior literature reports, which were then down-selected to only those reports that minimized or otherwise accounted for the impacts of electrolyte/surface contamination, electrode roughness, and mass transfer effects. Table 1 summarizes the experimental results. A detailed discussion of this down-selection process is included in the ESI.† We also chose to exclude metals that are expected to be oxidized under HER conditions in acidic solution, such as Mo, W, and Nb.<sup>69</sup> Finally, we added measurements on Cd, In, and Bi and Ru that were not included in ref. 23. Fig. 3 shows that considerably more experimental data are available for HER-active metals, which accounts for the greater density of points with small  $|\Delta G_H|$ . The spread in these data likely reflects uncertainty both in DFT-calculated  $\Delta G_H$  and experimental  $j_0$ .<sup>70</sup> Nonetheless, as shown in Fig. 3(a), there is a clear linear relationship between  $\ln k_0$  and  $|\Delta G_H|$  that can be described as  $\ln(k_0) = 23.16|\Delta G_H| + 3.17$ . This is specifically evidenced in clustering of three metal groups with characteristically different H binding energies: the precious metals (Pt, Ir, Pd and Rh) near  $|\Delta G_H| = 0.1$  eV, the metals near  $|\Delta G_H| = 0.5$  eV, and the HER inert metals near  $|\Delta G_H| = 1$  eV.

Our results clearly show that  $\Delta G_H$  more accurately describes  $j_0$  for the HER if we include an additional exponential relationship between  $|\Delta G_H|$  on  $k_0$ . However, it is conceivable that  $k_0$ , and hence the exchange current density, also depends on other metal properties besides  $\Delta G_H$ . For instance, previous studies postulated that the HER rate can





**Fig. 3** (a) Correlation between  $\ln(k_0)$  and  $|\Delta G_H|$  using “Present Data” of Fig. 1 (see Table S4†). From the linear fitting, we obtain  $\ln(k_0) = 23.16|\Delta G_H| + 3.17$  with a correlation factor of  $r^2 = 0.82$ . (b) The new volcano curve of  $j_0$  based on the present model/present data. The dotted and solid red lines are obtained using eqn (1) with the maximum and the minimum  $C_{\text{tot}}$  in our data, respectively.

be modeled by using atomic number, work functions, and Pauling electronegativities as material descriptors.<sup>10–16</sup> To investigate this, we used a machine learning approach based on SISSO (sure independence screening and sparsifying operator)<sup>71–74</sup> to develop an accurate and physically interpretable model for  $\ln k_0$ . We investigated the following primary atomic features in this analysis: empirical radius, mass, number, period in periodic table, electron affinity, ionization energy, and Pauling electronegativity, in addition to the following metal features: density and work function. In the SISSO approach, potential descriptors for  $\ln k_0$  are formed from the primary features with up to ten level interactions of complexity utilizing three mathematical operations (addition, multiplication, and division). The limited size of the experimental dataset (12 metals) precludes a full investigation, and thus, we used a relatively small number of primary features and mathematical operations in the construction of only one-dimensional descriptors. By searching the massive space of potential descriptors, SISSO identified many models for  $\ln k_0$  that capture a large proportion of the variations among different elements. Table S6† lists the best ten models with correlation coefficients  $r^2 > 0.975$ . Notably all these models are found to depend on  $|\Delta G_H|$  indicating its prime effect on  $k_0$ . However, a larger experimental database is needed to unambiguously validate the findings, and to identify other, if any, important material properties that affect  $k_0$ .

In summary, we agree with the original work by Nørskov and collaborators that the trend of  $j_0$  can be explained by a kinetic model that relies on  $\Delta G_H$  as the sole descriptor. However, after carefully analyzing the experimental and computational results, we propose that the same kinetic model better matches with experiments over a wide range of

metals by treating the logarithm of the rate constant  $k_0$  as a linear function of the absolute value of  $\Delta G_H$ .

## Conflicts of interest

There are no conflicts to declare.

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