

Oxidized Bacterial Cellulose Functionalized with SiO₂ Nanoparticles as a Separator for Lithium-Metal and Lithium-Sulfur Batteries

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Abstract:

It is highly desirable to develop lithium-metal batteries (LMBs), including lithium-sulfur batteries (LSBs), as the next-generation high-energy batteries. However, issues related to Li metal anodes and sulfur cathodes, such as non-uniform Li deposition and polysulfide shuttling, must be addressed. Here we report the study of bacterial cellulose (BC), modified by SiO₂ nanoparticles (NPs), as a separator material for LMBs and LSBs. To achieve uniform decoration of SiO₂ NPs on BC nanofibers, we oxidize and partly hydrolyze BC by introducing carboxyl groups and tetraethyl orthosilicate (TEOS). Electrochemical studies confirm that the composite BC film can smoothen the Li⁺ flux, regulate the Li deposition, and curb the polysulfide shuttling due to the strong interaction of oxygen functional groups on oxidized BC and SiO₂ with Li⁺ and polysulfides. As a separator used in lithium plating and stripping, the composite BC/SiO₂ film offers much better stability, lower polarization voltage, and higher Coulombic efficiency than conventional separators. When applied in Li//S and Li//LiFePO₄ batteries, it also demonstrates much-improved performance. Such a functionalized BC separator is very promising in LMB and LSB applications.

Keywords: *Bacterial cellulose; separator; lithium dendrite; polysulfide shuttle; lithium-sulfur battery; lithium-metal battery*

29 Introduction

30 Elemental lithium has the highest theoretical specific capacity (3861 mAh g^{-1}) and the
31 lowest negative potential (-3.04 V vs. standard hydrogen electrode), making it the most
32 attractive battery anode material. Li-metal batteries (LMBs)(Cheng et al., 2017; Cheng et
33 al., 2016; Li et al., 2014) use Li metal as the anode to substitute the conventional graphite
34 anode of Li-ion batteries (LIBs) and a cathode based on either traditional oxide materials
35 or more exotic sulfur(Hou et al., 2021; Zhao et al., 2018) and oxygen(Grande et al., 2015).
36 They can deliver an energy density significantly higher than LIBs(Whittingham, 2014).

37 However, several challenges of using Li metal anode must be overcome before LMBs
38 can be made available for widespread use. The formation of lithium dendrites and the
39 associated unstable solid electrolyte interface (SEI) are the most notorious ones(Fang et
40 al., 2019; Shen et al., 2019; Wu et al., 2018). Lithium dendrites can penetrate the
41 separator to shorten the cathode and the anode, raising severe safety concerns(Guo et al.,
42 2017; Wu et al., 2019a). They also can detach from the anode and form dead lithium after
43 encapsulation by insulating SEI(Chen et al., 2017; Kushima et al., 2017; Xu et al., 2019).
44 Moreover, the dendrite detachments expose fresh lithium to the electrolyte, causing a
45 continuous reaction between lithium and the electrolyte, resulting in fast capacity loss and
46 low Coulombic efficiency during battery operation(Fang et al., 2019; Liu et al., 2018).

47 Depending on battery chemistry, the pairing cathode may exacerbate the
48 aforementioned issues by introducing other side reactions. For example, lithium-sulfur
49 battery (LSB) employs sulfur as the cathode material, offering several intriguing merits
50 such as a large specific capacity (1675 mAh g^{-1}) and low cost(Li et al., 2022). However,
51 in the stepwise conversion between S_8 and Li_2S , many intermittent lithium polysulfide
52 species are formed, most of which are dissoluble in the electrolyte(Yen and Chung, 2021;
53 Zhao et al., 2022). The shuttling of these polysulfides between the cathode and the anode
54 gives rise to capacity fading, enhanced corrosion of the lithium anode, and self-
55 discharge(Moy et al., 2014).

56 Lithium dendrite formation is correlated to localized high Li^+ flux "hot spots", while

the commercial polyolefin-based battery separators, with their large and non-uniform pore distribution, are one of the significant factors causing localized high Li^+ flux hot spots (Li et al., 2020b; Wang et al., 2019). Therefore, engineering the separator to facilitate uniform Li^+ transfer and Li redeposition is one promising approach to addressing the lithium dendrite problem (Liu et al., 2017; Liu et al., 2019b). In addition, reducing the separator pore size or functionalizing the separator with charged moieties can block the polysulfide pathway to curb polysulfides' shuttling effect and self-discharging in LSBs, as reported by others (Huang et al., 2015; Yu et al., 2018; Zhu et al., 2019) and ourselves (Li et al., 2021).

Therefore, engineering separators with multifunction to simultaneously address Li dendrite formation and polysulfides shuttling are attracting intense interest. For example, the periodically arranged Co-O_4 moieties on metal-organic framework nanosheets were synthesized as a battery separator to homogenize Li^+ flux and suppress polysulfide shuttling (Li et al., 2020c). However, building these multi-functionalized separators is challenging due to the complicated structures and synthesis methods involved. Here we report our study using bacterial cellulose (BC) anchored with SiO_2 nanoparticles (NPs) to fabricate a multi-functionalized separator.

As a natural polymer-based nanofiber network, BC offers unique properties such as strong mechanical strength, outstanding thermal and chemical stability, excellent wettability, and low cost (Huang et al., 2014; Iguchi et al., 2000). It is being investigated for use as battery separators directly or after modification/chemical functionalization (Bharti et al., 2022; Gwon et al., 2019; Huang et al., 2020; Huang et al., 2021; Kim et al., 2020; Li et al., 2021; Lokhande et al., 2022; Xie et al., 2022; Yang et al., 2020). In terms of chemical modification, the dense hydroxyl groups on cellulose chains render BC a highly polar polymer. Its dense O-containing moieties enable the formation of oxide NPs on the BC nanofibers (Araújo et al., 2018; Chanthiwong et al., 2020). A strong interaction between Li^+ and oxide NPs (and BC) helps homogenize Li^+ flux, rendering stable lithium stripping/plating. The oxygen-related bonds also effectively

absorb polysulfide species, suppressing the shuttling process(Rehman et al., 2016; Suriyakumar et al., 2018; Wu et al., 2019b).

In this work, low-cost SiO₂ is chosen as an example to modify the BC separator. It is noted SiO₂/BC structures have been reported for various applications where the structures were formed by directly mixing SiO₂ NPs and BC fibrils that causes phase segregations and clustering(Kim et al., 2020; Kim et al., 2019; Rahman et al., 2021). In contrast, our SiO₂/BC composite films were obtained *via* in-situ nucleation of SiO₂ directly on BC to achieve uniform distribution, which is crucial to homogenize the Li⁺ flux in preventing lithium dendrite formation. Using such a BC/SiO₂ composite separator in the Li//Li symmetric and Li//Cu asymmetric cells to conduct the Li stripping/plating study, we observed lower polarization voltage, higher coulombic efficiency, and much longer lithium stripping/plating cycling stability when compared to cells using either the conventional Celgard 2400 (C-2400) separator or the pristine BC separator. As a result, the fabricated LSBs and Li//LiFePO₄ batteries had markedly improved electrochemical performances. For example, the LSB cell with 4 mg cm⁻² of sulfur loading can deliver ~1250 mAh g⁻¹ of specific capacity at 0.1C and maintain 83% capacity after 100 cycles at 0.25C. The LMB cell based on Li//LiFePO₄ shows high and more stable Coulombic efficiency (~99.5%) after 200 cycles. These experimental results demonstrate that the BC-based composite materials are a promising candidate for the battery separator in LMB and LSB applications.

Experimental section

BC purification and oxidation

BC pellicles produced *via* a fermentation process(Islam et al., 2017) were washed in deionized (DI) water, then boiled in 0.5 M KOH solution for one hour to remove impurities. The pellicles were then rewashed in DI water until a pH of ~7.0. To introduce carboxyl function groups into BC separators, the large BC pellicles were minced into BC

pulp and then subjected to an oxidation process(Saito et al., 2007). Briefly, 30 g of BC pulp was first dispersed into 100 mL of DI water under vigorous stirring, then 0.016 g of 2,2,6,6-tetramethylpiperidine-1-oxyl (TEMPO) and 0.1 g of NaBr were added into the solution sequentially. After they dissolved completely, 5 mL of 12% NaClO solution was added dropwise into the mixture. During the reaction process, the solution's pH was adjusted using 0.5 M NaOH to ~10. The oxidation reaction was carried out for 5 hours and then quenched by pouring 5 mL of ethanol directly into the solution. We experimented with different oxidation times to study their influence on the dispersive performance of oxidized BC (o-BC) in water. Five hours of oxidation resulted in a stable and well-mixed o-BC water suspension, avoiding sedimentation for several days. Such a stable suspension guarantees the subsequent uniform BC modification by SiO₂ NPs. The o-BC was collected *via* centrifuge and washed using 0.5 M HCl solution, DI water, and ethanol until the pH reached 7.0. The collected o-BC was homogeneously dispersed into ethanol or DI water because of their large carboxyl functional group concentration.

Fabrication of SiO₂ on oxidized BC (o-BC/SiO₂) composite films

400 μ L of TEOS was dissolved into 50 mL of ethanol solution of o-BC. After stirring for 30 min, 1.0 mL of ammonium hydroxide was added dropwise into the mixture. The resulting o-BC/SiO₂ composite was collected via centrifuge, washed sequentially with DI water and ethanol, and then dispersed into 50 mL of ethanol. The o-BC/SiO₂ was separated by filtrating 25 mL of the above mixture through a PTFE membrane (44 mm diameter, 0.22 μ m pore size)., the material was sandwiched between two glass slides and dried in a vacuum oven at 80 °C for 12 h to produce a flat film. The o-BC film without SiO₂ was also prepared using the same procedure.

Characterization and electrochemical test

The morphological features of the samples were studied using a field emission scanning electron microscope (FEI XL 30FE-SEM). The samples were directly attached to the sample holder using conductive tape. The images were taken under 5 kV electron accelerating voltage. X-ray diffraction (XRD) patterns of the samples were recorded in

140 refection mode at a step size of 0.05° by using a Rigaku MiniFlex 6G diffractometer
141 equipped with a Cu-K α radiation source operated at 30 kV and 15 mA. The samples were
142 attached to a Si low background holder using double-sided tape. The collected data were
143 corrected by subtracting the holder/tape background signals. Differential scanning
144 calorimetry (DSC) was conducted on a LABSYS EVO instrument. Before performing the
145 DSC measurement, the samples were dried at 80 °C in a vacuum overnight. They were
146 loaded into a 100 μ L Al₂O₃ crucible. The DSC data was recorded by heating the samples
147 from room temperature to 600°C at a heating rate of 20 °C/min under the argon
148 atmosphere.

149 To measure its Li⁺ ionic conductivity, a separator was first soaked in the blank
150 electrolyte (1 M LiTFSI in 1:1 1,3-dioxolane (DOL)/dimethylethane (DME)) and then
151 sandwiched between two stainless steel spacers and sealed in a coin cell. Electrochemical
152 impedance spectroscopy (EIS) test was performed to obtain the resistance, and the ionic
153 conductivity was calculated by using the equation $\sigma = \frac{l}{RS}$, where l is the thickness of the
154 separator, R is the resistance read from the Nyquist plot, and S is the area of the separator.
155 The transference number t^+ was calculated using the equation of $t^+ = I_s(V -$
156 $I_0R_0)/[I_0(V - I_sR_s)]$, where V is the applied DC voltage (10 mV), I_0 and I_s are the initial
157 and steady-state currents, respectively, which are read from the Chronoamperometry
158 curves. R_0 and R_s are the interfacial resistances before and after DC polarization,
159 respectively, obtained from EIS curves.

160 Li//Li symmetric coin-type cells (CR2400) were fabricated by employing lithium
161 plates as both electrodes, the C-2400 or the BC-based film as the separator, 1 M
162 bis(trifluoromethane)sulfonamide lithium salt (LiTFSI) dissolved in a 1:1 v/v% mixture
163 of DOL/DME solution with 1wt% LiNO₃ as the electrolyte. Cyclic voltammetry (CV) and
164 EIS (0.1-100 kHz with an AC voltage amplitude of 10 mV) tests were performed on a
165 Bio-logic SP-150 electrochemical workstation. The lithium stripping and plating cycling
166 were recorded on a battery tester (LANHE, CT2001A). Li//Cu asymmetric cells were also
167 characterized using a similar configuration, except a Cu foil was used for the positive

168 electrode.

169 Two different types of lithium metal batteries were chosen to demonstrate the
170 feasibility of the o-BC/SiO₂ separator, i.e., Li//S battery and Li//LiFePO₄ battery. For the
171 LSB, lithium metal was used as the anode, sulfur loaded in a carbonized BC (cBC) film
172 as the cathode (Li et al., 2017a), the C-2400 or the BC-based film as the separator, 1 M
173 bis(trifluoromethane)sulfonamide lithium salt (LiTFSI) with 1wt% LiNO₃ dissolved in a
174 1:1 v/v% mixture of 1,3-dioxolane (DOL)/dimethylethane (DME) solution as the
175 electrolyte. The sulfur loading in cBC film is around 4 mg cm⁻², which yields sulfur
176 weight percentage of ~65% in the cathode. The ratio of the electrolyte volume (μL) and
177 the sulfur mass loading (mg) is ~15 μL/mg. For the Li//LiFePO₄ battery, a commercial
178 LiFePO₄/aluminum foil (single side coated, 12 mg cm⁻², MTI corporation) was used as
179 the cathode, 1 M LiPF₆ in ethylene carbonate (EC), and ethyl methyl carbonate (EMC)
180 was used as the electrolyte (MTI corporation), the ratio of electrolyte and LFP is
181 ~10μL/mg

182

Results and discussion

Material characterization

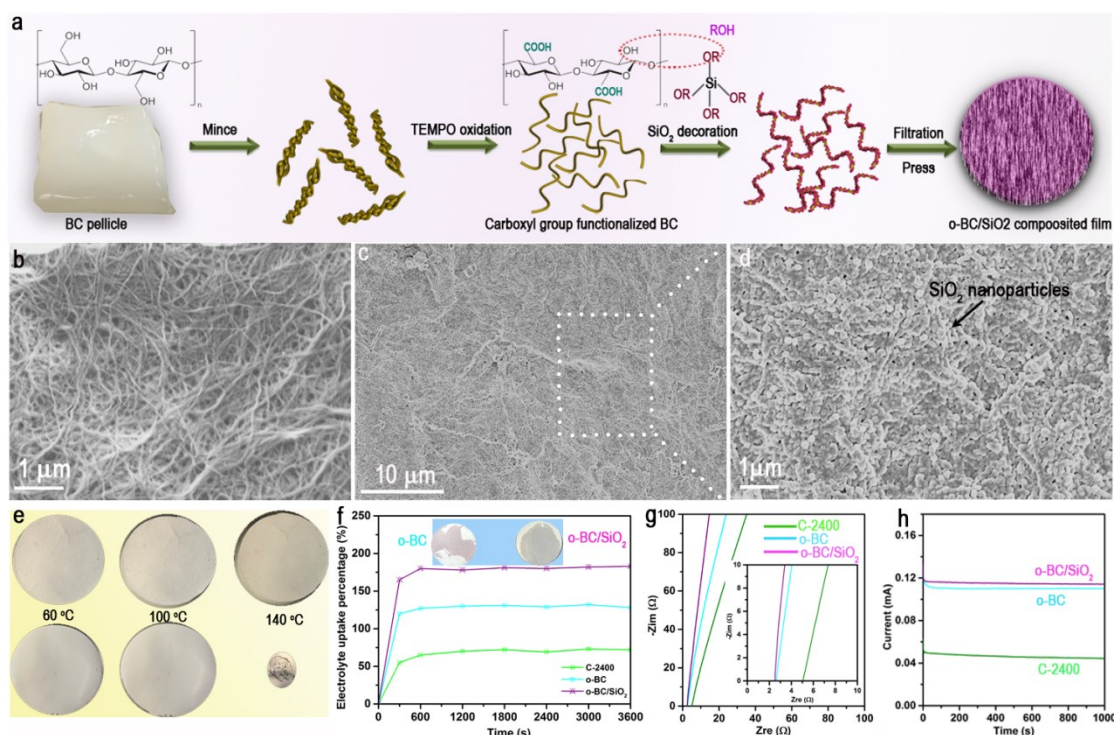


Figure 1. (a) Schematic illustration of the preparation process of the o-BC/SiO₂ film. SEM image of (b) o-BC and (c and d) o-BC/SiO₂. (e) Thermal stability comparison between o-BC/SiO₂ (the top line) and C-2400. (f) Electrolyte wettability and uptake capability, (g) Nyquist plots, and (h) I-t curves for the three different separator films.

Figure 1a summarizes the fabrication process for the o-BC/SiO₂ composite film. The purified BC pellicles were first minced into BC pulp and then exposed to the TEMPO oxidation process to selectively convert the C2-hydroxyl functional groups into carboxyl functional groups. The TEMPO oxidation process can also partly hydrolyze the thick fibrils into microfibrils, resulting in better dispersion in water and ethanol (Figure S1).

Previous works have reported BC materials modified with Ag, Au, and other metal nanoparticles (Chen et al., 2015; Ifuku et al., 2009; Kaushik and Moores, 2016). The distribution of the nanoparticles was significantly improved after introducing extrinsic functional groups on the BC due to the interaction between the functional groups and metal ions precursors and thinner BC fiber diameters. We imagined that a similar mechanism could also be used to produce evenly distributed metal oxides/nonmetal oxide

modified BC composites, as schematically shown in Figure 1a, where the SiO₂ precursor, TEOS (Braddock et al., 2018; Lemos et al., 2016), will react with the hydroxyl groups (Rama et al., 2019; Shafi and Zhao, 2020) and nucleate on the surface of BC nanofibrils. At the same time, the carboxyl functional groups can be preserved, which will serve as another polysulfide shuttling barrier because of the direct repulsive interaction between these carboxyl functional groups and polysulfides (Huang et al., 2021). After vacuum filtration and rolling-press steps, a BC/SiO₂ composite film with controllable thickness was obtained. The SEM image of o-BC is shown in Figure 1b. The cross-linked structure guarantees the flexibility of the resulting thin film (Figure S2). The ~100 nm SiO₂ nanoparticles uniformly decorate BC nanofibrils (Figures 1c and 1d). The XRD pattern of o-BC/SiO₂ is exhibited in Figure S3. The diffraction peaks located at 20~14.2° and 22.5° can be assigned to the (101) and (002) lattice plane, respectively. The characteristic peak of amorphous SiO₂ overlaps with the o-BC at around 22°. This in-situ nucleation process shows an obvious advantage over the SiO₂/BC films fabricated by directly mixing SiO₂ nanoparticles and BC fibrils that causes phase segregations (Kim et al., 2020; Kim et al., 2019; Rahman et al., 2021).

Safe operation at high temperatures is a crucial requirement of the battery separator. The commercial Celgard membranes can only endure a temperature of ~120 °C before dangerous fault modes become prevalent during operation (Arora and Zhang, 2004; Zhang, 2007). The o-BC-based films were tested at elevated temperatures in an oven, and the results are exhibited in Figure 1e. The o-BC (not shown) and o-BC/SiO₂ films maintain structural integrity (i.e., shape and dimensions) when temperatures reach 140 °C, while the commercial C-2400 separator film melts at this temperature. To quantitatively characterize the chemical changes at elevated temperatures, a differential scanning calorimetry (DSC) method was used (Figure S4). The C-2400 separator shows a prominent endothermic peak at ~150 °C, attributed to the melting of polypropylene. In contrast, the BC-based polymer films endured temperatures as high as ~350 °C before evidence of melting or decomposition was observed. These results suggest that

230 incorporating BC in batteries could enable safe operation at much higher temperatures
231 than can be achieved with the current C-2400 separator.

232 The electrolyte wettability and uptake capacity are critical parameters to access a
233 film's potential for use as a battery separator. As shown in Figure 1f, with their large
234 porosity and hydrophilicity, both o-BC and o-BC/SiO₂ films absorb more electrolytes
235 than C-2400. A further advantage is that the wettability of o-BC can be improved
236 significantly after being composited with SiO₂ nanoparticles (inset, Figure 1f). Table S1
237 summarizes the values of thickness, areal density and electrolyte uptake weight
238 percentage of different separators, giving a clear exhibition of the merits of the oBC/SiO₂
239 hybrid film.

240 The Li⁺ ionic conductivity and transference number were also measured. The
241 experimental results are presented in Figures 1g, 1h, S5, and S6. Separators with surface
242 functional groups such as oxygen- or nitrogen-containing groups have stronger binding
243 energy to Li⁺ (e.g., the binding energy between carbonyl and Li⁺ is ~ 3.08 eV(Lin et al.,
244 2016)) than bare separators. The Li⁺ conductivities through o-BC (0.36 mS cm⁻¹) and o-
245 BC/SiO₂ (0.39 mS cm⁻¹) films are higher than through C-2400 (0.23 mS cm⁻¹). The
246 enhanced conductivities result from the high Li⁺ affinity provided by the oxygen
247 functional groups to both o-BC and SiO₂(Liu et al., 2019a; Pathak et al., 2019). The Li⁺
248 transference number of o-BC-based films (0.63 for the o-BC/SiO₂ film and 0.65 for the o-
249 BC one) is higher than that of C-2400 (0.59), suggesting its favorable Li⁺ transport
250 capability.

251

252 Li stripping and plating study

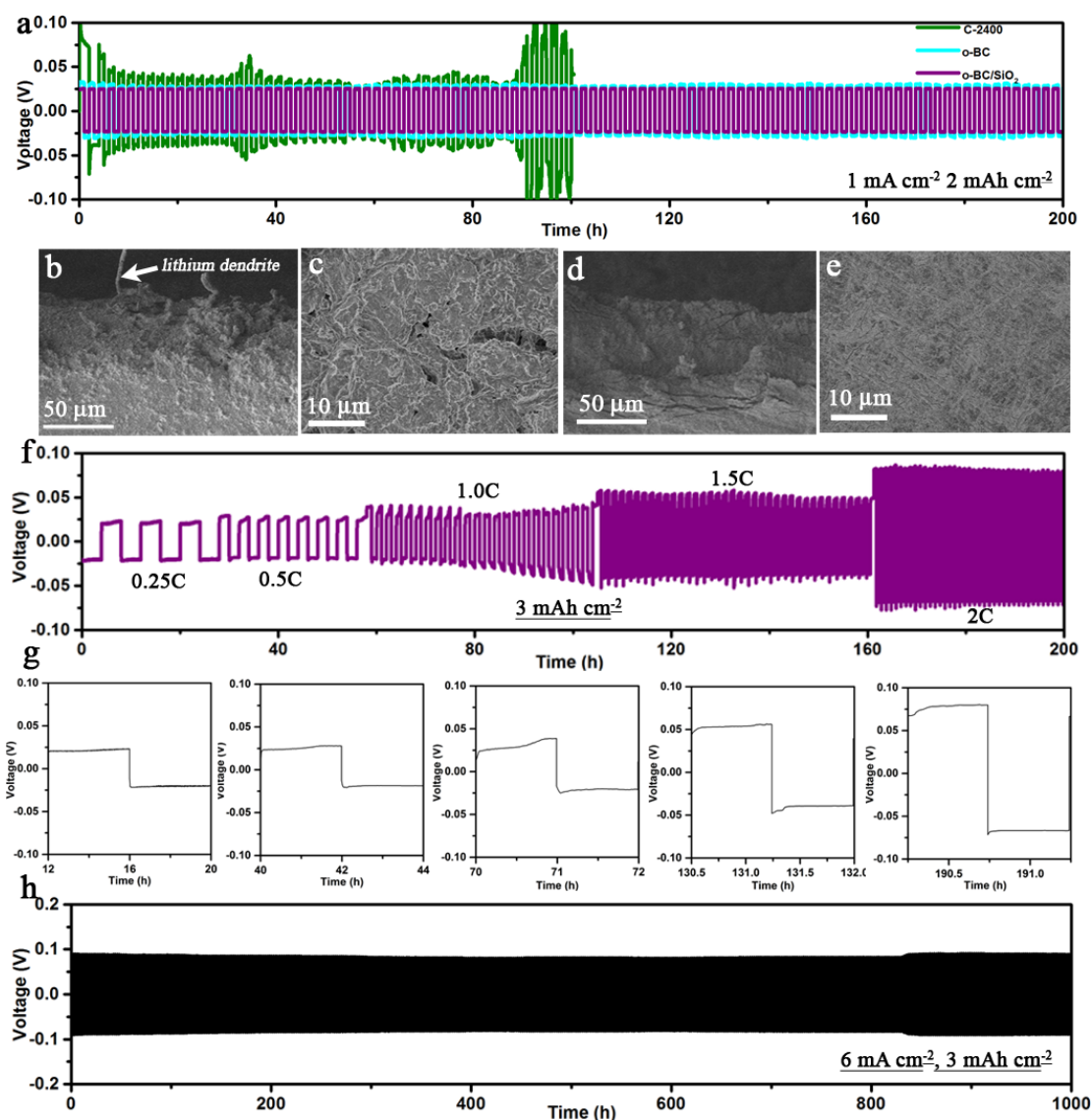


Figure 2. Lithium plating and stripping result: (a) lithium stripping and plating using symmetric cells with C-2400, o-BC, or o-BC/SiO₂ film as a separator (2 mAh cm⁻² of specific capacity and 1 mA cm⁻² of charge/discharge current density). SEM surface and cross-sectional images of the lithium plate after lithium stripping and plating cycling (b and c: C-2400 film as the separator after 60 h, d, and e: o-BC/SiO₂ film as the separator after 200 h.) (f) Rating performance of cell with the o-BC separator at 3 mAh cm⁻² of specific capacity. (g) Charge-discharge voltage profiles under different current densities were extracted from the rating curve in Figure 2f. (h) Long-term stability test of cell with o-BC/SiO₂ separator (3 mAh cm⁻² of specific capacity and 6.0 mA cm⁻² of charge-discharge current density).

Galvanostatic cycling of Li//Li symmetric cells was performed to compare the Li stripping and plating efficiency of the commercial C-2400 with the o-BC-based separators. A cutoff potential of 120 mV was pre-set. We fixed the specific capacity to 2 mAh cm⁻² and the charge-discharge current density to 1 mA cm⁻². The cells with o-BC and o-BC/SiO₂ separators exhibited very low polarization voltages (~27 and ~25 mV,

269 respectively) and stable cycling performance over 200 h of testing (**Figure 2a**). In
270 contrast, the cell using a C-2400 separator suffered from a higher polarization voltage
271 (~ 46 mV), which further increased to the pre-set cutoff potential of 120 mV after only 90
272 h.

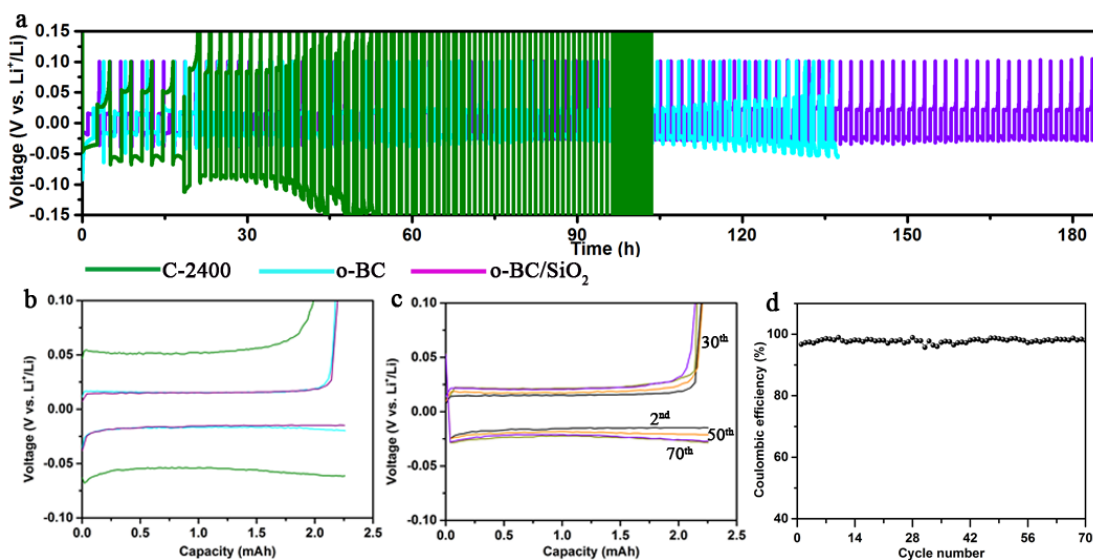
273 Cycled cells were disassembled, and the structural changes in the lithium electrodes
274 were imaged using an SEM. Figures 2b and 2c show the cross-section and surface SEM
275 images of a lithium plate from the symmetric cell with a C-2400 separator after 60 h of
276 testing. Lithium dendrites are visible, as indicated by the arrow in Figure 2b. The figures
277 also show that the surface is rough and granular, the signature of non-uniform Li plating.
278 In contrast, no lithium dendrites are observed in the lithium plate for the Li//Li cell with
279 an o-BC/SiO₂ separator (Figure 2d). The figure also shows that the surface is smooth and
280 uniform even after 200 h of cycling. These observations reveal that our o-BC/SiO₂
281 separators can more effectively regulate the lithium plating processes and suppress
282 lithium dendrite formation and surface coarsening than the C-2400 separators. The much
283 better performance of the o-BC/SiO₂ separator over C-2400 can be attributed to the higher
284 Li⁺ ion adsorption capability due to the more vital interaction between Li⁺ and o-BC/SiO₂.
285 The ability to absorb Li⁺ by a separator in a high-rate plating process will adjust
286 and homogenize Li⁺ flux toward the plated Li electrode, resulting in uniform deposition
287 and preventing dendrites formation and Li metal surface roughening.

288 Similarly, when using an o-BC film as the separator, the lithium plate is dendrite-free
289 and very dense after cycling, without the granular and porous structure (Figure S7). The
290 abundant oxygen functional groups on the BC are lithiophilic sites that can regulate and
291 homogenize the Li⁺ flux, leading to uniform Li deposition on the Li plate.

292 The stripping/plating rate performance of the Li//Li cell with the o-BC/SiO₂ separator
293 was further evaluated, and the results are presented in Figure 2f. With the cycling current
294 density increased from 0.75 to 6 mA cm⁻² and maintaining the same specific capacity of 3
295 mAh cm⁻², the polarization voltage rises from ~ 25 to ~ 90 mV and then holds a relatively
296 steady value of ~ 90 mV at 6 mA cm⁻² during cycling. Several representative voltage

297 profiles under different current densities are presented in Figure 2g. The charge and
 298 discharge plateaus are smooth without any spikes for the much higher 6 mA cm^{-2} current
 299 density, reflecting stable Li^+ redox reactions on the surface of the Li electrode.

300 To further demonstrate the potential of the o-BC separator for fast charge-discharge
 301 and long cycling stability, the Li//Li symmetric cell was cycled at the current density of 6
 302 mA cm^{-2} for 1000 h. As shown in Figure 2h, the overpotential maintains a value of ~ 90
 303 mV for the first 850 h and then increases to ~ 100 mV slowly upon cycling up to the
 304 1000^{th} h. This excellent performance for long cycling times at large current densities
 305 demonstrates the o-BC/SiO₂ film's ability to homogenize the Li-ion flux and prohibit the
 306 dendrite formation during the Li plating process. These results further support our notion
 307 that functionalized BC-based separators have the potential to be the choice of Li metal-
 308 based battery technology in the future. The long cycling performance of the o-BC
 309 separator is presented in Figure S8. The polarization voltage stabilizes at ~ 100 mV at a 6
 310 mA cm^{-2} current density for ~ 200 h and gradually increases to ~ 140 mV by the 1000^{th}
 311 cycle.



312

313 **Figure 3.** Li//Cu asymmetric cell testing results: (a) Cycling performance (The C-2400 and o-BC-
 314 based cells were cycled at the current density of 1.0 mA cm^{-2} at the first five cycles and the o-
 315 BC/SiO₂-based cell was cycled at the current density of 2.0 mA cm^{-2} from the beginning) and (b)
 316 Voltage profiles of cells using different separators. (c) Voltage profiles of the o-BC/SiO₂-based cell
 317 at different current densities in different cycles. (d) Coulombic efficiency of the o-BC/SiO₂ based
 318 cell within 70 cycles.

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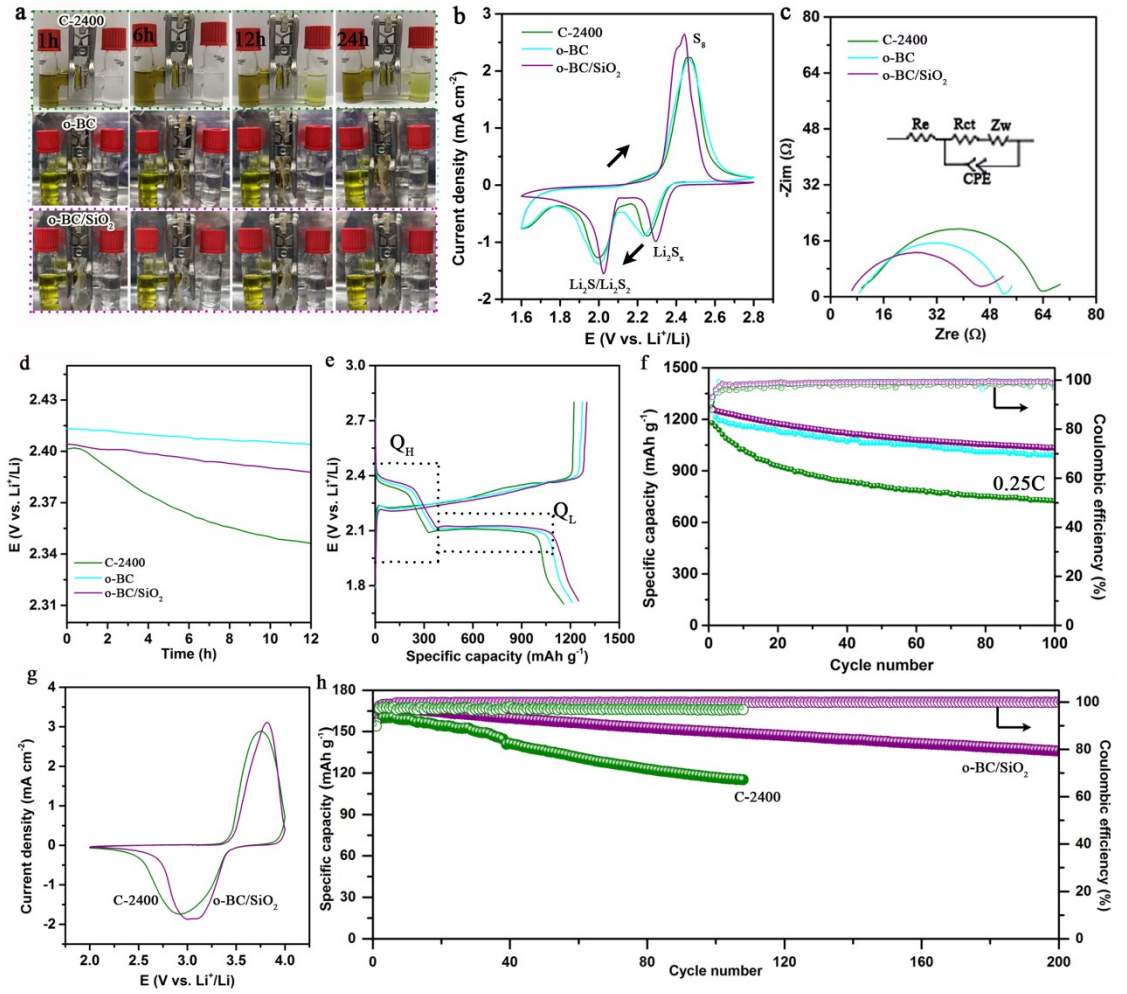
320 To further evaluate the performance of the different separator films, we fabricated and
321 tested asymmetric cells, which are comprised of a Li foil as the negative electrode, a
322 copper foil as the positive electrode, and the C-2400 or the o-BC based film as the
323 separators. For these tests, the charging cutoff voltage was set to 0.1 V. As shown in
324 Figure 3a, with the fixed capacity of 2 mAh cm^{-2} , the C-2400 cell can only survive for a
325 few cycles under a relatively low current density of 1.0 mA cm^{-2} . It is noted that although
326 the cutoff voltage was set at 0.1 V during the lithium stripping process, the voltage can
327 still jump over this limitation due to the suddenly increased large overpotential at the end
328 of the step with no capacity recorded.

329 The cell with the o-BC separator exhibits a much longer lifetime, failing after $\sim 130 \text{ h}$
330 at a current density of 2 mA cm^{-2} . Overall, the o-BC/SiO₂ separators offer the best
331 performance, as it is stable over 180 h of cycling. The voltage profiles at different
332 capacities of the three cells are compared in Figure 3b. Cells with o-BC and o-BC/SiO₂
333 separators have similar polarization potential ($\sim 24 \text{ mV}$), significantly lower than the C-
334 2400 cell ($\sim 50 \text{ mV}$). During cycling, the o-BC/SiO₂ based cell maintained its stability
335 (Figure 3c), and Coulombic efficiency of around 98.5% was achieved (Figure 3d).

336 **LSB and LMB performance**

337 In addition to addressing the above Li anode issues, for Li-S batteries, shuttling of
338 lithium polysulfides in Li-S batteries must also be inhibited to prevent low Coulombic
339 efficiency and short battery lifetime (Li et al., 2020a; Li et al., 2015). The separator used
340 in LSBs could help attack this problem by curbing the diffusion of polysulfides. With this
341 in mind, the o-BC and o-BC/SiO₂ films were subjected to the polysulfides diffusion
342 experiment, and the results are summarized in Figure 4a. All the films are shown to have
343 the ability to block polysulfide migration at the beginning. However, polysulfides
344 diffusion across the C-2400 film became apparent after 6 h, resulting in a color change in
345 the left compartment. In contrast, o-BC and o-BC/SiO₂ films can successfully curb the
346 polysulfide diffusion over 24 h of testing, a result of the strong interaction between the
347 polysulfides and SiO₂/oxygen functional groups. Without similar active binding sites on

C-2400, it can only physically block polysulfide diffusion for a short time.



349

Figure 4. (a) Polysulfide diffusion results using different separators. The two compartments are isolated by the separator, with the left side being 20 mM Li₂S₆ electrolyte and the right side being a blank electrolyte). (b) CV curves recorded at 0.1 mV s⁻¹, (c) EIS Nyquist plots, and (d) open-circuit voltage (OCV) of LSB cell with different separators. (e) Voltage profiles and (f) cycling performance of different separator-based LSBs at 0.25C. (g) CV curves and (h) cycling performance of Li//LiFePO₄ cells with C-2400 and o-BC/SiO₂ separators.

356

The coin-type LSB cells with the different separators were evaluated by CV and EIS techniques. As presented in Figure 4b, all cells show three peaks located at ~2.30, 2.05, and 2.45 V originating from the conversion of S₈ to Li₂S_x (x ≥ 4), Li₂S_x to Li₂S/Li₂S₂, and Li₂S/Li₂S₂ to L₂S_x, respectively (Guo et al., 2013). The peak currents and potential differences between the redox peaks can be used to compare the related reaction kinetics. The o-BC/SiO₂ based LSB has the highest peak currents and smallest peak potential differences among the three cells, indicating that the o-BC/SiO₂ separator has the attractive capability to boost the redox reactions of polysulfides.

364

365 The charge transfer resistance (R_{ct}) can be derived by fitting the Nyquist plots using
366 the equivalent circuit presented in Figure 4c. Again, the cell with o-BC/SiO₂ separator has
367 the lowest R_{ct} of $\sim 39 \Omega$, while around 55 and 44 Ω for C-2400 and o-BC based cells,
368 respectively. These fitting results can also help to explain why the oBC/SiO₂ based LSB
369 shows higher peak current and smaller polarization (peak current voltage difference) in
370 comparison with oBC and C-2400-based cells.

371 If the shuttling process of polysulfides is not suppressed, self-discharging can become
372 prevalent in the LSBs. After the first charging process, the open-circuit voltage (OCV) of
373 cells with different separators was monitored for 12 h, and the results are summarized in
374 Figure 4d. Due to the small uncontrollable differences between the freshly fabricated cells,
375 the initial cell voltage varies (even using the same materials) and is not suitable to be used
376 for comparing the quality of different separators. But the change of OCV along time can
377 be employed as an indicator to study the stability (such as self-discharging) of the cells.
378 The C-2400 cell experiences a relatively fast voltage drop from 2.41 to 2.35 V. In contrast,
379 both o-BC and o-BC/SiO₂ based cells exhibit very stable OCV, suggesting the self-
380 discharging, or polysulfides shuttling, has been effectively suppressed by the o-BC and o-
381 BC/SiO₂ separators.

382 LSB cells with a large sulfur loading of 4 mg cm⁻² were assembled to verify the
383 function of BC-derived separators in improving battery performance. A carbonized BC
384 nanofiber film loaded with sulfur was used for the cathode because it offers highly
385 conductive networks and abundant surfaces for sulfur/polysulfides to attach (Li et al.,
386 2017a; Li et al., 2017b). These cells were cycled at 0.25C for 100 cycles. As illustrated in
387 Figures 4e and 4f, the cell using an o-BC/SiO₂ separator delivers a larger capacity during
388 discharge, with both higher Q_H that corresponds to the discharge capacity for S₈ to Li₂S_x
389 conversion and Q_L that corresponds to Li₂S_x to Li₂S/Li₂S₂ conversion, than the o-BC-
390 based and the C-2400-based cells. The trend of discharge capacity variation of the three
391 cells is consistent with our expectations based on the CV results. During cycling, the C-
392 2400 cell shows a faster specific capacity decay than the other two and maintains a

capacity of $\sim 740 \text{ mAh g}^{-1}$ up to the 100th cycle. Comparatively, the cell with o-BC or o-BC/SiO₂ can still deliver $\sim 1000 \text{ mAh g}^{-1}$ of capacity up to the 100th cycle ($\sim 985 \text{ mAh g}^{-1}$ for the o-BC cell and $\sim 1033 \text{ mAh g}^{-1}$ for the o-BC/SiO₂ cell). In addition, the o-BC/SiO₂ cell also exhibits higher Coulombic efficiency ($> 99\%$) than its counterparts.

Li//LiFePO₄ cells with C-2400 and o-BC/SiO₂ separators were also assembled and tested. Figure 4f presents the CV curves recorded between 2.0 and 4.0 V at a scan rate of 0.1 mV s^{-1} . The redox peak currents and peak potential differences of the o-BC/SiO₂ based cell are also superior to those of the C-2400 based cell. When both cells are cycled at 0.2C, the one with the C-2400 separator suffers from quicker capacity decay and lower coulombic efficiency. These results are consistent with the previously reported unmodified LiFePO₄-based cells with Celgard separators (Chang et al., 2008; Deng et al., 2022). Although the o-BC/SiO₂ cell also shows a specific capacity decrease during cycling, it only slowly decreases from the initial value of 165 mAh g^{-1} after 200 cycles, again demonstrating the capability of the o-BC/SiO₂ separator in improving the battery performance. The improved performance is attributed to the capability of SiO₂ functionalized BC to regulate the Li⁺ flux to the anode during the Li deposition. A uniform Li deposition on the anode can lower the overpotential and suppress the battery degradation caused by the dead lithium and lithium dendrites.

Conclusions

The main goal of the work reported here is to engineer separators so that lithium metal anodes can be used to make practical LMBs for wide spread use. Electrochemical studies show that the composite o-BC/SiO₂ separator that we developed can (1) generate a smooth Li⁺ flux, (2) regulate the Li deposition, and (3) curb the polysulfide shuttling process as a result of the strong interaction between oxygen functional groups on oxidized BC and SiO₂ with Li⁺ and polysulfides. When such a composite film was used as the separator in lithium plating and stripping, much better stability, lower polarization voltage, and higher Coulombic efficiency were achieved than conventional separators. Benefiting

421 from the oxidation process implemented on pristine BC, the introduced carboxylate
422 groups can effectively modify the SiO₂ growth process resulting in a uniform coating on
423 BC. We expected using similar methods, other nonmetal or metal oxides/sulfides
424 materials can also be introduced uniformly onto the BC fibers, which may lead to better
425 structure and composition for the separator used in LMB or other batteries.

426 **Ethics approval and consent to participate**

427 Not applicable.

428 **Consent for publication**

429 Not applicable.

430 **Availability of data and materials**

431 Not applicable.

432 **Competing interests**

433 The authors declare the following financial interests/personal relationships which may be
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438 **Authors' contributions**

439 Wen Yue Li: Conceptualization, Methodology, Investigation, Writing. Shu Wang: Conceptual,
440 Resources, Writing. Zhaoyang Fan: Conceptualization, Methodology, Writing, Supervision. Shiqi Li:
441 Resources. Nathan Newman: Resources, Writing.

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