

# Development of microbeads from unmodified biomass with tunable size and competitive mechanical properties

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## Abstract

Despite national and international regulations, plastic microbeads are still widely used in personal care and consumer products (PCCPs) as exfoliants and rheological modifiers, causing significant microplastic pollution following use. As a sustainable alternative, microbeads were produced by extrusion of biomass solutions and precipitation into anti-solvent. Despite using novel blends of biodegradable, non-derivatized biomass including cellulose and Kraft lignin, resulting microbeads are within the shape, size, and stiffness range of commercial plastic microbeads, even without crosslinking. Solution processability and resulting bead shape and Young's modulus can be tuned *via* biomass source, concentration, and degree of polymerization; biomass concentration, extrusion geometry, and precipitation and extraction conditions control the bead size. Lignin incorporation reduces the solution viscosity, which improves processability but also produces flatter beads with higher moduli than cellulose-only microbeads. While some lignin leaches from the beads when stored in water, adding surfactants like sodium dodecyl sulfate suppresses this effect, resulting in good mechanical stability over two months with no noticeable structural degradation. The stability of these mixed-source biomass

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047 microbeads - despite the absence of chemical crosslinking or derivatization -  
 048 makes this route a promising, robust approach for obtaining environmentally-  
 049 benign microbeads of tunable size and stiffness for use in PCCPs.

050 **Keywords:** lignin, cellulose, biomass, microbeads, biodegradable, mechanical testing  
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052 **1 Introduction**  
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054 Plastic microbeads, typically composed of non-degradable synthetic polymers like  
 055 polyethylene and polypropylene, are used as exfoliants and rheological modifiers in  
 056 personal care and consumer products (PCCPs) to improve viscosity, bulking, film  
 057 formation, and abrasion (Leslie, 2014). The quantity of microbeads in PCCPs can  
 058 be substantial; exfoliating shower gels can contain as much microbead plastic as  
 059 their packaging (Programme, 2020). Yet unlike the plastic used to package these  
 060 products, microbeads cannot be readily collected for recycling as they directly enter  
 061 the water waste stream upon use. While 95-99.9% of microbeads are captured *via*  
 062 sedimentation during wastewater treatment (Rochman et al, 2015), an estimated 8  
 063 billion beads per day enter US aquatic habitats, where they enter the food chain and  
 064 detrimentally impact aquatic life (Rochman et al, 2015; Parker et al, 2021; Hart and  
 065 Arlinghaus, 2021).

066 While fourteen countries have some form of microbead regulations (Xanthos  
 067 and Walker, 2017), the United States (US) legislation on plastic microbeads which  
 068 became effective in 2017 is narrow. In applications outside “personal care” and  
 069 “rinse-off” products categories, including cosmetics, deodorants, and lotions, plastic  
 070 microbeads are not regulated (Usman et al, 2022; Rochman et al, 2015; McDevitt  
 071 et al, 2017). In applications where they are not banned, the cosmetic industry  
 072 continues to employ these microbeads due to their well-defined sizes and shapes,  
 073 which allow for reliable tuning of flow and abrasive properties as well as facilitating  
 074 the delivery of active ingredients (Leslie, 2014). While natural scrubs incorporating  
 075 ingredients like nut shells (Habib et al, 2020), seeds, or mineral abrasives like  
 076 pumice (Piotrowska et al, 2020) may provide the exfoliating characteristics of plastic  
 077 microbeads (Nadiratuzzahra and Tristantini, 2020), the rheological properties can  
 078 not easily be tuned with these ingredients. Biocompatible microbeads sourced from  
 079 synthetic polymers are also challenging for PCCP applications. For example, poly-  
 080 mers used in drug delivery like poly(D,L-lactide-co-glycolide) (PLGA) degrade too  
 081 rapidly to be considered in PCCP applications (Mi et al, 2002), and polymers such  
 082 as polylactic acid (PLA) are unsuitable, as they degrade incompletely in ambient  
 083 conditions (Rochman et al, 2015; Nam and Park, 2020; Programme, 2020).

084 Biocompatible and biodegradable microbeads sourced from biomass can pro-  
 085 vide a sustainable alternative to plastic microbeads currently sourced from synthetic  
 086 polymers. Microbeads from biomass like cellulose and lignin, which is typically  
 087 burned or used in low-value products (Graglia et al, 2015), have been previously  
 088 used for pollutant capture and environmental remediation (Sameni et al, 2018; Beisl  
 089 et al, 2017; Ge et al, 2016; Mohammed et al, 2018; Omo-Okoro et al, 2018). As  
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the majority of plastic microbeads in PCCPs are captured during wastewater treatment, these bio-based alternatives may have additional utility after consumer use due to their adsorption and water purification capabilities. Biomass-sourced microbeads are also capable of being produced using industrial equipment (Sameni et al, 2018), and biomass nanoparticles are currently being explored for drug delivery, adhesives, and crop additives (Sameni et al, 2018; Beisl et al, 2017; Mohammed et al, 2018). Unfortunately while synthesis of biomass nanospheres is extremely common, these widely-used processes are limited to producing particles with diameters from nanometers to tens of microns (Beisl et al, 2017; Zhao et al, 2016; Sameni et al, 2018).

Although microbeads are commonly defined as particles ranging in diameter from 0.1 to 5 mm (Canada, 2015; Moore, 2008; Leslie, 2014), particles in commercial PCCPs are anywhere from tens of microns in diameter to over a millimeter (Coombs OBrien et al, 2017; Cheung and Fok, 2017; Fendall and Sewell, 2009; Habib et al, 2020; Napper et al, 2015; Ziajahromi et al, 2017). However, wastewater treatment plants typically use screens and settling tanks to remove microparticles, meaning that particles smaller than  $\sim 200\ \mu\text{m}$  may be more likely to escape into the environment (Habib et al, 2020; Ziajahromi et al, 2017; Carr et al, 2016). Beyond this limit, the ideal size of microbeads depends on their intended application - whereas microbeads in toothpaste are usually less than  $400\ \mu\text{m}$  (Carr et al, 2016), many microbeads found in skin cleaning products like facial and body scrubs are larger, from 450 to  $800\ \mu\text{m}$  (Shareef and Shareef, 2021; Gouin et al, 2015; Duis and Coors, 2016). Larger beads are generally more powerful exfoliants (Shareef and Shareef, 2021), whereas smaller beads may be more suited as rheological modifiers due to the increased colloidal interactions between beads (Macosko, 1994). Consequently, while larger or smaller microbeads could be used as filler particles or as more powerful exfoliants respectively, a reasonable target range for sustainable microbeads in consumer products would be anywhere from 200 to  $800\ \mu\text{m}$  in diameter, large enough to be captured in wastewater treatment, and small enough to be used in different personal care consumer products.

As most current processes for synthesizing biomass microbeads produce particles too small for the desired PCCP applications (Beisl et al, 2017; Zhao et al, 2016; Sameni et al, 2018), limited sustainable alternatives to plastic microbeads on the desired size scale relevant to the PCCP industry currently exist (Coombs OBrien et al, 2017; King et al, 2017; Nam and Park, 2020; Volant et al, 2021). Current sustainable alternatives to plastic microbeads utilizing only biomass employ single sources of biomass like cellulose (Coombs OBrien et al, 2017; Xia et al, 2022) and chitin (King et al, 2017; Ju et al, 2021). However, King et al. (King et al, 2017) found that chitin microbeads only formed when the chitin feedstock was extracted from crustaceans, an expensive source that is also a common allergen (Alvarez, 2014); commercial chitin was unsuccessful. Other model systems employed covalent crosslinking to stabilize the microbeads or utilized derivatized biomass (Coombs OBrien et al, 2017; Bai and Li, 2006; Ge et al, 2016; Zhang et al, 2020). Crosslinking and derivatization can both negatively impact enzymatic degradation of microbeads, and certain types of derivatization also result in harmful degradation products (Hamdi and Ponchel, 1999; 137

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139 Bhattacharjee and Perlin, 1971; Puls et al, 2011; SAPEA, 2019). For instance, Ge et  
140 al. (Ge et al, 2016) produced lignin microspheres in the appropriate size range but  
141 used only 20% lignin by weight, with the remainder comprised of polyethyleneimine  
142 crosslinked with epichlorohydrin. Other systems are not characterized with respect  
143 to mechanical stability (King et al, 2017; Ju et al, 2021; Xia et al, 2022) or require  
144 highly specific conditions for cellulose dissolution that limit the window for industrial  
145 processing (Luo and Zhang, 2010; Luo et al, 2015; Trygg et al, 2013).

146 Here, we address these challenges by synthesizing a range of microbeads from  
147 nonderivatized biomass using low-temperature protocols with low volatility solvents  
148 that can be recovered and recycled. Expanding on previous work by Coombs O'Brien  
149 et al. (Coombs O'Brien et al, 2017) which employs a single biomass source and  
150 introduces covalent crosslinking, we utilize this low-energy and versatile synthetic  
151 approach to produce and characterize numerous microbead formulations that are  
152 mechanically tough without covalent stabilization, investigating the role of lignin  
153 incorporation and processing parameters on the resulting properties. *Via* image anal-  
154 ysis, scanning electron microscopy (SEM), and single-particle compression testing,  
155 we quantify the impact of biomass concentration and composition, cellulose molec-  
156 ular weight, precipitation and extraction solvents, and extrusion geometry on the  
157 microbead size, swelling behavior, shape, and stiffness. This straightforward method  
158 for producing biomass microbeads is a tunable and robust approach for controlling  
159 dimensions and stiffnesses of these beads for use in a range of consumer product  
160 applications.

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## 2 Materials and methods

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### 2.1 Materials

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166 Avicel PH-101 (degree of polymerization (DP)=230) and MCC 102 (DP=290) cel-  
167 lulose powders (Sigma-Aldrich) and Kraft dealkaline lignin (TCI Chemical) were  
168 used as-received. Ionic liquid (1-ethyl-3-methyl-imidazolium acetate, EMImAc) was  
169 purchased from Astatech (95%). Dimethyl sulfoxide (DMSO) was purchased from  
170 Oakwood Chemical (ACS-grade). Solvents include acetone (ACS-grade, Fisher),  
171 ethanol (100% vol., Pharmco-Aaper), distilled water (HPLC grade, Fisher), and 0.1  
172 M hydrochloric acid (HCl) diluted from concentrated ACS-grade (Macron).

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### 2.2 Biomass solution preparation

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176 Celluloses (DP=290 and DP=230) were dissolved at 8% wt in 70:30 by vol-  
177 ume dimethylsulfoxide (DMSO):1-ethyl-3-methylimidazolium acetate (EMImAc)  
178 adapted from Coombs O'Brien and coworkers (Coombs O'Brien et al, 2017). Cellu-  
179 lose was also dissolved at 7.2 % wt (DP=290), 7% wt (DP=230), 6% wt (DP=230),  
180 and 4% wt (DP=230) in the 70:30 DMSO:EMImAc solvent. Cellulose with different  
181 DP<sub>s</sub> were kept separate. Lignin-cellulose solutions were prepared with 8% wt overall  
182 biomass and fractions of lignin (*f*<sub>lignin</sub>) of 0.33 (2.7 % wt lignin / 5.3 % wt cellu-  
183 lose) and 0.5 (4 % wt lignin / 4% wt cellulose). Solutions were prepared by adding  
184 weighed biomass compositions to the 70:30 DMSO:EMImAc solvent and stirring at

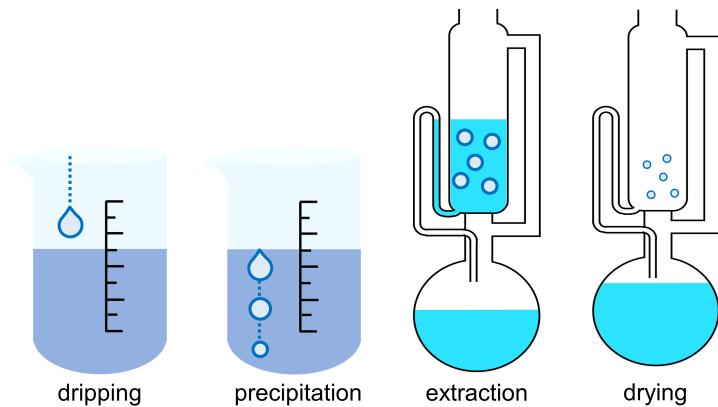
40 °C for a minimum of 16 h until all biomass visibly dissolved. Solutions were kept at room temperature until used for microbead preparation. 185  
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## 2.3 Extensional rheology *via* capillary-driven thinning 188

Capillary-driven thinning extensional rheology measurements were performed using the dripping-onto-substrate (DoS) method as described by Dinic and coworkers (Dinic et al., 2015), using an environmental control chamber as described by Robertson and Calabrese (Robertson and Calabrese, 2022). The primary purpose of this environmental control chamber was to limit water uptake by the hygroscopic ionic liquid solutions during microbead synthesis. Pendant drops of several solutions (8% wt DP290 cellulose, 8% wt DP230 cellulose, and 4% wt DP230 cellulose/4% wt Kraft lignin all in 70:30 DMSO:EMImAc) were brought into contact with glass substrates to form a semi-stable liquid bridge. High-speed videos of the thinning liquid bridges were recorded to determine the minimum radius  $R$  over time, using image analysis as described in our prior work (Lauser et al., 2021; Robertson and Calabrese, 2022; Zhang and Calabrese, 2022). Prior to contact with the substrate, the surface tension  $\sigma$  of each solution was measured *via* an ImageJ plugin (Daerr and Mogne, 2016), and subsequently used to determine apparent extensional viscosities  $\eta_E$ , where  $\eta_E = \frac{\sigma}{2dR(t)/dt}$ . Radial decay profiles were used to determine the Hencky strain,  $\varepsilon_H$ , where  $\varepsilon_H = -\ln(R/R_0)$ ; here,  $R_0$  is the initial radius, defined as 80% of the radius of the nozzle extruding the drop. Radial decay profiles and extensional viscosity as a function of  $\varepsilon_H$  are shown in SI.3. 189  
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## 2.4 Microbead synthesis & purification 209

Large batches of beads were synthesized *via* a dripping method adapted from Coombs-O'Brien and coworkers (Coombs O'Brien et al., 2017) using a syringe pump and subsequently purified *via* Soxhlet extraction (Fig. 1). Biomass solutions were loaded into syringes with variable nozzle size (30g, 26g, 22g), positioned to be normal to and 7 cm above the surface of the precipitation solvent at which was kept at room temperature ( $22 \pm 1$  °C) and ~30% humidity. For all trials except those examining nozzle size (Sec. 3.4), the widest 22g nozzle was used to provide optimal processing conditions. Every ~15 min of dripping, the nozzle was wiped to reduce accumulation of biomass solution on the outside of the nozzle, which could lead to larger drops and larger beads if proceeding unhindered (see Fig. S3). Following precipitation, ionic liquid remaining in the microbead was removed *via* Soxhlet extraction overnight (~12 hours) with 200 mL of the extraction solvent. After extracting using ethanol or water for extraction solvents, microbeads were removed and allowed to air dry overnight (~12 hours). ‘Deswelling,’ or shrinking of the bead, was visible after extraction due to drying of the solvent. Here, extracted and dried beads were as small as ~40% of the size of the precipitated drops for cellulose beads extracted in ethanol; the degree of deswelling was much lower for beads extracted in water. (SI.2). 210  
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**Fig. 1** Schematic of biomass microbead preparation and purification procedure. Biomass solutions were extruded through a nozzle to produce a liquid droplet, which precipitated upon contact with precipitation solvent. Beads were purified *via* Soxhlet extraction to remove residual solvent.

## 2.5 Precipitation and extraction screen

Precipitation and extraction conditions for the dripping synthesis were determined based on a solvent screen, using the precipitation solvents ethanol, acetone, water, 1:1 ethanol:water (vol.), and 0.1 M HCl. Biomass solutions (8% cellulose, 7.2% celulose, 2.7 % wt lignin / 5.3 % wt cellulose, and 4 % wt lignin / 4% wt cellulose.) were extruded from a 22g nozzle into these precipitation solvents to produce  $n = 5$  beads (with the exception of acetone, for which  $n = 1$ , and water and ethanol, for which  $n = 10$ ) and to assess differences in size and shape of the beads. Beads precipitated in ethanol and water were each extracted in both ethanol and water, and all other beads were extracted only in ethanol.

## 2.6 Microbead size quantification

Small batches of beads produced for solvent screen experiments were sized by imaging *via* a Chronos 1.4 high-speed camera with a 10x objective lens and pixel resolution of 1280 by 1024 - each bead was photographed separately. Large batches of beads were placed on white paper and photographed together from above *via* a Samsung Galaxy S9+ phone camera with pixel resolution of 4032 by 3024, with a reference of known size included in each image for calibration. In both cases, images were then analyzed using ImageJ to determine bead sizes, either by manually using the ellipse tool or using a color threshold depending on the quality and contrast of the image. Average diameters  $D_{bead}$  were determined based on the area of each ellipse as  $D_{bead} = \sqrt{4A/\pi}$ , and sphericities were determined based on the ratio of major to minor axes. Many beads ( $n \geq 100$  for larger samples,  $n = 5$  for smaller samples) were sized to produce a reliable estimate of variance based on sample standard deviation. Swelling ratio was determined as  $SR = \frac{D_{wet}}{D_{bead}}$  based on the average size of the extracted and dried beads after being re-swollen in water or SDS solution ( $D_{wet}$ ) and the average size of the same beads once dried again ( $D_{bead}$ ). The average bead size prior to extraction and drying ( $D_{precip}$ ) varied from  $D_{bead}$  to  $3D_{bead}$  depending on

precipitation and extraction solvents; this decrease in size after extraction and drying was attributed to removal of residual ionic liquid and collapse of the bead pore structure upon evaporation of the extraction solvent (SI.8). 277  
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## 2.7 Scanning electron microscopy (SEM)

Images of microbead surfaces were obtained using a scanning electron microscope (JEOL JSM-6010PLUS/LA). Microbeads were affixed to an adhesive carbon tape without sputter coating. SEM observations were carried out with secondary electron detector at an acceleration voltage of 2 kV to avoid charging effects, with magnifications from 50x to 1000x. Energy-dispersive x-ray spectroscopy (EDS) was performed at an acceleration voltage of 5 kV to ensure sufficient signal (at least 20000 counts per second) for elemental analysis. To determine the microbead internal structure, a microbead was flash-frozen in liquid nitrogen and sectioned with a scalpel. 281  
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## 2.8 Mechanical compression testing

Mechanical single-particle compression testing (Instron, 10kN load cell, see SI.1) was performed by compressing the microbeads at a rate of 0.1 mm per minute. Diameters of individual beads  $D_{bead}$  were measured by caliper and confirmed by image analysis prior to compression. The beads were placed on a steel bar which was then placed in between the parallel plates for compression testing. The top plate was lowered within 1 mm of the bead by eye, and bead height  $H$  was determined based on the initial gap height (measured by caliper) and the point of contact (as determined by the measured force). Novel bead formulations were tested until fracture or failure (Fig. S10). 293  
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To determine Young's modulus, curves of force ( $F$ ) vs. distance compressed ( $x$ ) were fit to a Hertzian contact model for the compression of a spheroid between parallel plates (E. Prussia et al, 2006; Rodriguez et al, 1990; Liu et al, 1998; Gao et al, 2021; Portnikov and Kalman, 2014) using Equation 1 where  $R_C$  is the bead contact radius (see SI.4) and  $E'$  is the apparent Young's modulus:

$$F = \frac{4E' \sqrt{R_C}}{3} x^{3/2} \quad (1)$$

The apparent Young's modulus  $E'$  is related to the real Young's modulus of the bead ( $E$ ) and plates ( $E_{plate}$ ) via Equation 2:

$$\frac{1}{E'} = \frac{1 - \nu^2}{E} + \frac{1 - \nu_{plate}^2}{E_{plate}} \quad (2)$$

where  $\nu$  and  $\nu_{plate}$  are the Poisson ratios of the bead and plates respectively. For  $E \ll E_{plate}$ , which is true given the high modulus of the steel plates, and small  $\nu$  ( $\nu \sim 0.2$  for measured beads),  $E \approx E'$ .

The fitting region for the Hertzian contact regime was determined by binning each trial and fitting to Equation 1 within each bin. The linear regime was determined to consist of consecutive bins in which the value of  $E$  was statistically equal and did not trend in time. This criterion corresponded visually with the onset of the linear region

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323 of the stress/strain curve indicating complete contact as well as the downturn indicating  
 324 a plastic response of the material (Portnikov and Kalman, 2014). This fitting  
 325 region was then fit to Equation 1 to extract a single value of  $E$ . Uncertainties from  
 326 each fit were negligible in comparison to the variation between trials, so uncertainties  
 327 for average values of  $E$  for each sample were calculated as the standard deviation  
 328 of the fit values for each trial. Statistical significances of differences between mod-  
 329 ules were determined *via* a two-sample, one-tailed Student's  $t$ -tests (assuming unequal  
 330 variances).

331 Due to the effect of contact radius  $R_C$  and bead shape in determining  $E$  (SI.4),  
 332 compressive strain ( $\varepsilon = x/H$ ) was plotted vs. force for representative trials following  
 333 precedent (Coombs O'Brien et al, 2017). Force was shown instead of an engineering  
 334 stress for ease of comparison between beads with different initial areas and shapes,  
 335 and for more direct assessment of durability under consumer use.

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## 337 2.9 Stability of microbeads in model systems

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339 Fifty extracted and dried microbeads each with lignin fractions  $f_{lignin}$  of 0, 0.33,  
 340 and 0.5 were re-suspended in water and 25% wt sodium dodecyl sulfate (SDS) in  
 341 water, for a total of six conditions. Five beads were removed from solution at weekly  
 342 intervals and dried for 16 hours in a vacuum oven at room temperature, before under-  
 343 going mechanical compression tests to assess stability over time. Swelling ratios  
 344  $SR = \frac{D_{wet}}{D_{dried}}$  were determined based on imaging wet beads immediately after removal  
 345 from solution and imaging dried beads prior to compression.

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## 347 2.10 Statistical analysis

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349 All error bars when shown indicate sample standard deviations for at least  $n = 5$   
 350 trials. Statistical significance was determined *via* a two-sample, one-tailed Student's  
 351  $t$ -tests (assuming unequal variances), with p-values less than 0.1 considered poten-  
 352 tially significant (\*), values less than 0.05 considered significant (\*\*), and values less  
 353 than 0.02 considered very significant (\*\*\*)�

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## 355 3 Results

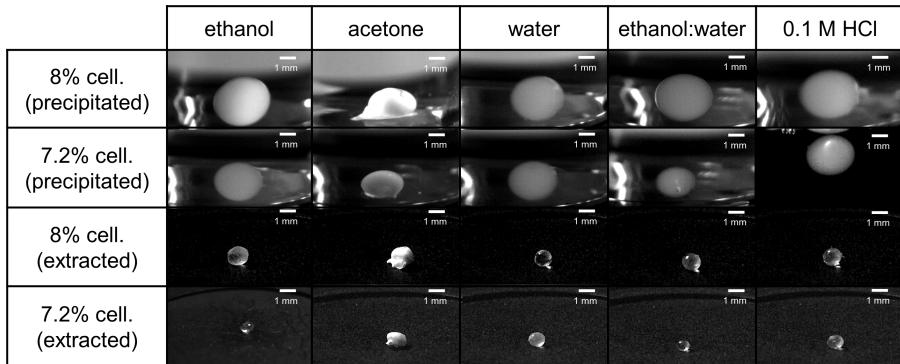
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### 357 3.1 Optimizing microbead precipitation conditions

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359 Precipitation and extraction conditions for the dripping synthesis were determined  
 360 based on a solvent screen performed on two biomass concentration (8% and 7.2%  
 361 DP290 cellulose), with the initial screening using the precipitation solvents ethanol,  
 362 acetone, water, ethanol:water, and 0.1 M HCl (Fig. 2). Microbeads prepared from  
 363 the same biomass concentration show distinct shapes based on precipitation solvent  
 364 (Table S1). Acetone was eliminated as a potential precipitation solvent, as its sol-  
 365 vent quality for cellulose was too poor to facilitate formation of spherical beads (Fig.  
 366 2, column 2). Here, microbeads precipitated immediately upon contact with the sol-  
 367 vent, creating a flattened non-spherical shape; as such, no additional screening was  
 368 performed with acetone. However, the four other ethanol and water-based precipita-  
 369 tion solvents were effective in precipitating cellulose microbeads slowly to produce

spherical beads (Fig. 2; see Table S1 for quantification of microbead shapes). However, weak HCl was also removed as a candidate precipitation solvent, as microbeads precipitated in this solvent had a higher propensity for floating near the air-solvent interface rather than settling, leading to irregular shapes for some microbeads.



**Fig. 2** Images of microbeads produced by extruding solutions of 8% wt and 7.2% wt DP290 cellulose into the given precipitation solvents. All microbeads were subsequently extracted in ethanol. Microbead diameters for all conditions in the solvent screen are listed in SI.2.

Precipitation of cellulose formulations into ethanol, rather than aqueous solvents, generally resulted in formation of beads with smaller average bead diameters,  $D_{precip}$ , upon solvent contact (Table S1). These smaller diameters, in addition to supplementary electron microscopy (Fig. S11) and elemental analysis (Fig. SI.8), suggest that ethanol is a more efficient solvent for removing residual ionic liquid than water. One possible explanation is that ethanol has a lower affinity for cellulose which causes microbeads to deswell further and expel ionic liquid more effectively (SI.2), consistent with literature on regenerated cellulose films (Tan et al., 2019). Microbeads both precipitated and extracted in water are more likely to retain non-spherical shapes, due to this residual IL and potentially incomplete water removal (Table S1, SI.8). Accordingly, all microbeads were subsequently extracted in ethanol to efficiently remove residual IL and ensure complete drying of the extraction solvent (Fig. 2). For both cellulose formulations across precipitation solvents, the extraction and drying steps resulted in a statistically significant decrease in microbead size, with the final bead diameter,  $D_{bead}$ , around one-half the size of  $D_{precip}$  (Table S1). Conversely, no substantial changes in bead diameter were observed between the precipitation and extraction stages when cellulose microbeads were instead extracted with water, suggesting that these beads retain a more porous microstructure. Additionally, these beads contain residual IL and solvent, confirmed by elemental analysis via energy-dispersive X-ray spectroscopy (EDS, SI.8).

Interestingly, reducing biomass concentration is a route for reducing bead size, but changing precipitation solvent is not. For example, a 10% reduction in cellulose concentration from 8% to 7.2% wt results in a reduction in the final bead diameter of over 20% for microbeads extracted in ethanol during the solvent screen (Table

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415 S1). However, the microbead size following extraction in ethanol and drying is inde-  
 416 pendent of precipitation solvent for both biomass concentrations (Table S1), despite  
 417 initial differences in  $D_{precip}$ . As the decrease in microbead size upon extraction is due  
 418 to removal of residual IL and subsequent drying of ethanol which causes the bead  
 419 to densify, the similarity in  $D_{bead}$  following ethanol extraction suggests that nearly  
 420 all IL is removed, and that all ethanol is dried, regardless of precipitation conditions;  
 421 this evidence is also consistent with elemental analysis *via* EDS (SI.8). Accordingly,  
 422 extraction solvent likely impacts the final microbead size more significantly than  
 423 precipitation solvent.

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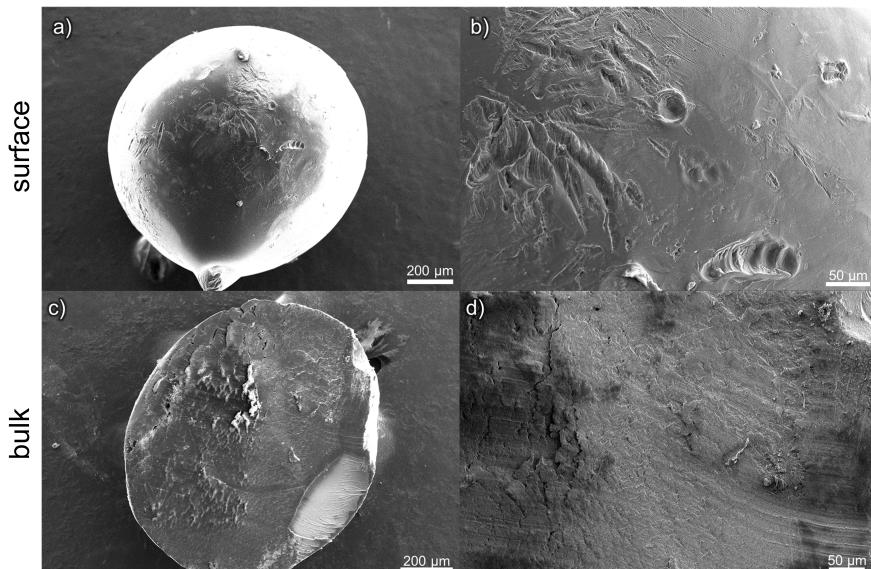
### 425 3.2 Microbead morphology following extraction in ethanol

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427 Scanning electron microscopy (SEM) images of dry microbeads (8% wt DP290 cel-  
 428 lulose) following extraction in ethanol reveal a fairly smooth surface morphology  
 429 (Fig. 3), which is ideal for a use as gentle exfoliants in personal care products (Leslie,  
 430 2014). Based on micrographs of the microbead surfaces and additional micrographs  
 431 of the bead cross-sections (Fig. 3), microbeads precipitated in ethanol appear densely  
 432 packed, with low porosity on the length scales shown in the images (tens to hundreds  
 433 of microns). While minor scratches and dimples are observed on the bead surface and  
 434 in the bulk, no regular pore structure is observed.

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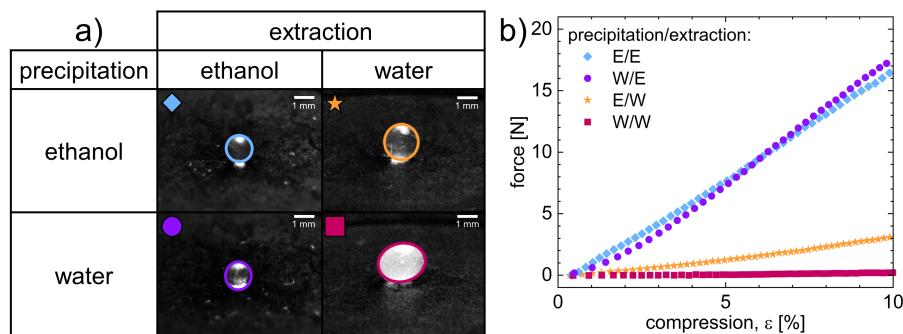
**Fig. 3** Surface (a,b) and internal structure (c,d) of microbeads (8% DP290 cellulose precipitated and extracted in ethanol) at a) 70x b) 270x c) 80x and d) 220x magnifications. No visual evidence of a regular pore structure either on the bead surface or in the bulk is observed; only light dimples on the bead surface and microfractures in the bulk (potentially due to sectioning) are observed.

This observation is supported by swelling ratio values near unity for beads extracted with ethanol, indicating that following extraction in ethanol and drying,

cellulose microbeads re-suspended in water are of similar size to extracted and dry microbeads. However, dye adsorption experiments on these cellulose microbeads re-suspended in water (SI.5) suggest a size exclusion phenomenon on  $\sim 1$  nm length scales, implying a degree of porosity in wet beads on small length scales. These observations for microbeads extracted in ethanol are in contrast to those for microbeads created from the same formulation but precipitated and extracted in water, which had highly porous and fibrous surface morphologies (Fig. S11).

### 3.3 Impact of precipitation and extraction conditions on mechanical properties

Following the initial solvent screen ( $n = 5$ ), a larger number ( $n = 50$ ) of 8% wt DP290 cellulose microbeads precipitated in either ethanol or water were extracted in either ethanol or water, for a total of four unique precipitation and extraction conditions. Representative images and average properties of microbeads resulting from each condition clearly illustrate the impact of precipitation and extraction solvent on bead diameter, de-swelling (SI.2), and circularity (Fig. 4a, Tables 1, SI.2). Consistent with results from the initial solvent screening, microbeads extracted in ethanol have the smallest diameters,  $D_{bead} \sim 1340 \mu\text{m}$ , with no statistically significant difference in diameter based on precipitation solvent (Table 1). When microbeads are instead precipitated in ethanol and extracted in water,  $D_{bead}$  is  $\sim 15\%$  larger. As these beads are free of IL (SI.8), this larger bead size could be due to the presence of residual water or due to the slow-drying water preventing a full collapse of the porous microstructure upon drying. However while beads either precipitated or extracted with ethanol remain spherical and relatively small (Fig. 4a), microbeads precipitated and extracted in water are large, soft, and ellipsoidal in shape, reflecting the more porous microstructure and presence of residual fluid.



**Fig. 4** a) 8% wt DP290 cellulose microbeads with precipitation and extraction solvents of either ethanol or water and b) representative force/compression curves. Beads extracted in ethanol (blue  $\blacklozenge$ , purple  $\bullet$ ,  $E \sim 0.5 \text{ GPa}$ ) were one to two orders of magnitude stiffer than beads extracted in water (orange  $\star$ , red  $\blacksquare$ , Table 1). Beads extracted in ethanol had statistically identical Young's moduli ( $p = 0.24$ ), but moduli of all other beads were significantly different (\*\*\*,  $p < 0.02$ , SI.13).

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507 Subsequent compression tests on microbeads from each of the four precipitation  
 508 and extraction conditions confirmed qualitative visual observations, where the  
 509 Young's moduli of microbeads extracted in water were one to two orders of mag-  
 510 nitude lower than for those extracted in ethanol (Fig. 4b, Table 1). Beyond having  
 511 equal bead diameters, beads extracted in ethanol had statistically identical Young's  
 512 moduli regardless of precipitation solvent ( $E \sim 0.5$  GPa,  $p = 0.24$ , Table 1). Com-  
 513 pression was performed until fracture when possible (Fig. S10); however, microbeads  
 514 extracted in water did not fracture. As such, all force curves are plotted until 10%  
 515 compression for ease of comparison (Fig. 4). Conversely, cellulose beads precipitated  
 516 and extracted in ethanol exhibit a single clean fracture upon break (Fig. S10). The  
 517 microbead upper surface is also noticeably flattened upon break, leading to a visible  
 518 radius of contact, as is used in Eqn. 1.

519

520

Precipitation	Extraction	$E$ [GPa]	$D_{bead}$ [ $\mu$ m]
Ethanol	Water	$0.048 \pm 0.014$	$1544 \pm 128$
Ethanol	Ethanol	$0.479 \pm 0.047$	$1332 \pm 82$
Water	Water	$0.003 \pm 0.001$	$2392 \pm 177$
Water	Ethanol	$0.508 \pm 0.076$	$1345 \pm 70$

521 **Table 1** Diameters and Young's moduli for microbeads (8% wt DP290 cellulose, 22g nozzle) produced  
 522 with water and ethanol as precipitation and extraction solvents.

523

524

525 While microbeads extracted in ethanol are significantly stiffer than beads  
 526 extracted in water regardless of precipitation solvent, beads extracted in water are  
 527 an order of magnitude stiffer when precipitated in ethanol (Fig. 4b, Table 1). The  
 528 stiffer beads extracted in ethanol are also substantially smaller than those extracted  
 529 in water. These results - paired with the identical properties for beads extracted in  
 530 ethanol - suggest that the softness of beads extracted in water is likely due to their  
 531 more porous microstructure (Fig. S11) and retention of ionic liquid or solvent serv-  
 532 ing as a plasticizer (Li et al., 2020; Pang et al., 2013). The identical properties for the  
 533 beads extracted in ethanol suggest that for those microbeads, residual solvent and IL  
 534 has been completely removed and that the porous structure has collapsed, leading to  
 535 a similar degree of de-swelling and thus similar  $E$ . Conversely, the varying size, and  
 536 mechanical properties for beads extracted in water suggest a different degree of IL  
 537 or solvent retention, an explanation supported by EDS measurements of microbead  
 538 composition (S1.8). Thus as the change in microbead size and mechanical properties  
 539 is likely in part due to significant quantities of residual IL, beads precipitated and  
 540 extracted in water are likely unsuitable for most commercial applications.

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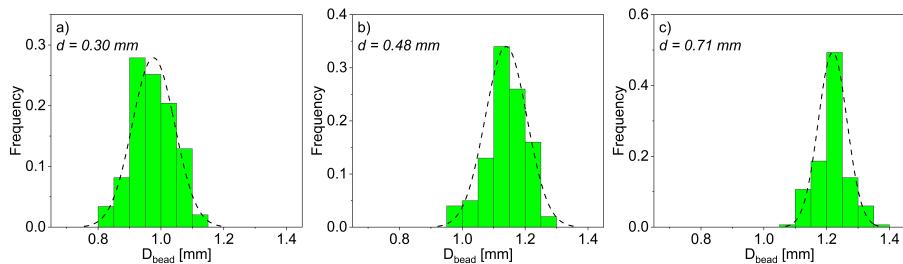
### 543 3.4 Impact of nozzle size on microbead diameter

544

545 While DP290 cellulose formulations produce microbeads with Young's moduli com-  
 546 parable to commercial plastic microbeads (Palombini et al., 2018; Sipe et al., 2022a),  
 547 these microbeads are challenging to produce *via* dripping synthesis due to the cel-  
 548 lulose molecular weight and solution concentration. These properties lead to high  
 549 solution extensional viscosities,  $\eta_E$ , and weakly elastic behavior in extensional flow  
 550 (Fig. S2). As such, these solutions can only be extruded through relatively large  
 551

552

nozzles (Fig. S3), limiting the resulting bead size to millimeter scale diameters. To circumvent these challenges and determine if the bead size could be further reduced by adjusting the nozzle size, 7% wt cellulose solutions were examined using a lower cellulose degree of polymerization (DP230, Table 2). Using DP230 cellulose allows several smaller nozzle gauges (22, 26, 30g) to be employed during bead synthesis, as DP230 cellulose solutions have several-fold lower  $\eta_E$  than DP290 solutions, and do not exhibit strain hardening or weakly elastic flow behavior in capillary-driven thinning extensional rheology measurements (SI.3).



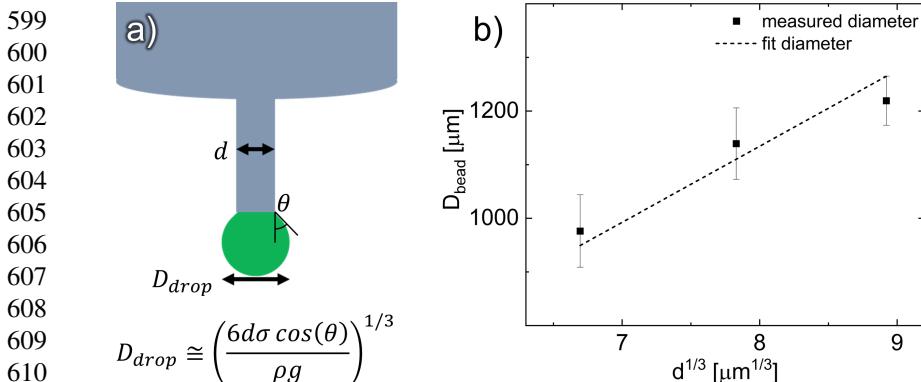
**Fig. 5** Diameter size distribution of microbeads (after extraction and drying) formed from 7% wt DP230 cellulose, extruded through nozzles of diameter a) 30 gauge (0.30 mm) b) 26 gauge (0.48 mm) c) 22 gauge (0.71 mm). Mean values and standard deviations determined by fitting a normal distribution (dashed lines) yield: a)  $1219 \pm 46 \mu\text{m}$  b)  $1139 \pm 67 \mu\text{m}$  and c)  $976 \pm 67 \mu\text{m}$ , with  $n \geq 100$  for all samples.

**Table 2** Diameters for microbeads (7% wt DP230 cellulose, precipitated and extracted in ethanol) produced with 22g, 26g, and 30g nozzles.

Gauge	$d$ [mm]	$D_{\text{bead}}$ [ $\mu\text{m}$ ]
22	0.71	$1219 \pm 46$
26	0.48	$1139 \pm 67$
30	0.30	$976 \pm 67$

Unsurprisingly, smaller nozzles result in smaller bead diameters; however, significantly reducing the nozzle size leads to diminishing returns in terms of reducing  $D_{\text{bead}}$  (Fig. 5, Table 2). For example, the smallest, 30g nozzle has an outer diameter,  $d$ , of 0.30 mm; the dried beads produced from this nozzle have an average  $D_{\text{bead}}$  of 0.98 mm, which is a 3.2x increase from the nozzle size (Fig. 5c). However, beads produced from the largest, 22g nozzle ( $d=0.71$  mm) have an average  $D_{\text{bead}}$  of 1.22 mm, an only 1.7x increase in size (Fig. 5a). Thus here, reducing the nozzle size by more than two-fold results in only a 20% reduction in final bead size (Fig. 6). Regardless of nozzle size, microbeads produced from each nozzle exhibit a fairly normal size distribution, with a minimum of  $D_{\text{bead}} \sim 0.8$  mm and  $D_{\text{bead}} \sim 1.1$  mm for the smallest and largest nozzle, respectively.

Differences between  $D_{\text{bead}}$  and nozzle diameter  $d$  result because  $D_{\text{bead}}$  is determined primarily by the drop size  $D_{\text{drop}}$ , rather than the nozzle diameter (Fig. 6);  $D_{\text{drop}}$  is always substantially larger than  $d$ . While the nozzle diameter influences the drop



**Fig. 6** a) Extruded drop size,  $D_{drop}$ , scales with nozzle size  $d$ , solution surface tension  $\sigma$ , critical angle  $\theta$ , and solution surface tension  $\sigma$  and density  $\rho$ . b) Bead size  $D_{bead}$  also scales with nozzle diameter as  $d^{1/3}$  within experimental uncertainty, suggesting that drop size is the primary determinant of bead size for 7% DP230 cellulose solutions.

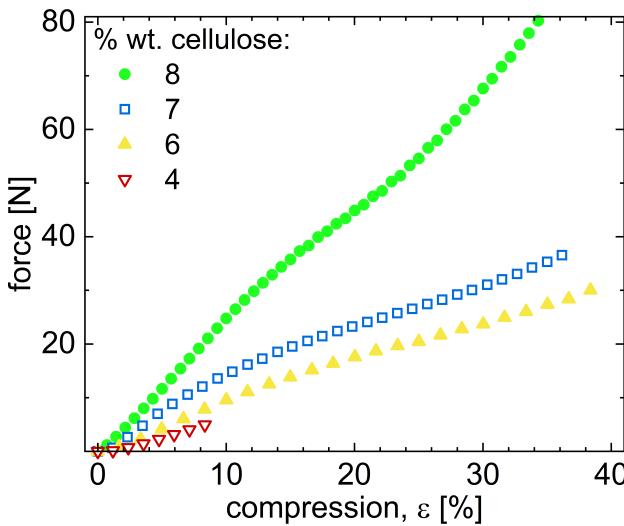
diameter,  $D_{drop}$  is also determined by material properties like surface tension  $\sigma$ , density  $\rho$ , and critical angle at breakup  $\theta$  (Fig. 6). Note that while the drop size is also impacted by the polymer elasticity and extensional relaxation time (Gaillard et al, 2022; Makhnenko et al, 2021), this effect is expected to be small based on the low extrusion flow rate and the absence of strain hardening in DP230 solutions in extensional flow (SI.3). Thus here, drop diameter is expected to scale with nozzle diameter  $d$  as  $D_{drop} \approx \left( \frac{6d\sigma \cos(\theta)}{\rho g} \right)^{1/3}$ , based on a balance of surface tension and gravitational forces at breakup (SI.4). In the resulting microbeads, the scaling  $D_{bead} \propto d^{1/3}$  fits well within the experimental uncertainty (Fig. 6), suggesting that the ratio of bead diameter  $D_{bead}$  to drop diameter  $D_{drop}$  remains nearly constant.

### 3.5 Impact of cellulose concentration on mechanical properties

Given the diminishing returns in reducing bead size by reducing nozzle diameter, reduction of the biomass concentration was pursued next, based on promising solvent screen results showing a significant reduction in  $D_{bead}$  from 8% to 7.2% wt cellulose. Given the poor processability of the DP290 cellulose solutions, here DP230 cellulose solutions were formulated at different concentrations (4% to 8% wt). As higher concentration solutions experience high extensional viscosities upon exiting the nozzle (Fig. S2), lower concentration cellulose solutions may provide a route for improving processability *via* increased flow rate through the nozzle.

Visual observations suggest that dilution of the cellulose suspension results in substantially softer beads upon precipitation, likely due to the lower biomass fraction in each initial drop; these differences in bead stiffness persist following extraction (Fig. 7). Here, lowering the cellulose concentration from 8% (green ●) to 7% wt (blue □), and again from 7% to 6% wt (yellow ▲) results in microbeads with statistically significant reductions in modulus (\*\*\*,  $p < 0.02$ , Fig. 7, Table S12). This reduction in modulus can be seen clearly by the shallower slope in representative force/compression traces with decreasing biomass content (Fig. 7). While the average modulus

of the 4% wt microbeads (red  $\triangledown$ ) is lower than that of the 6% formulations, this difference is not statistically significant (\*,  $p = 0.1$ , SI.13). Notably, microbeads formed from 4% solutions exhibit a high degree of variability in both size and mechanical properties (Table 3), leading to the statistical equivalence between the two lowest biomass content solutions; for all raw data, see SI.11. The lower biomass content, especially in the 4% biomass solutions, causes buckling and wrinkling of the surface during extraction and drying as the bead shrinks due to liquid expulsion and rapid collapse of the porous structure (Fig. S5). As a result, 4% microbeads often assume irregular shapes and have surface heterogeneities that lead to high variability in single particle measurements of moduli.



**Fig. 7** Representative force/compression curves of 8% (green ●), 7% (blue □), 6% (yellow ▲), and 4% (red ▽) wt DP230 cellulose microbeads extracted in ethanol. Bead moduli (Table 3) increased with concentration monotonically, as shown in the force/compression curves. Due to the high variability of the 4% sample, the 4% and 6% samples were statistically similar (\*,  $p = 0.1$ ), but moduli of all other samples were significantly different (\*\*\*,  $p < 0.001$ , SI.13).

The reductions in modulus with decreasing biomass content are accompanied by reductions in average bead size (Table 3). As with the Young's moduli, these reductions in average bead size are statistically significant when the biomass content is lowered from 8% to 7% and again from 7% to 6% (\*\*\*,  $p < 0.001$  between 8% and 7% and 7% and 6%) as beads shrink more upon extraction with lower initial biomass contents. Possible explanations for the differences in mechanical properties between beads from different biomass concentrations are the formation of microscale voids in the lower concentration beads during the process of precipitation (Schmalbach et al., 2021) or differences in entanglement phenomenon. Additionally, upon anti-solvent contact, cellulose at the droplet surface begins to densify in a region near the surface (see supplemental video), which likely impacts the ultimate mechanical properties of the bead. As lower concentration solutions have a lower density of polymer at the

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691 surface and throughout the drop, the thickness and density of the surface region is  
 692 expected to differ, likely changing the bead microstructure, especially in the near-  
 693 surface region, as IL is removed and the bead shrinks.

694

695

Cellulose [% wt]	$E$ [GPa]	$D_{bead}$ [ $\mu\text{m}$ ]
8	$0.605 \pm 0.023$	$1287 \pm 159$
7	$0.564 \pm 0.020$	$1219 \pm 46$
6	$0.443 \pm 0.020$	$1092 \pm 111$
4	$0.349 \pm 0.137$	$1102 \pm 210$

696 **Table 3** Microbead diameter and Young's modulus for formulations using: DP230 cellulose, 22g nozzle,  
 697 and ethanol as the precipitation and extraction solvent.

701

702

703 Interestingly, the microbeads formed here from DP230 cellulose solutions have  
 704 higher Young's moduli than for microbeads formed from the analogous solutions  
 705 prepared with DP290 cellulose, despite the lower molecular weight of the DP230  
 706 cellulose; see [SI.9](#) for direct comparison of mechanical compression tests. As direct  
 707 measurement of molecular weight distributions of cellulose is only possible *via* spe-  
 708 cialized instruments ([Dupont, 2003](#)), the higher moduli in the DP230 microbeads  
 709 could be due to differences in molecular weight distribution or differences in impu-  
 710 rities in the reagent powders. However while the beads are largely amorphous, the  
 711 higher moduli of the DP230 beads are consistent with higher bead crystallinities mea-  
 712 sured by XRD ([SI.9](#)). Another possible explanation is the lower surface tension of  
 713 the DP230 bead solutions vs. that of the DP290 solutions ([Table S9](#)), indicating that  
 714 the smaller DP230 cellulose chains are more active at the ionic liquid droplet surface.  
 715 As cellulose at the droplet surface begins to densify upon anti-solvent contact, the  
 716 density of DP230 cellulose at the surface of the final microbead may be higher than  
 717 that for DP290 cellulose, which could result in the higher moduli but lower strains at  
 718 break observed here ([SI.9](#)).

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### 3.6 Tuning microbead properties *via* lignin incorporation

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722 Following extensive characterization of microbeads prepared from cellulose-only  
 723 solutions, subsequent incorporation of Kraft lignin - a low-value byproduct of the cel-  
 724 lulose extraction process ([Graglia et al, 2015](#)) - into cellulose solutions demonstrates  
 725 the robustness of the bead production method to variable feedstocks. Additionally,  
 726 lignin incorporation provides a potential route for tailoring bead size and stiffness.  
 727 Lignin addition substantially reduces the extensional viscosity of biomass solutions  
 728 likely due to its smaller, highly branched structure ([SI.3](#)), reducing die swelling and  
 729 enabling facile and efficient bead production.

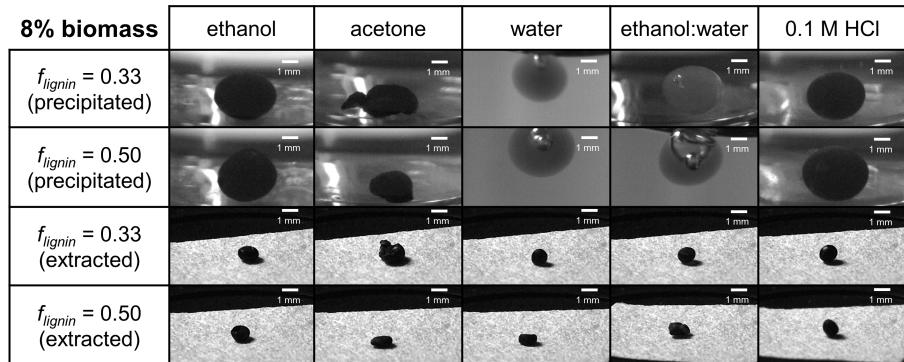
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731

#### 3.6.1 Optimizing precipitation conditions

732 Using the same solvent screen as for pure cellulose microbeads, the optimal precipi-  
 733 tation conditions for biomass formulations with increasing quantities of lignin were  
 734 found to be similar to that of their cellulose-only counterparts. Here, two weight frac-  
 735 tions of lignin ( $f_{lignin}$ ) were substituted into the cellulose to model the properties of  
 736

mixed biomass feedstocks, maintaining an overall biomass concentration of 8% with  $f_{lignin} = 0.33$  (2.7% wt lignin / 5.3% wt cellulose solution) and  $f_{lignin} = 0.5$  (4% wt lignin / 4% wt cellulose). As observed for cellulose-only formulations, the solvent quality of acetone is too poor to facilitate formation of spherical beads (Fig. 8); as such, only one bead was precipitated into acetone.



**Fig. 8** Images of microbeads produced by extruding solutions (overall 8% wt biomass) of given weight fraction lignin ( $f_{lignin}$ ) from a 22g nozzle into the given precipitation solvents and extracting in ethanol. Diameters of all microbeads in the second solvent screen are listed in [SI.2](#).

Resulting microbeads exhibit differences in size and shape depending on the precipitation solvent and solution composition; solvent screen results are detailed in [SI.2](#). Lignin-containing solutions generally produce flatter beads, as is evident in the bottom row of Fig. 8 with  $f_{lignin} = 0.5$ . Increasing lignin content generally increases the deviation in microbead shape from perfect spheres; however, certain precipitation solvents still produce beads with reasonable sphericities (ratio of major/minor axes  $\sim 1.2$ , Table [S1](#)) at 50% lignin content. However, substituting a smaller amount of lignin for cellulose ( $f_{lignin} = 0.33$ ) is a viable route for creating approximately spherical beads for a number of precipitation conditions. Interestingly, while precipitation and extraction in water produces larger microbeads for cellulose-only formulations, lignin-containing microbeads precipitated and extracted in water are substantially smaller than in all other conditions for both lignin fractions (Table [S1](#)).

As opposed to in the solvent screen conducted for pure cellulose compositions, trends in bead size following precipitation and extraction in different solvents for lignin-containing microbeads are more difficult to interpret; these changes in microbead size are complicated by the fact that lignin can diffuse out of the microbead during both processes. For example, discoloration of both the precipitation and extraction solvent occurs for both water and ethanol; however, this effect is substantially more significant in water due to the higher solubility of lignin in water vs. ethanol. Unsurprisingly, lignin-containing beads de-swelled further than their pure cellulose counterparts when extracted in water. Paired with the fact that the smallest beads are produced when precipitation and extraction are in water, lignin leaching likely plays a significant role in determining  $D_{bead}$  when water is used for both steps. However across precipitation solvents (Table [S1](#)),  $D_{precip}$  is significantly smaller for

783  $f_{lignin} = 0.33$  than for pure cellulose ( $p = 0.004$ ) and for  $f_{lignin} = 0.5$  than for  $f_{lignin}$   
 784 = 0.33 ( $p = 0.027$ ). This smaller  $D_{precip}$  may reflect substantial leaching during pre-  
 785 cipitation; however, the lower surface tension for lignin-containing solutions should  
 786 also reduce the initial drop size (Table S9), thus reducing  $D_{precip}$ .

787 Interestingly, precipitating formulations with moderate lignin contents ( $f_{lignin} =$   
 788 0.33) into water-containing solvents followed by extraction in ethanol produces the  
 789 most spherical lignin-containing microbeads (Table S1). These conditions all result in  
 790 similar microbead sizes, sphericities, and de-swelling ratios ( $\frac{D_{bead}}{D_{precip}} = 0.5\text{--}0.6$ ). These  
 791 ratios are substantially smaller than for all other conditions, suggesting that both  
 792 lignin leaching during precipitation in a water-containing solvent and size reduction  
 793 due to extraction in ethanol must occur. The improved sphericity in these microbeads  
 794 may reflect that the microbeads become increasingly cellulose-rich as lignin leaches  
 795 from the bead, leading to enhanced structural reinforcement; conversely, when pre-  
 796 precipitated and extracted in ethanol, more lignin remains in the microbeads, leading  
 797 to flattened morphologies. Interestingly, these flattened morphologies occur regard-  
 798 less of precipitation conditions at higher lignin content ( $f_{lignin} = 0.5$ ), suggesting  
 799 that a critical content of cellulose may be necessary to retain structural integrity  
 800 and a highly spherical morphology. Thus while ethanol was used in all large-scale  
 801 syntheses of lignin-containing beads, these findings suggest that use of water as a  
 802 precipitation or extraction solvent can provide an opportunity for further tuning the  
 803 microbead size, shape, and porosity.

804

### 805 3.6.2 Impact of lignin on mechanical properties

806

807 Following the solvent screen, larger-scale syntheses of lignin-containing microbeads  
 808 revealed that the average bead diameter is significantly smaller for lignin-containing  
 809 microbeads than for those made from pure cellulose (Table 4), though no difference in  
 810  $D_{bead}$  is observed between  $f_{lignin}$  of 0.33 and 0.5. Here,  $D_{bead}$  is reported as a spherical  
 811 average diameter after fitting the microbead cross-sectional areas as ellipses. Notably,  
 812 this diameter does not account for the flattened morphology in the vertical dimension  
 813 for lignin-containing beads; thus the similarity in  $D_{bead}$  for the two lignin-containing  
 814 formulations likely does not reflect the true bead volume, which is likely smaller for  
 815 the highest lignin content microbeads due to lignin leaching.

816

Cellulose [% wt]	Lignin [% wt]	$E$ [GPa]	$D_{bead}$ [ $\mu\text{m}$ ]
8	0	$0.479 \pm 0.047$	$1332 \pm 82$
5.33	2.67	$0.515 \pm 0.036^*$	$1091 \pm 71$
4	4	$0.550 \pm 0.038^*$	$1135 \pm 126$

817 **Table 4** Diameter and Young's moduli for microbeads (8% biomass, DP290 cellulose,  
 818 precipitated/extracted in ethanol) with  $f_{lignin} = 0, 0.33$ , and  $0.5$ . \* indicates  $E$  calculated using an oblate  
 819 spheroid model (SI.4) due to the flatter shape and lower curvature at contact for high  $f_{lignin}$ .

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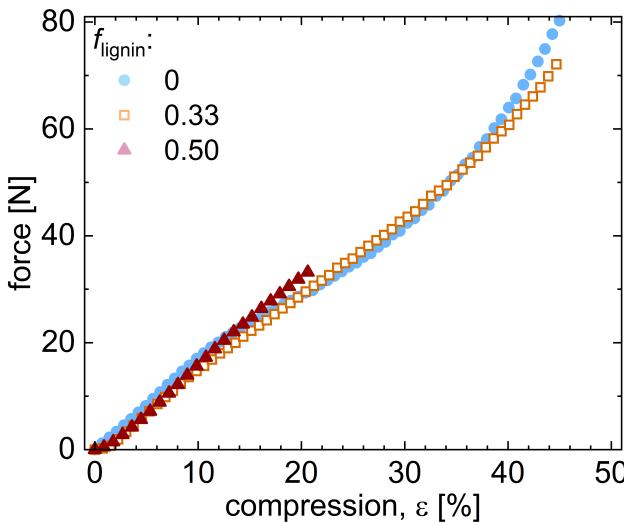
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822

823 Lignin-containing beads are flatter and tend to break at lower strains when com-  
 824 pressed (Fig. 9); however, their Young's moduli are comparable to those of pure  
 825 cellulose microbeads (Table 4), suggesting that these microbeads can be a route to  
 826 valorize this low-value biomass feedstock. In fact, compressing microbeads made  
 827

828

from pure cellulose and those containing up to 50% lignin yields nearly identical force/strain curves up to ~20% compressive strain or around 30 N of normal force (Fig. 9). These data suggest that lignin-containing beads may perform similarly in consumer product applications: while the intensity of scrubbing varies greatly, normal forces applied by the human hand are generally less than 25 N for even strenuous activities (Søgaard et al, 2001), and less than 10 N for gentler activities (Peng et al, 2021; Xu et al, 2019; Xu and Gerling, 2020). Given that the force/strain curves do not account for the smaller cross-sectional area in lignin-containing microbeads, the microbead Young's moduli actually increase with increasing lignin content (Table 4). Differences in  $E$  are statistically significant (\*\*\*,  $p < 0.02$ ) for  $f_{lignin} = 0$  and 0.5, but significant to only 90% confidence (\*,  $p = 0.1$ ) between 0 and 0.33 and between 0.33 and 0.5 (SI.13). Note that to calculate  $E$ , these data are also corrected for the non-spherical bead geometry at high lignin contents; see details in SI.4.



**Fig. 9** Representative force/compression curves of 8% (DP290 cellulose) microbeads with  $f_{lignin}$  of 0 (blue ●), 0.33 (orange □), and 0.5 (red ▲); curves are nearly independent of bead composition at low compressive strains, though higher  $f_{lignin}$  beads break at much lower  $\varepsilon$ . Higher  $f_{lignin}$  leads to smaller, flatter beads with higher moduli (Table 4, SI.4).

While microbeads made from pure cellulose or one-third lignin do not break until high compressive strains (>40%), microbeads containing 50% lignin are substantially more brittle, breaking at ~20% strain. These significant differences in compression-at-break for the highest lignin content microbeads likely reflect the flatter morphology in addition to the increased microbead stiffness with increasing lignin content, although even without the morphology adjustments, the smaller average bead contact would lead to higher measured moduli for lignin-containing beads. Although beads become stiffer and more brittle with the addition of lignin, even the microbeads with  $f_{lignin} = 0.5$  do not break with less than 30 N of force. Additionally, the microbeads precipitated and extracted in ethanol still appear approximately

875 spherical (Fig. 8) with reasonable sphericities ( $\sim 1.3$ ), suggesting that even high lignin  
 876 content microbeads may be commercially-relevant.

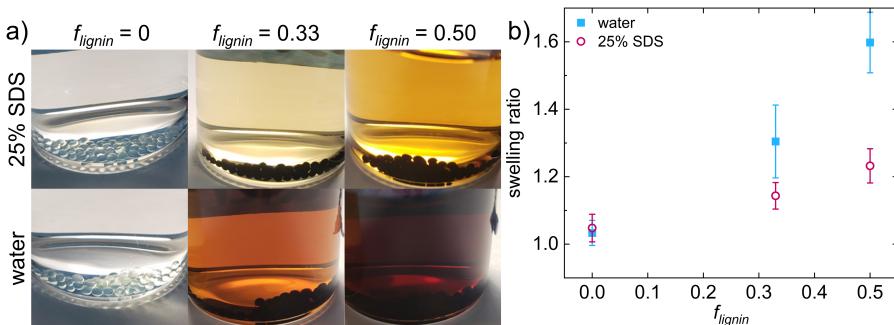
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### 878 3.7 Stability of microbeads in model systems

879

880 Two-month stability tests on microbeads submerged in water vs. 25% wt SDS  
 881 demonstrated that the presence of SDS suppressed diffusion of lignin out of lignin-  
 882 containing microbeads, illustrated in Fig. 10 for  $f_{lignin} = 0, 0.33$  and  $0.5$ . These  
 883 differences in diffusion are apparent even at early times ( $\sim 16$  h), where SDS solutions  
 884 with lignin-containing beads were lighter in color than analogous formulations  
 885 in water; the solutions darken proportionally to the amount of lignin leached from the  
 886 microbead. Microbead solutions in water and SDS with cellulose-only beads exhibited  
 887 no noticeable coloration. Notably, the solution colors after  $\sim 16$  h (Fig. 10) are  
 888 similar to those at the end of the two-month stability test (Fig. S7), indicating that the  
 889 majority of the lignin leaches from the microbead at early times when the initially dry  
 890 bead re-swells upon contact with the solution. As lignin leaches from the bead more  
 891 in pure water than in a model SDS solution (Fig. 10a), undesirable lignin leaching  
 892 could be suppressed upon incorporation of the microbeads into PCCPs. While lignin  
 893 leaching could potentially be mitigated *via* covalent crosslinking (as performed in  
 894 lignin-polyethylenimine (PEI) microbeads (Ge et al., 2016)), lignin leaching could  
 895 also provide a route for producing lower density, more porous microbeads with  
 896 enhanced suspension stability and sorbent properties (Chern et al., 2004; Ma et al.,  
 897 2016).

898



909 **Fig. 10** a) Mixed biomass microbeads ( $f_{lignin} = 0, 0.33, 0.5$  with DP290 cellulose) in (top) 25% SDS and  
 910 (bottom) water after 16 h. SDS mitigates diffusion of lignin from the bead, reflected by the lighter mixture  
 911 colors. b) Bead swelling ratios  $SR$  in water and 25% SDS remain constant over 2 months. (Fig. S8) but  
 912 increase with lignin content, though this effect is reduced in SDS solutions.

913

914 Microbead size measurements taken over the course of the two month stability  
 915 test indicate no statistically significant change in size over time after initial re-  
 916 swelling for all six solutions (Fig. 10, SI.6), suggesting that beads maintain good  
 917 structural stability over this time period. In these stability tests, microbeads were  
 918 removed from solution each week to understand the impact of the surrounding sol-  
 919 ution environment on the long-time microbead stability and mechanical properties;  
 920 for measurement accuracy, beads were thoroughly dried prior to mechanical testing.

For each set of beads, swelling ratios  $SR = \frac{D_{wet}}{D_{bead}}$  - which are related to bead porosity (Chern et al, 2004; Ma et al, 2016) - were determined by imaging and sizing wet beads immediately upon removal from solution and following the drying process. For all six solutions, the constant microbead swelling ratios in time indicate good structural stability (Fig. S8). As swelling ratios are related to the pore structure, this finding implies that no significant structural degradation or additional lignin leaching occurs over two months, as both of these events would be expected to alter  $SR$ . These data are also consistent with qualitative visual observations that suggest that additional lignin leaching is minimal after the initial re-swelling stage (Figs. 10, S7).

While trends in the swelling ratio are independent of solution condition, average swelling ratios vary in magnitude across conditions and depend on the surrounding medium (water vs. SDS). Microbeads submerged in SDS had consistently lower  $SR$  than their counterparts submerged in water, consistent with visual observations that beads submerged in SDS solutions leached less lignin (Fig. 10). For cellulose-only microbeads, average values of  $SR \approx 1$  indicate low porosity, and no significant difference in swelling is observed based on surrounding medium ( $p = 0.22$ ). However, lignin leaching - especially from beads suspended in pure water - leads to the recovery of some porosity in wet microbeads, as indicated by swelling ratios. Lignin beads had significantly higher average swelling ratios in water vs. SDS (\*\*\*,  $p < 0.001$  for both pairs), and the average  $SR$  increased three-fold faster with  $f_{lignin}$  in water than in SDS (Fig. 10).

Submerging beads in lignin vs. SDS also leads to differences in mechanical properties as the beads age. All beads exhibit decreases in compression at break ( $\varepsilon_{break}$ ) and significant increases in moduli (\*\*,  $p < 0.05$ ) of two- to three-fold over time (Fig. S9), pointing to brittleness resulting from increased crystallinity from aging (Graminski, 1970; Zervos, 2010). This change is especially noticeable in  $\varepsilon_{break}$ , with a large drop after week one for all formulations (SI.6); however promisingly, all formulations maintain compressive strains at break of at least 20% after 2 months. The presence of SDS decreases  $\varepsilon_{break}$  relative to that obtained in water only for all formulations, an effect which could be attributed to the formation of SDS deposits as the beads are dried before compression - these deposits would have very low mechanical strength, and if formed inside the bead, would cause earlier fracture. After week one, however  $\varepsilon_{break}$  decreases around 50% faster for beads in water as for beads in SDS (Table S8). Unfortunately, clear differences in moduli in time for formulations in water vs. SDS are not discernible, likely due to high variability between small samples ( $n=5$ ) measured each week.

## 4 Discussion

By altering the cellulose-to-lignin ratio and changing processing parameters like overall biomass concentration, nozzle gauge, and precipitation and extraction solvent strength, mechanically robust biomass microbeads of tunable modulus (MPa to ~1 GPa), size ( $D_{bead} = 800\text{-}2000 \mu\text{m}$ ), and swelling ratio (1 - 1.6) could be achieved without the need for covalent crosslinking. Importantly, these microbeads exhibit good mechanical stability over two months whether submerged in water or SDS,

967 maintaining moduli and compressive strains-at-break reasonable for PCCP applica-  
 968 tions (Palombini et al, 2018; Sipe et al, 2022a; Søgaard et al, 2001; Peng et al, 2021;  
 969 Xu et al, 2019; Xu and Gerling, 2020). Notably, PCCPs should have a shelf life  
 970 around 1-2 years (Diven et al, 2015; Baranova et al, 2014), and microbeads measured  
 971 here would likely become stiffer and more brittle over time (Zervos, 2010). However,  
 972 an increase in modulus could actually be beneficial, bringing the properties of these  
 973 beads closer to some commodity plastics (Sipe et al, 2022b). Additionally, under the  
 974 forces used by consumers, some decrease in compressive strain at break is possible  
 975 while retaining the efficacy of these beads during use.

976 While crosslinking can further increase mechanical properties like the Young's  
 977 modulus and can potentially mitigate effects from aging, this additional synthetic step  
 978 would likely negate many of the advantages associated with use of these biomass  
 979 microbeads. For example, the potentially improved stability imparted by crosslinking  
 980 would almost certainly reduce microbead degradability in the environment follow-  
 981 ing use (Hamdi and Ponchel, 1999; Bhattacharjee and Perlin, 1971). Additionally,  
 982 synthetic modification can result in harmful degradation products (SAPEA, 2019),  
 983 and may change how the microbeads are classified from a regulatory perspective,  
 984 potentially making them less desirable for industrial adoption. Finally, this chemical  
 985 modification step would likely hinder scalability due to additional equipment needs  
 986 and increased process complexity. However as is, the microbeads produced herein  
 987 can be sustainably sourced and readily biodegradable due to their composition of  
 988 non-derivatized biomass, providing a greener alternative to a major source of current  
 989 microplastic pollution.

990 Despite the broad range of accessible properties, some of the microbeads for-  
 991 mulations had undesirable properties for actual consumer use. For example, beads  
 992 around 2000  $\mu\text{m}$  in diameter and with moduli of several MPa resulted in beads that  
 993 showed evidence of residual IL, which may make them unsafe for use in consumer  
 994 products. Likewise, smaller beads produced from lower biomass concentrations were  
 995 more brittle and more often wrinkled or misshapen (Fig. S5), making them worse  
 996 candidates for consumer use - although these minor imperfections in surface mor-  
 997 phology and shape may be unrecognizable by the consumer once incorporated into a  
 998 PCCP. Accordingly, the practical size range of microbeads produced with this method  
 999 was  $\sim$ 800-1300  $\mu\text{m}$ , giving Young's moduli of order 0.5 GPa - on par with the size  
 1000 and moduli of beads resulting from commonly-used synthetic plastics (Palombini  
 1001 et al, 2018; Sipe et al, 2022a). Interestingly, incorporating lignin, a waste prod-  
 1002 uct from cellulose production, altered the microbead brittleness, size, and shape to  
 1003 a degree - but in general, similar Young's moduli and bead sizes were obtained  
 1004 regardless of biomass composition. This finding is promising for potential indus-  
 1005 trial adoption, signalling both that lignin can be used as a low-cost constituent of  
 1006 the microbeads and that the microbead preparation method and resulting properties  
 1007 are fairly robust to biomass source. As lignin tends to leach from the microbeads in  
 1008 water-based media, lignin can also potentially be used as a sacrificial filler molecule  
 1009 to generate more porous beads.

1010 While some of these microbeads meet the high end of the target size range for  
 1011 PCCP applications (Habib et al, 2020; Cheung and Fok, 2017; Shareef and Shareef,  
 1012

2021; Gouin et al, 2015; Duis and Coors, 2016; Ziajahromi et al, 2017), bead sizes that span the entire target range (200-800  $\mu\text{m}$ ) could not be produced due to limitations of the production method. The adaptation of this work to other production methods, like an emulsion-precipitation synthesis (Jo et al, 2019; Coombs OBrien et al, 2017; Volant et al, 2021; Park et al, 2020b,a), would both afford access to smaller bead sizes and enable better scalability using large batch reactors. While dripping methods can be accelerated to commercial scale *via* parallelization or additional apparatus like jet-cutting (Druel et al, 2018), batch reactor mixing is far cheaper to implement, and the supporting infrastructure largely already exists. Furthermore, due to the limitations of the high-viscosity solutions used, an emulsion route is necessary to access beads with diameters within the smaller end of the target range, on the order of 200-700  $\mu\text{m}$  (Habib et al, 2020; Cheung and Fok, 2017; Ziajahromi et al, 2017; Carr et al, 2016). Although previous work by Park and coworkers (Park et al, 2020b) incorporates other biopolymers like lignin into emulsion-based microbeads, the resulting microbeads are too small for use in most PCCPs (Palombini et al, 2018; Kalčíková et al, 2017; Yurtsever and Yurtsever, 2019; Nam and Park, 2020).

Finally, beyond the mismatch in microbead size for the intended PCCP applications, the microbeads examined by Park et al. (Park et al, 2020b) were also too small to perform traditional mechanical compression testing methods. In fact, the size of microbeads produced herein is near the lower limit of what can be measured with a standard single-particle bulk compression testing apparatus. Thus in addition to the numerous PCCP applications requiring larger bead sizes (Fendall and Sewell, 2009; Hintersteiner et al, 2015), the beads produced here also serve as a model system for assessing trends in bead size, bead shape, and mechanical properties *via* more straightforward imaging and mechanical testing methods. This insight can now guide the formulation of smaller beads with tunable properties *via* other methods such as the aforementioned emulsion-precipitation syntheses (Jo et al, 2019; Coombs OBrien et al, 2017; Volant et al, 2021; Park et al, 2020b,a).

## 5 Conclusion

In this work, biomass microbeads with tunable size, swelling behavior, and mechanical properties were prepared *via* extrusion of biomass solutions, altering both formulation parameters like biomass composition and concentration, and processing parameters including nozzle gauge, precipitation solvent, and extraction solvent. Resulting microbeads have properties on par with those of synthetic plastic microbeads, with moduli ranging from several MPa to nearly 1 GPa, diameters from  $\sim$ 800-2000  $\mu\text{m}$ , and swelling ratios from 1 to 1.6. To our knowledge, this is the first demonstration of microbeads for PCCPs composed of purely biomass which incorporate multiple biomass sources and are highly stable despite the absence of chemical crosslinking or modification. While all microbeads exhibit good structural stability when submerged in water for over 2 months, cellulose microbeads with added Kraft lignin did experience moderate lignin leaching from the bead into the surrounding water. However, use of a sodium dodecyl sulfate solution as a model personal care product leads to high retention of lignin within the microbead structure

1059 despite the absence of crosslinking, a result which is promising for consumer product  
1060 applications.

1061 Precipitation solvent, biomass concentration, and Kraft lignin fraction substan-  
1062 tially impact the resulting microbead shape. Numerous precipitation solvents produce  
1063 spherical beads; however, lower biomass content leads to nonuniformities in shape,  
1064 likely due to contraction of the bead surface during precipitation and extraction.  
1065 Incorporating larger amounts of Kraft lignin leads to flattening of microbeads upon  
1066 contact with the precipitation solvent, potentially due to a reduction in sample vis-  
1067 cosity. While the highly irregular particle shapes produced using acetone as an  
1068 precipitation solvent preclude its further use, formulations like lignin-containing  
1069 beads that exhibit smaller deviations from the ideal spherical morphology may still  
1070 be useful in commercial products.

1071 Incorporating lignin, altering biomass concentration, and using celluloses with  
1072 different degrees of polymerization provides routes to tune the microbead size, as  
1073 these factors all impact solution viscosity. Beyond reducing the bead size individ-  
1074 ually, higher lignin content, lower biomass concentration, and shorter cellulose all  
1075 result in solutions with lower viscosities that can be extruded through smaller nozzles  
1076 to produce even smaller beads. However, drastically reducing the nozzle size yields  
1077 diminishing returns, as the final bead diameter scales with nozzle size,  $d$ , as  $d^{1/3}$ .

1078 The most effective route for tuning the microbead Young's modulus is by alter-  
1079 ing the extraction solvent, with the initial precipitation solvent playing a minor  
1080 role. However, large changes in modulus due to extraction solvent result from a  
1081 more porous microstructure and residual ionic liquid, which is impractical for use  
1082 in PCCPs. Other routes for tuning the modulus include altering the concentration  
1083 of biomass and lignin incorporation - of these, altering the biomass concentration  
1084 may be the most effective, but the high solution viscosities restrict the potential  
1085 concentration range using the current method. Incorporating lignin, on the other  
1086 hand, increases the modulus without significantly impacting the force/compression  
1087 response for compressive strains up to 20%.

1088 While the aforementioned experimental constraints limit the dripping method of  
1089 microbead production to beads at the upper end of the commercially-relevant size  
1090 range, successful incorporation of both cellulose and lignin clearly demonstrates the  
1091 robustness of the method to biomass source. While lignin incorporation does impact  
1092 the microbead brittleness, size, and shape, remarkably similar ranges of Young's  
1093 moduli and bead sizes can be obtained regardless of biomass composition. This work  
1094 thus presents the first demonstration of stable, non-crosslinked biomass microbeads  
1095 at the PCCP-relevant length scale that incorporate multiple biomass sources, and  
1096 establishes guidelines for tuning the resulting microbead size, shape, and mechani-  
1097 cal properties *via* formulation and processing parameters. These guidelines can then  
1098 be extended to alternative synthetic approaches that afford access to a wider range  
1099 of microbead sizes, greatly expanding the number of PCCP applications that can be  
1100 pursued.

1101 **Supplementary information.** The Supporting Information includes tables summa-  
1102 rizing all solvent screen data; raw data from mechanical testing and dripping-onto-  
1103 substrate extensional rheometry; additional SEM images, calculations, and stability  
1104

test data; dye adsorption experiments; X-ray diffraction; and energy-dispersive X-ray spectra.	1105
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<b>Ethics approval and consent to participate.</b> Not applicable	1109
<b>Consent for publication.</b> All authors have provided consent for publication of this manuscript	1110
<b>Availability of data and materials.</b> Any data relevant to this study which are not given in the article or supplementary information are available upon request.	1111
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<b>Author contributions.</b> B.P.R., J.E.R., and L.M.H synthesized microbeads and performed sizing experiments. B.P.R. and L.M.H. performed compression tests. L.M.H. performed precipitation screen and dye absorption experiments. M.Q performed XRD experiments. B.P.R. performed all other experiments. B.P.R. analyzed data with assistance from M.A.C. B.P.R. and M.A.C. wrote the manuscript. All authors reviewed the manuscript.	1114
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<b>Author contributions.</b> Not applicable	1116
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