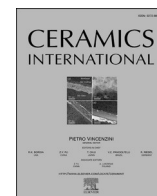




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# Converting commercial $\text{Fe}_2\text{O}_3$ to effective anode material using glucose as “etching” agent

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## ABSTRACT

$\text{Fe}_2\text{O}_3$  is an appealing anode material due to its high specific capacity ( $1007 \text{ mAh g}^{-1}$ ), low cost, natural abundance, and nontoxicity. However, its unstable structure during cycling processes has hindered its potential. In this study, we present a “green” synthesis method to fabricate stable porous  $\text{Fe}_2\text{O}_3$  encapsulated in a buffering hollow structure ( $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ ) as an effective anode material for Li-ion batteries. The synthesis process only involves glucose as an “etching” agent, without the need for organic solvents or difficult-to-control environments. Characterizations of the nanostructures, chemical compositions, crystallizations, and thermal behaviors for the intermediate/final products confirm the formation of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . The synthesized  $\text{Fe}_2\text{O}_3$  anode material effectively accommodates volume change, decreases pulverization, and alleviates agglomeration, leading to a high capacity that is over eleven times greater than that of the as-received commercial  $\text{Fe}_2\text{O}_3$  after a long cycling process. This work provides an attractive, “green” and efficient method to convert commercially abundant resources like  $\text{Fe}_2\text{O}_3$  into effective electrode materials for energy storage systems.

## 1. Introduction

Commercial lithium-ion batteries (LIBs) using conventional graphite anodes have been mass-produced to meet the expanding market of portable electronics and electronic vehicles because of their cycling stability and long lifespan [1]. However, graphite has a low theoretical capacity of  $372 \text{ mA h g}^{-1}$ , limiting the improvement of the energy density of LIBs. Therefore, many alternative anode materials with high theoretical specific capacities have been explored [2]. Transitional metal oxides, such as  $\text{Fe}_2\text{O}_3$ ,  $\text{Fe}_3\text{O}_4$ ,  $\text{FeO}$ ,  $\text{NiO}$ , and  $\text{MnO}$ , have received extensive attention owing to their high theoretical capacity and environment-friendly properties [3–8]. Among them,  $\text{Fe}_2\text{O}_3$  has been considered to be one of the most attractive anode candidates for LIBs because of the extra advantages of cost-effectiveness and natural abundance, in addition to the high theoretical capacity ( $1007 \text{ mAh g}^{-1}$ ). Despite these advantages,  $\text{Fe}_2\text{O}_3$  suffers from large volume change, pulverization and severe agglomeration in the conversion reaction ( $\text{Fe}_2\text{O}_3 + 6\text{Li}^+ + 6\text{e}^- \leftrightarrow 2\text{Fe} + 3\text{Li}_2\text{O}$ ) during the cycling process, leading to low Coulombic efficiency and rapid capacity decay [9].

To address the above-mentioned issues, many synthesis methods, such as coprecipitation [10,11], solvothermal [12], etching [13], and

sol-gel, have been studied to fabricate various nanostructures for  $\text{Fe}_2\text{O}_3$  anode (see Table S1). The coprecipitation methods were considered preferable synthetic methods to form nano- $\text{Fe}_2\text{O}_3$  because of their resulting facile size-controllable nanostructures obtainable (e.g., nanorod, nanocube, and nanoflower, etc.) and low-cost processing. For example,  $\text{Fe}_2\text{O}_3$  nanorods were fabricated by using a simple heating process of ferric chloride aqueous solution with ammonia as the size-modifying agent. In spite of the cost-effectiveness, the reported research suggested that these  $\text{Fe}_2\text{O}_3$  nanorods displayed poor capacity retention after long cycling processes, as a result of low porosity and agglomeration, which induced low ionic/electronic conductivities [10]. In contrast, the solvothermal methods using organic solvents were applied to fabricate nano- $\text{Fe}_2\text{O}_3$  with mesoporous structures (e.g., porous sphere, spindle, etc) and high specific surface area, which led to good cycling performances in LIBs. For instance, mesoporous  $\text{Fe}_2\text{O}_3$  sunflower-like spheres were synthesized by solvothermal synthesis using ferric nitrate in N,N-dimethylformamide (DMF) as an organic solvent medium [12]. However, the products of solvothermal methods were low-yield; the use of large amounts of organic solvents increases the cost and causes environmental pollution. Similarly, sol-gel methods were also concerned for a high fabrication cost because of the low-yield and

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large organic chemical consumption. Acids were needed to etch  $\text{Fe}_2\text{O}_3$  particles for generating porous structures such as spheres and nanodiscs [14,15]. For instance, the  $\text{Fe}_2\text{O}_3$  nanodiscs were etched by a high concentration (0.5 M) of oxalic acid to tune the porosity. Other acids such as hydrochloric acid and phosphoric acid were also used as the etching agents, but the use of acids increases the cost and causes new environmental issues [16,17]. Therefore, viable, “green” fabrication processes for the synthesis of desired  $\text{Fe}_2\text{O}_3$  nanostructures have not been realized to obtain  $\text{Fe}_2\text{O}_3$  anodes with high performance and low cost.

Numerous  $\text{Fe}_2\text{O}_3$  composites, such as  $\text{Fe}_2\text{O}_3/\text{C}$ ,  $\text{Fe}_2\text{O}_3/\text{metal oxides}$  and  $\text{Fe}_2\text{O}_3/\text{MXenes}$ , were synthesized through the methods mentioned above for enhancing the electrochemical performance of  $\text{Fe}_2\text{O}_3$  anodes. One of the most reported nanostructures is the composites of  $\text{Fe}_2\text{O}_3/\text{C}$ , such as  $\text{Fe}_2\text{O}_3@\text{C}$  nanoparticles and nano- $\text{Fe}_2\text{O}_3$  incorporated carbon matrices. In such composites, carbon materials have been used to buffer the volume change, decrease the pulverization and mitigate the agglomeration of  $\text{Fe}_2\text{O}_3$  [18]. For example, a  $\text{Fe}_2\text{O}_3@\text{C}$  composite with a carbon content of 50 wt% and a polypyrrole coating, stabilized the structure and enhanced the electronic conductivity of  $\text{Fe}_2\text{O}_3$  [19]. However, introduction of the large amount of carbon decreases the content of active materials in electrodes, leading to a low energy density of the entire electrode. Therefore, many inorganic compounds such as  $\text{TiO}_2$ ,  $\text{SnO}_2$ , and  $\text{MnO}_2$  have been used as a thin coating for  $\text{Fe}_2\text{O}_3$  nanoparticles to stabilize the structures [20]. For instance,  $\text{TiO}_2$ -coated  $\text{Fe}_2\text{O}_3$  [21] and  $\text{Fe}_2\text{O}_3@/\text{SnO}_2$  nanorods [22] were reported to exhibit stable nanostructures and alleviated aggregation of  $\text{Fe}_2\text{O}_3$ . Among the inorganic coatings,  $\text{TiO}_2$  possesses very stable nanostructures because of the extremely small volume change of 4% during lithiation/delithiation processes and fast lithium-ion diffusion [23]. Unfortunately, the essential non-elasticity of  $\text{TiO}_2$  makes the  $\text{TiO}_2$  surface coating hardly handle the volume change of active materials. Hence, hollow structures were reported as an efficient design for active materials to accommodate the large volume change. It is known that Si and  $\text{SnO}_2$  also have large volume expansions of 400% and 260% during cycles. Si nanospheres [24] and  $\text{SnO}_2$  nanowires [25] were encapsulated by a  $\text{TiO}_2$  shell to form hollow structures to accommodate the volume expansion, exhibiting specific capacities five to ten times higher than that of untreated samples. Moreover, large volume-expansion active materials (including  $\text{Fe}_2\text{O}_3$ , Si and  $\text{SnO}_2$ , etc.) that were fabricated into porous structures demonstrated excellent electrochemical performance. The porous structures not only provided large electrode/electrolyte interfaces and facilitated ionic/electronic diffusion among active materials, but also decreased the structural strain during repeated lithiation/delithiation processes. Therefore, constructing a hollow structure with  $\text{TiO}_2$  shell encapsulating porous  $\text{Fe}_2\text{O}_3$  is potentially effective for accommodating the volume change and alleviating the pulverization/agglomeration of  $\text{Fe}_2\text{O}_3$  during the cycling process, but complete studies of this have not been reported in the literature to date.

In the current study, we fabricate porous  $\text{Fe}_2\text{O}_3$  using glucose as an “etching” agent, and then prepare a hollow structure with a  $\text{TiO}_2$  shell encapsulating the porous  $\text{Fe}_2\text{O}_3$  ( $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ , where “p” stands for “porous” and “h” for hollow) from commercial  $\text{Fe}_2\text{O}_3$  particles (for cosmetic applications). This is a viable, “green” fabrication approach because the process only involves using glucose as the “etching” agent, and only simple heating processes under easily controllable environments are required, without using any organic solvents. Concentrations of raw materials are optimized to effectively form the desired hollow structures in high yields. The synthesis mechanism is analyzed through the characterizations of the nanostructure, chemical compositions, crystallization and thermal behavior of the intermediate, indicating the formation of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  as the final synthesis product. This hollow structural anode material has been demonstrated to be able to buffer the volume change, alleviate the pulverization, and reduce the agglomeration of  $\text{Fe}_2\text{O}_3$  particles. As the anode, the resulting anode material builds up a high specific capacity over eleven times higher than that of the as-received commercial  $\text{Fe}_2\text{O}_3$  in LIBs. This work provides an attractive

“green” and efficient fabrication method of converting commercial abundant resources such as  $\text{Fe}_2\text{O}_3$  into effective electrode materials for energy storage systems.

## 2. Experiments

### 2.1. Raw materials

The Li metal circuit plates with a diameter of 15.8 mm were purchased from China Energy Lithium Co., Ltd. The carbon ester electrolyte purchased from Sigma-Aldrich Co., Ltd is composed of 1.0 M  $\text{LiPF}_6$  in a mixed solvent of ethylene carbonate (EC) and ethyl methyl carbonate (EMC) (1:1 by volume).  $\text{Fe}_2\text{O}_3$  powder was purchased from Thermo Scientific Co., Ltd. Titanium (IV) oxysulfate ( $\text{TiOSO}_4$ ) and glucose were purchased from Sigma-Aldrich Co., Ltd. The separator (Celgard 2400) and electrode components including Cu foil, super C45 and polyvinylidene fluoride binder (PVDF) were purchased from MTI Co., LTD. N-methyl-2-pyrrolidone (NMP) was purchased from Sigma-Aldrich Co., Ltd.

### 2.2. Preparation of $\text{Fe}_2\text{O}_3@\text{C}$

$\text{Fe}_2\text{O}_3@\text{C}$  was synthesized by a hydrothermal process. Firstly, glucose solution (0.05 M) was prepared by dissolving 0.27 g glucose into 30 mL water. Then, 1 g commercial  $\text{Fe}_2\text{O}_3$  was dispersed into the glucose solution by sonication for 5 min. The solution was transferred into 40 mL Teflon-lined stainless-steel autoclave, sealed and heated at 170 °C for 10 h in an air-blowing thermostatic oven. After cooling to ambient temperature, the precipitates were collected by filtration with a nylon filter film and washed with deionized water and ethanol for three times. Thereafter, the precipitates were dried in a vacuum oven at 60 °C for 10 h. Other combinations of glucose concentrations (0.5 and 0.1 M) and  $\text{Fe}_2\text{O}_3$  amounts (0.1 and 0.5 g) were also used to synthesize samples during the optimization process of the synthesis design.

### 2.3. Preparation of $\text{Fe}_2\text{O}_3@\text{C}@\text{TiO}(\text{OH})_2$

$\text{Fe}_2\text{O}_3@\text{C}@\text{TiO}(\text{OH})_2$  was fabricated by a facile coating process.  $\text{TiOSO}_4$  solution was first prepared by dissolving 0.05 g  $\text{TiOSO}_4$  and 3 g  $\text{H}_2\text{SO}_4$  solution (1 mol  $\text{L}^{-1}$ ) in 100 mL deionized water. Note that the  $\text{H}_2\text{SO}_4$  solution was added into the solution by drop by drop. Then,  $\text{Fe}_2\text{O}_3@\text{C}$  was dispersed in  $\text{TiOSO}_4$  solution with sonication for 30 min and a continued magnetic stirring process for 5 h. After a filtration process with a nylon filter film, the precipitates were washed with deionized water and ethanol for three times and dried in a vacuum oven at 60 °C.

### 2.4. Preparation of $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$

$p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  was prepared by a calcination process. The as-prepared precursor,  $\text{Fe}_2\text{O}_3@\text{C}@\text{TiO}(\text{OH})_2$ , was calcined at 500 °C in air atmosphere for 2 h. The heating rate of calcination process is 5 °C  $\text{min}^{-1}$ . Finally,  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  was obtained and collected for further characterization and battery assembly.

### 2.5. Materials characterization

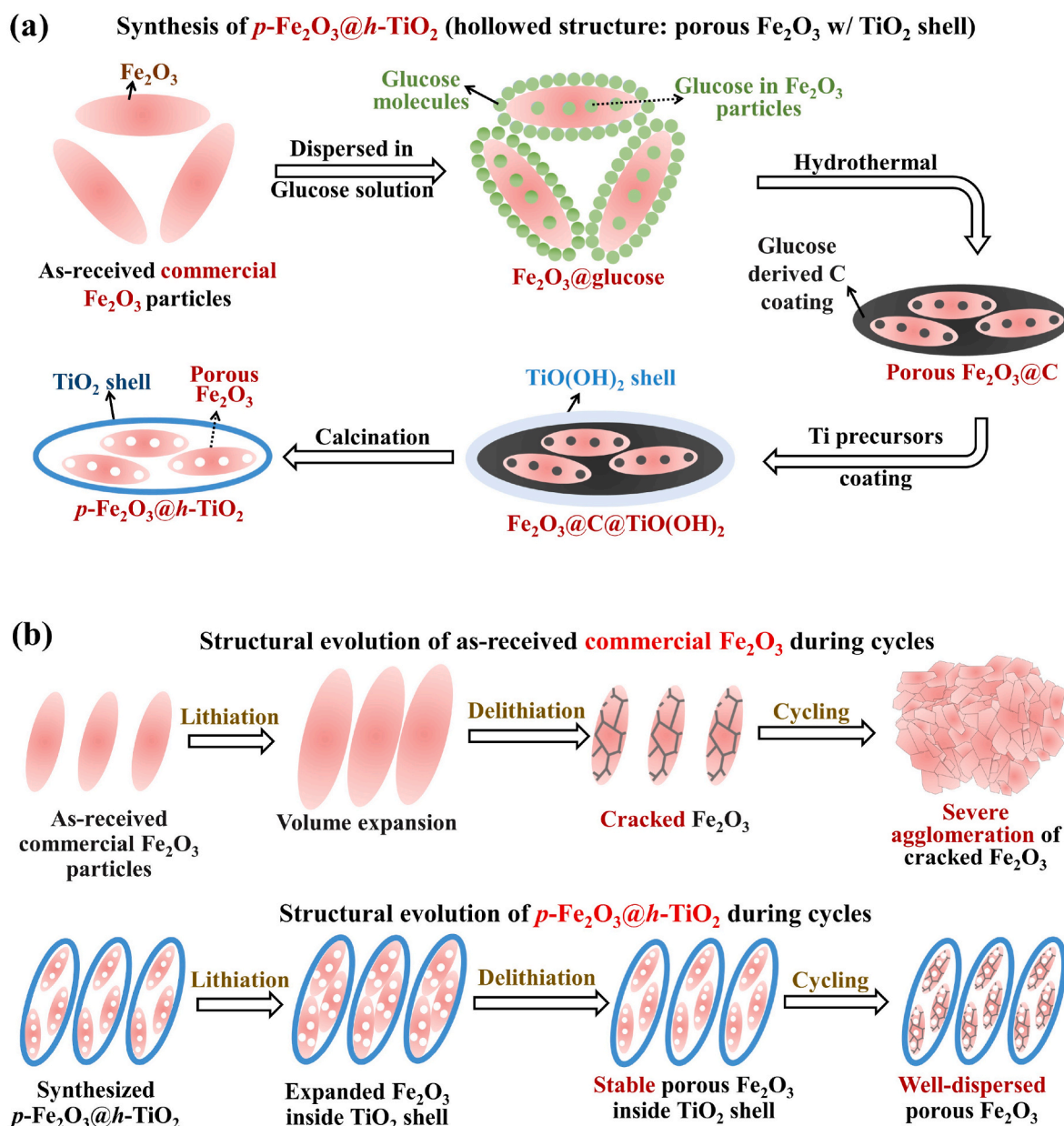
The morphologies of  $\text{Fe}_2\text{O}_3@\text{C}$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  were characterized by a scanning electron microscope (FE-SEM, S4800, Hitachi) and a transmission electron microscope (TEM, JEOL JEM-2100). The specific surface area and porosity were determined by a Micromeritics ASAP 2020Plus accelerated surface area and porosimetry system at 77 K; a degassing process under a vacuum of  $\sim 10^{-6}$  bar was conducted at 150 °C for 12 h to activate the samples. The chemical composition and crystallization of the commercial  $\text{Fe}_2\text{O}_3$ ,  $\text{Fe}_2\text{O}_3@\text{C}$ ,  $\text{Fe}_2\text{O}_3@\text{C}@\text{TiO}(\text{OH})_2$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  were investigated by Fourier transform

infrared spectroscopy-attenuated total reflectance (FTIR-ATR, Thermo fisher iS10), Raman spectroscopy (Thermofisher DXR2xi) and X-ray diffraction (XRD, Cu  $K_{\alpha}$ ,  $\gamma = 1.54 \text{ \AA}$ , Panalytical X'pert Pro). The scan step of FTIR is  $0.5 \text{ cm}^{-1}$ . The Raman laser excitation wavelength is 532 nm ( $4 \text{ cm}^{-1}$  spectral resolution) and the laser power was set to 5.2 mW. The exposure time of Raman is 0.0833 s and averaged over 80 scans. The composition ratio of all samples was measured by thermogravimetric analysis (TGA, SDT Q600, Switzerland) to analyze the carbon content of the composites at a heating rate of  $5 \text{ }^{\circ}\text{C min}^{-1}$  in air from room temperature to  $600 \text{ }^{\circ}\text{C}$ . Differential scanning calorimetry (DSC, Mettler Toledo) was applied to test the thermal properties of the films with a heating rate of  $5 \text{ }^{\circ}\text{C min}^{-1}$  in air.

## 2.6. Electrochemical measurements

To test the electrochemical performance, the 2025 coin-type cells were assembled. To fabricate the electrode sheet, a slurry was prepared

by mixing the synthesized  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  powders with conductive agent (super C45), binder (PVDF) at a weight ratio of 8:1:1 in NMP solvent by magnetic stirrer for 10 h. Thereafter, the homogenous slurry was dried on copper sheet and was transferred into a vacuum oven for 12 h under  $80 \text{ }^{\circ}\text{C}$  to further remove the remaining moisture. The obtained electrode sheet was cut into circular plates with a diameter of 12.7 mm, and the average area loading of active materials is  $\sim 2.8 \text{ mg cm}^{-2}$ . A Li plate was applied as the counter electrode. When assembling coin cells, the electrolyte amount (40  $\mu\text{L}$ ) and assembly pressure (50 MPa) were controlled to keep them consistent for comparison. The cycling performance was tested by a LAND multichannel battery cycler (Wuhan LAND Electronics Co., Ltd.). The assembled half cells were cycled in a voltage range of 0.1–3 V (vs  $\text{Li}^+/\text{Li}$ ) at various rates of 0.1 C, 0.2 C, 0.5 C, 0.8 C and 1 C. The electrochemical impedance spectroscopy (EIS) measurements were tested in a frequency range of 0.1– $10^6$  Hz on an electrochemical workstation (BioLogic VSP). Cyclic voltammetry (CV) experiments were also carried out by the electrochemical



**Fig. 1.** (a) Synthesis processes of the hollow structure with a  $\text{TiO}_2$  shell encapsulating porous  $\text{Fe}_2\text{O}_3$  ( $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ ). (b) The structure evolution of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  during cycling processes when applied as the anode in Li-ion batteries.



workstation from 0 V to 3 V.

### 3. Results and discussions

#### 3.1. Synthesis of $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$

Fig. 1a presents the schematic of the glucose-assisted synthesis process of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . As shown, within the glucose solution, the commercial  $\text{Fe}_2\text{O}_3$  particles (Fig. S1a) adsorb glucose molecules on their surface to form a glucose coating ( $\text{Fe}_2\text{O}_3@glucose$ ). Meanwhile, some glucose molecules permeate the defects of  $\text{Fe}_2\text{O}_3$  particles. In the hydrothermal process under a temperature of 170 °C for 10 h, the glucose molecules “etch” the  $\text{Fe}_2\text{O}_3$  particles into a porous structure [26,27]. At the same time, the coating is gradually carbonized into a carbon shell for  $\text{Fe}_2\text{O}_3$  particles ( $\text{Fe}_2\text{O}_3@C$ ). Progressively, the particles accumulate together to form larger  $\text{Fe}_2\text{O}_3@C$  particles containing a number of  $\text{Fe}_2\text{O}_3$  particles. To prepare the  $\text{TiO}_2$  shell, titanium oxysulfate ( $\text{TiOSO}_4$ ) is dissolved in water to form  $\text{TiO}(\text{OH})_2$  colloids as the titanium precursor [28]. The pH of the  $\text{TiOSO}_4$  solution is controlled by sulfuric acid to build a chemical equilibrium between  $\text{TiOSO}_4$  (aq) and  $\text{TiO}(\text{OH})_2$  (sol). After dispersing  $\text{Fe}_2\text{O}_3@C$  particles into the  $\text{TiOSO}_4$  solution, the carbon shell with rich O-containing functional groups adsorbs  $\text{TiO}(\text{OH})_2$  on the surface and generates a  $\text{TiO}(\text{OH})_2$  shell ( $\text{Fe}_2\text{O}_3@C@TiO(\text{OH})_2$ ) [23]. Then, the  $\text{Fe}_2\text{O}_3@C@TiO(\text{OH})_2$  powder is calcined at 500 °C for 2 h to remove carbon to generate the hollow structure with a  $\text{TiO}_2$  shell encapsulating the porous  $\text{Fe}_2\text{O}_3$  ( $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ ).

#### 3.2. Optimization of the synthesis process

To optimize the synthesis process, various concentrations of glucose and commercial  $\text{Fe}_2\text{O}_3$  particles were applied during the hydrothermal process (Table S2). In 0.5 M glucose solution without the addition of  $\text{Fe}_2\text{O}_3$  particles, the products of the hydrothermal process are carbon microspheres with diameters of 1.5–6  $\mu\text{m}$  (Fig. S1b). These carbon spheres are formed through a homogeneous nucleation process. After adding 0.5 g  $\text{Fe}_2\text{O}_3$  particles inside, many  $\text{Fe}_2\text{O}_3@C$  particles emerged among carbon microspheres in the hydrothermal process product (Fig. S1c). The diameter range of carbon spheres is 1–10  $\mu\text{m}$ . This diameter-range change is ascribed to the heterogeneous nucleation of carbon spheres with  $\text{Fe}_2\text{O}_3$  particles as nuclei. Hence, we proposed that glucose first forms a carbon coating and grows on  $\text{Fe}_2\text{O}_3$  nuclei; and then, the excessive amount of glucose generates carbon microspheres. When the glucose concentration decreases to 0.1 M and  $\text{Fe}_2\text{O}_3$  amount decreases to 0.1 g, both carbon spheres and  $\text{Fe}_2\text{O}_3@C$  particles appear in the hydrothermal product, indicating glucose amount is still in excess for the formation of  $\text{Fe}_2\text{O}_3@C$  (Fig. S1d). With a further increase of  $\text{Fe}_2\text{O}_3$  amount to 0.5 g and keeping glucose concentration at 0.1 M, more  $\text{Fe}_2\text{O}_3@C$  particles and fewer carbon microspheres are present in the products (Fig. S1e). Hence, we optimize the glucose concentration to 0.05 M and  $\text{Fe}_2\text{O}_3$  amount to 1 g. The optimized hydrothermal product only contains  $\text{Fe}_2\text{O}_3@C$  particles and no carbon microsphere included (Fig. S1f, 2a). In the below context, the samples for characterization refer to the products fabricated by the optimized synthesis process.

#### 3.3. Structural evolution of $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ during cycling processes

The stable cycling structural mechanism of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  is illustrated in Fig. 1b. During cycling processes in LIBs, the lithiation induces an expansion, while delithiation causes the shrinking of  $\text{Fe}_2\text{O}_3$  particles, which leads to the cracking of particles because of the volume change. After many cycles, the  $\text{Fe}_2\text{O}_3$  particles are severely agglomerated due to repeated severe volume changes and consequent pulverization of  $\text{Fe}_2\text{O}_3$ . Agglomeration of the  $\text{Fe}_2\text{O}_3$  particles results in low ionic/electronic conductivities of the electrode, leading to a low specific capacity and short lifespan [29]. On the contrary, for  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ , the expanded and cracked porous  $\text{Fe}_2\text{O}_3$  particles are confined in the

stable  $\text{TiO}_2$  shell, which effectively prevents the severe agglomeration of  $\text{Fe}_2\text{O}_3$ . The good dispersion and porous structure of  $\text{Fe}_2\text{O}_3$  inside the  $\text{TiO}_2$  shell together lead to good ionic conductivity even after many expansion-shrinkage cycles, thus resulting in superior cycling performance.

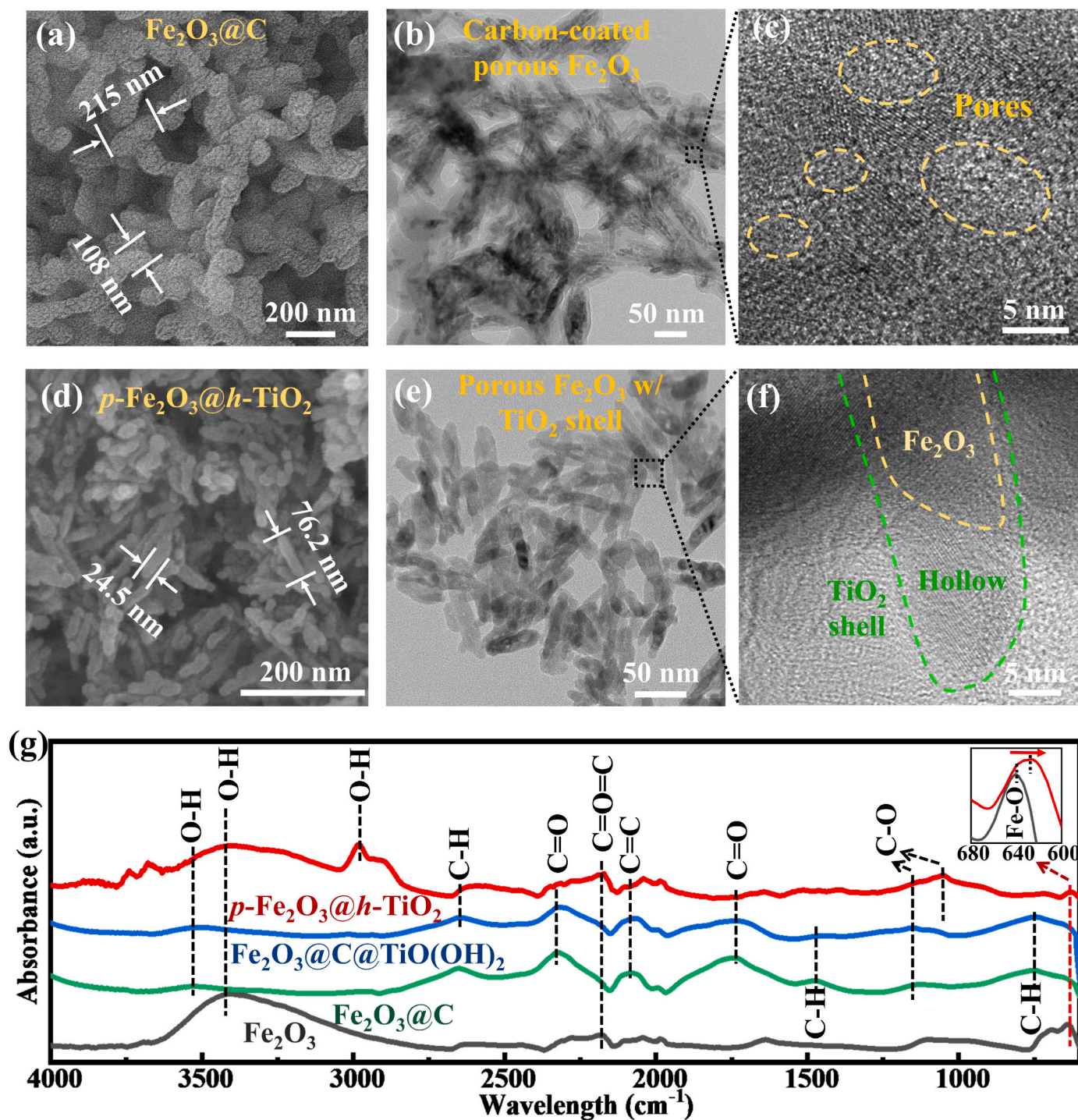
#### 3.4. Characterization of intermediate products and $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$

The morphology of  $\text{Fe}_2\text{O}_3@C$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  was investigated by scanning electron microscopy (SEM) and transmission electron microscope (TEM) to confirm the formation of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  nanostructures. Fig. S1f, 2a depict the SEM images of  $\text{Fe}_2\text{O}_3@C$ , which indicates the nanoworm-like structure of  $\text{Fe}_2\text{O}_3@C$ . In addition, their measured average dimensional length and width are 215 nm and 108 nm, respectively. The  $\text{Fe}_2\text{O}_3@C$  composite structure is further confirmed by TEM images. As shown in Fig. 2b, S2a-c, the nanoworm-like amorphous carbon particles are incorporated with many porous  $\text{Fe}_2\text{O}_3$  particles inside. The high-resolution transmission electron microscopy (HRTEM) images of  $\text{Fe}_2\text{O}_3@C$  reveal a lattice fringe value of 0.27 nm (Fig. S2d), which is approximate to the lattice fringe value of 0.25 nm for the (110) plane of  $\alpha\text{-Fe}_2\text{O}_3$  [30]. Meanwhile, abundant pores surrounded by  $\text{Fe}_2\text{O}_3$  crystals can be found in Fig. 2c, demonstrating the porous structure of  $\text{Fe}_2\text{O}_3$  particles. After titanium precursor coating, a very rough surface of the particles with adhered  $\text{TiO}(\text{OH})_2$  can be found in the SEM images of  $\text{Fe}_2\text{O}_3@C@TiO(\text{OH})_2$  (Fig. S3). Thereafter, followed by a calcination process,  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  particles with lengths of  $\sim 76.2$  nm and widths of  $\sim 24.5$  nm are obtained (Fig. 2d). The TEM images of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  demonstrate its hollow nanostructure (Fig. 2e, S4a, S4b). Fig. 2f, S4c show the  $\text{TiO}_2$  shell around  $\text{Fe}_2\text{O}_3$  particles, confirming the structure of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . In the HRTEM images (Fig. S4d), the lattice fringe of 0.351 nm is ascribed to the (101) plane of the anatase  $\text{TiO}_2$  shell [31].

The pore size and specific surface area of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  were examined by nitrogen adsorption/desorption isotherm analysis. As shown in Fig. S5, both samples show typical type-IV isotherm curves. The volumes of the pores with size range from 5 nm to 30 nm significantly increase (Insert of Fig. S5). This result demonstrates that more nanopores are present in  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  than that in the commercial  $\text{Fe}_2\text{O}_3$ . Moreover,  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  shows a larger specific surface area of  $63.83 \text{ m}^2 \text{ g}^{-1}$  (vs.  $50.13 \text{ m}^2 \text{ g}^{-1}$  of the commercial  $\text{Fe}_2\text{O}_3$ ) because of the increased amount of nanopores.

The chemical compositions of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  and its precursors were characterized by Fourier transform infrared spectroscopy (FTIR) to study the formation process (Fig. 2g). For the commercial  $\text{Fe}_2\text{O}_3$ , the broad peak at  $3388 \text{ cm}^{-1}$  is ascribed to the stretching vibration of O–H [32]. A weak peak at  $2169 \text{ cm}^{-1}$  can be attributed to the stretching of C=O=C. The presence of O–H and C=O=C is speculated due to the remaining functional groups on the surface of  $\text{Fe}_2\text{O}_3$  particles. The typical peak of Fe–O stretching mode is found at  $640 \text{ cm}^{-1}$ . After the formation of a glucose-derived carbon shell in the hydrothermal process, an extra peak of O–H is found at  $3504 \text{ cm}^{-1}$  in the spectra of  $\text{Fe}_2\text{O}_3@C$  and  $\text{Fe}_2\text{O}_3@C@TiO(\text{OH})_2$ . More peaks are present at  $2641 \text{ cm}^{-1}$ ,  $2315 \text{ cm}^{-1}$ ,  $2070 \text{ cm}^{-1}$ ,  $1733 \text{ cm}^{-1}$ , and  $744 \text{ cm}^{-1}$ , which belong to the stretching or bending vibration of carbon-related bonds such as C–H, C=O, C=C and C–O, respectively [33]. These carbon-related bonds demonstrate diverse functional groups in the amorphous carbon of  $\text{Fe}_2\text{O}_3@C$ , thus, leading to good absorption of  $\text{TiO}(\text{OH})_2$  colloids on the surface. Meanwhile, there is no significant difference between  $\text{Fe}_2\text{O}_3@C$  and  $\text{Fe}_2\text{O}_3@C@TiO(\text{OH})_2$ , indicating that the amorphous carbon of  $\text{Fe}_2\text{O}_3@C$  still keeps integrity and is not dissolved or dispersed into  $\text{TiOSO}_4$  solutions during the sonication and mixing process. Regarding  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ , a strong peak of OH appears at  $2978 \text{ cm}^{-1}$ , which is due to the surface functional groups on the  $\text{TiO}_2$  shell. Notably, compared to the commercial  $\text{Fe}_2\text{O}_3$ , the Fe–O peak of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  has a blue shift from  $640 \text{ cm}^{-1}$  to  $628 \text{ cm}^{-1}$ . This phenomenon is speculated induced by the impact of the hydrothermal and calcination





**Fig. 2.** Characterization of intermediate products and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . SEM images of (a)  $\text{Fe}_2\text{O}_3@\text{C}$  and (d)  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . TEM images of (b)  $\text{Fe}_2\text{O}_3@\text{C}$  and (e)  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . HRTEM images of (c)  $\text{Fe}_2\text{O}_3@\text{C}$  and (f)  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ ; the inset images are the enlarged area of lattice fringes. (g) ATR-FTIR curves of  $\text{Fe}_2\text{O}_3$ ,  $\text{Fe}_2\text{O}_3@\text{C}$ ,  $\text{Fe}_2\text{O}_3@\text{C}@\text{TiO}(\text{OH})_2$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ .

process on the crystallization of  $\text{Fe}_2\text{O}_3$  and the impact of  $\text{TiO}_2$  peaks [34].

The crystal structures of various samples were revealed by X-ray diffraction (XRD). As shown in Fig. 3a, the typical peaks of both  $\alpha\text{-Fe}_2\text{O}_3$  and  $\gamma\text{-Fe}_2\text{O}_3$  can be found in the curve of the commercial  $\text{Fe}_2\text{O}_3$  [35]. The curves of  $\text{Fe}_2\text{O}_3@\text{C}$  and  $\text{Fe}_2\text{O}_3@\text{C}@\text{TiO}(\text{OH})_2$  do not show new peaks, demonstrating that the hydrothermal and Ti-precursor-coating processes have a small impact on the primary crystal structure of  $\text{Fe}_2\text{O}_3$ . After the calcination process, typical peaks of  $\text{TiO}_2$  are found at  $24.3^\circ$ ,  $40.9^\circ$  and  $49.6^\circ$ , which belong to the planes of (101), (111) and (200),

respectively [36]. A strength-increased peak at  $33.3^\circ$ , which belongs to the (104) plane of  $\alpha\text{-Fe}_2\text{O}_3$  in  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ , demonstrates the increased amount of  $\alpha\text{-Fe}_2\text{O}_3$  in the sample [12]. This result is due to the calcination process that transforms the crystal structure of  $\text{Fe}_2\text{O}_3$  from  $\gamma$ -phase to  $\alpha$ -phase [37]. Moreover, the peaks in the range of  $42\text{--}80^\circ$  of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  display a right shift compared to the as-received commercial  $\text{Fe}_2\text{O}_3$ . This peak shift demonstrated the improved crystallization of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  that enhances the stability of the  $\text{Fe}_2\text{O}_3$  structure during the cycling process.

Fig. 3b illustrates the Raman spectra of various samples. Six typical

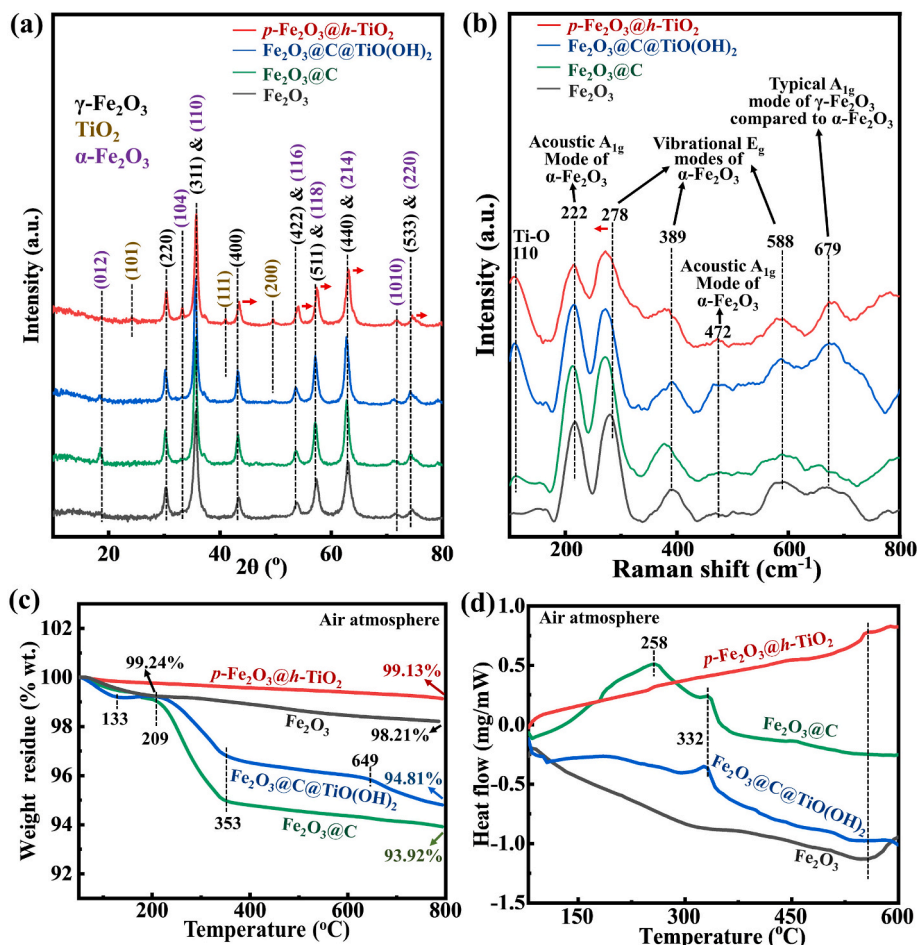


Fig. 3. (a) XRD, (b) Raman, (c) TGA and (d) DSC results of Fe<sub>2</sub>O<sub>3</sub>, Fe<sub>2</sub>O<sub>3</sub>@C, Fe<sub>2</sub>O<sub>3</sub>@C@TiO(OH)<sub>2</sub> and *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub>.

characteristic peaks of α-phase Fe<sub>2</sub>O<sub>3</sub> were found in all the spectra. The peaks at 278 cm<sup>-1</sup>, 389 cm<sup>-1</sup> and 588 cm<sup>-1</sup> are assigned to the vibrational E<sub>g</sub> modes of α-Fe<sub>2</sub>O<sub>3</sub>. The peaks derived from the acoustic A<sub>1g</sub> mode of α-Fe<sub>2</sub>O<sub>3</sub> are located at 222 cm<sup>-1</sup> and 472 cm<sup>-1</sup>. A typical A<sub>1g</sub> mode of γ-Fe<sub>2</sub>O<sub>3</sub> can be found at 679 cm<sup>-1</sup>, demonstrating the presence of γ-Fe<sub>2</sub>O<sub>3</sub> in the samples [12,38]. Moreover, a shift of the peak at 278 cm<sup>-1</sup> indicates the strain change and structural evolution during the hydrothermal and calcination processes of Fe<sub>2</sub>O<sub>3</sub> [39]. In addition, a peak of E<sub>g</sub> mode of TiO<sub>2</sub> presents at 110 cm<sup>-1</sup> on spectra of Fe<sub>2</sub>O<sub>3</sub>@C@TiO(OH)<sub>2</sub> and *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub>, indicating that the TiO(OH)<sub>2</sub> are adsorbed on the surface of Fe<sub>2</sub>O<sub>3</sub>@C and the formation of TiO<sub>2</sub> shell with a hollow space [40].

Thermal gravimetric analysis (TGA) was performed for all the samples under an air atmosphere from 50 °C to 800 °C to study the composition evolution at different synthesis processes (Fig. 3c). For the commercial Fe<sub>2</sub>O<sub>3</sub>, the weight residue decreases to 99.24% in the first stage from 50 °C to 209 °C, which is due to the loss of -OH on the surface. Then the weight of the commercial Fe<sub>2</sub>O<sub>3</sub> continues slowly decrease to 98.21% at 785.6 °C because of the loss of organic residues. In comparison, the curve of *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub> has only one stage and the weight decreases to 99.13% at 793.2 °C. This weight loss (0.87%) is close to that (1.03%) of the phase transformation of the commercial Fe<sub>2</sub>O<sub>3</sub>. In sharp contrast, Fe<sub>2</sub>O<sub>3</sub>@C has three clear stages that are attributed to water removal (50–209 °C), decomposition of organic compositions (209–353 °C) and Fe<sub>2</sub>O<sub>3</sub> phase transformation (353–800 °C) [41]. The weight loss of Fe<sub>2</sub>O<sub>3</sub>@C in the second stage is 4.07% which represents the carbon weight ratio in Fe<sub>2</sub>O<sub>3</sub>@C. For Fe<sub>2</sub>O<sub>3</sub>@C@TiO(OH)<sub>2</sub>, the weight ratio of carbon is 2.47%, smaller than that of Fe<sub>2</sub>O<sub>3</sub>@C. This phenomenon may be due to the partial dispersion

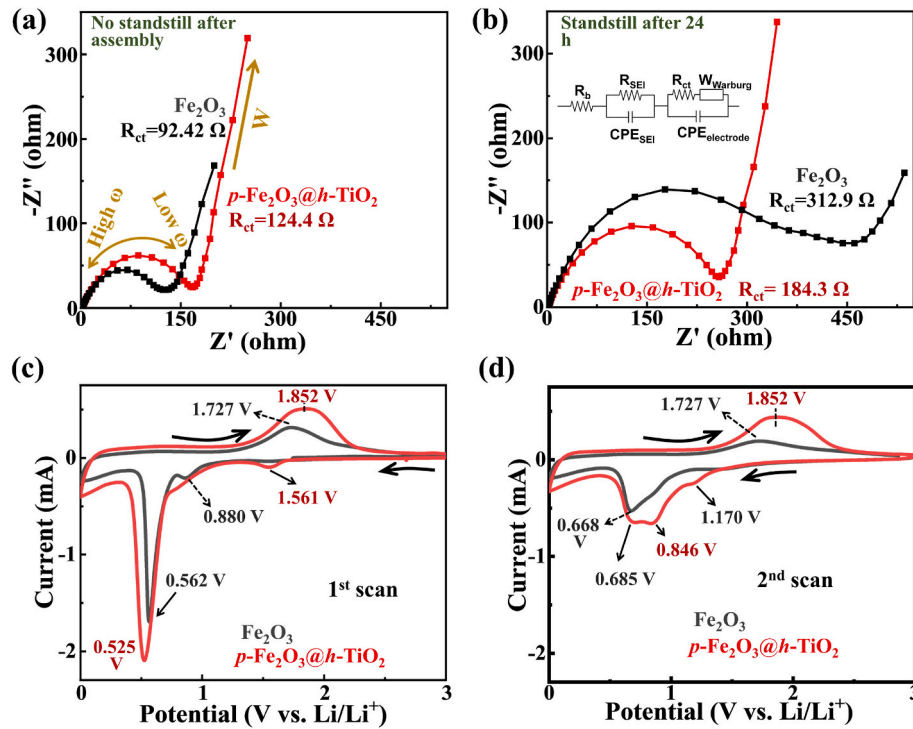
of amorphous carbon in TiOSO<sub>4</sub> solution. In specific, a peak at 649 °C on the curve of Fe<sub>2</sub>O<sub>3</sub>@C@TiO(OH)<sub>2</sub> could be caused by the Ti ion doping in surface Fe<sub>2</sub>O<sub>3</sub>. The small weight loss demonstrates the structure stability of *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub> [42].

Differential scanning calorimetry (DSC) analysis was applied to further study the phase transformation of Fe<sub>2</sub>O<sub>3</sub> and TiO<sub>2</sub> in various samples (Fig. 3d). The commercial Fe<sub>2</sub>O<sub>3</sub> has an endothermic peak at 557 °C because of the phase transformation of Fe<sub>2</sub>O<sub>3</sub> from γ-phase to α-phase. The peaks of Fe<sub>2</sub>O<sub>3</sub>@C and Fe<sub>2</sub>O<sub>3</sub>@C@TiO(OH)<sub>2</sub> at 332 °C are ascribed to the exothermic reaction of carbon. The smaller heat flow of Fe<sub>2</sub>O<sub>3</sub>@C@TiO(OH)<sub>2</sub> than that of Fe<sub>2</sub>O<sub>3</sub>@C can be assigned to the endothermic reaction of TiO(OH)<sub>2</sub> decomposition [43]. In contrast to the commercial Fe<sub>2</sub>O<sub>3</sub>, *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub> does not show an obvious strong peak on the curve, further proving its stable structure.

### 3.5. Electrochemical performance of *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub>

In order to characterize the electrochemical performance of as-synthesized samples, half cells with the sample electrodes were prepared and a series of electrochemical measurements were performed. The impedances in Nyquist plots of the assembled half cells at different stand-still times are shown in Fig. 4a and b [44,45]. At the time after cell assembly with no standstill, charge transfer resistance (R<sub>ct</sub>) of the cell with *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub> electrode (124.4 Ω) is larger than that of the cell with Fe<sub>2</sub>O<sub>3</sub> electrode (92.42 Ω) (Table S3). This result is due to the insufficient saturation and diffusion of liquid electrolytes in the hollow structure of *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub> within a short standstill time. Thus, the resistance (R<sub>SEI</sub>) of solid electrolyte interface (SEI) of the cell with *p*-Fe<sub>2</sub>O<sub>3</sub>@*h*-TiO<sub>2</sub> electrode (8.993 Ω) is smaller than that of the cell with





**Fig. 4.** Electrochemical characterization of  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrodes. EIS curves at (a) the initial state without standstill after assembly and (b) the stable state after the standstill for 24 h. (c) The 1st and (d) the 2nd cyclic voltammograms at a scan rate of  $2 \text{ mV s}^{-1}$ .

$\text{Fe}_2\text{O}_3$  electrode ( $3.784 \Omega$ ). After a standstill period of 24 h, SEI grows and the  $R_{SEI}$  increase to  $22.47 \Omega$  and  $17.22 \Omega$  for cell with  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  and  $\text{Fe}_2\text{O}_3$  electrode, respectively. Meanwhile, the cell with  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrode shows a smaller  $R_{ct}$  ( $184.3 \Omega$ ) than the cell with  $\text{Fe}_2\text{O}_3$  electrode ( $312.9 \Omega$ ), demonstrating that the liquid electrolyte has good contact with the porous  $\text{Fe}_2\text{O}_3$  core and  $\text{TiO}_2$  shell, and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  enhances the ionic/electronic conductivities in electrodes.

Fig. 4c and d shows the first and second cyclic voltammograms (CV) curve of half cells with the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrodes. In Fig. 4c, the sharp cathodic peak of  $\text{Fe}_2\text{O}_3$  at  $0.562 \text{ V}$  is attributed to the formation of SEI in the first cycle, while the peak shift to  $0.525 \text{ V}$  in the curve of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ , which is speculated as due to the partly phase change and increased crystallization of  $\text{Fe}_2\text{O}_3$  during hydrothermal and calcination processes as demonstrated in previously [46]. The weak peak at  $0.880 \text{ V}$  is due to the phase transformation (hexagonal to cubic) of  $\text{Li}_x\text{Fe}_2\text{O}_3$  during delithiation anodic process, while this peak is not found in  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ , indicating the high stability of  $\text{Fe}_2\text{O}_3$  crystal structure in  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . The peak at  $1.561 \text{ V}$  is the typical cathodic peak of  $\text{TiO}_2$  in the first cycle, which shows that the  $\text{TiO}_2$  shell of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  also takes part in the cycling process of batteries [47]. The broad anodic peak at around  $1.727 \text{ V}$  for  $\text{Fe}_2\text{O}_3$  is associated with the oxidation of  $\text{Fe}^0$  to  $\text{Fe}^{2+}/\text{Fe}^{3+}$ . In comparison to  $\text{Fe}_2\text{O}_3$ ,  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  has a broader anodic peak at  $1.852 \text{ V}$ , this shift of anodic peak may be due to the effect of the typical anodic peak of  $\text{TiO}_2$  at  $2.2 \text{ V}$  and the increased crystallization of  $\text{Fe}_2\text{O}_3$ . In Fig. 4d, the cathodic peak of  $\text{Fe}_2\text{O}_3$  in the second scan shifts to  $0.668 \text{ V}$  due to irreversible phase transformation compared to the first lithiation/delithiation processes [48]. A broad cathodic peak of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  is presented in  $0.685\text{--}0.846 \text{ V}$ , which is due to the high participation of the  $\text{Fe}_2\text{O}_3$  of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  in lithiation/delithiation process compared to the commercial  $\text{Fe}_2\text{O}_3$ . The partial lithiation peak of  $\text{Fe}_2\text{O}_3$  appears at  $1.170 \text{ V}$  in  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  while is not shown in the commercial  $\text{Fe}_2\text{O}_3$ . This phenomenon is induced by the high electrolyte contact area of porous  $\text{Fe}_2\text{O}_3$  in  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  that facilitates the lithiation process of  $\text{Fe}_2\text{O}_3$ .

The discharge/charge profiles of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  in the first, second and fourth cycles with a potential window from  $0.1 \text{ V}$  to  $3 \text{ V}$  are shown in Fig. 5a–c. For both samples, two plateaus at around  $0.8 \text{ V}$  and  $1.7 \text{ V}$  can be found in discharge and charge curves, respectively, which are attributed to the lithiation/delithiation processes of  $\text{Fe}_2\text{O}_3$ . At the first cycle of  $\text{Fe}_2\text{O}_3$  electrode with a current density of  $0.1 \text{ C}$  ( $1 \text{ C} = 1007 \text{ mA g}^{-1}$ ), a polarization at  $1.3644 \text{ V}$  of the charge curve and a small stage at  $0.9522 \text{ V}$  of the discharge curve can be found (Fig. 5a). This result indicates the sluggish  $\text{Li}$  ion diffusion of  $\text{Fe}_2\text{O}_3$  electrode. The  $\text{Fe}_2\text{O}_3$  delivers an initial discharge capacity of  $1043.8 \text{ mAh g}^{-1}$ . In comparison with the commercial  $\text{Fe}_2\text{O}_3$ ,  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  exhibits a high discharge capacity of  $1093.4 \text{ mAh g}^{-1}$  at the first cycle. Notably, this value is larger than the first charge capacity of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  ( $1006.2 \text{ mAh g}^{-1}$ ), which is likely due to the comparatively slower electrolyte saturation process of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . Moreover, due to the unstable electrode structure of the commercial  $\text{Fe}_2\text{O}_3$ , some unstable voltage points can be found at the end of delithiation process of the commercial  $\text{Fe}_2\text{O}_3$ , further demonstrating the pulverization and unstable electrode structure of  $\text{Fe}_2\text{O}_3$  that are caused by its volume expansion during cycles (Fig. 5b). The discharge capacity of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  at the second cycle are  $626.8 \text{ mAh g}^{-1}$  and  $882.7 \text{ mAh g}^{-1}$ , respectively. It is worthy note that the charge capacity of the first and second cycles are significantly larger than the discharge capacity. This phenomenon is because of new SEI formation on the surface of  $\text{Fe}_2\text{O}_3$  particles in initial several cycles. Meanwhile, the  $\text{Fe}_2\text{O}_3$  particles crack easily due to the unstable  $\text{Fe}_2\text{O}_3$  structure, leading to exposure of more fresh surfaces, responsible for further inducing formation of SEI and more charge consumption [49]. Under a current density of  $0.2 \text{ C}$  at the fourth cycle, the electrode structure of  $\text{Fe}_2\text{O}_3$  becomes stable but the discharge capacity decreases to  $482.7 \text{ mAh g}^{-1}$  because of the severe agglomeration of  $\text{Fe}_2\text{O}_3$  compared to  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  ( $893.3 \text{ mAh g}^{-1}$ ) (Fig. 5c).

The rate performance of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrodes was tested at various current densities from  $0.1 \text{ C}$  to  $2 \text{ C}$ . As



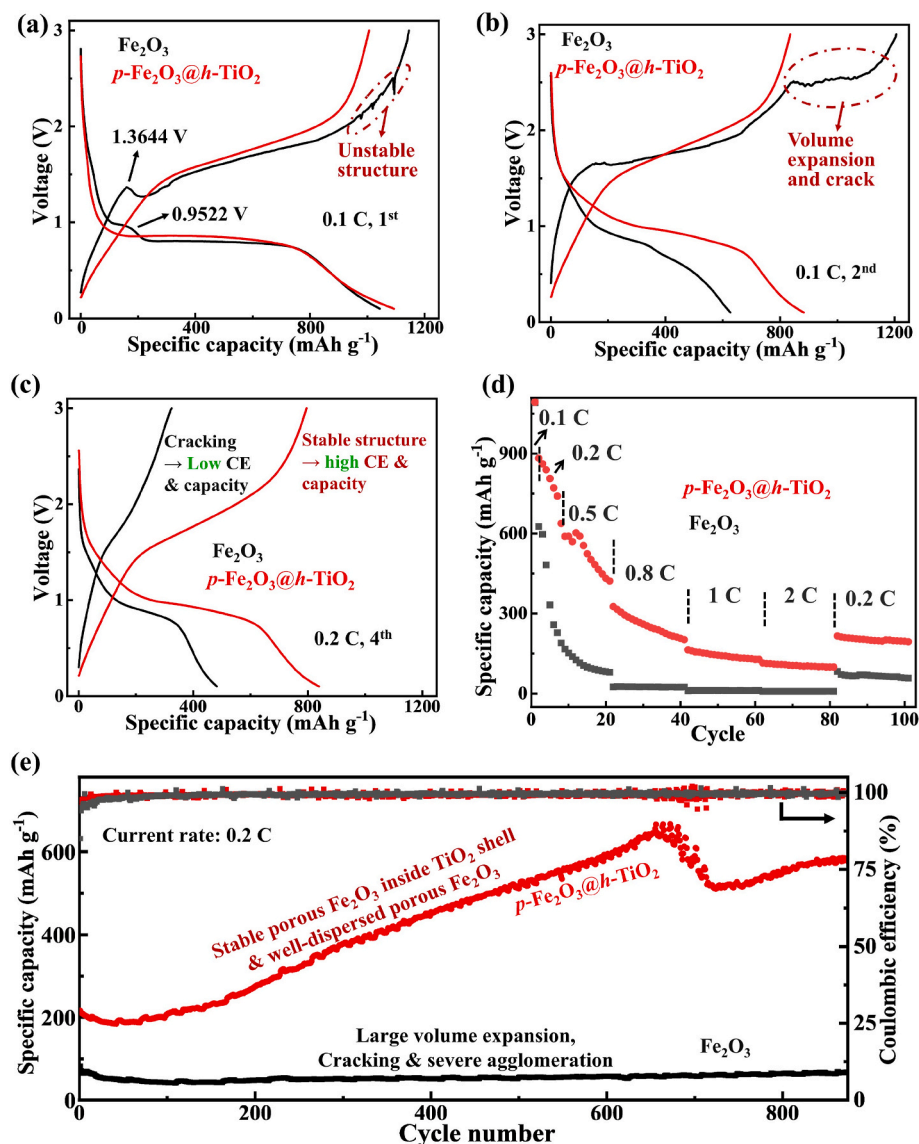


Fig. 5. Cycling performance of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrodes in half cells. Discharge/charge profiles for the (a) 1st, (b) 2nd and (c) 4th cycles at 0.1 C and 0.2 C, respectively. (d) Rate performance at 0.1, 0.2, 0.5, 0.8, 1 and 2 C. (e) Cycling performance at 0.2 C (1 C = 1007  $\text{mA g}^{-1}$ ).

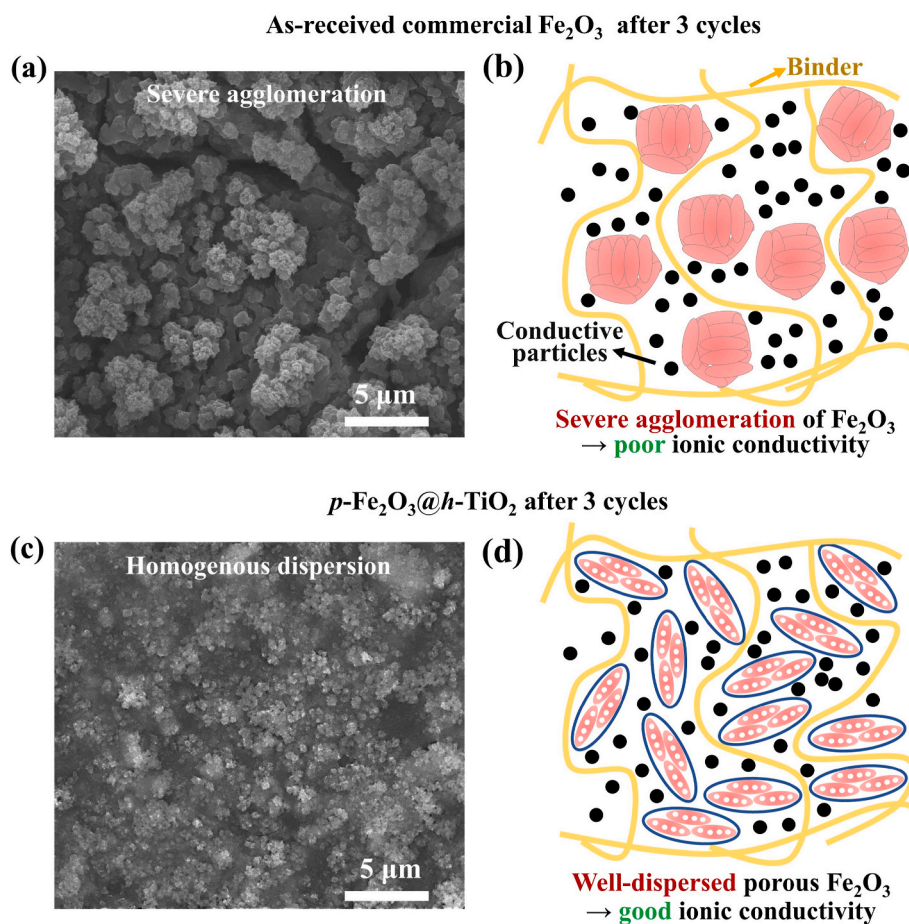
displayed in Fig. 5d, the commercial  $\text{Fe}_2\text{O}_3$  has a rapid capacity decay when the current density increases from 0.1 C (1043.8  $\text{mA h g}^{-1}$ ) to 0.2 C (167–626.8  $\text{mA h g}^{-1}$ ), which is due to the sluggish Li ion diffusion among agglomerated  $\text{Fe}_2\text{O}_3$  particles. In contrast,  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  builds high specific capacities of 1093.4  $\text{mA h g}^{-1}$  and 740.5–882.7  $\text{mA h g}^{-1}$  at 0.1 C and 0.2 C, respectively. Moreover, at 0.5 C, 0.8 C, 1 C and 2 C, the specific capacities of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  are  $\sim 502.4$   $\text{mA h g}^{-1}$ ,  $\sim 247.8$   $\text{mA h g}^{-1}$ ,  $\sim 141.1$   $\text{mA h g}^{-1}$  and  $\sim 102.4$   $\text{mA h g}^{-1}$ , respectively, while that of the commercial  $\text{Fe}_2\text{O}_3$  are  $\sim 105.2$   $\text{mA h g}^{-1}$ ,  $\sim 24.7$   $\text{mA h g}^{-1}$ ,  $\sim 11.3$   $\text{mA h g}^{-1}$  and  $\sim 8.1$   $\text{mA h g}^{-1}$ , respectively. When the current density decreases to 0.2 C again, the capacity of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  and the commercial  $\text{Fe}_2\text{O}_3$  increases to 201.4  $\text{mA h g}^{-1}$  and 67  $\text{mA h g}^{-1}$ , respectively. This significantly improved rate capacity of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  demonstrates its excellent Li-ion diffusion kinetics.

The long cycling performance was tested at a current density of 0.2 C. The evolution of specific capacities and their corresponding Coulombic efficiencies are shown in Fig. 5e. It is found the capacity of the commercial  $\text{Fe}_2\text{O}_3$  keeps at a very low value of  $\sim 41$   $\text{mA h g}^{-1}$ . In sharp contrast, the capacity of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  increases from 215.8  $\text{mA h g}^{-1}$  at the first cycle to 641.3  $\text{mA h g}^{-1}$  at the 666th cycle. The capacity increase is a common phenomenon for transition metal oxide anodes,

which can be ascribed to (1) the kinetic activation, (2) the enhanced interfacial lithium storage caused by the growth of SEI, and/or (3) the involvement of more inner active materials in electrochemical reactions after long cycles [49–51]. In the 666th–722nd cycles, due to some structure changes, the capacity of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  decreases to 516.3  $\text{mA h g}^{-1}$  at the 722nd cycle, and thereafter, slightly increases to 585.1  $\text{mA h g}^{-1}$  at the 874th cycle.

### 3.6. Characterization of cycled $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ electrodes

The morphology of the uncycled and cycled electrodes of the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  after 3 cycles was observed to study the improved electrochemical performance. For the uncycled electrodes (Fig. S6a, S6b, S7a, S7b), no specific difference can be found between the commercial  $\text{Fe}_2\text{O}_3$  and  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . Regarding the cycled commercial  $\text{Fe}_2\text{O}_3$  electrode, a rough surface can be found and large agglomerated particles are observed on the electrode (Fig. 6a, S6c). This result demonstrates the severe agglomeration of  $\text{Fe}_2\text{O}_3$  particles during cycling processes, which induces unstable electrode structure and poor ionic/electronic conductivity among active materials (Fig. 6b). On the contrary, the cycled  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrode shows a homogenous



**Fig. 6.** Morphology of (a) cycled commercial  $\text{Fe}_2\text{O}_3$  and (c)  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrodes after 3 cycles. Morphology evolution schematics of (b)  $\text{Fe}_2\text{O}_3$  and (d)  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  electrodes.

morphology, and the particles have a good dispersion after cycling process (Fig. 6c, S6d). It is confirmed that the  $\text{TiO}_2$  shell effectively prevents the agglomeration of  $\text{Fe}_2\text{O}_3$  and stabilizes the electrode structure of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  (Fig. 6d), improving the ionic/electronic conductivities, and thus, leading to excellent cycling performance.

#### 4. Conclusions

In conclusion, through a viable, “green” fabrication process with a high yield, we fabricate a hollow structure with a  $\text{TiO}_2$  shell encapsulating the porous  $\text{Fe}_2\text{O}_3$  ( $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ ) from as-received commercial  $\text{Fe}_2\text{O}_3$  particles (for cosmetic applications). The synthesis processes only include glucose as an “etching” agent and simple heating procedures without the involvement of any organic solvents or hard-controllable environments. Specifically, glucose and  $\text{Fe}_2\text{O}_3$  concentrations are optimized to effectively form a desirable hollow structure in high yields. Characterizations of the nanostructures, chemical compositions, crystallizations and thermal behaviors for the intermediate/final products demonstrate the successful synthesis of  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$ . The  $\text{TiO}_2$  shell effectively accommodates the volume change, decreases the pulverization, and lessens the agglomeration of the  $\text{Fe}_2\text{O}_3$  particles. Meanwhile, the porous  $\text{Fe}_2\text{O}_3$  core facilitates Li diffusion, decreasing the impedance of batteries. As a result, the  $p\text{-Fe}_2\text{O}_3@h\text{-TiO}_2$  anode displays an excellent capacity of  $664 \text{ mAh g}^{-1}$  (vs.  $58.7 \text{ mAh g}^{-1}$  of the commercial  $\text{Fe}_2\text{O}_3$ ) after 650 cycles at  $0.2 \text{ C}$ . This work provides an attractive “green” and efficient fabrication method of converting commercial abundant resources such as  $\text{Fe}_2\text{O}_3$  into effective electrode materials of energy storage systems.

#### Author contributions

Chenxu Wang: Writing-original manuscript, Experimental design, Investigation, Conceptualization, and Formal analysis. Pedaballi Sireesha: Writing-review & editing. Jing Shang: Raman & XRD testing, Review. John McCloy: Writing-review & editing, Supervision. Jin Liu: Writing - review & editing, Supervision, Funding acquisition. Wei-Hong Zhong: Writing - review & editing, Supervision, Funding acquisition.

#### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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#### Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.ceramint.2023.07.234>.

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