ELECTROCHEMISTRY

Zinc-copper dual-ion electrolytes to suppress dendritic growth and increase anode utilization in zinc ion capacitors

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The main bottlenecks that hinder the performance of rechargeable zinc electrochemical cells are their limited cycle lifetime and energy density. To overcome these limitations, this work studied the mechanism of a dual-ion Zn-Cu electrolyte to suppress dendritic formation and extend the device cycle life while concurrently enhancing the utilization ratio of zinc and thereby increasing the energy density of zinc ion capacitors (ZICs). The ZICs achieved a best-in-class energy density of 41 watt hour per kilogram with a negative-to-positive (n/p) electrode capacity ratio of 3.10. At the n/p ratio of 5.93, the device showed a remarkable cycle life of 22,000 full charge-discharge cycles, which was equivalent to 557 hours of discharge. The cumulative capacity reached ~581 ampere hour per gram, surpassing the benchmarks of lithium and sodium ion capacitors and highlighting the promise of the dual-ion electrolyte for delivering high-performance, low-maintenance electrochemical energy supplies.



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INTRODUCTION

Metal ion capacitors are hybrid electrochemical cells that bridge the divide between batteries and electrochemical capacitors, enabling them to provide high energy densities at rapid charging or discharging rates. These devices combine a redox metal anode, similar to that found in batteries, to enhance the capacity for charge storage and an electric double-layer cathode that allows fast kinetics and sustains high power density. The first metal ion capacitors were based on lithium (1) and sodium ions (2-4), but potential safety hazards associated with these metals prompted the search for other alternatives (5). In particular, zinc ion capacitors (ZICs) emerge as an appealing choice with advantages of environmental safety, a high theoretical capacity of 820 mAh/g as a divalent system, and an abundance of zinc reserves unaffected by geopolitical factors (6–8). However, zinc ion devices have been limited by instability upon redox cycling and low utilization of the anode, which substantially reduce the specific energy of the devices and hinder their commercial viability (9-13).

The challenges with cycling stability and low utilization of the anode are intertwined; as the amount of accessible zinc is depleted with cycling degradation, prior works compensated for it by using thick foils. This approach led to only a small fraction of the zinc being cycled, i.e., operating at low utilization, typically below a few percent (11). The excessive capacity of the anode creates a large imbalance in electrode utilization and results in poor energy density in a full cell, rendering it impractical for commercialization. Therefore, it is crucial to eliminate the cause of cycling loss to enable high utilization, ideally to achieve a balanced n/p ratio of 1, and achieve competitive metrics, targeting >40 Wh/kg and more than 2000 redox cycles (9, 11).

The dominant degradation mechanism involves the formation of zinc dendrites during plating and stripping processes on the anode.

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Grain growth along (101) and (100) planes of the hexagonal closed pack structure of zinc tends to be randomly oriented (14, 15). Upon redox cycling, the electric field concentration on the tips of grains would accelerate the deposition of zinc ions and lead to dendritic protrusions that can break off or even pierce the separator and cause catastrophic short circuits. To mitigate dendritic problems, researchers have added electrolyte additives (16-21) or ion distributors (22-26)to redirect zinc concentration for more uniform deposition, but these two methods slowed down the redox kinetics and consequently reduced the power densities. A third method that avoided the tradeoff with kinetics involved promoting zinc deposition on its (002) plane to favor a planar orientation (27–30). For example, it was shown that Cu (100) substrates (14) would enhance planar grain growth and that CuZn alloys (10, 31) suppress dendrites due to its low surface energy for zinc ions to bind evenly over the surface. While these surface modifications initially reduce dendrite formation close to the substrate, the effectiveness of the CuZn layer would diminish as thicker layers of zinc are plated. Thus, the anode loading is limited to a low areal capacity; otherwise, dendrite formation would resume and shorten the cycle life.

To suppress dendrites and enable high loading and utilization, our strategy is to design a zinc-copper dual-ion electrolyte for use with zinc anodes as shown in Fig. 1. The incorporation of copper ions in the electrolyte facilitates CuZn alloy deposition during the anode plating/stripping processes. In contrast to previous methods where alloys on the substrate surface would be screened by newly deposited zinc, here, the CuZn is replenished from the electrolyte to maintain the preference for planar grain growth. The potential use of copper ions in electrolytes might have been previously overlooked because of detrimental copper oxide formation in aqueous electrolyte; here, we chose nonaqueous solvents (32, 33) to circumvent the oxide problem. The plating/stripping overpotentials are analyzed to reveal the mechanism for preventing dendrites at the anode. Using the dual-ion electrolyte, ZICs consisting of activated carbon at the cathode and electroplated zinc at the anode were operated for 22,000 redox cycles (equivalent to 557 hours) to evaluate the cell stability and determine the cumulative capacity before cell shorting. The ZICs were fabricated with high areal capacities of 0.74 mAh/cm²

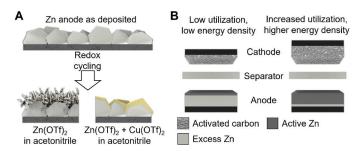


Fig. 1. Issues of dendrites and low utilization at the anode in zinc ion devices.

(A) Concept of using a dual-ion electrolyte to suppress dendrite formation.

(B) Minimizing excess zinc capacity by plating and stripping a higher portion of the anode to increase areal energy densities.

and better balanced n/p ratios to showcase their performance under practical conditions and to allow for comparisons with state-of-the-art metal ion capacitors.

RESULTS AND DISCUSSIONS

Evolution of the anode composition and surface morphology with redox cycling

Figure 2 presents the changes in morphology and composition observed at the anode, following galvanostatic charge-discharge (GCD) of the ZICs between 0 and 2 V at a current density of 25 mA/cm². The ZICs were coin cells prepared according to the descriptions in Methods, and, after GCD cycling, the cells were disassembled to image the anodes. Before any redox cycle, the as-fabricated zinc anode showed an average surface roughness (S_a) of 1.3 μm, with several protruded features more than 15 µm tall in the area scanned by the three-dimensional (3D) optical profiler. For the cell with 0.5 M zinc triflate electrolyte, the anode roughness increased to 2.3 µm after 1600 cycles, and the cell was short circuited because of some zinc dendrites piercing through the separator. Meanwhile, for the cell with the dual-ion Zn-Cu electrolyte [0.5 M zinc triflate Zn(OTf)₂ and 0.1 M copper triflate Cu(OTf)₂], the anode maintained a roughness comparable to the initial surface in Fig. 2A after undergoing 1600 cycles. With the Zn-Cu electrolyte, the cell continued to function even after 10,000 cycles, with a roughness of 2.0 µm as depicted in fig. \$1.

Figure 2B shows the x-ray diffraction patterns of the anodes after GCD cycling in either the Zn-only or Zn-Cu electrolyte. The asfabricated zinc film showed a dominant peak at 43.2° representing the Zn(101) crystal orientation. For the anode after 1000 cycles in the Zn-only electrolyte, the diffraction pattern remained similar to the initial measurement. Whereas after 1000 cycles in the Zn-Cu electrolyte, the anode showed a slight increase in the peak at 36.3°, indicating crystal growth in the Zn(002) orientation, which would favor planar grain deposition (14) as illustrated in Fig. 2C. As GCD proceeded to 5000 cycles, a peak at 41.8° emerged and corresponded to the incorporation of CuZn₅ alloy in the anode. Subsequently at 10,000 cycles, the CuZn₅ peak surpassed the intensity of the Zn(101) peak, showing the substantial involvement of the alloy in long-term cycling processes.

The scanning electron microscopy (SEM) images in Fig. 2 (D to G) compared the anode surface morphologies and showed the extent of dendrite formation in Zn-only and Zn-Cu electrolytes. After 1000 GCD cycles in the Zn-only electrolyte, the anode in Fig. 2E was covered

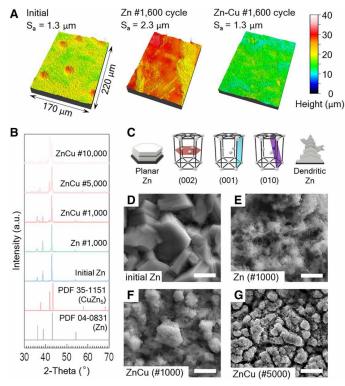


Fig. 2. Surface roughness and composition analyses. All cycles were carried out on full cells at a current density of 25 mA/cm². (A) Surface morphologies of Zn anodes after 1600 redox cycles in either Zn or Zn-Cu electrolyte. (B) X-ray diffraction patterns of anodes as a function of redox cycles and electrolytes. The reference powder diffraction files (PDF) are included for Zn and ZnCu₅. (C) Various crystallographic orientations of Zn. (D to G) SEM images of anode surfaces after cycling in different electrolytes. Scale bars, 2 µm.

by dendrites, and the initially large grains were stripped away. The anode cycled in Zn-Cu electrolyte showed that the stripping and plating process introduced submillimeter-scale roughness, but the granular structures were retained after 1000 GCD cycles, as seen in Fig. 2F. The CuZn alloy was detected in the anode, as evident from the weight percent of copper (11%) to zinc (89%) measured by energy dispersive x-ray spectroscopy in fig. S2. After 5000 cycles, the grain sizes were further reduced, but dendrites were not prevalent in Fig. 2G. By 10,000 cycles, the depletion of Cu ion in the anode was observed, where the percentage of Cu was only 0.5 wt % (fig. S2). Because of the Cu depletion in the electrolyte, the suppression of dendrite formation became ineffective. However, because of the underlying CuZn alloy, the growth of dendrites was isotropic and less inclined to develop only vertically toward the separator, as in the case of Fig. 2E. Consequently, the ZIC with the Zn-Cu electrolyte was not short circuited by the 10,000 cycles and continued to work up to 22,000 cycles with the anode at the n/p ratio of 5.93.

Since the ZICs were pseudocapacitive, the device current was influenced by both capacitive and diffusion-controlled factors. To separate the capacitive and diffusion-controlled contributions, we used the relation (34-37) $i/v^{0.5} = k_1 v^{0.5} + k_2$, where k_1 is the capacitive-controlled constant, k_2 is the diffusion-controlled constant, i is the current, and v is the scan rate. This relation was fitted to the total current; an example is shown in the inset of fig. S3A. For

the ZICs in this work, fig. S3 (B and C) shows that the contribution from capacitive current was at least four times higher than the diffusion-controlled current, indicating that the charge storage mechanism was dominantly capacitive and would support fast kinetics and high-power output.

Mechanisms of nucleation and growth in Zn versus Zn-Cu electrolyte

The zinc nucleation and grain growth mechanisms (38-41) in the two electrolytes were revealed by examining the changes of the anode potential during the plating and stripping processes with respect to the reference electrode of $\rm Zn/Zn^{2+}$. The examples in Fig. 3A showed that an overpotential up to -0.2 V was needed for zinc plating at a current density of 25 mA/cm². In the Zn-only electrolyte, there was a rapid jump of potential from -0.1 to -0.2 V as the current was applied, and then the potential change was relatively small, below 20 mV over a period of 25 s. The abrupt initial increase in potential was linked to the nucleation step of forming zinc clusters. The subsequent change in potential was referred to as the plateau overpotential (38) associated with the growth of already existing nuclei. Since the plateau overpotential was small relative to that of nucleation, this observation indicated that addition of zinc to

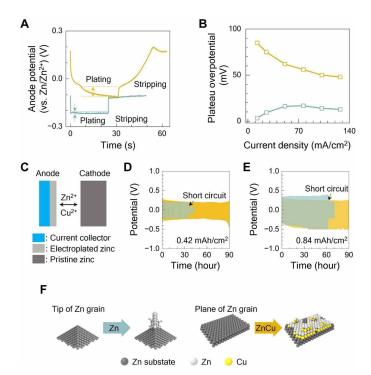


Fig. 3. Effects of electrolytes on anode potential. Blue, Zn-only electrolyte; orange, Zn-Cu electrolyte. (**A**) Anode potential change measured with a three-electrode configuration at a current density of 25 mA/cm². The plateau overpotentials are labeled by the arrows. (**B**) The plateau overpotentials of Zn anodes in Zn-Cu and Zn-only electrolytes as a function of charging current densities. (**C**) Device structure of Zn/Zn symmetric cell. Potential change with cycling at a current density of 25 mA/cm² of Zn/Zn symmetric cells with a cutoff capacity of (**D**) 0.42 and (**E**) 0.84 mAh/cm² in the Zn-Cu electrolyte. The cells shorted in Zn electrolyte but continued cycling in Zn-Cu electrolyte. (**F**) Schematics of grain growth mechanisms of Zn and CuZn on the anode surface.

preexisting nuclei was more favorable and had a lower energy barrier than forming new clusters.

In the Zn-Cu electrolyte, upon applying the deposition current, the anode potential was initially at 0.2 V and dropped to -0.03 V within the first 5 s. This change was attributed to the process of reducing copper ions. As the deposition progressed, the potential gradually shifted from -0.03 to -0.115 V, resulting in a plateau overpotential of ~75 mV. The relatively large shift in potential suggested that additional zinc plating in the Zn-Cu electrolyte involved both nucleation and growth and that the preference for zinc growth over nucleation was not as pronounced as in Zn-only electrolyte.

The radius of electrodeposited zinc clusters can be estimated by using the Gibbs free energy equation for nucleation (38): $\Delta G_{nucleation} = -(4/3)\pi r^3 \Delta G_V + 4\pi r^2 \Upsilon, \text{ where } r \text{ is the radius of spherical nuclei, } \Delta G_V \text{ is the free energy change per volume, and } \Upsilon \text{ is the surface energy between the electrolyte and the anode. The radius of a cluster is assumed to be at an equilibrium point when the bulk free energy <math>(-4/3\pi r^3\Delta G_V)$ equals to the surface free energy $(4\pi r^2\Upsilon)$, that is, when $\Delta G_{nucleation} = 0$. The deposition overpotential η is related to ΔG_V by $= F|\eta|/V_m$, where F is the Faraday's constant and V_m is the molar volume (42) of zinc $(V_m = 9.157 \times 10^{-6} \text{ m}^3/\text{mol})$. Solving for the cluster radius r when $\Delta G_{nucleation} = 0$, the expression becomes

$$r = \frac{3\Upsilon}{\Delta G_V} = \frac{3\Upsilon V_m}{F|\eta|} \tag{1}$$

The expression demonstrates the inverse correlation between the cluster radius and the overpotential. As shown in Fig. 3B, the plateau overpotential of the anode in the Zn-Cu electrolyte was higher than in the Zn-only electrolyte, while the surface energy was slightly lower in the Zn-Cu system (measurements provided in the Supplementary note). From the calculations included in Supplementary note based on fig. S4, the cluster radius was estimated to be 1.63 nm in the Zn-Cu electrolyte and 12.1 nm in the Zn-only electrolyte. The smaller cluster radius in the Zn-Cu electrolyte facilitated more uniform, planar coverage compared to the large nuclei that led to vertical dendritic growth as shown in Fig. 3F.

To check the reversibility of zinc anode in each electrolyte, Zn/Zn symmetric cells in Fig. 3C were tested and shown to reach the cutoff capacity of 0.42 and 0.84 mAh/cm². The higher cutoff capacity was achieved by increasing the Cu concentration from 0.1 to 0.2 M in the Zn-Cu electrolyte. In Fig. 3 (D and E), the cells with Zn-only electrolyte were short circuited after 36 and 62 hours. Meanwhile, the symmetric cells with Zn-Cu electrolyte remained functional for 90 hours, and the overpotential shifted only after ~1000 cycles. Thus, the Zn-Cu electrolyte facilitated better cycling stability compared to Zn-only electrolyte across different cutoff capacities.

Performance comparisons of ZICs with Zn versus Zn-Cu electrolyte

Figure 4 displays the characteristics of ZICs using the Zn-only (blue curves) and the Zn-Cu (orange curves) electrolytes. The cyclic voltammetry current-voltage characteristics of the Zn-Cu device exhibited a more square shape compared to that of the Zn-only device, resulting in 14% higher capacitance of 1.6 F for Zn-Cu and 1.4 F for Zn-only, from Fig. 4 (A and C), respectively. In Fig. 4 (B and D), the GCD data at current densities \geq 22.5 mA/cm² showed longer

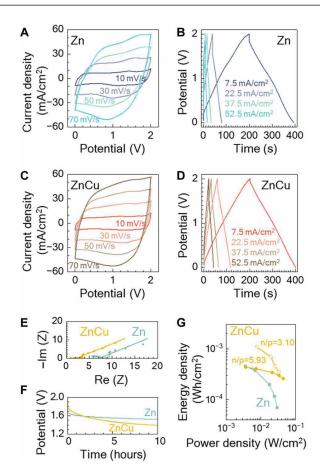


Fig. 4. Performance comparison of ZICs with different electrolytes. Cyclic voltammetry was measured at scan rates of 10 to 70 mV/s with (**A**) Zn and (**C**) Zn-Cu electrolytes. GCD measurements were taken at current densities of 7.5 to 52.5 mA/cm² with (**B**) Zn and (**D**) Zn-Cu electrolytes. (**E**) Nyquist plots of capacitors in different electrolytes in the frequency range of 0.01 Hz to 100 kHz. (**F**) After being charged to 2 V and set to the open-circuit state, the potential decay of two cells with different electrolytes. (**G**) Energy densities versus power densities of the capacitors with the Zn or Zn-Cu electrolyte.

discharging times and therefore higher capacities for the Zn-Cu capacitor than the Zn-only device. At a current density of 7.5 mA/cm², while both types of capacitors showed similar discharging times, the Zn-Cu capacitor displayed a smaller voltage drop at the start of discharge. This observation was further supported by electrochemical impedance measurements in Fig. 4E, where the equivalent series resistance (ESR) was three times lower in the Zn-Cu cell than Zn alone.

The self-discharge (43) characteristics in Fig. 4F were measured after the capacitors were charged to 2 V, and the open-circuit voltage was sampled once every 0.1 s. Since the electrodes were made with the same materials and loading, the differences in self-discharge were attributed to the influence of electrolytes. The voltage decay was slightly worse in the Zn-Cu device with 0.6 V drop, in contrast to the 0.5 V drop in the Zn-only device after 10 hours. The reason for higher self-discharge in Zn-Cu electrolyte was due to the spontaneous reaction between zinc and copper ions. As copper ions have a higher standard cell potential (E^0 of $Cu^{2+}+2e^- \rightarrow Cu$ is 0.34 V) compared to zinc (E^0 of $Zn^{2+}+2e^- \rightarrow Zn$ is -0.76 V), the reduction of

copper ions by oxidizing zinc occurred spontaneously. Consequently, a portion of the zinc electrode was stripped away and manifested as the voltage decay. Nonetheless, the reaction between copper ions and the zinc electrode did reach equilibrium after 10 hours because the increased Cu concentration on the anode surface changed the surface redox potential, stabilizing the anode and preventing further electrolyte reaction as seen in the cell voltage plateau in Fig. 4F.

The areal energy and power densities of the Zn-Cu and Zn-only capacitors are summarized in Fig. 4G. The cells showed similar energy densities at low power $< 0.02~\mathrm{W/cm^2}$, but for high-power charging/discharging, the Zn-Cu cell with its improved ESR maintained the energy densities better than the Zn-only cell.

The loading of active materials at the cathode and the anode should be matched in their capacities to avoid unused materials and maximize the energy density. However, with ZICs, the anode typically contained excess capacity compared to the cathode. In this work, we mitigated this imbalance and decreased the n/p ratios to 3.10 by increasing the loading of activated carbon per unit area at the cathode. The calculations of n/p ratio and cumulative capacity are defined in Methods. The ideal n/p ratio is 1 to maximize cathode and anode balance. As shown in Fig. 4G at the power density of 22 mW/cm², the energy density was improved to 0.74 mWh/cm² at the n/p ratio of 3.10, compared to 0.34 mWh/cm² at the n/p ratio of 5.93. The areal capacity was doubled by improving the n/p ratio.

Comparison of metal ion capacitors on stability and cumulative capacity

While the smaller n/p ratio enhanced the energy densities, it was observed to trade-off with redox cycling stability. Figure 5A presents the capacity retention of the devices as a function of the n/p ratio. For the capacitor at the n/p ratio of 5.93, the Zn-Cu electrolyte had suppressed dendritic formation and allowed the cell to retain 90% of its original capacity after 25,000 GCD cycles. However, at the n/p ratio of 3.10, the cell retention dropped below 90% by 6700 cycles. This degradation with decreasing n/p ratio was partially caused by the depletion of copper ions in the electrolyte, leading to the reappearance of dendrites, which caused short circuits.

Figure 5B demonstrates that the cycle life and cumulative capacity of Zn-Cu capacitors were improved by adjusting the copper ion concentration in electrolyte (0.1 M for the n/p ratio of 5.93 and 0.2 M for the n/p ratio of 3.10). We note that there was an optimal concentration of copper ion for different n/p ratios. With a decreasing n/p ratio, more zinc cations were dissolved into the electrolytes as the cell discharged; thus, there was an increasing concentration of Zn. To match that Zn increase as the n/p ratio decreased, the concentration of Cu ions should be increased to provide sufficient Cu for ZnCu alloy formation. However, when the copper ion concentration was increased beyond 0.2 M, the large extent of spontaneous copper reduction at the anode interfered with the zinc plating and stripping process, and, therefore, we kept the maximum copper ion concentration to be 0.2 M in the electrolyte.

The cumulative capacities of ZICs generally showed a similar tendency with n/p ratio as depicted in Fig. 5C. In prior works as listed in Table 1, the cumulative capacity of (44) reached up to 4.5 Ah/cm² due to dendrite suppression, but the anode was at very large excess with the n/p ratio = 55.6, meaning that a substantial portion of the anode remained unused and ultimately not contributing to energy storage. For a more balanced n/p ratio of 3.88 from (10), the reported cumulative capacity was below 3.2 Ah/cm² on the

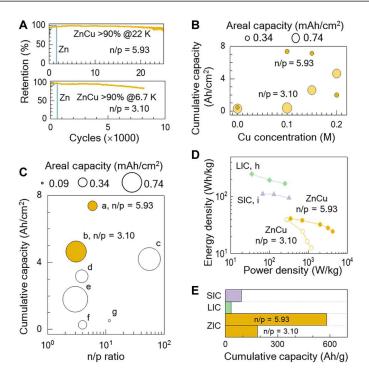


Fig. 5. Comparisons of metal ion capacitors on cycling stability and cumulative capacity. Redox cycling of ZICs was carried out between 0 and 2 V at a current density of 25 mA/cm². (A) Capacity retention for the Zn-only or Zn-Cu electrolyte, for cells with different n/p ratios. (B) Cumulative capacities as a function of copper ion concentration in the Zn-Cu electrolyte. (C) Cumulative capacities as a function of n/p ratios. Black circles are from state-of-the-art references as listed in Table 1. Orange circles are from the capacitors with Zn-Cu electrolyte in this work. (D) Gravimetric energy and power densities of metal ion capacitors: lithium (LIC), sodium (SIC), and zinc with the Zn-Cu electrolyte in this work. (E) Gravimetric cumulative capacities of metal-ion capacitors. The references for SIC and LIC are provided in Table 1.

Table 1. Structure and metrics of metal ion capacitors. AC, activated carbon. DES, deep eutectic solvent. AN, acetonitrile. DMF, dimethylformamide. ME, methanol. NHP, ammonium dihydrogen phosphate. EC, ethylene carbonate. DEC, diethyl carbonate. DMC, dimethyl carbonate.

	Electrode (Anode Cathode)	Electrolyte	Current density (A/g)	Areal capacity (mAh/cm²)	n/p ratio	Cumulative capacity (Ah/cm²)	Ref.
a	Zn AC	0.5 M Zn(OTf) ₂ and 0.1 M or 0.2 M Cu(OTf) ₂ in AN	2.5	0.340	5.93	7.4	This Work*
b	Zijji/C		1.3	0.738	3.10	4.7	
С	DES-Zn AC	ZnSO ₄ in H ₂ O	4	0.45	3.88	3.2	(10)
d	Zn AC	ZnSO ₄ in H ₂ O/ DMF	0.5	1.00	55.6	4.2	(44)
e	Zn AC	ZnSO ₄ in H ₂ O/ME	2	0.9	3	1.8	(45)
f	Zn AC	ZnSO ₄ in H ₂ O/ NHP	0.5	0.3	4	0.27	(46)
g	Zn AC	ZnSO ₄ in H ₂ O	4	0.087	11.5	0.5	(26)
h	LiFe₃O₄/G G- raphene	LiPF ₆ in EC/DEC/ DMC	2	205 mAh/g	-	31 Ah/g	(47)
i	Na-C AC	NaClO₄ in EC/ DEC	5	107 mAh/g	-	90 Ah/g	(4, 48)

^{*}The cumulative capacity was calculated from the sum of GCD cycles for which the Coulombic efficiency was over 99%, and the capacity retention exceeded 90%.

 $CuZn_4$ alloy substrate with a lifetime of ~7000 cycles (250 hours). In this study, by replenishing the CuZn alloy with Zn-Cu electrolyte, the cumulative capacity of our devices surpassed previous state-of-the-art records and achieved 7.4 Ah/cm² at n/p ratio = 5.93 and

 4.7 Ah/cm^2 at n/p = 3.10. The cycle lifetime was 22,000 cycles (equivalent 557 hours) and 6700 cycles (347 hours), respectively.

The gravimetric energy and power densities of our ZICs with the Zn-Cu electrolyte were compared to those of lithium and sodium

	Components	Dimensions	Notes	
Fig. 3, A and B	 Cathode loading of activated carbon: 8.24 mg 	Round samples with 1-cm diameter	Zn-Cu electrolyte was 0.5 M Zn(OTf) ₂ and 0.1 M Cu(OTf) ₂	
	Anode loading of Zn: 1.62 mg			
•	Cathode loading of Zn: 10.9 mg	•	Zn-Cu electrolyte was 0.5 M Zn(OTf); and 0.1 M Cu(OTf) ₂ or 0.2 M Cu(OTf);	
Fig. 3, C and D	• Anode loading of Zn: 2.74 mg	Round samples with 1.3-cm diameter		
	• 160 μl electrolyte			
	 Cathode loading of activated carbon: 14 mg 		Zn-Cu electrolyte was 0.5 M Zn(OTf) ₂ and 0.1 M Cu(OTf) ₂	
Fig. 4	• Anode loading of Zn: 2.74 mg	Round samples with 1.3-cm diameter		
	• 160 μl electrolyte			
	 Cathode loading of activated carbon: 14 mg (n/p = 5.93) or 34 mg (n/p = 3.10) 		Calculations of gravimetric energy/	
	• Anode loading of Zn: 2.74 mg			
Fig. 5	• 160 μl electrolyte	• 160 µl electrolyte Round samples with 1.3-cm diameter		
	• Separator: 13.5 mg		carbon cloth or separator.	
	• Carbon cloth current collectors: 16 mg total			

ion capacitors in Fig. 5D. At a power density of 300 W/kg, the ZICs demonstrated an energy density of 41 Wh/kg for the cell at the n/p ratio of 5.93. This energy density was calculated on the basis of active materials, which were the sum of zinc and activated carbon. When including the weights of current collector and separator components, the energy density was 14.9 Wh/kg, still within an order of magnitude of the level practical for commercialization (>40 Wh/kg) according to (9, 11). While the energy densities of ZICs were lower than their lithium and sodium counterparts, the power densities of ZICs were superior, reaching up to 3.5 kW/kg. Moreover, the cumulative capacities of ZICs were far higher than lithium and sodium ion capacitors, better by 2- to 18-fold as shown in Fig. 5E, because of the excellent cycling stability of ZICs when dendritic formation was suppressed with the appropriate choice of electrolyte.

The remarkable cumulative capacity demonstrated by our ZICs indicates that this class of hybrid devices effectively combines the desirable attributes of electrochemical capacitors, such as the long cycle life and high-power densities, with energy densities approaching those of batteries. This combination is very attractive as power sources for autonomous electronics and Internet-of-Things applications because a long cycle life is crucially needed to lower maintenance costs by avoiding the need for frequent battery replacement. The long cycle lifetime is particularly advantageous when considering large-scale networks consisting of millions of sensors, where the maintenance burden could quickly become unsustainable if frequent battery replacements were required.

In summary, this work demonstrated an easy approach to significantly improve the cycle lifetime and energy density of ZICs by using an electrolyte that facilitated CuZn alloy deposition to suppress dendrites during redox cycling. The characterization of grain orientations and overpotentials during the growth plateau phase revealed the reduced energy barrier for planar growth under the Zn-Cu electrolyte, clarifying the fundamental origins of the enhanced

cell stability. ZICs with an n/p ratio of 3.10 showed a high energy density of 41 Wh/kg and capable of enduring 6700 GCD cycles, equivalent to 347 hours before the capacity dropped below 90%. The cumulative capacities of ZICs surpassed previous benchmarks including those of lithium and sodium ion capacitors. The Zn-Cu electrolyte in this study is very promising for implementing robust ZICs for high-performance, low-maintenance electrochemical energy supplies.

METHODS

Preparation of electrolytes

For the Zn-Cu electrolyte, 0.5 M of zinc trifluoromethanesulfonate $[Zn(OTf)_2$, Sigma-Aldrich, 98%] and 0.1 or 0.2 M of copper trifluoromethanesulfonate $[Cu(OTf)_2$, Sigma-Aldrich, 98%] were dissolved in acetonitrile (ACN, Thermo Fisher Scientific, 99.9%) solvent at room temperature. For the Zn-only electrolyte, it was 0.5 M of $Zn(OTf)_2$ dissolved in ACN.

Fabrication of ZICs

For the anode, zinc was deposited on a graphite sheet with electroplating method under $12.5~\text{mA/cm}^2$ for 10~min. A 0.5~M of zinc triflate electrolyte was used for electroplating solution, and the deposited zinc film was roughly 5 μ m thick. The Zn/Zn symmetric cell was fabricated using a CR2032 coin cell package. A pristine Zn foil (10- μ m thickness with a diameter of 1.3~cm) and the electroplated zinc electrode were used for cathode and anode, respectively. For the zinc-ion capacitors, the cathodes were activated carbon (Calgon Carbon, YP-50F), conductive carbon black (MTI Corporation), and polyvinylidene fluoride (Solvay PVDF 5130) mixed at a ratio of 8:1:1. The mixture was suspended in 1-methyl-2-pyrrolidinone (Thermo Fisher Scientific, >99.5%) to make a solution of 16.7% solids by weight. The solution was deposited over an area of 1.33 cm² on

the carbon cloth (AvCarb, 1071 HCB) with a loading of 10.5 to 25.5 mg/cm^2 . The electrode was annealed at 100°C . The anode and cathode were separated by a glass microfiber separator (Cytiva, Whatman GF/A). After adding 160 μ l of the electrolyte, the sandwich structure was encapsulated in coin cells (CR2032) by a hydraulic crimping machine (MTI Corporation, MSK-110). The specific details for the cells used in each figure are listed in Table 2. Each measurement was done at least three times and on four samples.

Material and electrochemical characterizations

The morphology change was measured by SEM (FEI Apreo) at 20 kV. The arithmetic mean height was measured by 3D optical profiler (Filmetrics Profilm 3D). The x-ray diffraction patterns were recorded by Rigaku Miniflex XRD at Cu. The measurements of Zn/Zn symmetric cells were conducted by using a galvanostat (Neware) based on two electrode configurations with a cutoff capacity of 0.42 and 0.84 mAh/cm² at a current density of 25 mA/cm². Other electrochemical measurements were conducted by a potentiostat (SP-200, Bio-Logic). Cyclic voltammetry was scanned between 0 and 2 V with the voltage scan rate range of 1 to 70 mV/s. GCD was conducted under constant current densities in the range of 7.5 to 52.5 mA/cm². Electrochemical impedance spectroscopy was performed in the frequency range of 0.1 Hz to 200 kHz at 0 V. Cycling stability measurements were conducted by Neware battery tester.

The energy density E was calculated from GCD characteristics based on the equation of $E = (\int VIdt)/A$ or $E = (\int VIdt)/m$, where A is the electrode area, m is the loading of cathode and anode, V is the potential, and I is the applied current. The power density P was calculated with the equation of P = E/t, where t is the discharging time.

The capacitance was calculated by $C = \frac{1}{\Delta V_V} \int_{V_1}^{V_2} i \ dV$. Here V_1 and

 V_2 are the starting and ending potentials in the discharge portion of the measurement, i is the current at each potential, $\Delta V = V_2 - V_1$ is the potential window, and ν is the voltage scan rate.

The n/p ratio was calculated through dividing the capacity of the zinc anode by the discharge capacity of the cathode. The capacity of the zinc anode was calculated by multiplying the measured weight of the electrodeposited zinc with the theoretical gravimetric capacity of zinc: $Capacity_{anode} = \frac{820 \text{ mAh}/\text{g} \times w_{anode}}{A}$, where w_{anode} is the anode Zn loading, and A is the area of the anode. The discharge capacity of the cathode was extracted using the equation $Capacity_{cathode} = \frac{I \times t_d}{A}$, where t_d is the discharging time at a current density of 25 mA/cm², and A is the area of the cathode.

The cumulative capacity was calculated from the summation of discharge capacity ($\sum_{i=1}^{n} discharge \ capacity$) for the number of cycles for which the Coulombic efficiency was over 99%, and the capacity retention exceeded 90%. The GCD data are included in fig. S6.

Supplementary Materials

This PDF file includes: Notes S1 to S3 Figs. S1 to S6

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