

Dynamic Electrodeposition on Bubbles: An Effective Strategy toward Porous Electrocatalysts for Green Hydrogen Cycling

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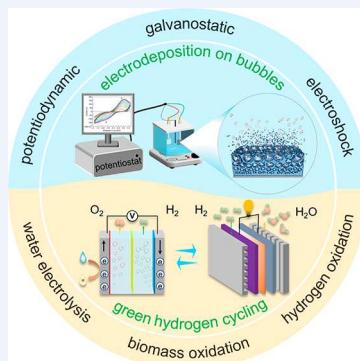
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CONSPPECTUS: Closed-loop cycling of green hydrogen is a promising alternative to the current hydrocarbon economy for mitigating the energy crisis and environmental pollution. It stores energy from renewable energy sources like solar, wind, and hydropower into the chemical bond of dihydrogen (H_2) via (photo)electrochemical water splitting, and then the stored energy can be released on demand through the reverse reactions in H_2 – O_2 fuel cells. The sluggish kinetics of the involved half-reactions like hydrogen evolution reaction (HER), oxygen evolution reaction (OER), hydrogen oxidation reaction (HOR), and oxygen reduction reaction (ORR) limit its realization. Moreover, considering the local gas–liquid–solid triphase microenvironments during H_2 generation and utilization, rapid mass transport and gas diffusion are critical as well. Accordingly, developing cost-effective and active electrocatalysts featuring three-dimensional hierarchically porous structures are highly desirable to promote the energy conversion efficiency. Traditionally, the synthetic approaches of porous materials include soft/hard templating, sol–gel, 3D printing, dealloying, and freeze-drying, which often need tedious procedures, high temperature, expensive equipment, and/or harsh physiochemical conditions. In contrast, dynamic electrodeposition on bubbles using the *in situ* formed bubbles as templates can be conducted at ambient conditions with an electrochemical workstation. Moreover, the whole preparation process can be finished within minutes/hours, and the resulting porous materials can be employed as catalytic electrodes directly, avoiding the use of polymeric binders like Nafion and the consequent issues like limited catalyst loading, reduced conductivity, and inhibited mass transport. In this Account, we summarize our contributions to the dynamic electrodeposition on bubbles toward advanced porous electrocatalysts for green hydrogen cycling. These dynamic electrosynthesis strategies include potentiodynamic electrodeposition that linearly scans the applied potentials, galvanostatic electrodeposition that fixes the applied currents, and electroshock which quickly switches the applied potentials. The resulting porous electrocatalysts range from transition metals to alloys, nitrides, sulfides, phosphides, and their hybrids. We mainly focus on the 3D porosity design of the electrocatalysts by tuning the electrosynthesis parameters to tailor the behaviors of bubble co-generation and thus the reaction interface. Then, their electrocatalytic applications for HER, OER, overall water splitting (OWS), biomass oxidation (to replace OER), and HOR are introduced, with a special emphasis on the porosity-promoted activity. Finally, the remaining challenges and future perspective are also discussed. We hope this Account will encourage more efforts into this attractive research field of dynamic electrodeposition on bubbles for various energy catalytic reactions like carbon dioxide/monoxide reduction, nitrate reduction, methane oxidation, chlorine evolution, and others.



KEY REFERENCES

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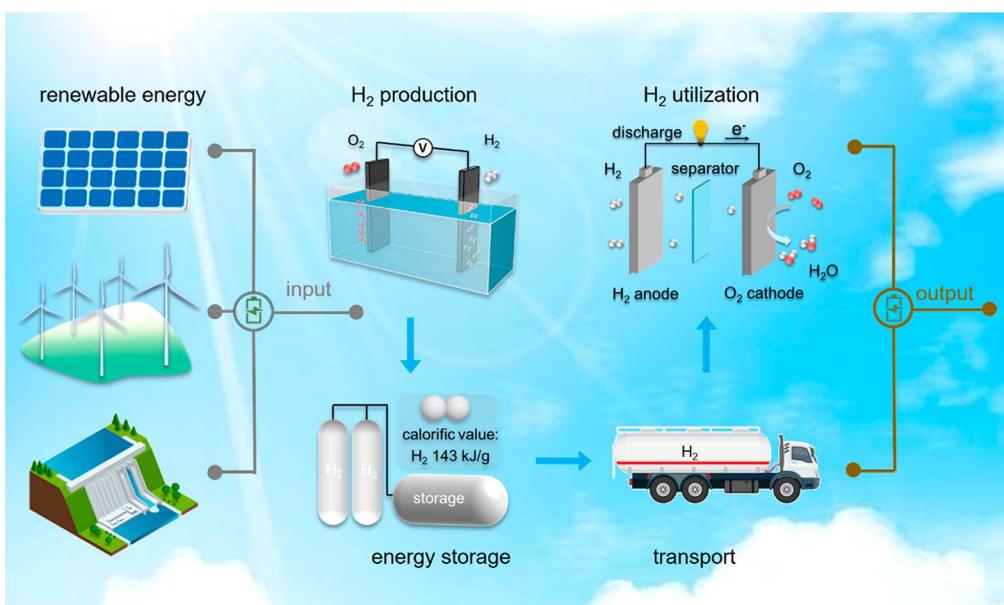


Figure 1. A simplified diagram of green hydrogen cycling.

Table 1. Comparison of Various Strategies toward Porous Materials Including Template, Pore Size, Advantages, and Disadvantages

method	template	pore size	advantages	disadvantages
soft templating	surfactants	micro/meso	controllable, high porosity	expensive, multistep, post-treatment
hard templating	porous solids	micro/meso/macros	controllable, versatile, high porosity	multistep, time-consuming, harsh leaching
sol-gel	template-free	micro	scalable, efficient	limited versatility, time-consuming, post-treatment
3D printing	template-free	macro	controllable, flexible	high cost, limited versatility, low porosity
dealloying	template-free	meso/macros	controllable	multistep, limited versatility, harsh leaching
freeze-drying	ices	meso/macros	ecofriendly, versatile	high cost, multistep, low porosity
electrodeposition on bubbles	<i>in situ</i> bubbles	meso/macros	rapid, versatile, scalable, ambient	moderate porosity

Generation. *Nat. Commun.* 2021, 12, 2008.³ This paper highlights the galvanostatic electrodeposition of a 3D hierarchically porous Ni framework for biomass oxidation upgrading.

- Du, L.; Xiong, H.; Lu, H.; Yang, L.-M.; Liao, R.-Z.; Xia, B. Y.; You, B. Electroshock Synthesis of a Bifunctional Nonprecious Multi-Element Alloy for Alkaline Hydrogen Oxidation and Evolution. *Exploration* 2022, 2, 20220024.⁴ This paper elucidates the electroshock synthesis of 3D hierarchically porous NiCoCuMoW alloy for both HER and HOR.

1. INTRODUCTION

The energy crisis and environmental pollution due to excessive depletion of nonrenewable fossil fuels accelerate the exploration of sustainable energy sources.^{5,6} In response, a new energy paradigm based on green hydrogen cycling has been proposed as a promising alternative to the current fossil fuel-based hydrocarbon economy.⁷ As shown in Figure 1, renewable energy resources, such as solar, wind, and hydropower, can be harvested to drive water splitting to produce H₂, which can be further stored and used as an energy carrier to release electric energy via H₂–O₂ fuel cells with no greenhouse gas emission.^{8,9} The generation and utilization of H₂ involve four half-reactions including hydrogen evolution reaction (HER), oxygen evolution reaction (OER), hydrogen oxidation reaction (HOR), and oxygen reduction reaction (ORR). Their sluggish kinetics

usually result in low efficiency.¹⁰ Moreover, considering their local gas–liquid–solid triple-phase microenvironments, the interfacial mass transport and gas diffusion are also critical. Accordingly, cost-effective and active electrocatalysts with excellent mass transfer are necessary. It is known that hierarchically porous architectures with interconnected porosity and large specific surface area are beneficial for mass transport and exposure of active sites, conferring great potential for electrocatalysis.¹¹

Currently, various synthetic approaches have been explored toward hierarchically porous materials including soft/hard templating that uses surfactants or porous solids as porogens¹² and template-free methods like sol–gel,¹³ 3D printing,¹⁴ dealloying,¹⁵ and freeze-drying (Table 1).¹⁶ In particular, dynamic electrodeposition on bubbles that employs *in situ* formed bubbles in electrolytes as templates is rapid, efficient, and scalable to obtain hierarchically porous structures under ambient conditions. Additionally, the resulting porous materials can be directly employed as catalytic electrodes, avoiding the use of polymeric binders like Nafion and the concomitant issues including limited catalysts loading, reduced conductivity, and inhibited mass transport. Specifically, taking dynamic hydrogen bubble-templated electrodeposition as an example, metal deposition from the corresponding salt solution is accompanied by HER. At the early stage, the competitive HER induces the supersaturation of dissolved H₂ and thus heterogeneous nucleation of bubbles takes place on the electrode surface followed by rapid growth of H₂ bubbles (Figure 2a).^{17,18} The

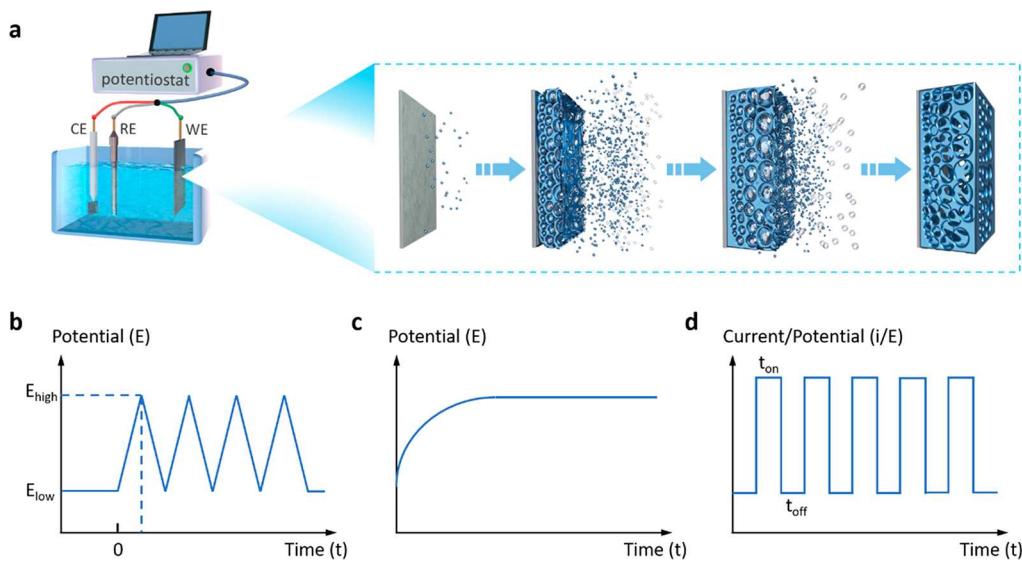


Figure 2. (a) Scheme of an electrodeposition device with the formation process of hierarchically porous materials by electrodeposition on bubbles. (b) Potential–time curve for potentiodynamic electrodeposition. (c) Recorded time-dependent potential in galvanostatic electrodeposition. (d) Pulsed signal applied in electroshock.

covering bubbles partially block the access of metal ions to the electrode and hence guide their electrodeposition around the electrode–bubble interface.¹⁹ With the lapse of time, numerous bubbles could generate pores in the deposits with increasing thickness and walls, and the formed high-surface-energy sites on the electrode–bubble interface could in turn induce subsequent metal/bubble nucleation and deposition. Meanwhile, the coalescence of H_2 bubbles could disrupt the inward diffusion of metal ions, affecting metal deposition as well. It is expected that the pore size of deposits increases with the distance away from electrode surface due to the coalescence and growth of H_2 bubbles, leading to the formation of hierarchical porosity. Such a dynamic electrodeposition process was witnessed by Margaritondo's group in 2002 using phase-contrast radiology with synchrotron radiation.²⁰ These results imply that the parameters that can vary the behaviors of bubble and metal deposition including substrate features, applied potential/current, hydrodynamic conditions, and electrolyte additives, could modulate the porous structure of the resulting materials,²¹ providing a powerful toolbox to interrogate the underlying porosity–activity correlation.

In this Account, we describe our recent progress in dynamic electrodeposition on bubbles to prepare advanced porous electrocatalysts to tackle the challenges in electrocatalytic green hydrogen cycling. Three innovative strategies including potentiodynamic electrodeposition, galvanostatic electrodeposition, and electroshock are presented. Subsequently, their electrocatalytic applications in HER, OER, overall water splitting (OWS), biomass oxidation (to replace OER), and HOR are discussed. The remaining challenges and future perspectives are presented finally.

2. DYNAMIC ELECTRODEPOSITION ON BUBBLES

Electrodeposition can be conducted under ambient conditions using an electrochemical workstation in a three (or two)-electrode configuration containing a working electrode (WE), a counter electrode (CE), and a reference electrode (RE) (or WE and CE), as shown in Figure 2a. Based on the manner of bubble generation, the dynamic electrodeposition can be divided into

potentiodynamic electrodeposition, galvanostatic electrodeposition, and electroshock. Potentiodynamic electrodeposition means periodically and linearly scanning the potential between a high potential (E_{high}) and a low potential (E_{low}) (Figure 2b). Galvanostatic electrodeposition uses a fixed current, and the time-dependent potential response is recorded (Figure 2c).²² Electroshock implies periodically switching the potential/current on and off (Figure 2d).

Considering the templating role of *in situ* electrogenerated bubbles, these different electrochemical modes would largely determine the bubble behavior, leading to various pore sizes and densities of the electrodeposited materials. Generally, potentiodynamic electrodeposition enables the periodical generation of bubbles and the oxidation/reduction of metal species at the triphase interface, beneficial to the growth of uniform and conformal porous materials. Galvanostatic electrodeposition generates bubbles continuously, which favors the nucleation, growth, coalescence, and fusion of bubbles, such that the as-prepared materials feature hierarchical porosity with large pore size and wide aperture distribution. Electroshock implies rapid generation and dissipation of bubbles, which inhibits in part the coalescence and fusion of bubbles and hence benefits the formation of relatively small and uniform pores. Moreover, other parameters that affect bubble behavior and metal species deposition, like substrate features (structure, type, and surface),²³ applied potentials/currents,²⁴ hydrodynamic conditions,²⁵ and electrolyte additives (surfactants, halides, and polymers),²⁶ could modulate the porous structures of the resulting materials as well.

2.1. Potentiodynamic Electrodeposition

Potentiodynamic electrodeposition is achieved via scanning potentials periodically within a certain potential window. The species on the electrolyte/electrode was repeatedly oxidized and reduced, beneficial to the growth of uniform and conformal porous films.²² Our group used this method to successfully synthesize porous cobalt-sulfide films (Co–S) on fluorine-doped tin oxide (FTO) by consecutive linear scanning between -1.2 and 0.2 V vs Ag/AgCl.²⁷ Scanning electron microscopy (SEM) images revealed that both as-prepared and annealed

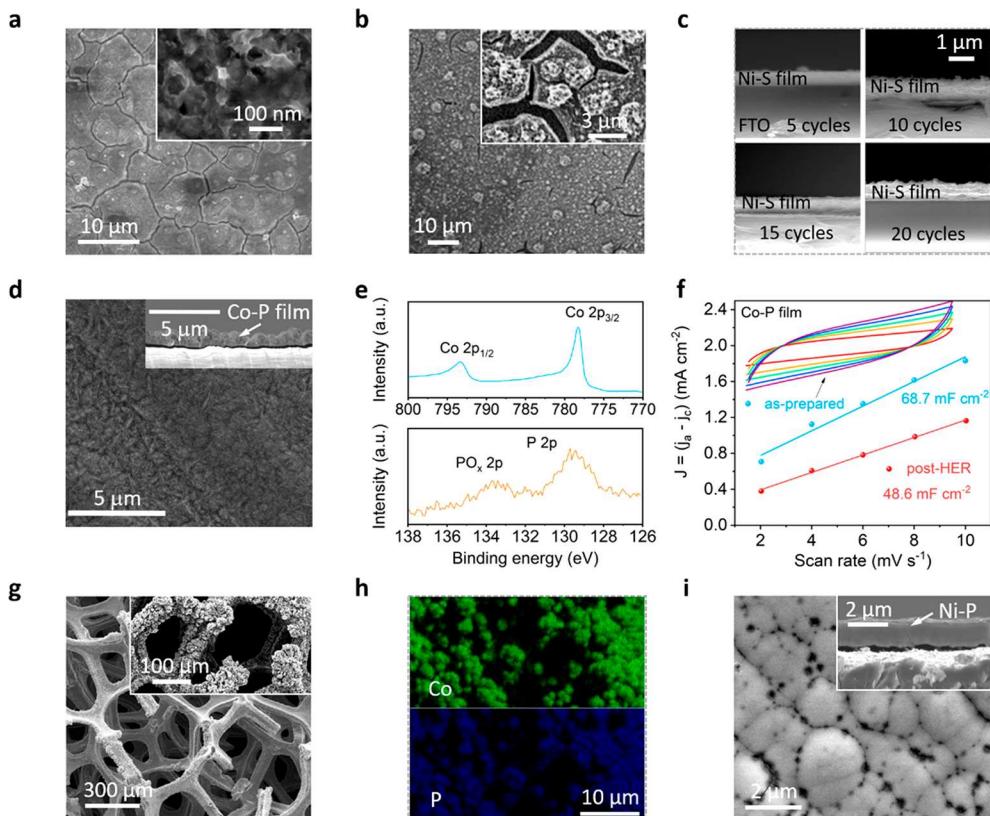


Figure 3. SEM images of (a) freshly prepared and (b) annealed Co–S. Reproduced with permission from ref 27. Copyright 2013 American Chemical Society. (c) Cross-section SEM images of Ni–S with different cycles. Reproduced with permission from ref 28. Copyright 2014 Royal Society of Chemistry. (d) SEM and cross-sectional SEM images of fresh Co–P. (e) XPS spectra of Co–P. (f) Scan rate dependence of the current densities for Co–P before and after electrolysis. Reproduced with permission from ref 1. Copyright 2015 Wiley-VCH. (g) SEM and (h) elemental mapping images of Co–P/CF. Reproduced with permission from ref 29. Copyright 2016 American Chemical Society. (i) Top-view and cross-section SEM images of Ni–P. Reproduced with permission from ref 30. Copyright 2016 Wiley-VCH.

Co–S exhibited uniform porous morphology due to the evolution of H_2 bubbles during electrodeposition (Figure 3a,b). Such a facile potentiodynamic electrodeposition is also effective to synthesize porous amorphous nickel-sulfide films (Ni–S) with tunable thickness (Figure 3c).²⁸ Similarly, cobalt–phosphorus-derived films (Co–P) on Cu foil (CF) can be obtained as well.¹ SEM and cross-sectional SEM images (Figure 3d) revealed the complete coverage of Co–P with a thickness of 1–3 μm . X-ray photoelectron spectroscopy (XPS) revealed the metallic nature of Co and the phosphide-like form of P (Figure 3e). Electrochemically active surface areas (ECSAs) estimated from electrochemical double-layer capacitance (C_{dl}) unveiled that the Co–P before and after HER possessed much higher C_{dl} values (68.7 and 48.6 mF cm^{-2}) than a planar electrode (Figure 3f), suggesting their larger ECSAs. In addition, we also deposited Co–P on porous copper foam (Co–P/CF).²⁹ SEM and elemental mapping images (Figure 3g, h) suggested the uniform coverage of Co–P. The porous nickel–phosphorus film (Ni–P) can also be prepared by a similar method.³⁰ Due to the co-generation of H_2 bubbles, Ni–P showed black holes, as revealed by the SEM image (Figure 3i). The plentiful porosity is beneficial to mass transport and exposure of active sites.

2.2. Galvanostatic Electrodeposition

Galvanostatic electrodeposition refers to constant current electrolysis along with continuous bubble evolution as templates (Figure 2c), so that hierarchically porous architectures can be acquired. We used this strategy to prepare a hierarchically

porous Ni framework on commercial Ni foam (hp-Ni) at -3.0 A cm^{-2} for 500 s.³¹ The abundant macropores ($\sim 10 \mu\text{m}$) were templated by H_2 bubbles (Figure 4a). As expected, the ECSA of hp-Ni was nearly 9 times higher than that of pristine nickel foam (NF) (Figure 4b). Besides monometallic porous materials, bimetallic frameworks can also be obtained via a similar galvanostatic electrodeposition. For example, by simply changing the Ni^{2+} precursor to a mixture of Ni^{2+} and Co^{2+} in the electrolyte, a bimetallic NiCo alloy framework could be obtained.² More recently, we synthesized porous pine needle-like Cu_3Ag_7 on copper foam ($\text{Cu}_3\text{Ag}_7/\text{CF}$) at -3.0 A cm^{-2} for only 30 s from an aqueous electrolyte containing both Ag^+ and Cu^{2+} species.³² The high C_{dl} (51.8 mF cm^{-2}) relative to a planar electrode suggested larger ECSA and plentiful porosity of $\text{Cu}_3\text{Ag}_7/\text{CF}$.

In addition, we explored the synthesis of 3D hierarchically porous urchin-like Ni_2P superstructures on NF ($\text{Ni}_2\text{P}/\text{Ni}/\text{NF}$) via galvanostatic electrodeposition of hp-Ni followed by phosphorization.³³ SEM images (Figure 4c) of $\text{Ni}_2\text{P}/\text{Ni}/\text{NF}$ indicated porous superstructures composed of stacked microspheres with urchin-like surface. Meanwhile, due to the formation of H_2 bubbles during electrodeposition, the macro-porous walls of $\text{Ni}_2\text{P}/\text{Ni}/\text{NF}$ featured numerous smaller macropores ($\sim 10 \mu\text{m}$). The open primary and secondary macropores can facilitate substrate migration to the inner surface of $\text{Ni}_2\text{P}/\text{Ni}/\text{NF}$ and favor outward diffusion of produced gases. Elemental mapping images (Figure 4d) revealed the uniform distribution of Ni and P in $\text{Ni}_2\text{P}/\text{Ni}/\text{NF}$. We also prepared

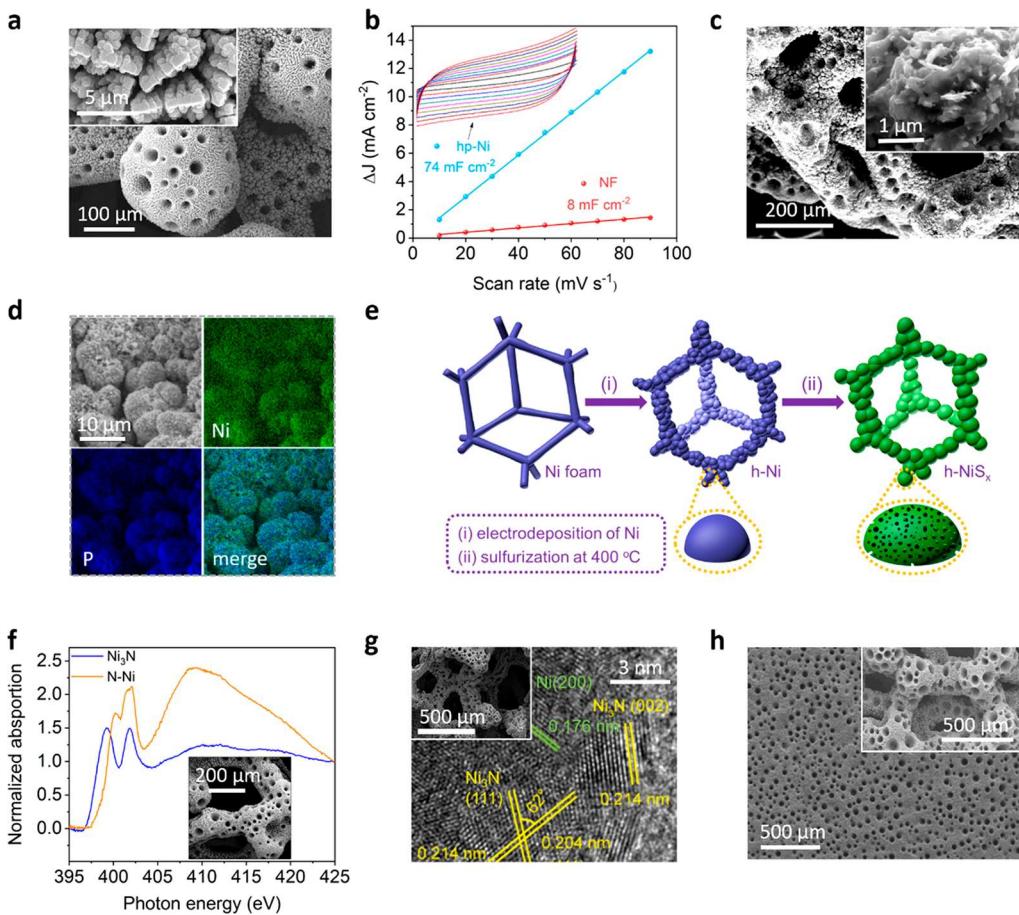


Figure 4. (a) SEM images of hp-Ni. (b) CV curves and scan rate dependence of the current densities of hp-Ni and NF. Reproduced with permission from ref 31. Copyright 2017 American Chemical Society. (c) SEM images and (d) elemental mapping of $\text{Ni}_2\text{P}/\text{Ni}/\text{NF}$. Reproduced with permission from ref 33. Copyright 2015 American Chemical Society. (e) Synthetic scheme for h-NiS_x . Reproduced with permission from ref 34. Copyright 2016 Wiley-VCH. (f) N K-edge XANES spectra of N–Ni and Ni framework with the SEM image of N–Ni. Reproduced with permission from ref 2. Copyright 2017 American Chemical Society. (g) HR-TEM and SEM images of the $\text{Ni}_3\text{N}/\text{Ni}$ interface. Reproduced with permission from ref 35 under the terms of a CC-BY 4.0 license. Copyright 2018 The Authors, published by Springer Nature. (h) SEM images of $\text{Co}_2\text{N}/\text{Ni}/\text{CP}$ and $\text{Co}_2\text{N}/\text{Ni}/\text{CF}$ (inset). Reproduced with permission from ref 36. Copyright 2019 American Chemical Society.

hierarchically porous nickel sulfide superstructures (h-NiS_x) with both macropores and mesopores via a similar galvanostatic electrodeposition followed by sulfurization (Figure 4e).³⁴

Inspired by the high specific surface area of hp-Ni, we obtained diverse surface nitrogen modified porous metals (e.g., N–Ni, N–Fe, N–Co, N–Cu, and N–NiCo alloy) by galvanostatic electrodeposition and subsequent low-temperature ammonium carbonate treatment.² The SEM image (Figure 4f, inset) revealed an interconnected 3D macroporous network for N–Ni. The N K-edge XANES spectrum (Figure 4f) showed a positive shift to higher energy for N–Ni relative to Ni_3N , indicative of weaker interaction and less electron transfer from Ni to N in N–Ni.²

Furthermore, partially nitriding the hp-Ni through high-temperature annealing in ammonia creates the interfaces between Ni and Ni_3N in the resulting 3D macroporous $\text{Ni}_3\text{N}/\text{Ni}/\text{NF}$ (Figure 4g, inset).³⁵ Their high-resolution transmission electron microscopy (HR-TEM) image clearly showed the interface of hexagonal Ni_3N and cubic Ni. A similar structure (Figure 4h) could be obtained via partial nitridation of cobalt nanoparticles on cobalt foam ($\text{Co}_2\text{N}/\text{Co}/\text{CF}$) or carbon paper ($\text{Co}_2\text{N}/\text{Co}/\text{CP}$).³⁶

2.3. Electroshock

Electroshock that rapidly switches potentials or currents on and off enables quick bubble generation and dissipation and thus partially inhibits their coalescence and fusion, beneficial to the formation of relatively small and uniform porous structures.^{37,38} We synthesized a porous NiCoCuMoW multielement alloy (MEA) by electroshock in which pulsed potential of -6 V was applied with an on time of 0.2 s and an off time of 0.8 s for 400 cycles (Figure 5a).⁴ SEM images (Figure 5b) revealed an inherited 3D porosity of the NF skeleton covered by coarse stacked particles with numerous cavities. Elemental mapping images suggested the uniform distribution of Ni, Co, Cu, Mo, and W (Figure 5c). X-ray diffraction (XRD) (Figure 5d) analysis revealed a body-centered cubic structure (BCC) crystal for NiCoCuMoW, similar to reported results.³⁹

3. POROUS ELECTROCATALYSTS FOR GREEN HYDROGEN CYCLING

3.1. Hydrogen Evolution

As a vital half-reaction in water splitting, HER is of great significance for green hydrogen cycling.⁴⁰ In view of the multistep pathway, an ideal HER electrocatalyst should have optimal affinity/repellency to balance the sorption/diffusion of

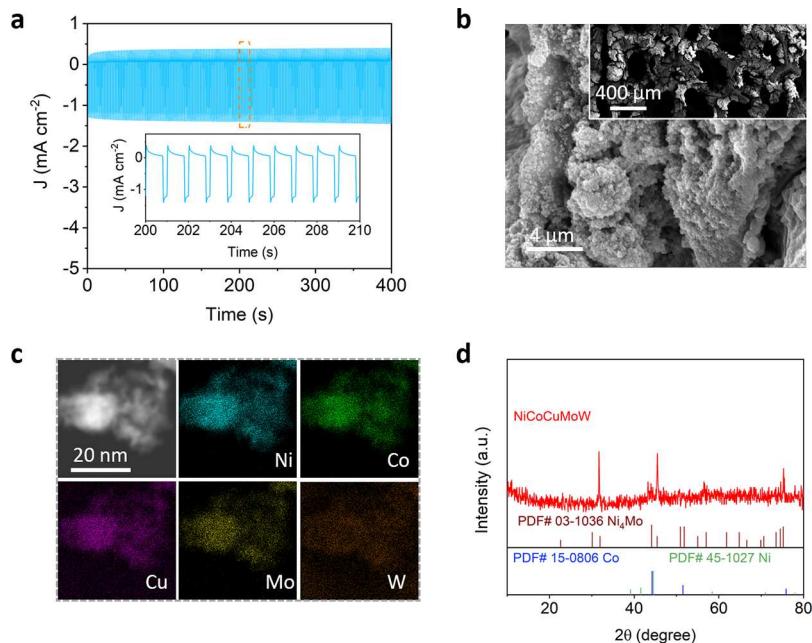


Figure 5. (a) Current density–time curve in electroshock electrodeposition. (b) SEM images, (c) elemental mapping, and (d) XRD pattern of the NiCoCuMoW MEA. Reproduced with permission from ref 4. Copyright 2022 Wiley-VCH.

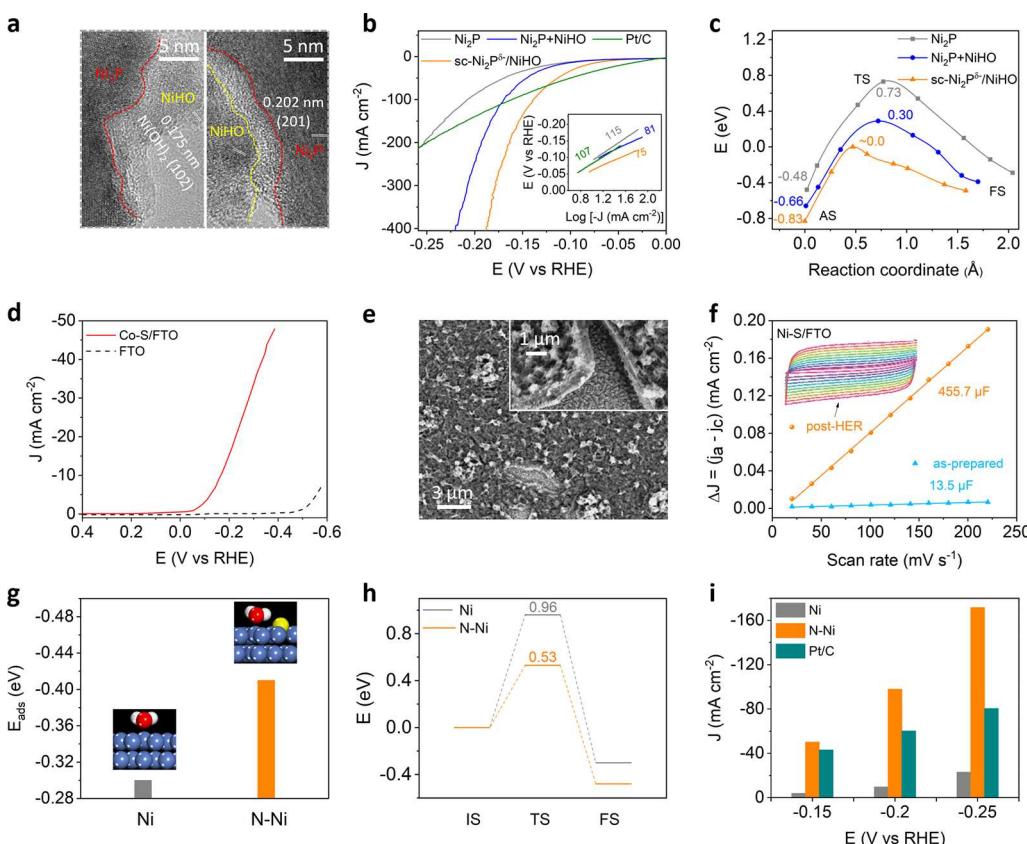


Figure 6. (a) HR-TEM images of sc-Ni₂P^δ-/NiHO (left) and Ni₂P + NiHO control (right), along with the corresponding Tafel slopes. (c) Reaction energy diagrams of the elemental steps in alkaline HER on Ni₂P(111), Ni₂P(111) + NiHO and sc-Ni₂P^δ-(111)/NiHO. Reproduced with permission from ref 43. Copyright 2019 Wiley-VCH. (d) Polarization curves of annealed Co–S after 3 h electrolysis and FTO substrate. (e) SEM images of Co–S after 3 h electrolysis. Reproduced with permission from ref 27. Copyright 2013 American Chemical Society. (f) Scan rate dependence of current densities and the CV curves (inset) of Ni–S. Reproduced with permission from ref 28. Copyright 2014 Royal Society of Chemistry. (g) Adsorption energy of water and (h) free energy barrier profiles of water dissociation on Ni(111) and N–Ni(111). (i) Comparison of current densities at different overpotentials for N–Ni, Ni framework, and Pt/C for neutral HER. Reproduced with permission from ref 2. Copyright 2017 American Chemical Society.

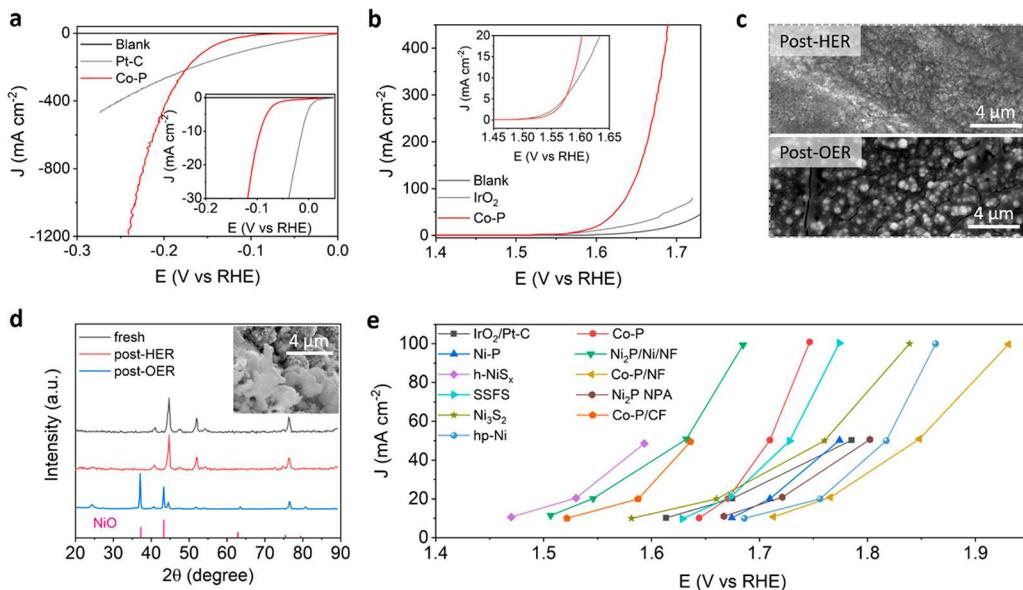


Figure 7. LSV curves for (a) HER and (b) OER over Co-P. (c) SEM images of post-HER and post-OER Co-P. Reproduced with permission from ref 1. Copyright 2015 Wiley-VCH. (d) XRD pattern for fresh, post-HER, and post-OER Ni₂P/Ni/NF samples with the SEM image of post-OER Ni₂P/Ni/NF. Reproduced with permission from ref 33. Copyright 2015 American Chemical Society. (e) Comparison of overall water splitting performance for our reported bifunctional electrocatalysts.

intermediates/substrates, which are mainly governed by the surface charge density and porosity of the electrocatalyst.^{41,42} We therefore fabricated strong electronically coupled and negatively charged porous nickel phosphide/nickel hydr(oxy)-oxides hybrids (sc-Ni₂P^{δ-}/NiHO) via galvanostatic electrodeposition followed by phosphorization and *in situ* electrochemical oxidation.⁴³ As shown in Figure 6a, the interplanar spacing of NiHO in sc-Ni₂P^{δ-}/NiHO was calculated to be 0.175 nm, suggesting the successful partial oxidation of Ni₂P to Ni(OH)₂. The tight contact between Ni₂P and NiHO in sc-Ni₂P^{δ-}/NiHO (Figure 6a), different from the gaps in the Ni₂P + NiHO control, revealed their strong electronic coupling.⁴³ Linear sweep voltammetry (LSV) was then conducted to investigate their HER performance in 1.0 M KOH (Figure 6b). The overpotential at 10 mA cm⁻² (η_{10}) for sc-Ni₂P^{δ-}/NiHO was only 60 mV, lower than those of fresh Ni₂P (90 mV) and Ni₂P + NiHO (85 mV). The smaller Tafel slope further underscored more favorable HER kinetics on sc-Ni₂P^{δ-}/NiHO (Figure 6b, inset). DFT calculations suggested that the negatively charged Ni₂P surface in sc-Ni₂P^{δ-}/NiHO favor the adsorption of electron-deficient H atom in H₂O and facilitate subsequent water dissociation by repelling the electron-rich OH in H₂O. As presented in Figure 6c, the adsorption energy (-0.83 eV) for the H₂O adsorption state (AS) and the energy barrier (0.83 eV) for the transition state (TS) of water dissociation on sc-Ni₂P^{δ-}/NiHO were significantly lower than those on fresh Ni₂P (-0.48 and 1.21 eV) and Ni₂P + NiHO (-0.66 and 0.96 eV).

In addition, interfacing porous Ni and Ni₃N can also optimize water and hydrogen adsorption. The best hydrogen adsorption site on porous Ni₃N/Ni/NF exhibited a H adsorption energy (ΔG_{H^*}) of 0.01 eV, very close to the ideal amount of 0 eV.³⁵ Ni₃N/Ni/NF demonstrated excellent HER activity with η_{10} of only 12 mV in 1.0 M KOH. Even in a neutral potassium phosphate (KPi) buffer, the η_{10} of Ni₃N/Ni/NF was low at 19 mV. We then extended this interfacing strategy to prepare porous Co-based electrocatalysts on cobalt foam (Co₂N/Co/

CF) or carbon paper (Co₂N/Co/CP).³⁶ Remarkably, the η_{10} of Co₂N/Co/CF was only 12 mV.

Given the corrosiveness and environmental issues caused by the use of strong acidic and alkaline electrolytes, we developed advanced catalysts for neutral HER. For example, we prepared a porous Co-S via potentiodynamic electrodeposition on FTO for HER in neutral 1.0 M KPi.²⁷ After electrolysis activation, the η_{50} was lowered to 397 mV (Figure 6d). Elemental analysis of the Co-S after 3 h electrolysis showed the retention of Co-S, consistent with SEM characterizations (Figure 6e). Analogous activation during neutral HER was observed for the porous Ni-S,²⁸ as indicated by the increased C_d from 13.5 to 455.7 μ F after electrolysis (Figure 6f). We speculated that the activation process is caused by evolved H₂ bubbles, which induce surface reorganization of the underlying electrocatalysts.

Recently, we found that surface nitrogen modification can considerably enhance the activity of first-row transition metal frameworks for neutral HER (Figure 6g–i).² Using the porous Ni framework as an example, DFT calculations showed that the electron-rich nitrogen in N–Ni facilitates water adsorption via the electron-deficient H atom as revealed by the enhanced adsorption energy (E_{ads}) from -0.30 eV to -0.41 eV (Figure 6g). Also, the energy barrier for water dissociation on N–Ni was decreased from 0.96 to 0.53 eV (Figure 6h), indicative of promoted water dissociation. Consequently, the resulting N–Ni rivaled Pt/C for HER at pH 7 (Figure 6i).

3.2. Overall Water Splitting

The efficiency of water splitting is mainly limited by OER. To simplify electrolyzer configuration, we explored porous bifunctional electrocatalysts with both OER and HER activities in the same electrolyte to achieve overall water splitting. For instance, the electrocatalytic HER, OER, and OWS performance of Co-P were investigated in 1.0 M KOH.¹ As shown in Figure 7a, the η_{10} of Co-P for HER was only 94 mV (Figure 7b). After 24 h electrolysis of HER, the post-HER Co-P still maintained a uniform coverage and morphology (Figure 7c). Regarding OER, subsequently, the η_{10} of Co-P was 345 mV, smaller than that of

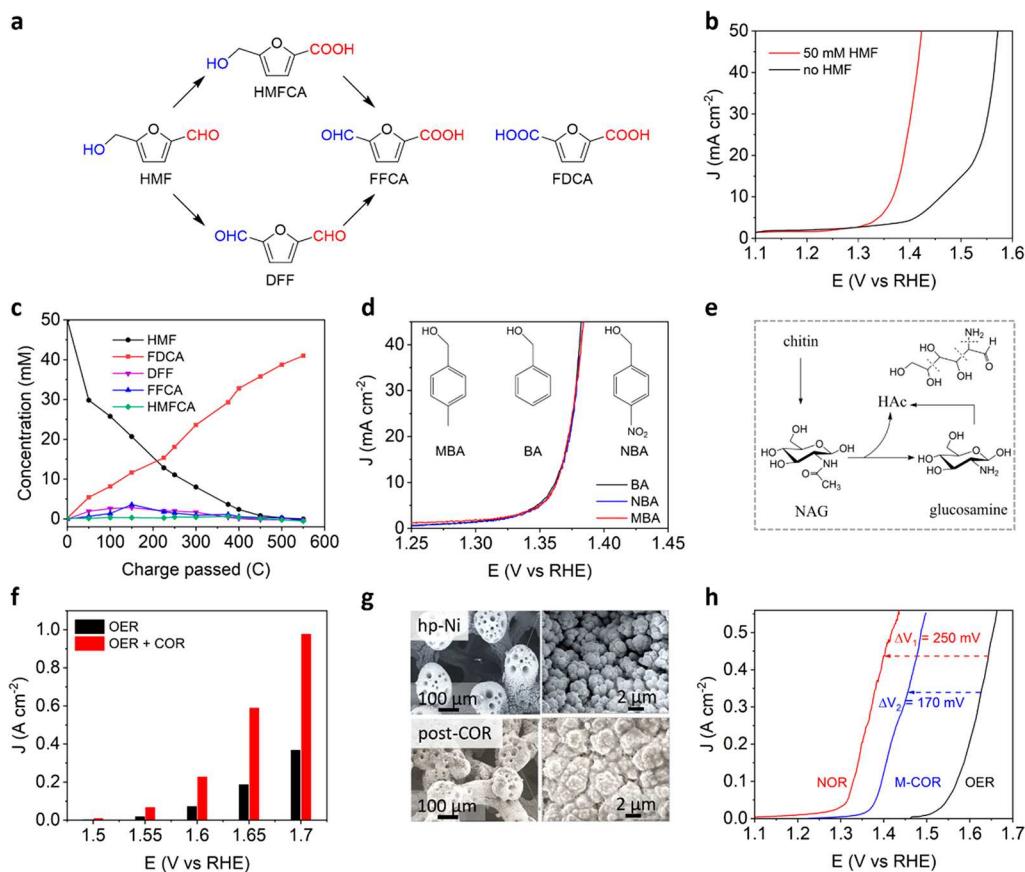


Figure 8. (a) Two possible pathways of HMF oxidation to FDCA. (b) LSV curves of Co-P/CF in 1 M KOH with and without 50 mM HMF. (c) Conversion of HMF and yields of oxidation products over passed charge during electrolysis at 1.423 V vs RHE in 1.0 M KOH containing 50 mM HMF. Reproduced with permission from ref 29. Copyright 2016 American Chemical Society. (d) LSV curves on hp-Ni in 1.0 M KOH with 10 mM MBA, BA, and NBA, together with their corresponding chemical structures. Reproduced with permission from ref 31. Copyright 2017 American Chemical Society. (e) Possible main reaction pathways of chitin oxidation. (f) Comparison of current densities at various potentials in 1.0 M KOH with and without 33.3 mg L⁻¹ chitin. (g) SEM images of fresh and post-COR hp-Ni. (h) LSV curves of anodic reactions in 1.0 M KOH containing 2.2 g L⁻¹ NAG or 3.5 g L⁻¹ milled chitin, and OER. Reproduced from ref 3 under the terms of the CC-BY 4.0 license. Copyright 2021 The Authors, published by Springer Nature.

IrO₂ (Figure 7b). Interestingly, the post-OER Co-P showed large nanoparticle aggregates (Figure 7c), suggesting *in situ* surface reconstruction to OER-active cobalt oxides/(oxy)-hydroxides.¹ For OWS in 1.0 M KOH, the Co-P couple exhibited larger current density than that of IrO₂/Pt-C at 1.67 V. Likewise, the porous Ni-P also displayed bifunctional HER and OER performance.³⁰

To further accelerate the electrocatalytic kinetics, we synthesized 3D hierarchical and interconnected macroporous Ni₂P/Ni/NF.³³ For HER, its current density beyond -112 mV also largely exceeded that of Pt/C. A 20 h HER stability test did not alter the composition and urchin-like morphology of Ni₂P/Ni/NF (Figure 7d). Additionally, Ni₂P/Ni/NF exhibited excellent OER activity with a small η_{10} of 200 mV. SEM images (Figure 7d, inset) of the post-OER Ni₂P/Ni/NF revealed the featureless monoliths plus urchin-like microparticles, different from that for fresh Ni₂P/Ni/NF (Figure 4c), suggesting a similar *in situ* surface oxidation reconstruction. A Ni₂P/Ni/NF couple-based alkaline water electrolyzer reached 10 and 100 mA cm⁻² at cell voltages of 1.49 and 1.68 V, respectively. The improved activity of Ni₂P/Ni/NF originated from its 3D interconnected porosity and high ECSA.³³ In addition, the bifunctional catalytic activity of hierarchically porous h-NiS_x was also explored.³⁴ As shown in Figure 7e, the h-NiS_x couple required a voltage of only

1.47 V to afford 10 mA cm⁻² for OWS in 1.0 M KOH. The alkaline OWS performance for other bifunctional electrocatalysts reported by us was also included in Figure 7e.^{1,29-31,33,34,44-47}

3.3. Biomass Oxidation

Although developing active electrocatalysts can reduce the overpotential of OER for efficient water splitting to generate H₂, this reduction is insufficient. Moreover, the low value of O₂, possible crossover of H₂/O₂, and detrimental effects of reactive oxygen species (ROS) may pose cost and safety issues.^{47,48} We therefore reason that replacing OER with more favorable organic oxidation reactions is economically attractive. This strategy can not only circumvent H₂/O₂ mixing and ROS formation, but also reduce the voltage input for H₂ production, as well as generate value-added products at the anode. Among biomass-derived intermediates, 5-hydroxymethylfurfural (HMF) is a platform precursor (Figure 8a). For instance, 2,5-furandicarboxylic acid (FDCA), one of the valuable oxidation products of HMF, has been regarded as a green replacement of terephthalic acid to synthesize polyamides, polyesters, and polyurethanes.⁴⁷

Interestingly, the porous Co-P can be directly utilized to catalyze HMF oxidation to FDCA in 1.0 M KOH.²⁹ For example, the Co-P on copper foam (Co-P/CF) achieved 20

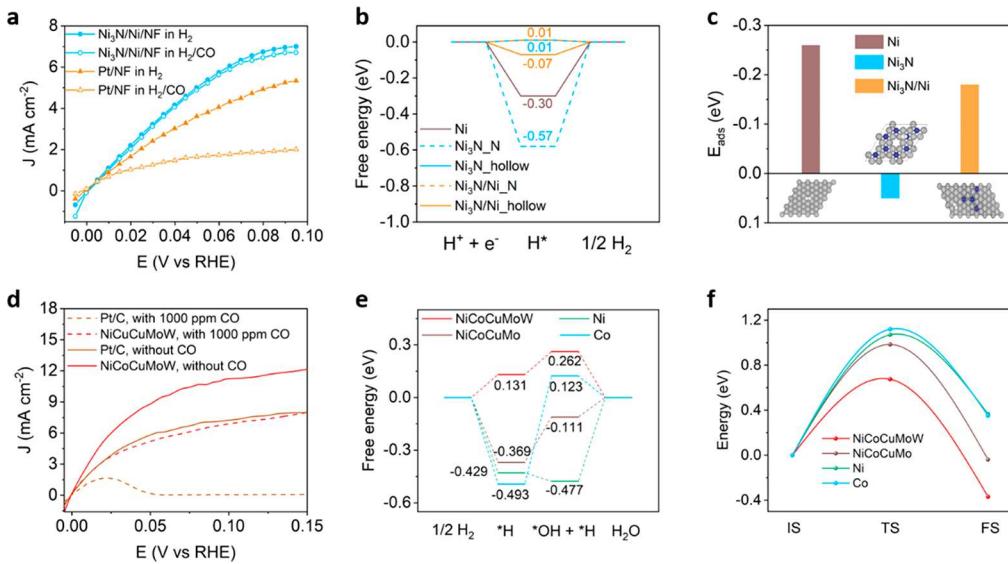


Figure 9. (a) Comparison of HOR polarization curves of Ni₃N/Ni/NF and Pt/NF in 0.1 M KOH saturated with H₂ or H₂ with 2% CO (v/v). (b) Hydrogen adsorption free energy, (c) adsorption energy of H₂ on Ni, Ni₃N, and Ni₃N/Ni. Reproduced from ref 35 under the terms of the CC-BY 4.0 license. Copyright 2018 The Authors, published by Springer Nature. (d) Comparison of the polarization curves and Tafel plots of NiCoCuMoW and Pt/C in 1.0 M KOH saturated with H₂ or H₂ with 1000 ppm of CO. (e) Gibbs free-energy and (f) reaction energy barrier diagrams of alkaline HOR pathway on Ni, Co, NiCoCuMo, and NiCoCuMoW. Reproduced with permission from ref 4. Copyright 2022 Wiley-VCH.

mA cm⁻² at 1.38 V vs RHE with 50 mM HMF, which was smaller than that for OER (1.53 V vs RHE, Figure 8b). Product quantification (Figure 8c) confirmed a nearly 90% yield of FDCA. Subsequently, a two-electrode electrolyzer based on Co-P/CF for simultaneous production of FDCA and H₂ was constructed, and the electrocatalyst couple required only 1.44 V to achieve 20 mA cm⁻², whereas a higher voltage of 1.59 V was required for OWS.

Encouraged by the above results, we continued to explore the oxidative upgrading of various alcohols paired with H₂ co-production.⁴⁷ To avoid the potential influence of nonmetal elements in the catalyst composition, we purposely prepared a 3D hierarchically porous hp-Ni.³¹ Benzyl alcohol (BA), 4-nitrobenzyl alcohol (NBA), and 4-methylbenzyl alcohol (MBA) (Figure 8d) were selected as the organic substrates. Surprisingly, we found that the electronic effects of diverse substituents at the para position of BA have negligible impact on their electro-oxidation over hp-Ni, as indicated by the overlapped LSV curves (Figure 8d). We speculated that oxidation of these three alcohols primarily depended on the potential to realize a high oxidation state of nickel species, instead of the intrinsic thermodynamics. Recently, we extended the organic substrates to raw biomass, chitin, the most abundant natural amino biopolymer found in nature.³ Figure 8e shows its possible main reaction pathways. The monomer of chitin, N-acetylglucosamine (NAG), can be oxidized to acetic acid (HAc) and glucosamine by deacetylation, which can be further converted to HAc by opening the pyranose ring. As plotted in Figure 8f, the current density for chitin oxidation reaction (COR) was larger than that of OER at the same potential. The morphology retention (Figure 8g) of the hp-Ni after 4 h of COR electrolysis suggested its long-term stability. Milling chitin (M-chitin) can increase its solubility to 3.5 g L⁻¹, and the LSV curve (Figure 8h) for milled-chitin oxidation reaction (M-COR) showed much higher current density with a decreased potential by ~170 mV compared to OER under the investigated current densities. This oxidation potential can be further reduced by ~250 mV using

the monomer of chitin, NAG, as a substrate (NAG oxidation reaction, NOR).

3.4. Hydrogen Oxidation

Apart from efficient H₂ generation from water splitting, the utilization of H₂ via H₂-O₂ fuel cells to produce electricity on demand is equally important, such that advanced electrocatalysts are needed to accelerate the kinetics of involved H₂ oxidation reaction (HOR).⁴⁹ Accordingly, we explored the porous interface of Ni and Ni₃N.³⁵ The HOR performance of Ni₃N/Ni/NF was investigated in H₂-saturated 0.1 M KOH. Compared to Pt/NF, Ni₃N/Ni/NF exhibited more superior HOR activity (6.95 vs 5.25 mA cm⁻² at 0.09 V vs RHE, Figure 9a) and higher tolerance against CO poisoning. DFT computations suggested that the ΔG_{H^*} of two interfacial sites (Ni₃N/Ni_N and Ni₃N/Ni_hollow) were close to the ideal value of 0 eV (0.01 and -0.07 eV), higher than that of pure Ni (-0.30 eV) (Figure 9b). As for Ni₃N, there existed one type of site which had a ΔG_{H^*} of 0.01 eV but also another type of site exhibiting very strong hydrogen affinity with calculated ΔG_{H^*} close to -0.57 eV. Furthermore, the Ni₃N/Ni interface and Ni possessed stronger H₂ adsorption than Ni₃N, indicating favored H₂ adsorption on Ni₃N/Ni and Ni (Figure 9c). Both the ideal ΔG_{H^*} (0.01 and -0.07 eV, Figure 9b) and strong H₂ adsorption (Figure 9c) of Ni₃N/Ni supported its excellent HOR performance. Similarly, the interfacial sites of Co₂N/Co/NF also exhibited improved HOR performance.³⁶

Recently, our group reported an electroshock method toward a rous NiCoCuMoW MEA for alkaline HOR and HER.⁴ The NiCoCuMoW afforded 11.2 mA cm⁻² at 0.1 V vs RHE for HOR, higher than those for NiCoCuMo (7.1 mA cm⁻²) and Pt/C (Figure 9d). Benefiting from the multi-active-site nature, CO poisoned NiCoCuMoW was still comparable to Pt/C under pure H₂ feeding. In contrast, Pt/C suffered from severe CO poisoning and lost its activity completely at potentials exceeding 0.05 V vs RHE. Note that hydrogen binding energy (HBE) and/or hydroxide binding energy (OHBE) are critical for alkaline HOR. Figure 9e shows that Co(111) and NiCoCuMo(111)

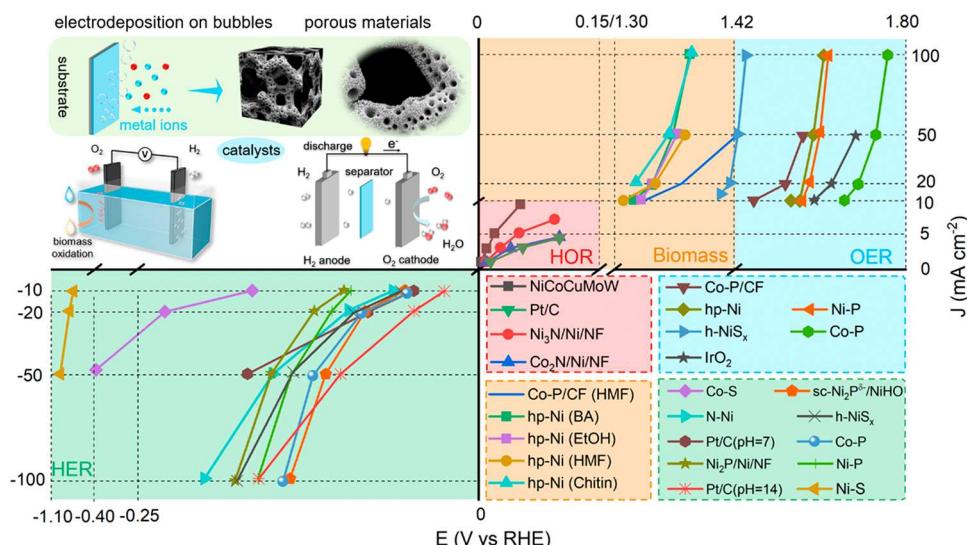


Figure 10. Summary of diverse electrocatalysts prepared by dynamic electrodeposition on bubbles for various reactions in green hydrogen cycling.

possess too strong H binding and too weak OH binding, accounting for their poor HOR activity. Although Ni(111) revealed an appropriate OHBE (-0.018 eV), the strong H binding (-0.429 eV) led to a high energy barrier (0.477 eV) for the combination of $^*\text{H}$ and $^*\text{OH}$ to H_2O . In contrast, NiCoCuMoW(111) exhibited similar HBE and OHBE of 0.131 eV. Kinetic analysis confirmed the low energy barrier of NiCoCuMoW for HOR (0.675 eV) relative to control samples (Figure 9f). These thermodynamic and kinetic results clearly indicated the great HOR activity of NiCoCuMoW MEA.

4. SUMMARY AND OUTLOOK

This Account has summarized our recent work of dynamic electrodeposition on bubbles toward advanced porous electrocatalysts for green hydrogen generation from water splitting and utilization in H_2 – O_2 fuel cells. These electrosynthesis methodologies include potentiodynamic, galvanostatic, and electro-shock electrodepositions and the resulting porous electrocatalysts range from metals to alloys, nitrides, sulfides, phosphides, and their hybrids, with promising performance for HER, OWS, biomass oxidation, and HOR (Figure 10). Looking ahead, there are still some challenges that deserve further investigation.

First, assisted by advanced electrochemistry and microscopic characterizations, we have preliminarily determined the nucleation, growth, and template role of bubbles,⁵⁰ while full understanding of the whole electrodeposition is still not yet complete due to the complex convolution of reaction, transport, and interface which involve multiple processes like bubble formation, mass transport, and species deposition at the triphase interface, and the dynamic changes of surface forces, lubrication, intermolecular force, electric field, adsorption, and so on. Therefore, more advanced operando techniques along with their combination are desirable to provide multidimensional information on the dynamic interface. How to accurately control the bubble formation, size, and density, and identify the underlying origins necessitates long-term research. In fact, recent works of mesostructure-induced selectivity in CO_2 reduction reported by Surendranath's group imply that the assumption of high porosity benefiting the exposure of active sites and mass transport may be too simplistic.^{51,52} Instead, deep

understanding of the complex interplay at electrocatalytic interface deserves further study.

Second, although the dynamic electrodeposition on bubbles is simple, rapid, and environmentally benign, it commonly obtains porous electrocatalysts on a small conductive substrate in the laboratory. The scaling-up for membrane electrode assemblies may suffer from severe controllability issues due to abundant bubble aggregation and evolution. Massive bubbles like H_2 may pose safety issues as well. Therefore, novel devices and protocols for scalable electrosynthesis are needed for practical applications. Alternatively, exploring the *in situ* electrochemical generation of inert or nonexplosive gases like N_2 and CO_2 for templating could be appealing options, awaiting further investigation.

Third, closing the green hydrogen cycling needs advanced electrocatalysts for the oxygen reduction reaction (ORR), a cathode half-reaction in H_2 – O_2 fuel cells. In fact, ORR is thermodynamically more challenging than HOR. Its kinetics, even on Pt benchmarks, is still sluggish.^{53,54} It is thus worth exploring the synthesis of porous ORR electrocatalysts by dynamic electrodeposition on bubbles. However, to our knowledge, relevant works have been rarely reported.

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Notes

The authors declare no competing financial interest.

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