

Elucidating the Intrinsic Relationship between Redox Properties of CeO₂ and CH₄ Oxidation Activity: A Theoretical Perspective

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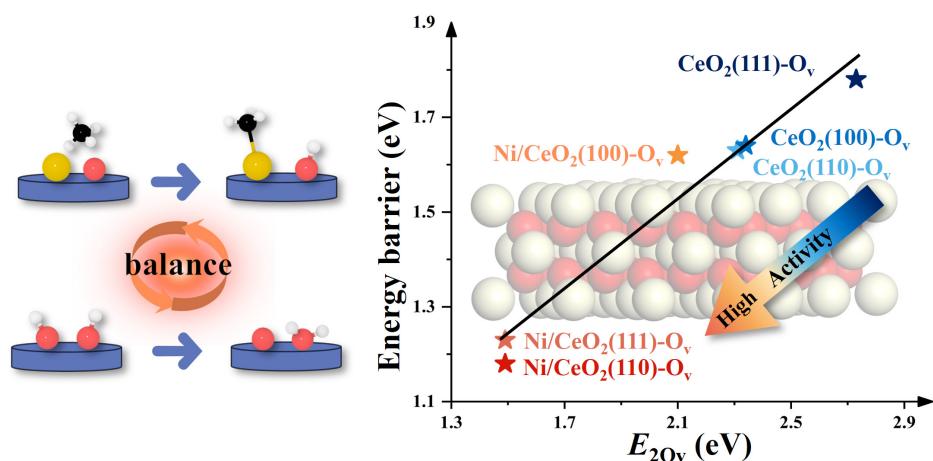
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ABSTRACT: Methane (CH_4) oxidation is an important reaction to reduce the greenhouse effect caused by incomplete combustion of CH_4 . Here, we explored the mechanism of CH_4 oxidation catalyzed by CeO_2 and Ni-doped CeO_2 , focusing on the redox properties of these catalyst surfaces, using density functional theory (DFT). We found that the barriers for CH_4^* activation and H_2O^* formation are correlated with the surface redox capacity, which is enhanced by Ni doping. Furthermore, the complete reaction mechanism is explored by DFT calculations and microkinetic simulations on bare and Ni-doped CeO_2 surfaces. Our calculations suggest that the doping of Ni leads to a much higher overall reactivity, due to a balance between the CH_4^* activation and H_2O^* formation steps. These results provide insights into the CH_4 oxidation mechanism and the intrinsic relationship between redox properties and the activity of CeO_2 surfaces.

Keywords: DFT; Reaction mechanism; CeO_2 ; CH_4 oxidation; Microkinetic simulation

Graphical abstract



I. INTRODUCTION

Natural gas, which is primarily composed of methane (CH₄), is considered as a much cleaner energy source than other fossil fuels due to its high H: C ratio. However, with the widespread use of natural gas engines, incomplete combustion of CH₄ could result in its escape to the atmosphere.¹ As a greenhouse gas twenty-five times more potent than CO₂, CH₄ oxidation towards the less harmful CO₂ is regarded as a practicable solution for reducing the greenhouse effect and has garnered much recent attention.²⁻⁵ Since the complete conversion of CH₄ to CO₂ and H₂O is difficult due to the strong C–H bond,⁶ it is desirable to uncover the structure-activity relationship in order to design catalysts that are capable of effectively CH₄ oxidation at relatively low exhaust gas temperatures.

Noble metal and metal oxide-based catalysts are commonly used in catalyzing CH₄ oxidation. For example, Pt and Pd exhibit high affinities for CH₄ adsorption, leading to the efficient activation of C–H bonds.^{7, 8} Huang et al.⁹ for example, prepared a Pd–NiCo₂O₄/SiO₂ catalyst that achieved a 100% CH₄ conversion rate at 378 °C under lean CH₄ conditions. However, catalysts based on noble metals are known to have poor water tolerance, making them susceptible to deactivation in steam environments.³ Ceria (CeO₂) is an alternative candidate for catalytic oxidation of CH₄ due to its reversible oxygen storage properties and the abundant Ce⁴⁺/Ce³⁺ pairs. Its hydrothermal stability in the presence of H₂O is also noteworthy.^{10, 11} There is ample evidence that the ability of the CeO₂ surface to store and release oxygen is closely related to the activity of catalytic oxidation reactions.¹²⁻¹⁶ Su et al.¹⁷ reported that Pd doping of CeO₂ surfaces

formed two Pd^{2+} cations replacing a Ce^{4+} cation. This led to stronger CH_4 adsorption and more reactive surface oxygens, ultimately reducing the CH_4 dissociation energy barrier and promoting oxygen vacancy recovery. More recently, Chen et al.¹⁸ synthesized CeO_2 -based catalysts with different morphologies, including nanoparticles, cubes, and rods, for catalyzing the complete oxidation of CH_4 . The CH_4 oxidation activity of these catalysts was found to be closely related to their intrinsic redox properties, as demonstrated by H_2 temperature-programmed reduction and oxygen storage capacity measurements. Furthermore, the activity was greatly enhanced by Ni doping. Other studies also suggested that the introduction of dopants such as Rh, Pd, Pt, and Au into CeO_2 can increase the concentration of oxygen vacancies and the amount of active oxygen species in the respective morphologies of CeO_2 , thereby promoting the reaction activity.^{19, 20}

However, the detailed mechanism for CH_4 oxidation, in particular, the role of surface oxygen in CH_4 oxidation on CeO_2 surfaces and its impact on the overall catalytic performance remains obscure. Due to the high stability of the CH_4 molecule, its activation is often considered to be crucial for evaluating the activity of CH_4 conversion reactions, while vacancy formation energy is commonly used to describe the C–H activation properties.^{21–23} On the other hand, the formation of the final product, H_2O , is also closely related to the surface redox properties. Previous studies have shown that the formation barrier of H_2O on the pristine $\text{CeO}_2(111)$ surface can be as high as 3.54 eV.²⁴ By doping metals, the stability of lattice oxygen can be reduced, facilitating the conversion of oxygen to H_2O , which significantly enhances the activity of H_2 .

oxidation and CH_2O combustion reactions.^{24, 25} Recently, Jung et al. reported a model of solid oxide fuel cells constructed with Sm-doped $\text{CeO}_{2-\delta}$ thin films.²⁶ The electrochemical impedance spectra and *in situ* XPS confirmed that the H_2O formation step, rather than C–H cleavage or CO_2 formation, limits the overall reaction rate in the CH_4 electrooxidation process. Mechanistic studies also suggested that the formation of H_2O is the rate-determining step in the complete oxidation of CH_4 in Ni/CeO_2 and MgAl_2O_4 systems.^{27, 28} Hence, it is important to investigate both reaction steps in assessing the catalytic activity of CeO_2 catalysts for CH_4 oxidation.

In our previous research, we reported a significant reduction of the energy required for oxygen vacancy formation upon Ni doping of $\text{CeO}_2(111)/(110)$,^{29, 30} which suggests a potential link between the surface redox properties and catalytic capacity of CeO_2 surfaces. In this work, we systematically investigate the three most stable surfaces of CeO_2 ($\text{CeO}_2(111)$, (110), and (100)), along with their corresponding Ni-doped surfaces. This study is particularly relevant in light of the recent experimental work on the Ni-doped CeO_2 catalysis of CH_4 oxidation.¹⁸ Our study emphasizes the importance of a comprehensive assessment of the key steps of the activation of CH_4^* and the formation of H_2O^* . The analysis of surface properties and kinetics elucidates the fundamental reasons behind the enhancement of CH_4 oxidation activity facilitated by improved surface redox properties. Through DFT calculations and microkinetic simulations, we explored the complete reaction pathway and kinetics of CH_4 oxidation on both CeO_2 and Ni-doped CeO_2 surfaces. Our findings suggest that Ni doping modifies the surface properties of CeO_2 , which in turn balances the energy barriers of the two key steps, thus

enhancing the overall reaction activity. This work provides new insights for the rational design of oxide catalysts for low-temperature CH₄ oxidation.

II. COMPUTATIONAL DETAILS

A. Methods

Spin-polarized DFT calculations were performed using the Vienna Ab initio Simulation Package (VASP) with the projector-augmented wave (PAW) treatment of the core electrons, while a plane-wave kinetic energy cutoff of 400 eV was applied to treat valence electrons.³¹⁻³³ The Perdew–Burke–Ernzerhof (PBE) functional with the generalized gradient approximation (GGA) was employed for the exchange-correlation potential and van der Waals dispersion forces between the adsorbate and surface were accounted for using the zero damping DFT-D3 method of Grimme.^{34, 35} The DFT + *U* approach with a *U* value of 4.5 eV was utilized to address the strong on-site Coulomb and exchange interaction of localized Ce 4*f* electrons.³⁶ Structural optimizations utilized a 3 × 3 × 1 *k*-point grid in the Monkhorst-Pack scheme, while electronic structure calculations employed a 5 × 5 × 1 *k*-point mesh.³⁷ Convergence criteria for force and energy were set to 0.05 eV/Å and 10⁻⁴ eV, respectively.

The climbing image-nudged elastic band (CI-NEB) method and the dimer approach were employed to locate the saddle points.^{38, 39} The reaction energy (ΔE) for an elementary step was determined by the energy difference between the initial state (IS) and its corresponding final state (FS). The activation barrier (E_a) was identified as the energy difference between the transition state (TS) and its corresponding initial state.

The formation energies of oxygen vacancies were calculated using the following equations: $E_{O_v} = E_{\text{surface}-O_v} - E_{\text{surface}} + 1/2E_{O_2}$ and $E_{2O_v} = E_{\text{surface}-2O_v} - E_{\text{surface}-O_v} + 1/2E_{O_2}$. Here, E_{surface} represents the energy of the clean surface, $E_{\text{surface}-O_v}$ the energy of the surface with an oxygen vacancy, $E_{\text{surface}-2O_v}$ the energy of the surface with two oxygen vacancies and E_{O_2} the energy of a gas-phase O_2 molecule.

Microkinetic simulations were conducted employing the CATKINAS package⁴⁰,⁴¹ under experimental conditions¹⁸ spanning temperatures from 400 to 1000 K and pressures from 0.01 to 1 bar. The feed ratio utilized was $CH_4:O_2:Ar = 1:5:9$, with a total flow rate of 30 sccm. The elementary reactions employed for the microkinetic simulations are enumerated in Table S1. In the microkinetic analysis, entropic (S) effects and zero-point energies (ZPE) were considered to estimate the Gibbs free energy change (ΔG) of each elementary step, calculated as $\Delta G = \Delta H - T\Delta S + \Delta ZPE$.

B. Models

The DFT optimized lattice parameter of bulk CeO_2 is 5.42 Å, which closely matches the experimental value of 5.41 Å.⁴² Three crystal facets, namely (111), (110) and (100), were chosen for investigation in this study. For the $CeO_2(111)$ surface, a 3×3 nine-layer slab comprising 27 Ce atoms and 54 O atoms was utilized. The bottom three layers of the slab were kept fixed. Similarly, the $CeO_2(110)$ surface was modeled with a 2×3 five-layer slab containing 30 Ce atoms and 60 O atoms, with the bottom two layers fixed. **For $CeO_2(100)$, the surface instability is susceptible to reconstruction due to a dipole moment perpendicular to the surface. Therefore, we moved half of the**

oxygen atoms in the top layer of the model to the opposite surface to eliminate the dipole, a method has been applied in previous studies.⁴³⁻⁴⁵ Accordingly, a 2×2 seven-layer $\text{CeO}_2(100)$ slab consisting of 24 Ce atoms and 48 O atoms was used, with its bottom two layers fixed. A vacuum space of 15 Å was set along the z -direction to avoid interactions between periodic images. Furthermore, $\text{Ni/CeO}_2(111)$, $\text{Ni/CeO}_2(110)$, and $\text{Ni/CeO}_2(100)$ surfaces were obtained by replacing a surface Ce atom with a Ni atom with Ni doping mass fractions of 1.29, 1.16, and 1.46 wt %, respectively, which are close to the experimental measurement.²⁹

III. RESULTS AND DISCUSSION

A. Structures and properties for pristine and Ni-doped CeO_2 surfaces

Models of the Ni-doped CeO_2 surfaces were obtained by replacing Ce at different layers by Ni. Fig. 1 shows the lowest energy optimized geometries of the pristine CeO_2 and Ni-doped CeO_2 surfaces, denoted as $\text{CeO}_2(111)$, $\text{CeO}_2(110)$, $\text{CeO}_2(100)$, $\text{Ni/CeO}_2(111)$, $\text{Ni/CeO}_2(110)$, and $\text{Ni/CeO}_2(100)$, respectively. These favorable structures are all attributable to doping near the surface layer, with doping energies of 0.71, -0.25, and -0.58 eV, respectively (Table S2). Several other higher energies doping structures have been found as shown in Fig. S1, but they are not used in the mechanistic studies discussed below. As shown in Fig. 1, the introduction of Ni causes significant distortions on the $\text{CeO}_2(111)$ and $\text{CeO}_2(110)$ surfaces. To maintain structural stability, the Ni atom migrates downward and coordinates with four neighboring oxygens, forming a stable square planar structure. This motif suggests that the Ni is stable and

unlikely to participate in catalysis directly, as confirmed by DFT results discussed below. The two surface oxygens that were originally bonded to the replaced Ce are transformed into a two-coordinated configuration that bonded to two neighboring Ce atoms. As shown below, these oxygens are labile and involved in the catalysis. However, Ni doping does not change the surface lattice on $\text{CeO}_2(100)$, with the Ni coordinated with four oxygen atoms, but not at a square planar geometry.

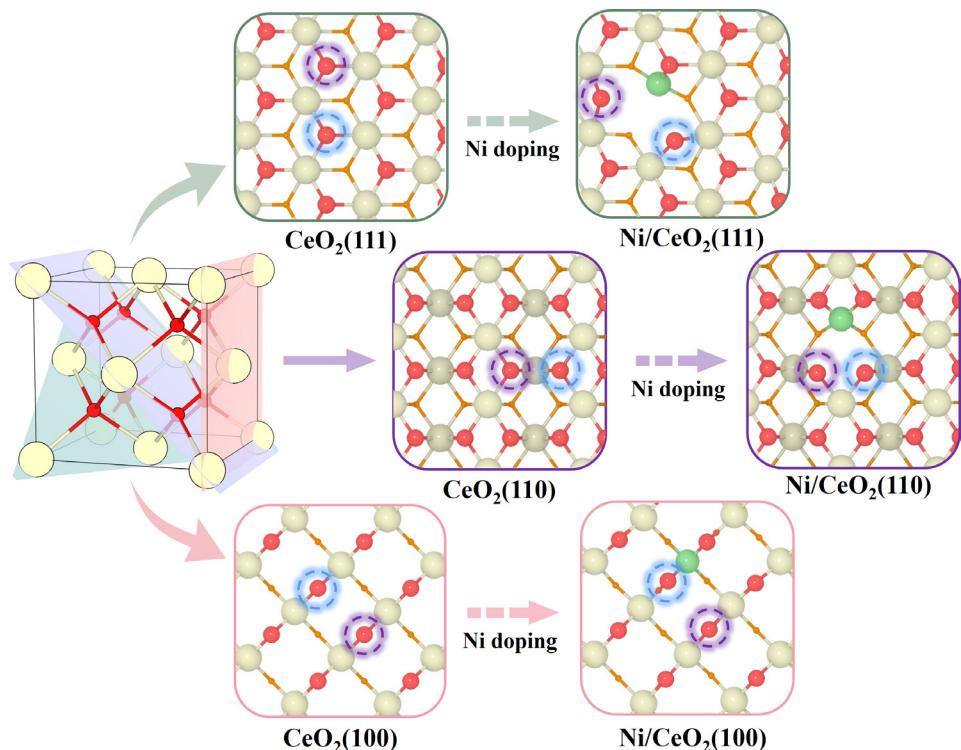


FIG. 1. Top view of optimized structures of pristine CeO_2 and Ni-doped CeO_2 surfaces.

The dashed blue and purple circles represent locations of the first and second oxygen vacancies. Color scheme: Ce, yellow; Ni, green; surface O, red; subsurface O, orange. The (111), (110) and (100) facets of CeO_2 are color coded as green, violet and pink, respectively.

As discussed earlier, the catalytic activity of CeO_2 -based catalysts for CH_4

oxidation is known to be strongly affected by their redox properties, which are related to the ease of surface oxygen vacancy formation. Therefore, we first investigated the formation of oxygen vacancy on CeO_2 and Ni/CeO_2 surfaces and named it as the first oxygen vacancy (O_v). The location of the first oxygen vacancy is indicated by the dashed blue circles in Fig. 1. The calculated lowest formation energy (E_{Ov}) of the first oxygen vacancy on pristine and Ni-doped CeO_2 surfaces is listed in Table 1. On pristine CeO_2 , E_{Ov} follows the order as $(111) > (100) > (110)$, with $\text{CeO}_2(110)$ having the lowest value of 1.73 eV, which is consistent with the previous conclusion by Wu et al.⁴⁶ Ni doping effectively promotes defect formation, especially on $\text{CeO}_2(111)$ and $\text{CeO}_2(110)$. The first oxygen vacancy formation on the $\text{Ni}/\text{CeO}_2(111)$ and (110) surfaces is actually exothermic, with E_{Ov} of -0.42 and -0.59 eV, respectively. This was also mentioned in our earlier papers.^{29,30} In comparison, the reduction of E_{Ov} of $\text{CeO}_2(100)$ is more modest, decreasing from 1.90 to 0.41 eV. Due to the easy formation of O_v on Ni-doped CeO_2 surfaces, models with one O_v ($\text{Ni}/\text{CeO}_2-\text{O}_v$) were used to simulate the CH_4 oxidation. To allow comparison with $\text{Ni}/\text{CeO}_2-\text{O}_v$, we also utilized the models with a single O_v (denoted as CeO_2-O_v) for undoped CeO_2 .

TABEL 1. The formation energy of the first (E_{Ov}) and second ($E_{2\text{Ov}}$) oxygen vacancies on the CeO_2 and Ni/CeO_2 surfaces.

Surface	E_{Ov} (eV)	$E_{2\text{Ov}}$ (eV)	Surface	E_{Ov} (eV)	$E_{2\text{Ov}}$ (eV)
$\text{CeO}_2(111)$	2.57	2.73	$\text{Ni}/\text{CeO}_2(111)$	-0.42	1.49
$\text{CeO}_2(110)$	1.73	2.31	$\text{Ni}/\text{CeO}_2(110)$	-0.59	1.49

CeO ₂ (100)	1.90	2.34	Ni/CeO ₂ (100)	0.41	2.10
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B. Methane activation and water formation on CeO₂-O_v and Ni/CeO₂-O_v surfaces

Activation of CH₄ has often been considered the most crucial elementary step in the CH₄ conversion reactions.^{21, 47} However, the formation of H₂O is closely related to oxygen release and has recently been noted to play a key role in CH₄ oxidation.^{24, 25} Therefore, we first focused on the energetics of the CH₄* activation and H₂O* formation steps on the CeO₂-O_v and Ni/CeO₂-O_v surfaces.

Metal cations with strong Lewis acidity and oxygen anions with strong Lewis basicity are known to be active in C–H bond cleavage.⁴⁸ Frustrated Lewis Pairs (FLPs), with a suitable spatial blockage between acidic sites and basic sites,^{49, 50} have capacity to activate the CH₄ molecules.⁵¹ In Fig. 2, the electron density isosurface displays the electrostatic potential distribution of the CeO₂-O_v and Ni/CeO₂-O_v surfaces. The exposed surface Ce atoms can form a Ce-O(a) FLP with non-adjacent oxygen atoms, which might serve as active sites for CH₄ activation. Our initial investigation is focused on the breakage of the first C–H bond by these FLP sites. To this end, CH₄ first adsorbs at the FLP site, followed by the breaking of the first C–H bond resulting in the adsorption of CH₃* and H* on the Ce cation and lattice oxygen sites, respectively. The corresponding geometries and energy barriers are shown in Fig. S2 and Table 2, respectively.

Table 2 and Fig. 3(a) show that for the CeO₂-O_v surfaces, the (100) surface has the

most effective activation of the C–H bond, with an energy barrier of 0.78 eV. The (111) and (110) surfaces have higher energy barriers of 1.19 and 1.03 eV, respectively. These reactions are all endothermic. For the Ni/CeO₂-O_v surfaces, the energy barrier for C–H bond breaking on the (100) surface has the lowest value at 1.07 eV. On the (111) surface, this step requires an energy barrier of 1.23 eV. On the (110) surface, the reaction has no barrier but with an endothermicity of 1.25 eV. This suggests that the ability of FLP sites for C–H bond breaking was weakened after Ni doping. This may be due to the less negative Bader charge values of the O(a) after Ni doping (Fig. 2), e.g., from $-1.22|e|$ to $-1.15|e|$ on the (111) surface, which reduces the ability of O(a) for accepting the hydridic H*. **We also tried to calculate the C–H activation by the H abstraction mechanism, however the unstable CH₃• still returns to the surface to CH₃* during the optimization process.** However, the above results seems to conflict with the positive correlation between surface redox properties and catalytic activity of CeO₂ observed in a previous experiment.¹⁸

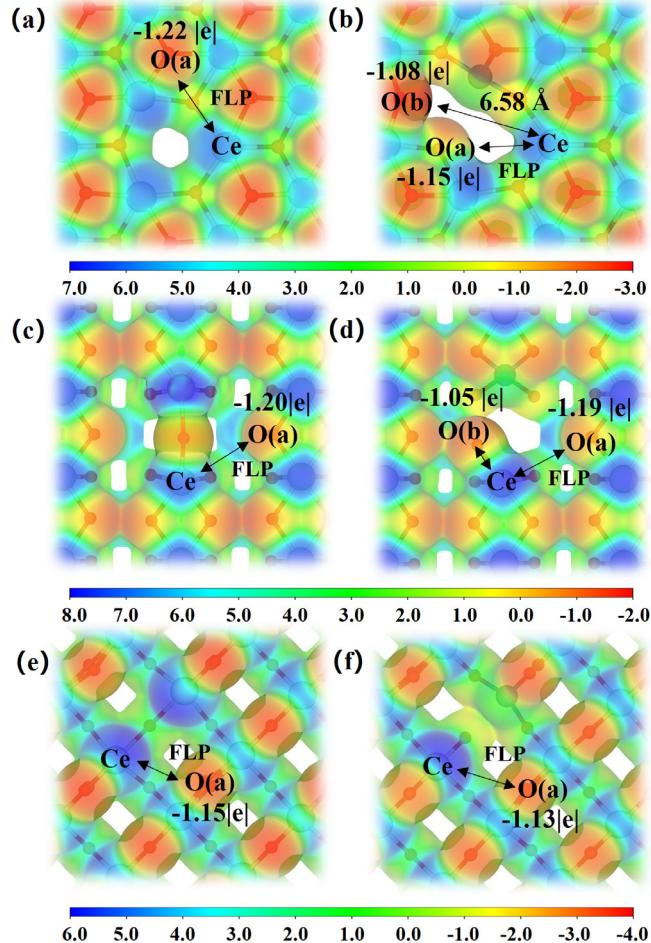


FIG. 2. Electron density isosurfaces of (a) $\text{CeO}_2(111)\text{-O}_v$, (b) $\text{Ni}/\text{CeO}_2(111)\text{-O}_v$, (c) $\text{CeO}_2(110)\text{-O}_v$, (d) $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$, (e) $\text{CeO}_2(100)\text{-O}_v$ and (f) $\text{Ni}/\text{CeO}_2(100)\text{-O}_v$. The electron-density isosurfaces are plotted at 0.01 e bohr^{-3} . The color bar represents the electrostatic potential scale. The black numbers are the calculated Bader charge values. The Ce-O FLP sites are marked with arrows.

TABLE 2. Energy barriers for CH_4^* activation (E_{a1}) and H_2O^* formation (E_{a2}) on the $\text{CeO}_2\text{-O}_v$ and $\text{Ni}/\text{CeO}_2\text{-O}_v$ Surfaces.

Surface	E_{a1} (eV)	E_{a2} (eV)	Surface	E_{a1} (eV)	E_{a2} (eV)
$\text{CeO}_2(111)$	1.19	1.78	$\text{Ni}/\text{CeO}_2(111)$	1.23	0.83
$\text{CeO}_2(110)$	1.03	1.62	$\text{Ni}/\text{CeO}_2(110)$	1.25/1.18	1.06
$\text{CeO}_2(100)$	0.78	1.64	$\text{Ni}/\text{CeO}_2(100)$	1.07	1.63

Note: The numbers of 1.78, 1.64, and 1.25 eV are ΔE values without a transition state.

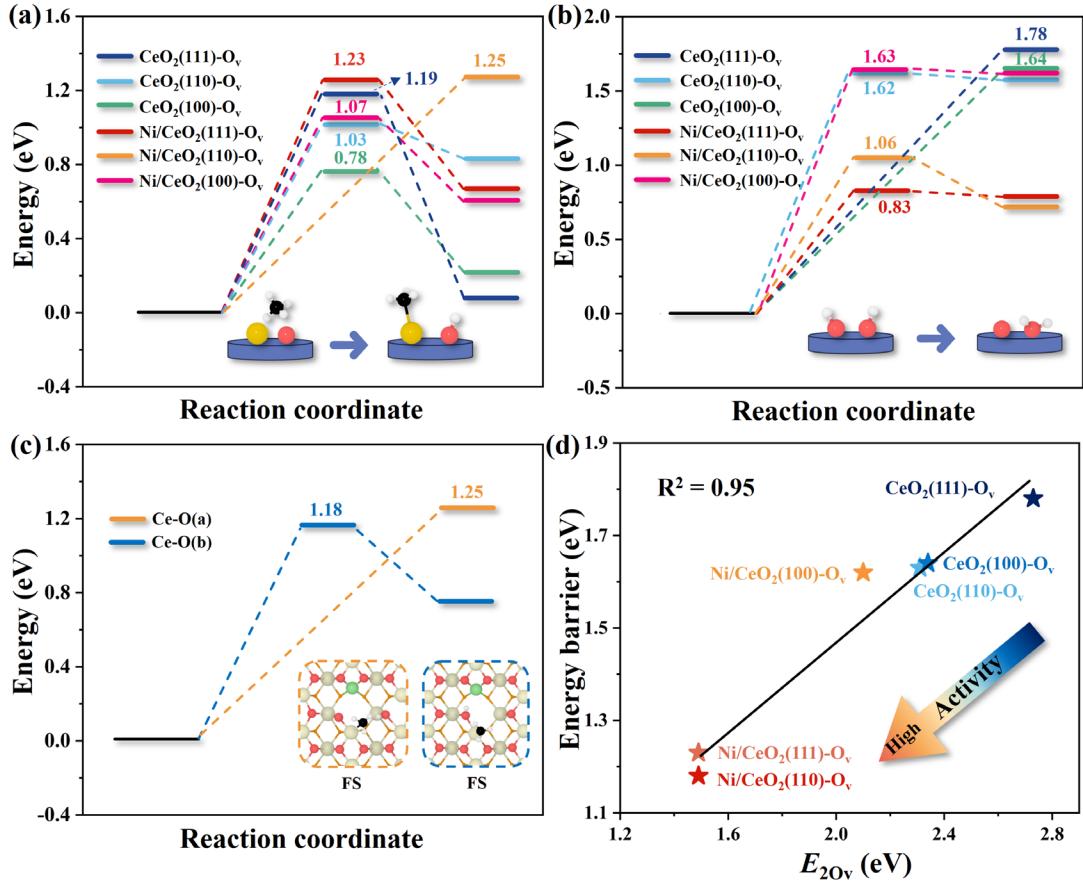


FIG. 3. Calculated energetics of (a) $\text{CH}_4^* \rightarrow \text{CH}_3^* + \text{H}^*$ and (b) $2\text{OH}^* \rightarrow \text{H}_2\text{O}^* + \text{O}^*$ on the CeO_2-O_v and $\text{Ni/CeO}_2-\text{O}_v$ surfaces. (c) Calculated energetics of $\text{CH}_4^* \rightarrow \text{CH}_3^* + \text{H}^*$ on the Ce-O(a) site and Ce-O(b) sites of the $\text{Ni/CeO}_2(110)-\text{O}_v$ surface. (d) Relationship between the highest energy barriers of key steps and the $E_{2\text{O}_v}$ values.

Next, we investigated the H_2O^* formation on the CeO_2-O_v and $\text{Ni/CeO}_2-\text{O}_v$ surfaces. To determine which O atom is the most easily reduced to H_2O^* , we investigated the formation of a new oxygen vacancy on the CeO_2-O_v and $\text{Ni/CeO}_2-\text{O}_v$ surfaces and named it as the second oxygen vacancy (2O_v) (see Fig. S3). Fig. 1 shows the location for generating the second oxygen vacancy with the lowest energy cost, indicated by the purple dashed circles. The data shown in Table 1 demonstrate that the

second oxygen vacancy ($E_{2\text{Ov}}$) on the CeO_2 surface follows the same trend as the E_{Ov} . The (111) surface has the highest $E_{2\text{Ov}}$ of 2.73 eV, while the (110) surface has the lowest $E_{2\text{Ov}}$ of 2.31 eV. In contrast, the $E_{2\text{Ov}}$ values on the Ni/CeO_2 surfaces are markedly smaller. Compared to the pristine CeO_2 surface, the trend changes from (111) > (100) > (110) to (100) > (111) = (110). Upon the comparison of the above results, it is observed that on the Ni/CeO_2 (111) and (110) surfaces, the second oxygen vacancy tends to be generated by the two-coordinated oxygen (O(b)) rather than the oxygen of the FLP site (O(a)). According to Bader analysis, the Bader charges of O(a) and O(b) are -1.19 and $-1.05 \text{ } |\epsilon|$, respectively. Therefore, compared to O(a), O(b) has less electron transfer with Ce sites, indicating a weaker interaction with the surface. This makes O(b) more reactive as a lattice oxygen (see Figs. 2(b) and 2(d)).

Then, the energetics of H_2O^* formation on these surfaces were calculated, and the optimized geometries of stationary points along the reaction path are shown in Fig. S4. Table 2 and Fig. 3(b) show that the H_2O^* formation barriers (or endothermicities in the absence of barriers) on CeO_2 (111), (110) and (100)- O_v surfaces are 1.78, 1.62 and 1.64 eV, respectively. Interestingly, these values are higher than the corresponding CH_4^* activation barriers, suggesting that the formation of H_2O on pristine surfaces is more difficult. We further investigated the effect of H coverage on the H_2O^* formation step as shown in Fig. S5. The results show that on the CeO_2 (111)- O_v surface, a small amount of H coverage promotes H_2O^* formation. On the CeO_2 (110)- O_v and CeO_2 (100)- O_v surfaces, it is found that the additional H increases the reaction energy of H_2O^* formation. However, the formation of H_2O is still more difficult than the activation of

CH₄* on all three surfaces. Therefore, solely considering CH₄* activation as an indicator for evaluating catalytic activity is apparently inadequate and potentially misleading. On Ni-doped CeO₂ surfaces, the energy barriers of H₂O formation are reduced to 0.83, 1.06 and 1.63 eV for (111), (110) and (100) facets, respectively, indicating that H₂O* formation is easier on Ni/CeO₂-O_v surfaces compared to the CeO₂-O_v surfaces. It is worth mentioning that the H₂O* formation barriers remain higher than CH₄* activation on the Ni/CeO₂(100)-O_v surface.

To verify if CH₄* activation on the Ni/CeO₂(111)/(110)-O_v surfaces can occur on O(b) sites, additional calculations on the energy barrier of the C-H bond on the Ce-O(b) site were conducted. However, the distance between Ce-O(b) on the Ni/CeO₂(111) surface is too long (6.58 Å) to serve as the site for CH₄* dissociation into CH₃* and H* (see Fig. 2(b)). In contrast, the Ce-O(b) site on the Ni/CeO₂(110)-O_v surface exhibits superior activation of the C-H bond, with a lower barrier than the Ce-O(a) FLP site (1.18 vs. 1.25 eV, as shown Fig. 3(c)). This implies that on the Ni/CeO₂(110)-O_v surface, the two-coordinated oxygen serves as the primary site for both CH₄ activation and H₂O formation.

To further understand the influence of O_v formation on the catalytic activity, the relationship of E_{2Ov} with the highest energy barriers of the key steps is investigated, as displayed in Fig. 3(d). The data shows a linear relationship between the barriers and E_{2Ov} , indicating that lower E_{2Ov} values correspond to lower barriers. Given the multiple possibilities revealed by these results, a comprehensive assessment of both CH₄* activation and H₂O* formation steps seems to be necessary to explain the

experimentally observed positive correlation between the redox properties of CeO_2 surfaces and catalytic activity. As shown in Fig. 3(d), the activity is most significantly enhanced on $\text{Ni}/\text{CeO}_2(111)/(110)\text{-O}_v$ surfaces due to the formation of active two-coordinated oxygen species upon Ni doping, which enhances surface redox properties. Unlike many other doped metals on CeO_2 surfaces that directly participate in the reaction,⁵²⁻⁵⁴ the Ni dopant serves as a single-atom promotor as it is not actively involved in the catalysis.^{29, 30} Overall, we have compared the effects of different crystal planes and Ni doping on the key steps of the CH_4 oxidation reaction under the same vacancy coverage, but there are some other factors that could be further investigated in the future, such as the oxygen vacancy concentration.

C. Methane oxidation mechanism on $\text{CeO}_2(110)\text{-O}_v$ and $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$

To gain a more complete understanding of the reaction pathways, we studied the entire process of CH_4 oxidation on the most promising $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ surface and compared it with the corresponding $\text{CeO}_2(110)\text{-O}_v$ surface. The corresponding geometries, reaction energies (ΔE), and barriers (E_a) for elementary steps are shown in Figs. S6-S7 and Table 3. Fig. 4 illustrates the potential energy diagram for the catalytic cycle on the $\text{CeO}_2(110)\text{-O}_v$ and $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ surfaces with illustrations of the stationary point geometries.

TABLE 3. Reaction energies (ΔE) and energy barriers (E_a) for the elementary steps in CH_4 oxidation on $\text{CeO}_2(110)\text{-O}_v$ and $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ surfaces.

Steps	$\text{CeO}_2(110)\text{-O}_v$	$\text{Ni}/\text{CeO}_2(110)\text{-O}_v$	Notes
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	ΔE (eV)	E_a (eV)	ΔE (eV)	E_a (eV)	
S0 to S1	−0.61	—	−0.33	—	CH ₄ adsorption
S1 to S2	0.83	1.03	0.75	1.18	First C–H bond cleavage
S2 to S3	−0.28	—	0.27	0.37	H* migration
S3 to S4	0.90	1.01	0.50	0.79	Second C–H bond cleavage
S4 to S5	1.07	1.37	0.72	1.06	H ₂ O* formation
S5 to S6	0.80	—	0.95	—	H ₂ O* desorption
S6 to S7	−1.62	—	−3.41	—	O ₂ adsorption
S7 to S8	−1.49	0.28	—	—	O ₂ --CH ₂ * complex formation
S8 to S9	−2.84	—	−2.85	0.06	O–O bond cleavage and CH ₂ O* formation
S9 to S10	0.06	0.27	0.06	0.93	Third C–H bond cleavage
S10 to S11	−0.35	—	0.16	0.31	H* migration
S11 to S12	—	—	0.68	—	CHO* transformation
S12 to S13	−1.11	0.33	−2.72	—	Fourth C–H bond cleavage
S13 to S14	1.58	1.62	1.00	—	H ₂ O* formation
S14 to S15	0.74	—	1.03	—	H ₂ O* desorption
S15 to S16	−3.05	—	−1.58	—	O ₂ adsorption
S16 to S17	−1.35	0.53	0.71	0.77	O ₂ --CO* complex formation
S17 to S18	−1.25	0.23	−4.09	0.45	O–O bond cleavage and CO ₂ * formation
S18 to S0	0.31	—	0.48	—	CO ₂ * desorption

Note: “—” represents the absence of transition states or corresponding intermediates.

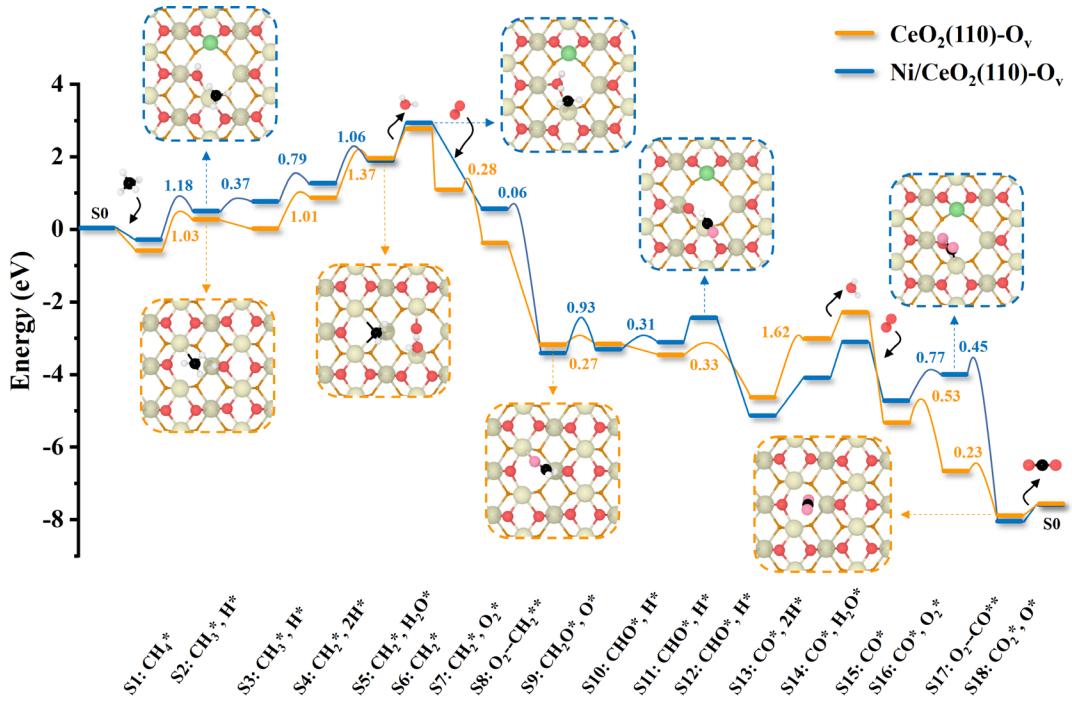


FIG. 4. Potential energy diagram for the reaction $\text{CH}_4 + 2\text{O}_2 \rightarrow 2\text{H}_2\text{O} + \text{CO}_2$ on $\text{CeO}_2(110)\text{-O}_v$ and $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ surfaces. The structures of selected intermediates are illustrated (all structures in Figs. S6 and S7). Color scheme: Ce, yellow; Ni, green; C, black; H, white, surface O, red; subsurface O, orange; O in adsorbate, pink; The adsorbed species are denoted with asterisks (*).

On $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$, CH_4 is first adsorbed above an oxygen vacancy with an adsorption energy of -0.33 eV, followed by the first C–H bond activation, leading to a CH_3^* species adsorbed on the Ce site and H^* captured by the O(b) (S1 to S2) after overcoming a barrier of 1.18 eV. Since the further dehydrogenation of the CH_3^* species requires a high barrier of up to 1.68 eV (Fig. S8), the H^* species first migrate to the adjacent lattice oxygen with a low barrier of 0.37 eV (S2 to S3) before breaking the second C–H bond, forming CH_2^* and H^* adsorbed on the vacant O(b) site with an

endothermicity of 0.50 eV and a barrier of 0.79 eV (S3 to S4). Next, the migrated H* species returned to the O(b) site through a 1.06 eV barrier, producing the first H₂O* and CH₂* co-adsorbed on the Ni/CeO₂(110)-O_v surface (S4 to S5).

Likewise, the further activation of the third C–H bond before forming the first H₂O* is also an unfavorable step compared to H₂O* formation (Fig. S9). Desorption of the product H₂O* leaves an oxygen vacancy on the surface (S6). Next, an O₂ molecule fills this vacancy and spontaneously forms the O₂–CH₂** complex by attacking CH₂* (S8). After that, the O–O bond in O₂–CH₂** breaks, releasing 2.85 eV of energy. One O atom restores the oxygen vacancy, and CH₂O* remains adsorbed on the Ce site (S8 to S9). The activation of the third C–H bond is slightly endothermic. After overcoming a 0.93 eV barrier, O(b) captures the H atom, forming CHO* (S9 to S10).

The fourth C–H bond undergoes barrierless activation (S10 to S13) through H* migration and CHO* transformation, resulting in the oxidation of CH₄* to CO*. Similarly, the migrating H* returns to the O(b) site and combines with the hydroxyl group, producing the second H₂O*. This step has no transition state but an endothermicity of 1.00 eV (S13 to S14). The resulting H₂O* species desorbs, creating an oxygen vacancy to accommodate the adsorption of the second O₂ (S15). Upon O₂ adsorption, the O–O bond is activated with an adsorption energy of –1.58 eV (S16). The combination of co-adsorbed O₂* and CO* leads to the formation of O₂–CO** complex, which requires an endothermicity of 0.71 eV and a barrier of 0.77 eV (S16 to S17). Finally, the O₂–CO* undergoes further O–O bond cleavage, restoring the oxygen vacancy and yielding the final oxidized product CO₂* (S17 to S18). **Meanwhile, we**

also explored the mechanism starting from O_2 adsorption, as shown in Fig. S10 and Table S3. O_2 tends to adsorb on the Ce site of the Ni/CeO₂(110)-O_v surface, yielding an adsorption energy of -0.47 eV. However, the subsequent dissociation of O_2^* into two O* atoms is highly endothermic up to 2.86 eV, thus hindering the reaction progress and is not considered further. Overall, the rate-determining step of the entire reaction cycle is the activation of CH_4^* , where O(b) plays a crucial role in trapping the H* species and participating in the reduction to H₂O*.

On the CeO₂(110)-O_v surface, CH₄ adsorption is stronger than that on Ni/CeO₂(110)-O_v with a calculated adsorption energy of -0.61 eV. The first chemical step involves CH_4^* dissociation into CH_3^* and H* at the Ce-O(a) FLP site by overcoming an energy barrier of 1.03 eV. Subsequently, the resulting CH_3^* undergoes continuous dehydrogenation and oxidation to CO₂* through a similar pathway as on Ni/CeO₂(110)-O_v. Compared to the Ni/CeO₂(110)-O_v surface, the CeO₂(110)-O_v surface has a lower barrier for CH_4^* dissociation but a higher barrier for the subsequent H₂O* formation, which is the rate-determining step in the overall reaction pathway due to the more stabilized lattice oxygen. The energy barrier for the second H₂O* formation is 1.62 eV. In fact, at the beginning of the reaction, the active site is likely to be blocked and the reaction may be hindered due to the strong competition between O_2 and CH₄ adsorption on the CeO₂(110)-O_v surface and the difficulty of dissociating O_2^* into active oxygen with a reaction energy of 1.76 eV (Fig. S11 and Table S3).

The above results suggest that CH₄ oxidation on the CeO₂(110)-O_v and Ni/CeO₂(110)-O_v catalysts proceeds via the Mars-van Krevelen (MvK) mechanism,

which is typical for metal oxide catalysts. For example, Chen et al. proposed that CH₄ oxidation on Ni₁₀/CeO₂(111) catalysts proceeds through CH₄* activation at the Ni-CeO₂ interface, followed by CH₄* dissociation and H₂O* formation.²⁸ The calculated heats of reaction for these steps are about 1.10 and 2.00 eV, respectively. The reaction eventually oxidizes to CO₂ and H₂O via the MvK mechanism.²⁸ The major difference of our model from that of Chen et al. is that Ni in our models is a dopant while the previous work studied a Ni cluster adsorbed on the CeO₂ surface.

In short, based on this work and some earlier studies^{27, 28} of the CH₄ oxidation mechanism, both CH₄* activation and H₂O* formation are shown to be the key catalytic steps. As an atomic dopant, Ni regulates the surface properties and balances the kinetics of CH₄* activation and H₂O* formation, leading to a shift in the rate-determining step and an improvement in overall reactivity of CeO₂ catalysts.

IV. Microkinetic simulations

Microkinetic simulations facilitate our understanding of the overall reaction mechanism of complex reactions under realistic conditions. To further elucidate the activity of catalyzed CH₄ oxidation under different working conditions and to quantify the contribution of the elementary reaction steps, we performed microkinetic simulations based on the energetics of all of the aforementioned elementary reaction steps.

The turnover frequencies (TOF) of CO₂ products calculated on the CeO₂(110)-O_v and Ni/CeO₂(110)-O_v catalysts at a temperature range of 400 to 1000 K and a pressure

range of 0.01 to 1 bar are displayed in Figs. 5(a) and 5(b). The results show that the TOF for CO₂ production varies significantly with temperature, while only at medium-high temperatures a weak variation with pressure was observed. This is apparently due to the significant effect that small molecules have on the entropy value at medium and high temperatures. Moreover, the Ni/CeO₂(110)-O_v catalyst exhibits 3-4 orders of magnitude higher TOFs of CO₂ production than the CeO₂(110)-O_v catalyst at all temperature and pressure ranges. Specifically, the TOF of CO₂ formation on Ni/CeO₂(110)-O_v at 900 K and a total pressure of 1 bar can reach 5.83×10^{-3} s⁻¹, compared to 2.75×10^{-6} s⁻¹ on the CeO₂(110)-O_v catalyst. This difference is consistent with the DFT barriers. Furthermore, changing the ratio of CH₄:O₂ has a minor effect on the TOFs of CO₂ production (see Figs. S12 and S13). Unfortunately, there is still no report on measurements of TOF on these catalysts.

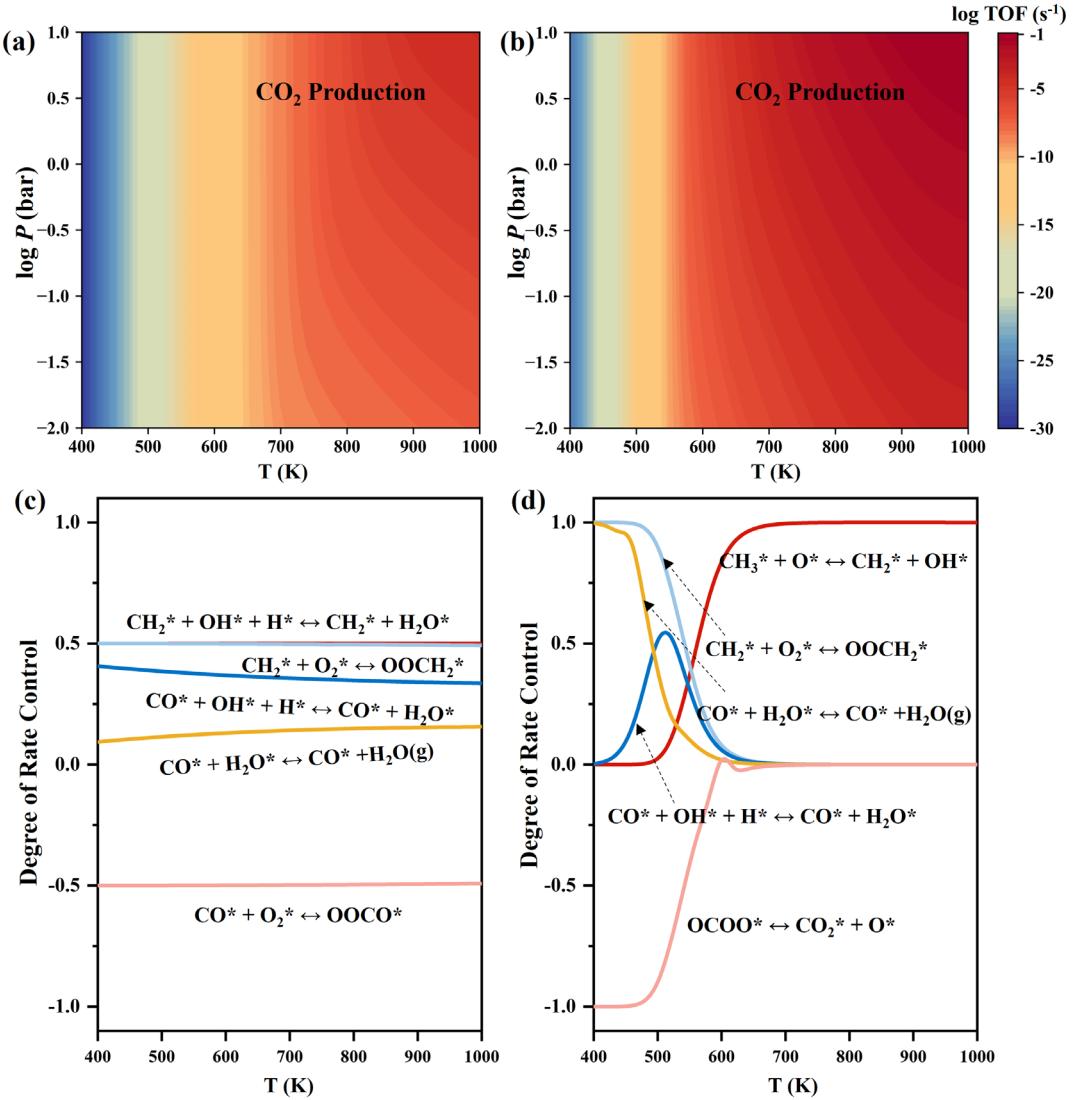


FIG. 5. Map of TOF under different pressure (P) and temperature (T) working conditions for the CH₄ oxidation reaction on the (a) CeO₂(110)-O_v and (b) Ni/CeO₂(110)-O_v surfaces for CO₂ production. Degree of rate control analysis as a function of temperature on (c) CeO₂(110)-O_v and (d) Ni/CeO₂(110)-O_v surfaces.

The degree of rate control (DRC) reflects the sensitivity of elementary steps throughout the entire reaction.⁵⁵ As shown in Fig. 5(c), DRC analysis indicates that reducing the H₂O* formation barrier and accelerating the coupling of CH₂* with O₂* are crucial for enhancing the overall reaction rate on the CeO₂(110)-O_v catalyst. This is

because the high energy barrier of the former limits the reaction rate, while the latter promotes the consumption of CH_2^* species facilitating the reaction in a positive direction. For the $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ catalyst, DRC analysis revealed that the generation and desorption of H_2O^* and the coupling of CH_2^* to O_2^* were important steps affecting the overall reaction rate only at low temperatures, but became irrelevant above 600 K (Fig. 5(d)). This is attributed to the reduced energy barrier for H_2O^* formation on the $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ catalyst, which becomes less challenging after 600 K. Under these circumstances, the formation of OH^* species makes the largest contribution to the overall reaction rate. These results indicate that Ni-doped $\text{CeO}_2(110)$ significantly enhances the activation of catalytic CH_4 oxidation under simulated conditions, consistent with the recent experimental observations¹⁸. This provides useful insights for designing low-temperature CH_4 oxidation catalysts.

V. Conclusions

In summary, we performed a comprehensive assessment of the key steps of CH_4 oxidation and their dependence on surface properties in pristine and Ni-doped CeO_2 surfaces using DFT. Several models, including $\text{CeO}_2(111)$, $\text{CeO}_2(110)$, $\text{CeO}_2(100)$, $\text{Ni}/\text{CeO}_2(111)$, $\text{Ni}/\text{CeO}_2(110)$ and $\text{Ni}/\text{CeO}_2(100)$ containing one O_v , have been constructed to understand the impact of the redox properties on the catalysis. The CH_4 oxidation activity and reaction mechanism on $\text{CeO}_2(110)\text{-O}_v$ and $\text{Ni}/\text{CeO}_2(110)\text{-O}_v$ were explored further using microkinetic simulations. The main conclusions are as follows: (1) The ease of oxygen vacancy formation (E_{ov}) for the pristine CeO_2 surface ranks as $(111) > (100) > (110)$. However, the Ni doping generates two-coordinated

oxygen on the (111) and (110) surfaces, and oxygen vacancies are formed spontaneously. As a result, the order of E_{OV} changes to (100) > (111) = (110). (2) The highest energy barriers for CH_4^* activation and H_2O^* formation on the $\text{CeO}_2\text{-O}_\text{v}$ and $\text{Ni/CeO}_2\text{-O}_\text{v}$ surfaces are linearly correlated with E_{2OV} , with the $\text{Ni/CeO}_2\text{-O}_\text{v}$ (110) surface possessing the best activity for CH_4 oxidation. (3) The CH_4 oxidation reaction on CeO_2 (110)- O_v and Ni/CeO_2 (110)- O_v surfaces follows the MvK mechanism. With Ni doping, the rate-determining step shifts from CH_4^* activation to H_2O^* formation. The energy barrier of the rate-determining step decreases from 1.62 to 1.18 eV upon Ni doping, which significantly improves the overall activity of the CeO_2 catalyst. (4) Microkinetic simulations demonstrate that the TOFs values of CO_2 conversion on $\text{Ni/CeO}_2\text{-O}_\text{v}$ (110) are 3-4 orders of magnitude higher than those of $\text{CeO}_2\text{-O}_\text{v}$ (110), which rationalizes the experimental observation of the superior performance of Ni-doped CeO_2 catalysis of CH_4 oxidation. Finally, it is concluded that the formation of H_2O^* as an elementary step significantly contributes to the overall reaction rate. These insights help to shed light on the mechanisms of CH_4 oxidation catalyzed by metal oxide catalysts.

ASSOCIATED CONTENT

Supporting Information: Additional results.

Notes

The authors declare no competing financial interests.

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