

Role of sodium sulfate in electrical conductivity and structure of lignin-derived carbons

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Abstract

Lignin is a promising renewable alternative to fossil fuels for producing carbon materials such as carbon fibers, activated carbons, or carbon black. Despite extensive research, lignin-derived carbon materials show limited graphitization relative to comparable petroleum-derived carbons. Further, ligninderived carbons show high variation in graphitization and electrical conductivity depending on the source of the lignin. Herein, nine lignins, derived from various feedstocks and isolation procedures, are pyrolyzed to produce biochar at 1100 °C. These lignins have a range of chemical compositions, carbon structures, and particle sizes. As a result, the pyrolysis behavior of these lignins varies, with powdered, clumped powder, and "foam" biochar morphologies resulting from finely powdered lignin. The produced biochars vary widely

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in both electrical conductivity, from 0.19 to 19 S/cm, and in-plane graphitic crystallite size, from 3.4 to 41.2 Å. A significant decrease in electrical conductivity is identified when Na₂S₀4 is removed from lignin, accompanied by an increase in graphitic crystallite size. Based on this finding, a quadratic relationship between biochar graphitic crystallite aspect ratio and electrical conductivity is proposed that builds on established quasi-percolation models for biochar electrical conductivity.

Keywords: Biochar, biocarbon, pyrolysis, non-graphitizing carbon, graphitization.

¹ 1. Introduction

² Developing renewable alternatives to petroleum-derived materials is criti3
cal to reducing our society's reliance on fossil fuels. Of particular interest are
4 carbon materials, such as carbon black, carbon fibers, and artificial graphite,
5 whose application is expected to grow rapidly in the coming decades [1]. 6
Lignin looks to be a promising alternative feedstock to petroleum due to 7 its
high aromatic carbon content [2]. Further, 50-100 Mt of lignin are iso8 lated
annually as a byproduct of paper-making and biorefinery industries [3], 9
which is anticipated to grow as cellulosic biorefineries continue to expand 10
in the coming decade [4]. However, economic factors primarily limit upcy11
cling of lignin waste streams [5]. As carbon materials are considered some 12
of the most valuable products of lignin [6], the development of simple pro13
cesses to convert this lignin to renewable carbon materials has the potential 14
to both reduce reliance on petroleum products and upcycle this important 15
waste stream.

¹⁶Lignin-derived carbon materials can be produced via pyrolysis and have
17 been extensively studied [2, 7, 8, 9, 10, 11]. During pyrolysis, oxygen and
18 hydrogen present in lignin react with carbon to form liquid and gas de19

composition products, reducing the content of hydrogen and oxygen in the 20 solid phase [12]. The resulting solid material has a graphitic carbon structure, porous morphology, and high electrical conductivity. With optimal 21 processing conditions and feedstock properties, lignin-derived carbons have 22 the potential to replace petroleum-derived materials such as carbon black 23 [11, 13], carbon fibers [7], and activated carbons[14]. Lignin-derived 24 biochars 25 and biocarbons have been examined for a broad set of applications, includ26 ing electrically conductive plastic additives, replacements for carbon black, 27 and active materials in battery electrodes [11, 13, 15, 16]. Lignin-derived 28 carbons are limited by lower graphitization and increased defects relative 29 to petroleum-derived carbon materials [7, 13, 17, 18]. Further, a large 30 range of electrical conductivity is observed for biochars graphitized at 31 around 1000 $^{\circ}\text{C}$, from 0.009 S/cm to 62.96 S/cm for lignins isolated with 32 different processes [10, 19].

33 These past studies point to lignin as a promising feedstock for various 34 carbon materials; however, its performance is consistently limited by lower 35 graphitization than petroleum-derived carbon materials [7, 13, 17, 18]. Fur36 ther, wide ranges of electrical conductivity and graphitization have been 37 reported for carbons derived from lignins isolated with different processes. 38 Since graphitization of lignin-derived carbons does not continue to increase 39 above pyrolysis temperatures of approximately 1000 $^{\circ}\text{C}$, graphitization can40 not typically be increased with higher carbonization temperatures [7, 20, 21].

41 Lignin molecular weight, inorganic content, and particle size have been 42 iden42 tified as critical factors that influence the graphitization of lignin during 43 pyrolysis [7, 10, 15]. Past studies differ in the role that common inorganic 44 compounds, such as sodium sulfate (Na₂SO₄) present in kraft lignins, play 45 in lignin pyrolysis. Some studies have proposed that Na₂SO₄ catalyzes the

46 formation of graphitic structures, while others propose that Na₂S₀4 inhibits
47 the formation of graphitic structures [22, 23, 24, 25], while recent
reviews 48 have highlighted this as an area in need of study [18].

49 This study investigates the role of different lignin isolation procedures, 50
dominant monomers, parameters, and feedstocks in the graphitization of 51
lignin-derived biochar. Lignins from nine different isolation approaches are 52
characterized for chemical structure, molecular weight, and thermal transi53
tions. These lignins are then pyrolyzed to form biochar at 1100 °C, and the 54
morphology, chemical composition, carbon structure, and electrical conduc55
tivity of these biochar are investigated. First, the relationship between lignin
56 processing and biochar carbon structure is examined. We hypothesize that
57 lignin oxygen content, which is expected to be strongly driven by the ratio
of
58 monomers in the lignin, will significantly affect biochar carbon structure and 59
electrical conductivity. Next, the role that Na₂S₀4 plays in lignin pyrolysis
60 is tested directly by removing Na₂S₀4 from lignin. We hypothesize that the
61 presence of Na₂S₀4 in lignin will increase biochar graphitization. This work
62 sheds light on how lignin properties impact carbon structures formed dur63
ing pyrolysis and can inform feedstock optimization to utilize this important
64 waste stream to create renewable and high-performance carbon materials.

65 2. Materials and Methods

66 2.1. Lignin sources and isolation

67 Three commercial lignins were obtained: alkaline lignin (TCI America, 68
Portland, OR, USA, product # L0082), dealkaline lignin (TCI America,
69 Portland, OR, USA, product # L0045), and alkali lignin (Sigma-Aldrich,
70 Inc., St. Louis, MO, USA, product # 370959). In addition, six laboratory71
isolated lignins were produced from hybrid poplar or corn stover using vari72
ous approaches for lignin isolation and recovery. These lignins vary in feed73
stock, isolation process, and isolation parameters (Table 1). These processes 74

are described in detail in the Supplemental Information. After isolation, 75 alkali-corn140, alkali-poplar 150, alkali-poplar 115, and alkali-poplar 145 were 76 washed with deionized water to remove Na₂SO₄, following previously applied 77 procedures [26].

78 Three different treatments were used to reduce lignin particle size prior 79 to pyrolysis to examine the impact of particle size on lignin pyrolysis. The 80 commercial lignins (TCI Alkaline, TCI Dealkaline, and Sigma Alkali) are 81 pyrolyzed as provided. Alkali-poplar 150, alkali-corn140, and alkali-poplar95 82 were ball milled (Retsch Mixer Mill 400) for 3 min at 30 Hz (1800 rpm).

Table 1: Summary of lignin isolation methods and molecular weights (weight average (M_n), number average (M_n), and polydispersity index (PDI)). Listed temperatures are the maximum processing temperatures.

Name (Abbreviation)	Feedstock	Process type	Max. process temp. (°C)	Mw (Da)	Mn (Da)	PDI (Mw/Mn)
TCI Alkaline (TA)	Wood	Commercial, Lignosulfonate	Unk.	60000 [27]	-	-
TCI Dealkaline (TD)	Wood	Commercial, Lignosulfonate	Unk.	60000 [27, 28]	-	-
Sigma Alkali (SA)	Softwood	Commercial, Kraft	Unk.	28000 [28]	5000	5.6
Alkali-corn140 (AC140)	Corn stover	Alkali pretreatment, acidification		11400	3100	3.7
alkali-poplar150 (AP150)	Poplar	Alkali pretreatment, acidification	150	12100		3.4
Alkali-poplar95 (AP95)	Poplar	Alkali pretreatment, acidification	95	8000 [29]	4300	5.3
Hydrolysis-corn (HC)	Corn stover	Alkali pretreatment, enzymatic hydrolysis	150	10000	4100	2.4
Alkali-poplar115 (AP115)	Poplar	Alkali pretreatment, acidification	115	8700	3500	2.5
Alkali -poplar145 (AP145)	Poplar	Alkali pretreatment, acidification	145	8400	3200	2.7
		Alkali pretreatment, acidification				
		Alkali pretreatment, acidification				

83 Alkali-poplar115, alkali-poplar 145, and hydrolysis-corn were ground with a
84 pestle and mortar for 3 min.

85 2.2. Biochar production

86 All nine lignins were converted to biochar via pyrolysis in a tube furnace.

87 Prior to pyrolysis or analysis, all lignins were stored in a drying oven at
105 88 °c for at least 24 h to reduce moisture content. Approximately 500
mg of

89 lignin was placed in an alumina boat (100 mm X 20 mm X 13 mm) within
90 the tube furnace (Lindberg/Blue M Mini Mite) fitted with an alumina tube.

91 The tube furnace was purged with nitrogen at 100 mL min⁻¹ for 10 min prior
92 to heating. During heating, the purge rate for nitrogen was reduced to 30
93 mL min⁻¹, and the lignin was heated at 10 °C min⁻¹ from room temperature
94 to 1100 °C, held for 1 h, and then allowed to cool to room temperature.
The 95 maximum pyrolysis temperature of 1100 °C was selected as past
studies show 96 limited increases in electrical conductivity at higher
pyrolysis temperatures 97 for non-graphitizing feedstocks, such as lignin
[21, 30].

98 After pyrolysis, the biochar was ball milled (Retsch Mixer Mill 400 with 99 a 50
mL steel jar and a 25 mm steel ball) for 3 min at 30 Hz (1800 rpm). 100 Biochar was
stored in a drying oven at 105 °C until analysis. A single batch 101 of biochar was
produced for each lignin type. Samples were weighed both
102 before and after pyrolysis to determine pyrolysis yield.

103 2.3. Sodium sulfate removal

104 As a secondary experiment, the impact of lignin Na₂SO₄ content was 105
directly studied by removing Na₂SO₄ from alkali-poplar95 lignin. To this
106 end, the alkali-poplar95 lignin was triple washed at a mass ratio of 1
part 107 original mass to 50 parts deionized water to remove Na₂SO₄ and
centrifuged 108 to separate after each washing cycle following established
procedures [26]. 109 Lignin was freeze-dried after washing and then stored
at 105 °C until py110 rolysis. Biochars were then prepared with this lignin
and compared against 111 unwashed alkali-poplar95 biochar. Both biochars
and washing residues were 112 measured with X-ray diffraction (XRD) and
energy dispersive x-ray (EDX) 113 spectroscopy, as described in Section
2.4 to verify the removal of Na₂SO₄. 114 For this set of experiments,
biochar samples were produced in triplicate.

115 2.4. Lignin and biochar characterization

116 Biochar pyrolysis conditions were simulated in a thermogravimetric analyzer (TGA, TA Instruments Q80001R) to examine the weight loss as a 117 function of temperature. Approximately 5 mg of each lignin was placed 118 in a HT-platinum TGA pan and heated from 30 °c to 1000 °c at a rate 119 of 10 °c

120 min- under a 30 mL min¹ flow of nitrogen gas. Lignin thermal transitions 121 at low temperatures were examined with differential scanning calorimetry 122 (DSC, TA Instruments Discovery 2500). For DSC, approximately 5 mg of 123 each lignin was placed in a TZero DSC pan and heated from 30 °c to 400 124 °c at a rate of 10 °c min⁻¹.

125 Atomic species present in biochar were examined with EDX spectroscopy 126 with an Oxford Ultim Max EDX detector on a Zeiss SUPRA 55VP field 127 emission scanning electron microscope (FESEM). Based on the EDX 128 results

129 (Supplemental Figure S7), C, H, N, S, Na, Mg, Ca, and K were selected 130 for

131 quantified analysis. The C, H, N, and S content of all lignins and 132 biochars

133 were characterized with combustion analysis by Atlantic Microlab Inc. 134 (Norcross, Georgia, USA). Lignin and biochar Na, Mg, Ca, and K 135 content were

136 characterized with inductively coupled plasma optical emission 137 spectrometry (ICP-OES). Biochar and lignin samples were digested in trace 138 metal grade HN03 (Fisher Scientific, product #A509P500, Pittsburgh, PA 139 USA) on a Mars6 iWave digester at 220 °c with a ramp time of 15 min, a 140 hold time of 15 min, and under 800 psi of pressure. Dilution factors for 141 ICP-OES are shown in Supplemental Table S2. Digested samples and 142 cation standards were run in a matrix of 2% HN03 on a SpectroBlue ICP- 143 OES in axial view mode (high sensitivity). Oxygen content was then 144

calculated as the remain140 ing mass not accounted for by combustion analysis or ICP-OES. Organic

141 oxygen content was calculated with the assumption that Na2S04 was the
142 sole oxygen-containing inorganic species due to the lack of evidence for other
143 molecular species present. Na2S04 content was calculated based on the lower
144 stoichiometric value of either sodium or sulfur content (e.g., if 2 mol sodium
145 and 5 mol sulfur were present, 1 mol Na2S04 would be used). Given the low
146 concentrations of Ca, Mg, and K in all lignins (<0.06% for Ca, Mg, and K
147 content summed) and biochar (<0.41% for Ca, Mg, and K content
148 summed), this estimation represents the majority of inorganic oxygen
149 present.

150 The chemical structure of all lignins and biochars was examined with
151 Fourier-transform infrared spectroscopy (FTIR) and XRD, and biochar was
152 additionally characterized with Raman spectroscopy. FTIR measurements
153 were performed on a ThermoFisher Nicolet iS50 FTIR spectrometer with a
154 Smart iTX attuned total reflectance (ATR) accessory with a diamond
155 crystal.

156 Spectra were collected from wavenumbers of 600-4000 cm⁻¹, at a resolution
157 of 4 cm⁻¹, with 64 scans per sample. XRD of all lignins and biochars was
158 performed on a Bruker D8 Advance powder X-ray diffractometer with Kal₂ 159
radiation, from 20 values of 10-70⁰ with a step size of 0.02⁰. Raman spec160 tra
161 were measured on a Horiba LabRam HR Evolution spectrometer with a
162 long-working distance objective and a frequency-doubled Nd:YAG laser
163 (wavelength of 532 nm) at a power of 1 mW. Carbon D and G peaks
164 were deconvoluted to determine Idg ratios, and XRD spectra were
165 fit to determine 166 graphitic crystallite sizes as previously described
167 [31, 32].

168 Gel permeation chromatography (GPC) was employed to determine the

164 number and weight average molar masses of the laboratory-isolated
165 lignins, 166 with acetylated samples utilized for the analysis [29]. An
167 Agilent HPLC 1260

168 equipped with a Waters Styragel HR 4 (7.8 X 300 mm, Milford, MA, USA)
169 column was used, with HPLC grade THF as the mobile phase with a 0.5
170 mL/min flow rate with UV detection at 280 nm and column temperature at
171 35 °c. As a reference, monodisperse polystyrene standards (Readycal,
172 Fluka 173 Analytical) were used in the range of 484 to 65,000 Da.

173 Lignin particle size was measured on a Malvern Mastersizer 2000 laser
174 particle size analyzer with water as the dispersant and the assumption of
175 non-spherical particles, as the biochar was ball milled. Before measurement,
176 all samples except TCI alkaline and dealkaline lignins were placed in
177 deionized water and sonicated for 5 min to disperse lignin particles.
178 TCI alkaline

179 and dealkaline lignins were placed directly into the particle size analyzer to
180 limit dissolution. Biochar and lignin morphology were examined on a Zeiss
181 SUPRA 55VP field emission scanning electron microscope (SEM) with
182 an electron high tension voltage of 20 kV and a working distance of
183 approximately 8.2 mm.

184 Biochar electrical conductivity was measured on 100 mg of biochar with
185 a
186 compressive guard electrode setup, as described in previous work [33].
187 Direct
188 current resistance measurements were taken on a Keithly 2540
189 Sourcemeter
190 from the point of first contact between the electrode and the biochar, as
191 de192 terminated by the sourcemeter reaching its lower current limit until
193 no more 194 pressure could be applied. Biochar packing fractions were
195 calculated assum196 ing a skeletal density of 2 g/cm³ for all biochars.

188 Biochar surface area and pore size distribution were characterized with 189 nitrogen sorption on a Micromeritics 3-Flex sorption analyzer 77 K for A95 190 biochar with and without Na₂SO₄. The Brunauer-Emmett-Teller (BET) 191 model was used to determine surface area, and the non-local density func192 tional theory carbon slit pore model was used to determine the pore size 193 distribution. Gas sorption isotherms and pore size distributions are shown 194 in Supplemental Figure S10.

195 2.5. Data analysis

196 All statistical analyses were performed in Minitab (vers. 19.2020.1, 197 Minitab LLC, State College, PA, USA), with a critical alpha set a priori to 198 0.05. Trends in shifts in the biochar elemental content with lignin 199 elemental content were analyzed with linear regression, with lignin 200 elemental content as the predictor variable and biochar elemental 201 content as the response variable. Impacts of lignin properties (H:C and 202 O:C at. ratios, Na and S content, 203 molecular weight, particle size, 204 dominant monomer, and lignin thermal transitions) on biochar 205 electrical conductivity or in-plane graphic crystallite size 206 were 206 analyzed with a forward selection regression model. The alpha value 207 for inclusion in the model was set a priori to 0.25. The impacts of biochar 208 treatments on biochar electrical conductivity were examined with 209 analysis of variance (ANOVA), including particle size treatment 210 (commercial, milled, or ground), washing to remove Na₂SO₄ (washed, 211 as prepared, or hydrolysis), feedstock (commercial, poplar, or corn 212 stover), or treatment type (hydrolysis, alkali, or commercial). 213 Additionally, the impact of washing to remove Na₂SO₄ on alkali- 214 poplar biochar electrical conductivity was examined with 215

216 one-factor ANOVA.

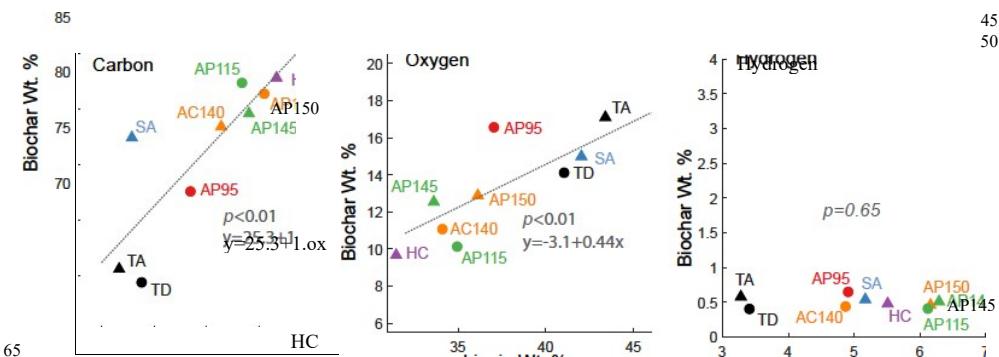
217 3. Results and Discussion

214 3.1. Lignin characterization

215 The lignins examined show a range of weight percentages of atomic species
216 present (Figure 1). Carbon is the most abundant element in all lignins,
217 ranging from 46.7 wt.% in TCI alkaline lignin to 61.7 wt.% in alkali-
poplar 150

218 lignin. Additionally, all lignins show oxygen (31.5-43.4 wt.%) and
219 hydrogen (3.3-6.3 wt.%) content. Lignin inorganic content varies by
isolation method. 220 All commercial lignins (TCI alkaline, TCI dealkaline,
Sigma alkali) and un221 washed alkali lignins (alkali-poplar95) show the
presence of sulfur (2.93-5.22 222 wt.%) and sodium (0.7-1.8 wt.%). In contrast,
all other lignins show limited 223 sulfur content (0-0.31 wt.%) and sodium
content (0.02-0.19 wt.%). Magne224 sium, calcium, and potassium are present
in limited quantities in all lignins 225 (<0.1 wt.%).

226 As a result of the different methods used to reduce lignin particle size, 227 lignins show a range of median particle sizes (8.36-375 pm) and particle 228 size distributions (Supplemental Figure S1). The three commercial lignins 229 (TCI alkaline, TCI dealkaline, Sigma alkali) all show approximately 100 gm 230 median particle sizes. All ball-milled lignins (alkali-poplar 150, hydrolysis231 corn, and alkali-corn140) show smaller particle sizes than other processing 232 methods at 8-34 gm median particle size. Lignins that were ground with 233 a pestle and mortar (alkali-poplar 145, alkali-poplar 115, and alkali-poplar95)



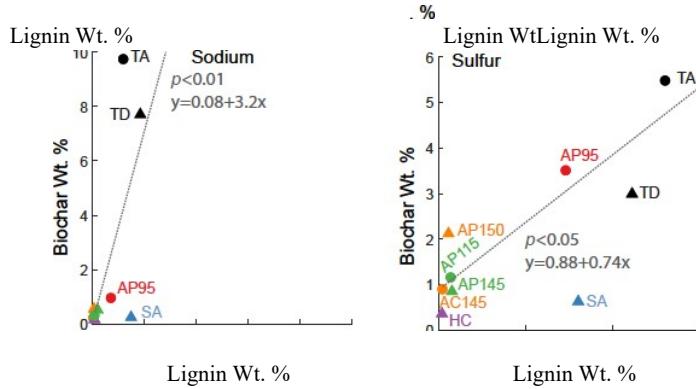


Figure 1: Comparison of weight % of C, H, O, Na, and S in all lignins before and after pyrolysis at 1100 °c. Linear regression trend lines are shown for all elements with a significant relationship ($p < 0.05$).

were found to have the largest median particle sizes between 160 and 375 gm. Ball-milled and commercial lignins show narrower particle size distributions than ground samples. This range of median particle sizes allows for the testing of particle size as a variable previously identified as a key factor impacting biochar electrical conductivity [33].

FTIR spectra were used to broadly categorize the lignins by their dominant monomer (Supplemental Figure S2a and full peak assignments given in

Supplemental Table S5). TCI alkaline, TCI dealkaline, alkali-poplar95, 115, 145, and 150 and hydrolysis-corn lignins show a stronger response for peaks associated with syringyl monomers at 1113 cm (aromatic C-H in-plane formation) and 1323 cm ¹ (C-O in syringyl ring), while Sigma-Aldrich alkali 245 and alkali-corn140 lignins show a stronger response in peaks associated with 246 guaiacyl monomers at 1032 cm (aromatic C-H in plane deformation) and 247 1263 cm ¹ (C-O in guaiacyl) [34]. Different lignin isolation procedures have 248 limited impacts on monomer ratios. However, hydrolysis-corn shows a sy249 ringyl dominant spectra, while alkali-corn140 shows guaiacyl dominant spec250 tra. Sigma-Aldrich alkali

and alkali-corn140, which show stronger guaiacyl 251 peaks, are isolated from spruce and corn, respectively, rather than the hard252 wood feedstocks used for the other lignins besides hydrolysis-corn [35, 36]. 253 While the primary Na₂S0₄ peak (1112 cm⁻¹) overlaps with the primary sy254 ringyl peak, the presence of Na₂S0₄ can be identified by the secondary S0₄ 255 peak at 627 cm⁻¹ [37], present as a strong peak in TCI alkaline, TCI dealka256 line, alkali-poplar95, and alkali-poplar 145 lignins, with weak peaks present 257 in Sigma-Aldirch alkali, alkali-poplar 115, and alkali-corn140 lignins. This 258 finding is supported by the relative concentrations of Na in these lignins, 259 with higher concentrations of Na present in TCI alkaline, TCI dealkaline, 260 and alkali-poplar95 lignins than others. The presence of Na₂S0₄ in TCI 261 dealkaline, alkali-poplar95, alkali-poplar 115, and alkali-poplar 145 is further 262 supported by XRD patterns (Supplemental Figure S2b). Despite high levels 263 of Na and S and FTIR peaks attributed to S0₄, TCI alkaline does not show a 264 crystalline Na₂S0₄ response in XRD, indicating the presence of amorphous 265 Na₂S0₄. The range of organic elemental composition, amount of Na₂S0₄ 266 present, non-lignin contaminants, and dominant lignin monomers present in 267 these lignins allow for the impact of these properties on the resulting 268 biochar

268 to be examined.

269 3.2. Lignin thermal transitions and biochar morphology

270 DSC curves of lignin show two distinct patterns of behavior when heated 271 (Supplemental Figure S3). The hydrolysis-corn lignin and washed alkali 272 lignins (alkali-poplar 145 and alkali-poplar 115) show strong, broad glass 273 transitions at 110 °c. In contrast, the commercial lignins (TCI alkaline, TCI 274 dealkaline, and Sigma-aldrich alkali), alkali-corn140 and alkali-poplar 150 show

275 sharp, weak glass transitions at approximately 150 °C. Above this second
276 glass transition, lignins that are high in Na₂SO₄ (as identified by elemental
277 composition, FTIR, and XRD) show a sharp transition that is attributed to
278 a polymorphic transition in Na₂SO₄ [38]. Finally, at high temperatures, a
279 lignin softening transition is observed for all lignins [39, 40]. This
280 begins at a lower temperature (118-200 °C) for hydrolysis
281 lignins than for alkali or Kraft lignins (236-336 °C). In some lignins
(alkali-poplar 115, 145, 282 and 150), the onset of thermal degradation can
283 be observed as noise in the DSC data above 300 °c.

284 The structure of the biochar post-pyrolysis varies as a result of these 285
differences in thermal transitions (Figure 2). In biochar produced from the 286
three commercial lignins (TCI alkaline, TCI dealkaline, and Sigma-Aldrich 287
alkali), a powdered structure is observed, with particle sizes similar to the 288
original lignins (Figure 2 and Supplemental Figure S1). In alkali-corn140 289
and hydrolysis-corn biochars, a clumped particle structure is observed (Figure 290
291). In contrast, in alkali-poplar95, alkali-poplar 150, alkali-poplar 115, 291
and alkali-poplar 145 biochars, a "carbon foam" structure is observed. Optical 292
microscopy (Supplemental Figure S4) and SEM reveal that this "carbon 293
foam" structure shows minimal distinction between individual particles 294
(Figure 2), with small (<200 nm) clumped, primarily carbon "cubbling" 295
observed via EDX and larger (1-2 um), higher sodium content particles observed
296 (Supplemental Figure S8). We hypothesize that this difference in behavior
is 297 related to thermal transitions in the lignin. In lignins with a powdered
298 structure (TCI alkaline and dealkaline, Sigma-Aldrich alkali) or weakly
clumped

299 structure (hydrolysis-corn and alkali-corn140), DSC curves show weak or
no 300 glass transition. In contrast, lignins with a continuous, "carbon foam"
301 structure (alkali-poplar 150, 115, 145, and 95) all show strong glass
transitions. Depending on the strength of these transitions, the structure of

the result303 ing biochar shifts from a powder similar in size to the original lignins to a 304 continuous material.

305 The formation of "carbon foam" structures could be attributed in part 306 to the melting of Na2S04. However, this behavior has previously been ob307 served at pyrolysis temperatures as low as 300 °C, below the melting tem308 perature of Na2S04 [41]. Further, this behavior is not observed in the two 309 highest Na2S04 content biochars - TCI alkaline and dealkaline. Notably, 310 all corn-derived lignins show clumped particle structures, all alkali-poplar 311 lignins show "carbon foam" structures, and all commercial lignins have pow312 dered structures. This finding indicates stronger softening transitions in 313 poplar-derived lignins than corn-derived lignins prior to the formation of 314 carbonized structures during pyrolysis. However, as previously observed 315 [42], lignin melting behavior shows a significant relationship with molecu316 lar weight ($p=0.002$), with the highest molecular weight lignins (TA, TD, 317 and SA Mw 28-60 kDa) showing no transition, moderate molecular weight 318 lignins (HC and AC140, Mw 10-11.4 kDa) showing packed powder mor319 phologies, and low molecular weight lignins, (AP 95, 115, 145, 150 and AP95320 Na, Mw 8-12.1 kDa) all showing continuous morphologies.

321 Notably, past studies have found that particle size may play an impor322 tant role in the graphitization of lignin during pyrolysis [7, 10]. Based on 323 the softening transitions observed and the resulting biochar morphology, we 324 hypothesize that in lignins with a strong softening transition, particle size 325 plays a limited role in resulting graphitization, as this size will have been 326 lost before most pyrolysis reactions. Particle size does not appear to play a 327 role in this transition, as similar lignins with large differences in size (such as 328 alkali-poplar 115 at 19 gm and alkali-poplar 145 at 375 pm) 329 have these same

329 thermal transitions and form similar structures. However, particle size may
330 still play a role in the pyrolysis of lignins with a weak softening transition
331 (such as Sigma-Aldrich alkali and TCI alkaline and dealkaline lignins).

332 3.3. Biochar characterization

333 Biochar yield varied between 21 and 45 wt.%, depending on lignin feed334
stock (Figure 3a). Typically, lignins with higher sodium content (TCI alka-

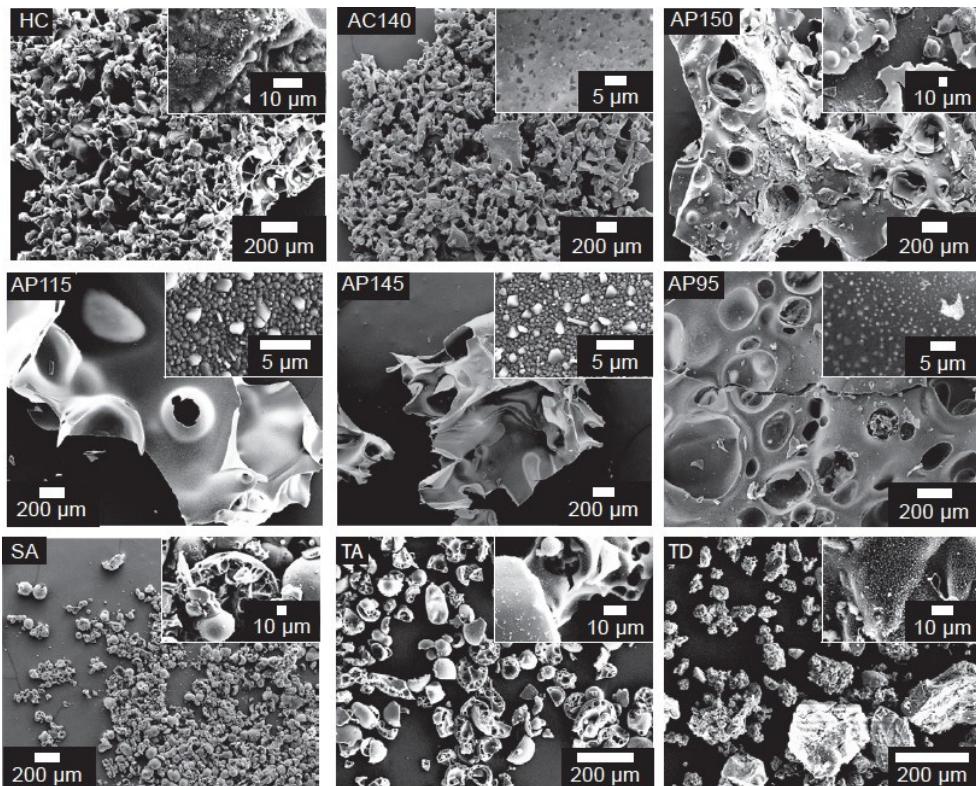


Figure 2: SEM micrographs of biochars produced from all lignins. Main images are at 50-250 \times magnification to highlight particle geometry, while insets are at 1000-3000 \times magnification to highlight surface features.

335 line, TCI dealkaline, Sigma-Aldrich alkali, and Alkali-poplar95) resulted in 336
higher biochar yields, which is attributed to the lack of reaction of Na₂SO₄ 337 during
pyrolysis. In biochar that formed a carbon foam structure, the biochar 338 had
expanded out of the alumina boat used. Therefore, some biochar was
339 lost during pyrolysis. The reactions that were responsible for these pyrolysis340 sis
yields were examined with TGA, and final masses at 1000 °C generally

341 agreed with trends in biochar production yields (Figure 3b). At low temper-

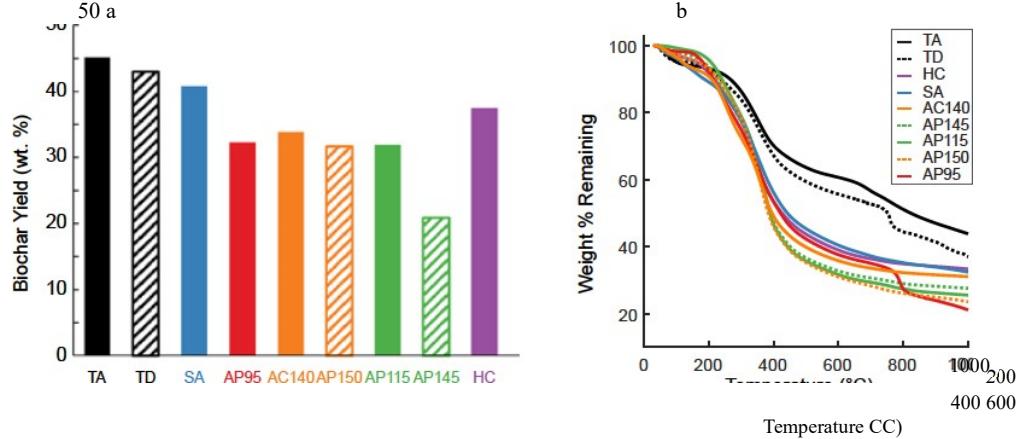


Figure 3: (a) Pyrolysis yield for each lignin. (b) TGA curves for each lignin under heating rates replicating tube furnace pyrolysis. Legend order shows the weight percent remaining at 1000 °c from highest to lowest.

342 atures (30-110 ° C), all lignins show small mass losses (0.9-5.3%)

343 associated with moisture evaporation. At high temperatures, two

344 distinct pyrolysis behaviors are observed - with the TCI alkaline and

345 dealkaline lignins and the alkali-poplar lignins all showing

346 degradation in the 600-800 ° c region. 347 In contrast, other lignins show

348 only minor mass loss in this region. This mass loss has previously been

349 associated with the degradation of ether linkages into CO and CO₂ [43].

350 Additionally, these three lignins are some of the highest in sodium and

351 sulfur content (Figure 1), and decomposition of

352 Na₂SO₄ has previously been observed at around 850 ° c in the presence of

353 carbon [44]. Additionally, the presence of alkali metals, such as sodium, has

354 previously been observed to catalyze the decomposition of biomass during

355 pyrolysis, which could be responsible for the presence of this mass loss in

356 high Na₂SO₄ lignins [25].

357 The carbon, oxygen, sodium, and sulfur content in the biochar is found

358 to be significantly impacted by the concentration of that element present

359 in lignin ($p < 0.05$, Figure 1). Carbon content shows a consistent

360 increase of approximately 25 wt.% with pyrolysis, attributed to loss of

oxygen and 359 hydrogen with pyrolysis. As a result of this shift, biochar carbon content is 360 additive to starting lignin carbon content (e.g., lignin that started at 50% 361 C results in approximately 75% C biochar). Only SA shows a meanin gful 362 variation from this trend, gaining approximately 35 wt.% carbon. Due to 363 limited evidence for the presence of carbon-containing inorganic compounds, 364 this carbon is assumed to be entirely organic. We note that some inorganic 365 species, such as Ca, were found via ICP-OES, which would commonly be 366 present in biomass as carbon-containing species (e.g., CaC03), which could 367 indicate the presence of some inorganic carbon [16], but also could be 368 present as CaO or CaS04 following thermal decomposition of CaC03.

369 Similarly, biochar oxygen content increases with increasing lignin oxygen 370 content, however, at a slower rate than carbon, with approximately 44% 371 of the lignin oxygen remaining after pyrolysis on average. Biochar organic 372 oxygen content is expected to play an important role in biochar electrical 373 conductivity [10, 20]. Lignin hydrogen content was not found to have a 374 significant impact on biochar hydrogen content ($p = 0.65$). All biochars 375 showed hydrogen content of approximately 0.5 wt.%, while lignin hydrogen 376 content varied from 3.3-6.3 wt.%. This similar hydrogen content indicates 377 that in these biochars, H:C atomic ratios, and therefore inferred graphitic 378 structure diameters [45], are driven primarily by carbon content. Biochar 379 and lignin atomic compositions are tabulated in Supplemental Tables S3 and

381 All biochars showed low (<0.2 wt.%) Mg, Ca, and K concentrations 382 (Supplemental Table S4). In contrast, biochars from acidification processes 383 with washing steps (TCI alkaline and dealkaline, alkali-poplar95, and Sigma 384 Aldrich alkali) show high concentrations of Na and S. These 385 concentrations are found to be typically significantly higher than the

concentration of sodium 386 or sulfur in the lignin feedstock ($p < 0.01$ and < 0.05 for Na and S, respectively). In the case of sodium, this increase in concentration (3.2) roughly 388 matches the change in mass (average yield of 35%, Figure 3), indicating that 389 minimal sodium has reacted off during pyrolysis. Molar ratios of sodium 390 to sulfur in biochar show differing shifts depending on the lignin feedstock, 391 which indicates the presence of multiple sodium and sulfur-containing compounds 392 pounds of organic sulfur. However, XRD and FTIR spectra of both lignin 393 and biochar show Na_2S_4 as the predominant form of both sodium and sulfur in all biochar. A meaningful portion of biochar and lignin oxygen is 395 inorganic, with between 3 and 35% of total oxygen present in Na_2S_4 based on sodium content (Supplemental Table S4).

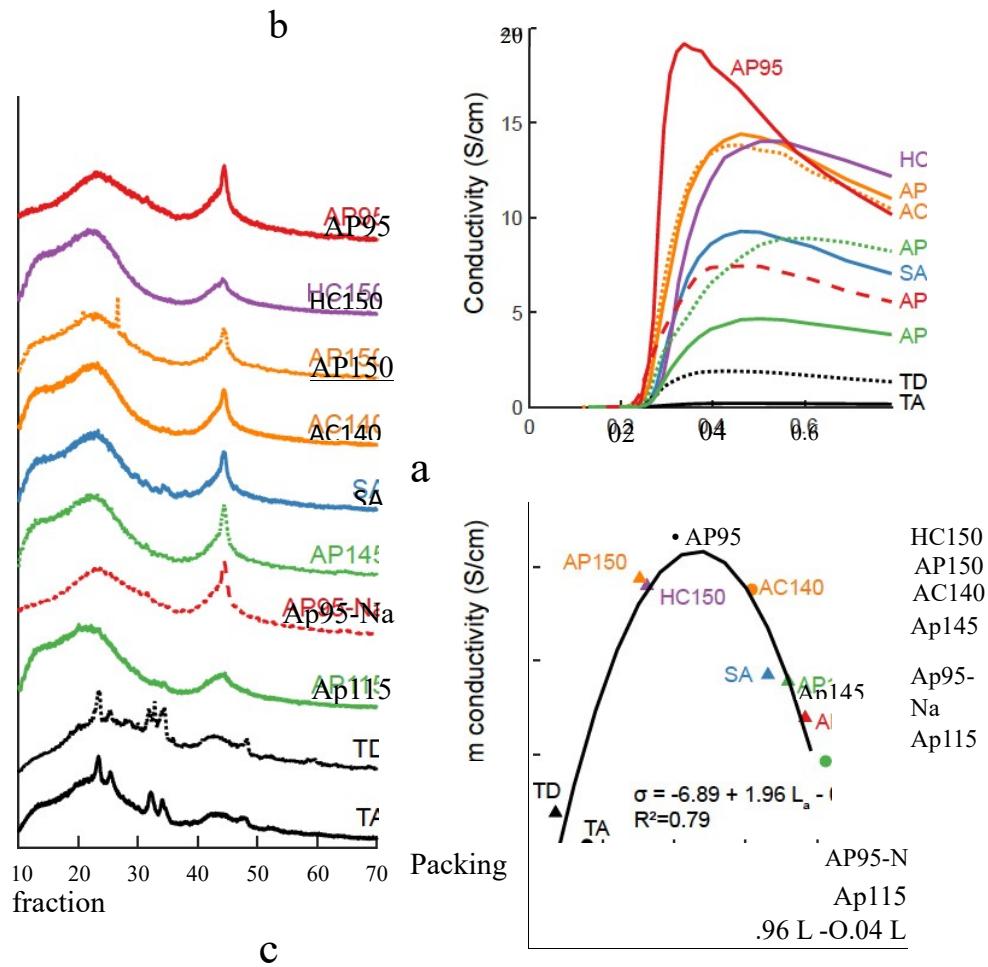
397 Sigmoidal electrical percolation behavior is observed in all biochars as 398 they are compressed (Figure 4b). At low compressions, all biochars show 399 highly resistive behavior, as the non-conductive air dominates the unpacked

400 powder. At a packing fraction of approximately 0.25, the percolation threshold 401 is reached, and electrical conductivity rapidly increases. The percolation threshold 402 is similar for all biochars, indicating similar particle geometry and 403 packing despite differences in the structure after pyrolysis but before ball 404 milling. The peak electrical conductivity of all biochars varied by two orders 405 of magnitude between biochars, from 0.19 S/cm for TCI alkaline biochar 406 to 18.9 S/cm for alkali-poplar95 biochar. These variations are consistent 407 with what has previously been observed for pyrolysis of lignin at 1100 °c

408 with electrical conductivity measured with the same method and in the middle 409 of a range of values previously observed for all lignin-derived biochars 410 [10]. The upper range (>10 S/cm) of these conductivities are comparable 411 to those of electrically conductive carbon blacks [33, 46], and are sufficient 412 for many electrical applications, including anti-static

materials, sensors, and 413 conductive additives in batteries. At a pyrolysis temperature of 1100 $^{\circ}\text{C}$, no 414 further increase in electrical conductivity is expected with further increases 415 in pyrolysis temperature [21].

416 A number of factors impact biochar electrical conductivity: the size of 417 graphitic crystallites, displacements and deformations on those crystallites, 418 biochar surface groups, and biochar particle size [10, 20, 21]. XRD patterns 419 of the biochar show variation in the in-plane size of graphitic crystallites (La) 420 but minimal shifts in size or distance between sheets in the stacking 421 direction (Lc and d002) with an average and standard deviation of 1.2 ± 0.1 422 graphene planes per crystallite across all samples. The in-plane size of 423 graphitic crystallites varies from 3.4 \AA for TCI dealkaline biochar to 41 \AA for alkali-poplar 115-



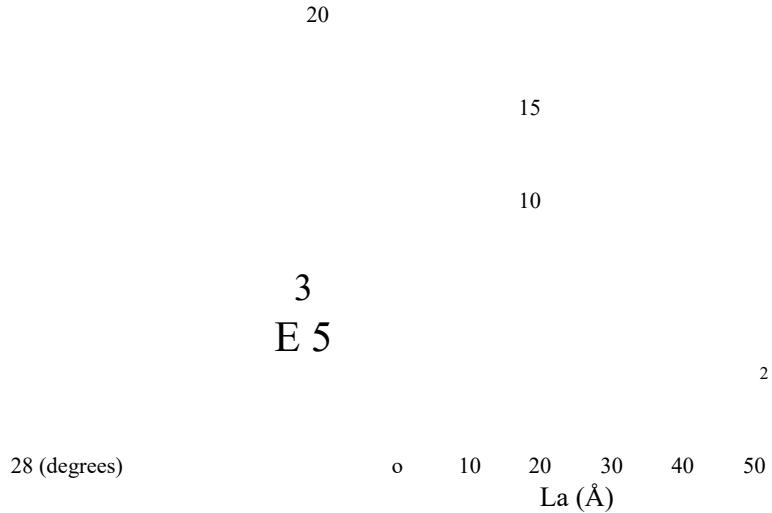


Figure 4: Characterization of biochar graphitic structure and electrical conductivity showing (a) XRD patterns. Lines are stacked in order of maximum electrical conductivity from highest (top) to lowest (bottom), (b) electrical conductivity as a function of packing fraction, and (c) relationship between in-plane graphitic crystallite size and electrical conductivity. Error bars in (b) and (c) represent the maximum and minimum values of peak conductivity for three samples from a comparison of AP95 with and without Na₂SO₄, and the point or line represents the median value.

424 biochar. TCI alkaline and dealkaline biochar show poor fits of XRD
 425 patterns relative to other biochar, which is attributed to the high contribution
 426 of in organic components to the XRD pattern in these biochars, which were
 not

427 included in the fitting procedure (Supplemental Figure S6a and b). Minimal
 428 shifts are observed in Raman spectra between samples (Supplemental
 Fig429 ure S5). All biochars show the typical D and G peaks that are typical
 for

430 non-graphitizing carbons [31]. The intensity ratio of these peaks (I_{DG})
 ranges

431 from 1.03-1.18. In TA, an additional peak is observed at 1058 cm¹, which
 432 is attributed to Na₂SO₄ (Supplemental Figure S5) [47]. TCI alkaline
 and

433 dealkaline biochars have a shallower valley between the D and G peaks than
 434 other biochars. The ratio of this valley depth to the height of the G-peak has

435 previously been correlated with the degree of graphitization [48]. Combined
 436 with limited 101 peaks in the XRD patterns of TCI alkaline and dealkaline
 437 biochars and low electrical conductivity, this finding demonstrates that
 438 these biochars have lower graphitization than the other biochars
 439 examined. A full 439 summary of fit values from XRD and Raman is given
 440 in Table 2.

440 Despite the range of properties and electrical conductivity identified
 441 herein, no statistically significant relationship was found with a linear re442
 442 gression between any of the examined lignin properties (H:C and O:C at.
 443 ratios, Na and S wt. %, molecular weight, particle size, dominant monomer,
 444 and lignin thermal transitions) and biochar electrical conductivity ($p > 0.05$
 445 for all, Figure 5). Similarly, one-factor ANOVAs found no statistically sig446
 446 nificant differences ($p > 0.05$ for all) between treatment groups, including 447
 447 particle size treatment (commercial, milled, or ground), washing to remove 448
 448 Na₂SO₄ (washed, as prepared or received, or hydrolysis), feedstock (commer-

Table 2: Calculated XRD (in-plane graphitic crystallite size (La), out-of-plane graphitic crystallite size (Lc), crystallite aspect ratio (La/Lc), and space between planes (d) and Raman values (Intensity ratio of fit d peak to g peak IDG and width of G peak (WG)) and peak electrical conductivity for all biochar. Complete Raman spectra are given in Supplemental Figure S5, and XRD fits are given in Supplemental Figure S6.

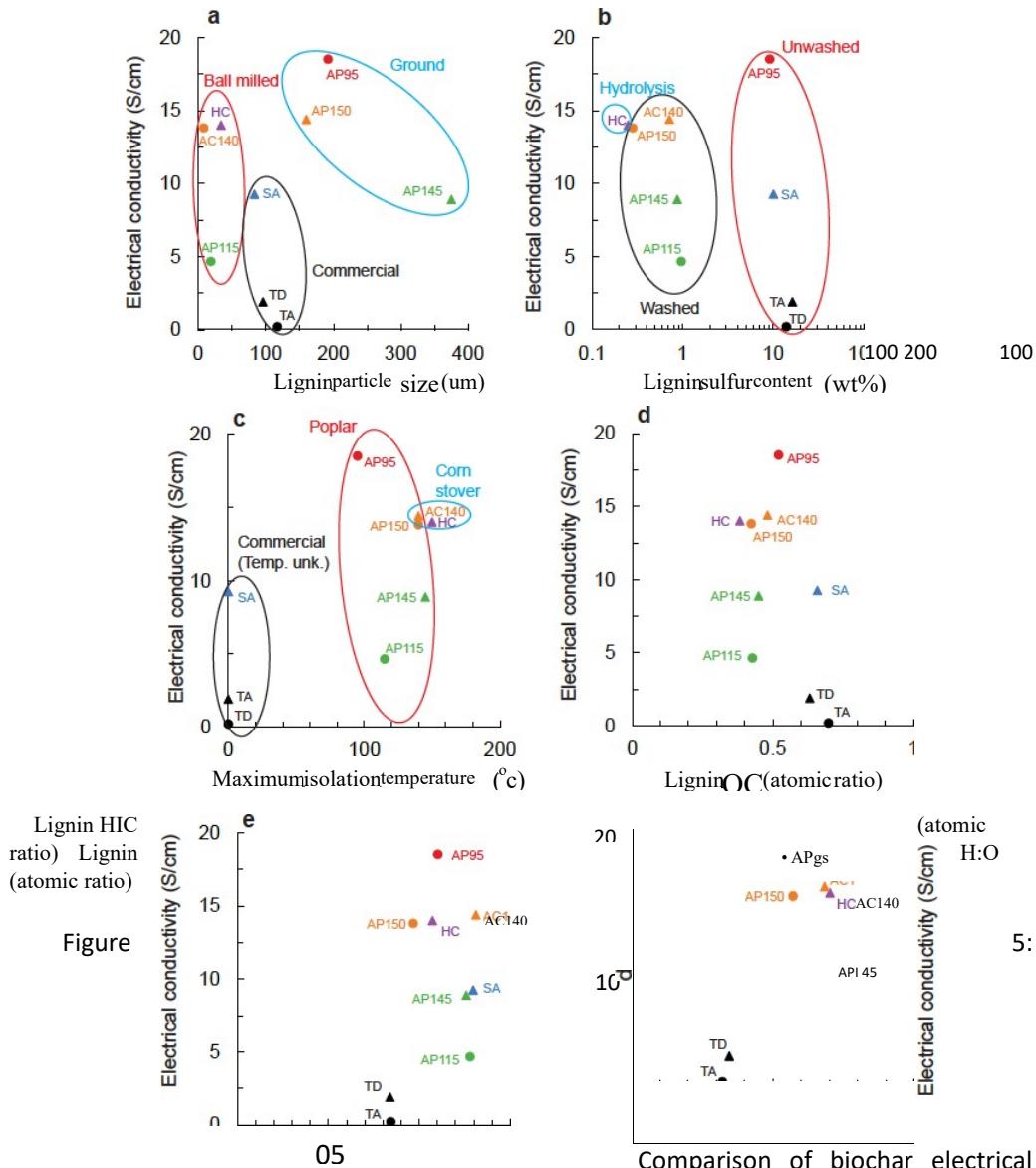
	La(Å)	Lc(Å)	La/Lc	IDG	WG	Conductivity (S/cm)
TCI alkaline	7.8	4.6	1.7	4.0	1.1	148.0
TCI dealkaline	3.4	5.2	0.7	3.7	1.1	133.9
Sigma-Aldrich alkali	33.1	5.0	6.6	4.1	1.1	151.2
Hydrolysis-corn	16.2	4.9	3.3	4.1	1.2	147.7
Alkali-corn140	15.2	4.3	3.5	4.4	1.1	153.9
Alkali-poplar 150	30.9	4.6	6.7	4.3	1.1	137.5
Alkali-poplar 115	41.2	4.9	8.4	4.2	1.0	146.8
Alkali-poplar145	35.9	4.9	7.3	4.3	1.0	146.0
Alkali-poplar95	19.5	5.1	3.8	4.4	1.1	146.1
					1.2	18.5
Alkali-poplar95-Na	38.3	4.0	9.5	3.8		7.0

449 cial, poplar, or corn stover), or treatment type (hydrolysis, alkali, or com450
 450 mercial). This lack of significance holds even when processing methods and
 451 feedstock for commercial lignins are ungrouped, and feedstock is assumed to

452 be mixed wood for TCI alkaline and dealkaline lignin, softwood for
453 Sigma Aldrich alkali lignin, and treatment type is assumed to be alkaline
454 for TCI alkaline and dealkaline lignin and alkali for Sigma-Aldrich
455 alkali lignin.

456 However, when examining the relationship between lignin properties
457 and biochar in-plane graphitic crystallite size (La, Supplemental Figure
458 (p = 0.042). This relationship shows an increasing graphitic
459 crystallite size

460 with an increasing H:C ratio. Notably, despite a wide range of hydrogen
461 content in the lignin feedstocks, the biochar produced shows limited
462 variation in hydrogen content (Figure 1). This finding indicates that
463 feedstock hydrogen



conductivity with (a) lignin particle size, (b) lignin sulfur content, (c) lignin max. isolation temperature, (d) lignin organic O:C ratio, (e) lignin H:C ratio, and (d) lignin organic H:O ratio. Labeled groups are treatment groups.

462 content has a limited effect on the final molecular structure. Instead, hydro463 gen plays a role in the pyrolysis reactions that lead to the formation of those 464 structures. This finding is consistent with past models of biomass pyroly465 sis, which state that when insufficient hydrogen is present in a feedstock to

466 react with oxygen, which forms distortions in the graphitic structure, these 467 distortions persist, even at high pyrolysis temperatures, limiting the

possible degree of graphitization of the feedstock [20]. As oxygen content shows lower variation between lignin feedstocks (O:C ratios of 0.38-0.70, relative to H:C ratios of 0.84-1.31), the hydrogen content is the primary driver of variation in graphitization of the lignin feedstocks examined. Future work examining a wider range of lignin oxygen content could better highlight the role of oxygen in these reactions. As a result, it may be preferable to produce lignin with higher guaiacyl monomer content (H:O at. ratio of 4) rather than syringyl dominant lignin (H:O at. ratio of 3.3). We note, however, that no relationship is observed between the biochar H:O ratio or in-plane graphitic crystallite size and the dominant monomer in this work, and relatively few guaiacyl-dominant lignins (AC140 and SA) were examined. Further, those two lignins show relatively small differences in electrical conductivity, both within the upper half of electrical conductivities examined (14.4 and 9.3 S/cm for AC140 and SA, respectively).

Alkali-poplar95 biochar, as the highest electrical conductivity biochar, was selected for further testing to examine the impact of inherent Na₂SO₄ on lignin-derived biochar electrical conductivity and carbon structure. After washing to remove Na₂SO₄ from alkali-poplar95 (alkali-poplar95-Na), limited sulfur or sodium content was observed via EDX, and no Na₂SO₄ peaks were observed via XRD (Supplemental Figure S9). An ANOVA assessing the impact of Na₂SO₄ removal treatment on alkali-poplar95 biochar electrical resistivity found a statistically significant impact from Na₂SO₄ treatment ($p < 0.01$). Alkali-poplar95 biochar had an average electrical conductivity of 17 ± 1.6 S/cm (Figure 4 and Supplemental Figure S9). With Na₂SO₄ removed, electrical conductivity was reduced to 7.0 ± 0.5 S/cm. The mechanisms behind this difference in electrical conductivity were further explored with XRD, finding a meaningful increase in crystallite size

of 495 the graphitic 10 plane (La) with the removal of Na₂SO₄ (Figure 4a and Table

496 2). Alkali-poplar95 biochar shows an in-plane crystallite size of 16.2 Å on
497 average. With the removal of Na₂SO₄, in-plane crystallite size
meaningfully 498 increases to 38.3 Å. In contrast, crystallite size in the
stacking 002 direction (Lc) only shows minor shifts between 4-5 Å for
both treatments with a 500 distance of approximately 4 Å between each
layer. Importantly, this finding 501 indicates that the presence of Na₂SO₄
inhibits graphitization in lignin-derived 502 biochars. Further, the BET
surface area of the biochar decreases from 27.10 503 m² /g in alkali-
poplar95 with Na₂SO₄ to 8.16 m²/g when Na₂SO₄ is removed. 504 This
decrease in surface area with Na₂SO₄ removal is driven by a decrease 505
in pores with a width of less than 35 Å (Supplemental Figure S1Ob). The
506 combination of increased graphitic crystallite size and decreased BET
surface 507 area of smaller pores is consistent with past findings of micro-
pore closure 508 with increasing graphitization [49]. This is further
supported by increased 509 hysteresis during desorption in alkali-poplar95
relative to with Na₂SO₄ removed, indicating the presence of constricted
pores when Na₂SO₄ is present, 511 that are closed when Na₂SO₄ is not
present [49].

512 Beyond alkali-poplar95 with and without Na₂SO₄ removal, individual
513 comparisons can be made based on similar lignins with individual
differences

514 in processing. Alkali-poplar 150 and alkali-corn140 were processed similarly,
515 but different feedstocks (poplar and corn Stover) and particle sizes (34
gm 516 and 160 pm), but the resulting biochars have similar electrical
conductivities 517 (13.8 and 14.4 S/cm). However, they have different
graphitic crystallite

518 sizes with an in-plane graphitic crystallite size of 15.2 and 30.9 Å for corn

519 and poplar, respectively. Alkali-poplar95, which was processed similarly to
520 alkali-poplar 150 but with a lower treatment temperature and no washing to
521 remove Na₂SO₄, resulted in higher electrical conductivity. Similarly,
522 alkali poplar 115 and alkali-poplar 145 have similar processing,
523 chemical content, 524 and graphitic crystallite size with differences in
525 treatment temperature, but 526 alkali-poplar 145 shows higher electrical
527 conductivity than alkali-poplar 115.

528 The two corn-stover-derived lignins examined (hydrolysis-corn and alkali529
530 corn140) show broadly similar properties despite the different processing
531 methods used; as alkali-corn140 was washed to remove Na₂SO₄, both have
532 low sodium and sulfur content, and both lignins were ball milled and
533 therefore show similar particle sizes. When alkali-poplar95 is washed
534 to remove 535 Na₂SO₄, the electrical conductivity decreases, and the in-
536 plane graphitic 537 crystallite size increases to be comparable to alkali-
538 poplar 115 and alkali539 poplar 145. These two lignins were processed
540 similarly to alkali-poplar95, except they were washed to remove
541 Na₂SO₄, indicating that this washing step 542 drives the large differences
543 between these three otherwise similar lignins.

544 As biochar graphitic crystallite size only meaningfully varies in the in545
546 plane direction, the aspect ratio of graphitic crystallites varies greatly be547
547 between different biochars. This shift in graphitic crystallite size is found to 548
548 play a key role in biochar electrical conductivity. A strong quadratic re549
549 relationship is found between in-plane graphitic crystallite size and biochar 550
550 conductivity ($p < 0.01$, Figure 4c). This relationship peaks in electrical con551
551 ductivity at an in-plane graphitic crystallite size of 23 Å. We propose two 552
552 mechanisms for this behavior, which expand on the previously developed 553
553 quasi-percolation model for biochar electrical conductivity [21, 30]. At small
554 in-plane graphitic crystallite sizes, such as are found in TCI alkaline and

545 dealkaline biochar, limited graphitization has occurred due to the presence
546 of high quantities of Na₂SO₄ as indicated by elemental composition, XRD,
547 and Raman spectroscopy. Graphitic crystallites in these materials have
548 limited electrically conductive contact between crystallites and are
separated by 549 lower electrical conductivity displaced graphitic carbon, as
predicted by previous quasi-percolation models [21]. As the size of these
550 crystallites expands, 551 such as in alkali-corn-140 and hydrolysis-corn
biochar, there are increased 552 contacts between electrically conductive
regions. These contacts reach a 553 maximum at in-plane graphitic crystallite
sizes of approximately 23 Å, corresponding to a graphitic crystallite aspect
ratio of 3.8 La/Lc. Above this 555 contact, the high aspect ratio and the random
orientation of graphitic crystallites [50] limit contacts between the
crystallites, resulting in lower electrical 557 conductivity. This proposed
behavior matches those previously observed for

558 percolation in packed powder systems, where higher aspect ratios result in
559 reduced electrical conductivity [46]. In addition, the graphitic crystallite
size 560 that results in the highest biochar electrical conductivity is similar to
that 561 of highly electrically conductive carbon blacks [11]. This similarity
suggests 562 that similar mechanisms for crystallite packing occur in
petroleum-derived 563 carbon black.

564 A complex series of multi-phase reactions is observed during pyrolysis, 565
driven by the melting behavior of some lignins at low temperatures, melting
566 of Na₂SO₄ at high temperatures, and secondary reactions of liquid oil and
tar

567 pyrolysis products back to solid biochar. No statistically significant trends
568 were observed in electrical conductivity or graphitic crystallite size based
on 569 the melting behavior of the biochar. However, this may in part be due to
the

570 compounding of other effects, as two of the lignins with no observed melting 571 behavior (TA and TD) were also the highest in Na₂S04, and the two lignins 572 that showed clumped-powder behavior (HC and AC140) were the lowest in 573 Na₂S04 content, while continuous morphologies showed a range of Na₂S04 574 content. Further, at 1000 °C, lignins that showed no melting behavior showed 575 the highest yields at 200-1000 °c via both TGA and pyrolysis yields at 1100 576 °c (Figure 3), followed by clumped powder morphologies, with continuous

577 morphologies having the lowest yields. While previous studies have observed 578 increased decomposition at low pyrolysis temperatures in lignins that show 579 melt behavior [42], an alternative explanation is that non-melting lignins have 580 a higher molecular weight, which is also correlated with increased biochar 581 yields, rather than the melting itself. Further, at present, it is unknown how 582 these shifts in low-temperature behavior impact the formation of graphitic 583 structures at pyrolysis temperatures above 900 °C. Critical examination of 584 this phenomenon, controlling for the identified compounding factors herein, 585 could provide additional insight into which lignin isolation procedures and 586 lignin properties provide the best feedstock for differing carbon applications.

587 Multiple structures of Na₂S04 were observed via SEM-EDX, with Na₂S04 588 being present as both a "skin" on the outside of the biochar and integrated as 589 approximately 1 pm structure between the majority carbon structures (Sup590 plemental Figure S8). The impacts of Na₂S04 melting on lignin pyrolysis, 591 as well as the mechanisms responsible for the herein observed shifts in car592 bon structure with Na₂S04 presence, is a particularly interesting area for 593 further study. A better understanding of these mechanisms would allow for 594 the carbon structures of lignin-derived carbons to be better optimized for 595 specific applications. Past work on molten salt interactions during pyrolysis 596 has shown molten salt to impact carbon structures [51, 52], and a better 597 understanding of these interactions in lignin pyrolysis is

needed to modify 598 the structures of lignin-derived carbons to specific applications.

599 This study highlights the development of low aspect ratio graphitic crys600 tallites but well-graphitized carbon structures as a potential method to in601 increase the electrical conductivity of carbons produced from non-graphitizing 602 feedstocks. Future work should examine if biochar could be produced with 603 limited disordered and displaced graphitic content but with graphitic crys604 tallite aspect ratios approaching 1, as higher electrical conductivities of the 605 bulk material may be possible. Importantly, this work demonstrates that 606 Na₂S₀4 levels in lignin can be controlled to selectively control graphitization 607 of lignin-derived biochar and tune graphitic crystallite size and electrical 608 conductivity to a desired application. Modification of pore size distributions 609 and surface area via selective Na₂S₀4 removal can tune these critical factors 610 for carbon applications such as battery active materials [53]. Further, in 611 future work, multiple variables, such as pyrolysis temperature and Na₂S₀4 612 level, could be tuned to examine combinations that maximize highly elec613 trically conductive carbon production while minimizing energy consumption 614 during production. Given the strong performance previously demonstrated 615 by lignin-derived carbons across multiple applications [7, 11, 14, 15], this 616 work provides key guidance on feedstock selection and modification to meet 617 the requirements of carbons as commercial application of lignin-derived car618 bons continues to grow. However, the additional processing step required 619 to remove Na₂S₀4 would be expected to introduce additional costs, and the 620 benefits of additional tuning of the carbon properties should be carefully 621 evaluated against these costs. Process considerations, such as tuning the 622 amount of NaOH added during delignification and the sulfuric acid addition 623 during precipitation of alkali lignins or selection of sulfur-free processes (e.g.,

624 hydrolysis), could allow for tuning the sodium sulfate content of lignin to a
625 desired carbon application without additional washing steps. However,
626 these process changes would need to be carefully evaluated against the
627 outputs of the biorefinery process as a whole. The simple water
628 washing method demonstrated herein would be expected to be lower
629 cost compared to other methods to tune biomass-derived carbon
630 properties such as iron catalysts, which must be removed with acid
631 washes [15] or activation processes that
632 consume more costly activation agents, such as KOH [14].

632 4. Conclusions

633 This work highlights that all lignins are not equal for producing electrically
634 conductive biochar, with a 100-fold difference in electrical conductivity
635 between the most and least conductive biochar measured. The wide range
636 of electrical conductivities observed herein for lignin-derived biochars
637 confirms that similar ranges observed between past studies are not
638 exclusively due to differences in biochar production or electrical
639 conductivity measurement methods. Na₂SO₄ content in lignin is identified
640 as a significant factor in lignin-derived biochar carbon structure, with
641 Na₂SO₄ inhibiting the formation of larger graphitic crystallites. However,
642 the aspect ratio of graphitic crystallites in lignin-derived biochar plays an
643 important role in the electrical conductivity of the resulting biochar, with a
644 quadratic relationship observed with a maximum electrical conductivity at
645 an aspect ratio of 4. Many of

646 the examined lignin-derived biochars have higher aspect ratios, resulting in
647 lower electrical conductivity despite larger graphitic crystallites. Therefore,
648 the presence of moderate amounts of Na₂SO₄ can be used to selectively
649 tune the carbon structure in lignin-derived carbons and maximize
electrical conductivity. This finding builds on past quasi-percolation

models that describe 650 the packing of graphitic crystallites within carbon particles as an important 651 contributor to their bulk electrical conductivity and can help to inform the
652 development of future electrically conductive, non-graphitizing carbons.

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CRediT author statement

S.K.: conceptualization, methodology, validation, formal analysis, investigation, writing — original draft, writing — review & editing, visualization.

D.B.H.: methodology, writing — review & editing, supervision, funding acquisition

B. S.: methodology, investigation, writing — original draft

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Declaration of interests

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

Electrical conductivity of lignin pyrolyzed at 1100 °c varies by a factor of 100

Na₂SO₄ in lignin increases the size of graphitic crystallites, decreases conductivity

High aspect ratio graphitic crystallites are proposed as cause of this behavior Lignin-derived biochar carbon structure can be tuned by varying Na₂SO₄ content