

# Accurately Measuring Slowly Propagating Flame Speeds: Application to Ammonia/Air Flames

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## Abstract:

Environmental concerns have driven the development of alternative fuels and refrigerant working fluids with low global warming potential. Ammonia ( $\text{NH}_3$ ) is a potential zero-carbon fuel, while hydrofluorocarbons (HFCs) like R-32 and R-1234yf are being adopted as refrigerants. When mixed with air, these compounds can sustain slowly propagating flames with laminar flame speeds less than 10 cm/s. Unlike typical hydrocarbon-fueled flames, these slow flames are influenced by buoyancy-induced flow and radiation heat loss. In this study, we experimentally investigate the flame speeds of  $\text{NH}_3$ /air mixtures using the constant-pressure spherically expanding flame method, while circumventing gravity-induced natural convection, and account for radiation-induced inward flow. To mitigate buoyant convection, a low-cost drop tower was built and used to study slow spherically expanding flames in free fall. A computational model (SRADIF) is utilized that combines thermodynamic equilibrium and finite rate optically thin limit radiation heat loss calculations to estimate the inward flow. The developed methodology is utilized to investigate slowly propagating  $\text{NH}_3$ /air flames over a range of equivalence ratios. A systematic approach was undertaken to understand and quantify the errors that could arise when deriving the laminar flame speed. It was found that attempting to study slowly propagating flames in a static configuration, as opposed to in free fall, results in large differences in flame dynamics and subsequently all derived quantities. It is necessary to study slowly propagating flames in free-fall. Additionally, using experimental data that has not been corrected for radiation-induced flow leads to large errors in all derived quantities. Furthermore, direct comparisons of experimental measurements and detailed flame simulations are found to be necessary to determine if existing extrapolation approaches are applicable to these slowly propagating flames, which are challenging to study.

**Keywords:** Laminar Flame Speed; Sustainable Fuel; Ammonia combustion; Microgravity

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## Novelty and Significance Statement:

In this study, a novel methodology to accurately quantify slowly propagating flame speeds is presented. It consists of a combined, experimental approach to circumvent gravity-induced natural convection and a computational approach that accurately accounts for radiation-induced inward flow. This constitutes the first study that systematically investigates the errors that can arise while deriving the laminar flame speeds of slowly propagating flames from expanding rate measurements. Furthermore, accurate measurements are performed for the first time for  $\text{NH}_3$ /air flames.

## Author Contributions:

JM: Experimental; Validation; Investigation; Methodology; Data Analysis; Writing

JT: Software; Validation; Investigation; Data Analysis; Writing

JJ: Conceptualization; Software; Investigation; Methodology; Data Analysis; Writing; Resources; Supervision

## 1. Introduction

Environmental concerns have motivated the development of alternate fuels and refrigerant working fluids that have low global warming potential. Ammonia ( $\text{NH}_3$ ) is a candidate zero-carbon fuel and hydrofluorocarbons (HFCs) such as R-32, R-1234yf, etc. are being adopted as refrigerants. Upon mixing with air, these compounds can sustain flames that are slowly propagating i.e., with laminar flame speeds less than 10 cm/s. These flames are referred to as *slow* as they are affected by gravity (buoyancy-induced flow) [1, 2] and radiation heat loss [3], in contrast to typical hydrocarbon-fueled flames. Quantifying their reactivity is key to assessing the explosion risk associated with the storage, transportation, and utilization of these compounds.

The laminar flame speed ( $S_u^0$ ) is a fundamental combustion property of a combustible mixture [4-6].  $S_u^0$  measurements are useful for assessing the reactivity of fuels and working fluids. More importantly, they serve as validation targets to constrain the uncertainty of chemical kinetic models [7]. Constrained kinetic models are invaluable. In the case of HFCs, they can estimate the reactivity of mixtures of HFCs, thereby enabling the development of refrigerant blends with favorable flammability, sustainability, and performance characteristics [8]. Kinetic models can also be used in conjunction with fluid models to assess fire and explosion risk associated with leakage followed by accidental ignition of these compounds [6].

A survey of literature reveals that the vast majority of measurements for  $\text{NH}_3$ /air and HFC/air flames have been made using the spherically expanding flame (SEF) configuration. The reason is that  $\text{NH}_3$ , and the products of HFC combustion, hydrogen fluoride and carbonyl fluoride, are toxic. The counterflow and heat flux approaches need a continuous flow of reactants. In contrast, the SEF approach utilizes only a small amount of reactants, resulting in a correspondingly small quantity of products, which are contained in a sealed combustion chamber, and can be exhausted safely. Additionally, the well-defined stretch rate and short experimental time scales (which make the configuration more amenable to be studied in a drop tower as discussed later) make this configuration attractive [6]. Consequently, we utilize the constant pressure SEF (CONP-SEF) approach for measuring  $S_u^0$ . The CONP approach (as opposed to the constant volume approach (CONV-SEF) [6] is preferred as optical access allows for tracking the onset of flame-front instabilities, and the distortion of flames due to natural convection. All subsequent discussions concern CONP-SEFs unless specifically mentioned.

Two aspects make accurate measurements of slowly propagating flame speeds challenging: buoyancy-induced flow and radiation heat loss. Although ubiquitous, they affect flame propagation only when the relevant time scale becomes comparable to, or less than, the characteristic time scale of flame propagation [2].

Gravitational forces induce flow due to the significant difference in density between the hot burned and cold unburned gases [1]. For SEFs, this buoyant convection results in the flame deforming into a dimpled, oblate-ellipsoid [1, 9]. The extent to which a flame is deformed can be estimated using the Richardson number ( $Ri$ ), which compares the characteristic time scale of flame propagation to the characteristic time scale of buoyant convection [1, 9].

$$Ri = \frac{(\rho_u - \rho_b)}{\rho_u} \frac{g R_f}{(\dot{R}_f)^2}$$

Here  $\rho_u$  and  $\rho_b$  are the unburned and (adiabatic) burned gas densities, respectively,  $g$  is the gravitational acceleration,  $R_f$  is the flame radius and  $\dot{R}_f$  is the flame expansion rate in the laboratory frame of reference. Using direct numerical simulations (DNS), Berger et al. [9] showed that SEFs with  $Ri$  approaching or greater than unity become significantly distorted, and as a result, the extracted  $S_u^0$  could be erroneous. Since,  $R_f$  is ill-defined for a buoyant flame, they evaluated a variety of methods to extract flame speed information from the distorted flames to determine if  $S_u^0$  can be accurately derived [9]. The only relatively accurate method they found is the surface-averaged displacement speed which uses the

geometrical features of the buoyant flame. However, the derived expression is contingent on the assumption that the average burned gas density does not change with time [9]. However, this is not applicable for slowly propagating flames, which are known to have significant radiation heat loss.

For a slowly expanding flame with  $S_u^0 \sim 8 \text{ cm/s}$ ,  $R_f = 3 \text{ cm}$ , and  $\rho_u/\rho_b \sim 7$ ,  $Ri \sim 1$ . Whereas for  $S_u^0 \sim 30 \text{ cm/s}$  with everything else being similar,  $Ri \sim 0.04$ . Based on this analysis, it is evident that slowly propagating spherical flames (such as  $\text{NH}_3/\text{air}$ ,  $\text{R-32}/\text{air}$ , etc.) will be deformed by buoyancy, making measurements of  $S_u^0$  challenging.

Buoyancy-induced flow can be minimized by studying SEFs in *free fall* (as opposed to in the typical *static* configuration). However, the inaccessibility of microgravity combustion facilities (e.g., parabolic flight vehicles, drop towers, low earth orbit space vehicles) has restricted free fall experimental investigations of slow flames to a handful of datasets [10-17]. Measurements have been performed for HFC/air [11, 17], and  $\text{NH}_3/\text{air}$  [12]. However, these measurements do not account for the effects of radiation heat loss. Ronney [12] examined the role of chemical kinetics and transport properties of near-limit flames in free fall. He found that  $\text{NH}_3/\text{air}$  flames display near-limit behavior (i.e., ignition limits, extinguishment limits, and near-limit burning velocities) similar to hydrocarbon/air mixtures that have similar effective Lewis numbers or transport properties [12]. Hesse et al. [11] measured the  $S_u^0$  for nitrogen-diluted  $\text{R-32}/\text{air}$  flames in free fall. They found that accurate measurements for these flames are greatly hindered by ignition effects [11]. Specifically, they observed that ignition effects lasted beyond flame radii of 1 cm, which restricts the available data range to derive  $S_u^0$  [11]. This is significant considering that the useable  $R_f$  range for their combustion chamber is from 1 cm to 2 cm [11]. This is attributed to the increased energy required for ignition due to conduction heat loss to the electrodes, which is not present in static experiments as the flame detaches rapidly from the electrodes [11]. Ronney [12] also found ignition challenging and argues that for large Lewis number mixtures, he observed ignition limits as opposed to flammability limits. Takizawa et al. [17] found good agreement between static and free fall experiments for  $\text{R-32}/\text{air}$  flames using the CONV-SEF approach. However, aside from Hesse et al. [11], these free fall measurements do not account for stretch effects which can lead to large errors in  $S_u^0$ .

Radiation heat loss effects in strongly burning and near-limit hydrocarbon/air flames have been extensively studied in the literature [3, 18-21]. Recently, the study of radiative effects was extended to slowly propagating HFC/air and  $\text{NH}_3/\text{air}$  flames [22-28]. Radiation heat loss results in a reduction of the maximum flame temperature, and consequently the overall reactivity and  $S_u^0$  [3, 19, 21, 29]. This effect is henceforth referred to as flame zone losses.

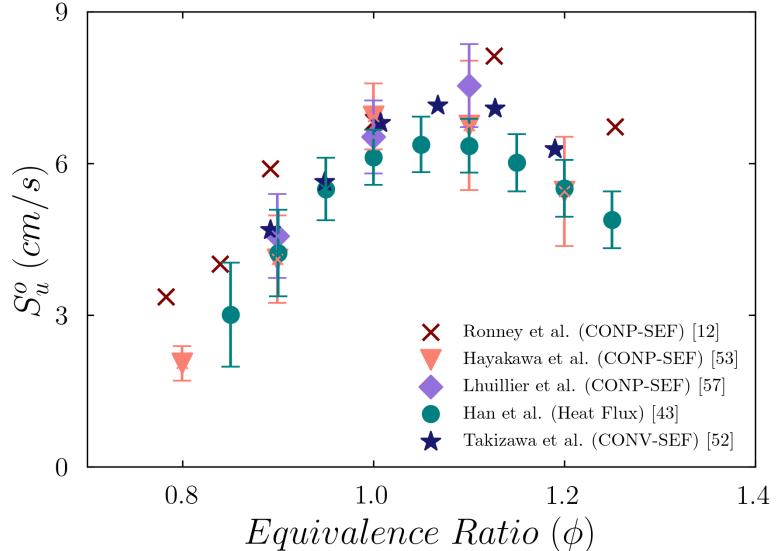
For SEFs, in addition to flame zone losses, cooling of the burned gas due to radiation heat loss induces an inward flow (radiation-induced inward flow,  $u_b$ ) directed towards the center of the flame [3, 20, 21, 28]. Not accounting for this induced flow while interpreting expanding rate measurements of slow flames can result in large errors in the derived  $S_u^0$  values [3, 20, 21]. Yu et al. [30] developed a correlation for correcting SEF data (mixtures of  $\text{H}_2$ ,  $\text{CO}$ , and hydrocarbons with air) to retrieve the *adiabatic*  $S_u^0$ . This correlation, which was obtained from simulations performed for an extensive range of mixture thermodynamic conditions, subtracts both the effects of radiation-induced flow and flame zone losses. Faghih et al. [27] developed a similar correlation for slow  $\text{NH}_3/\text{air}$  flames. Despite being easy to implement, the accuracy of the correlation depends inherently on the accuracy of the kinetic model used. Specifically, the cooling time which determines the extent of heat loss, and the sensitivity of burning rate to changes in adiabatic flame temperature ( $T_{ad}$ ) which is required to estimate flame zone losses, are both dependent on reactivity and hence the kinetic model utilized. And, since kinetic models for  $\text{NH}_3$  and HFC combustion are in their early stages of development (compared to hydrocarbons) and have large uncertainties, it is not desirable to utilize these correlations for such flames [28].

Santner et al. [21] developed an analytical model to estimate  $u_b$  for hydrocarbon/oxidizer SEFs at high pressures. Hesse et al. [24] utilized this model to interpret and correct  $\text{R-32}/\text{air}$  SEF data at elevated initial unburned gas temperatures ( $T_u$ ) and pressures ( $P$ ). However, as noted by Santner et al. [21], the analytical model becomes less accurate for very low flame speeds due to large reductions in flame temperature. Additionally, the model is best suited for flames that are thermo-diffusional neutral, such

that the propagation speed is only a weak function of  $R_f$ . Tavares et al. [28] recently showed that applying Santner et al.'s model to slowly propagating R-32/air SEFs at normal  $T_u$  and  $P$  results in errors of up to 70% when estimating  $u_b$ . Tavares et al. [28] also introduced a computational model, SRADIF, which utilizes chemical equilibrium and radiative cooling in the optically thin limit (OTL) model to estimate the burned gas state and inward flow. This model was shown to accurately estimate the inward flow for R-32/air SEFs by relaxing a couple of key assumptions made in the analytical model: a) SRADIF allows for burned gas composition to change with cooling, which accurately captures changes in the extent of burned gas species ( $\text{CO}_2$  and  $\text{H}_2\text{O}$ ) dissociation, and b) SRADIF accounts for variation in thermodynamic and radiative properties (Planck mean absorption coefficient ( $\kappa_p$ )) with burned gas cooling. SRADIF (and the Santner et al. model [21]) uses experimental data to determine the timescale of radiative cooling, hence not requiring a kinetic model to estimate  $u_b$ .

Given the challenges with accurately measuring  $S_u^0$ s of slow flames, the purpose of this study is to develop a combined experimental and computational methodology that addresses the aforementioned issues presented by buoyancy-induced flow and radiation heat loss. A low-cost drop tower with a free fall time of 0.5s and a short turnaround time is developed and utilized to experimentally investigate spherical slowly propagating flames with a minimal influence of buoyant convection. The SRADIF model is utilized to account for the effect of radiation-induced flow, and accurately interpret the experimental results. The methodology is first applied to measure  $S_u^0$  of a slowly propagating flame fueled by the most studied hydrocarbon, a  $\text{CH}_4$ /air flame at an equivalence ratio,  $\phi = 0.6$ ,  $P = 2$  atm and  $T_u = 300$  K. After demonstrating the ability of the adopted approach to accurately measure  $S_u^0$ s of slowly propagating flames,  $S_u^0$ s of  $\text{NH}_3$ /air flames at  $P = 1$  atm and  $T_u = 300$  K are measured over a range of  $\phi$ . This study constitutes the first study, to the authors' knowledge, that circumvents buoyancy-induced flow and accurately accounts for radiation heat loss effects, and systematically investigates the errors that can arise while deriving  $S_u^0$ s of slowly propagating flames. The paper is organized as follows. Section 2 presents an overview of existing  $\text{NH}_3$ -fueled flame measurements. Section 3 details the experimental (3.1) and computational methodologies (3.2). This is followed by results and discussion for  $\text{CH}_4$ /air and  $\text{NH}_3$ /air mixtures in Sec. 4, and conclusions in Sec. 5.

## 2. Overview of $\text{NH}_3$ -fueled flame studies



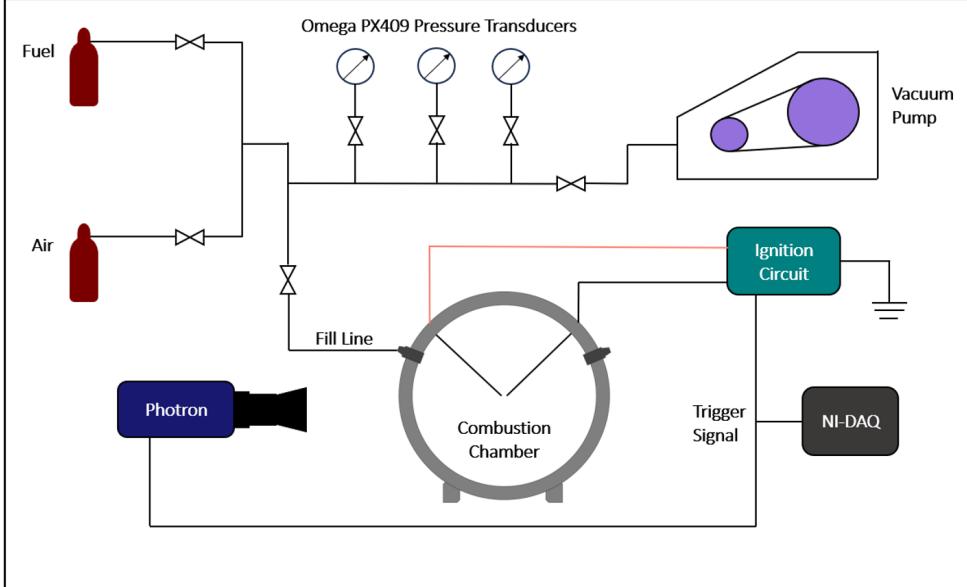
**Figure 1:** Select  $S_u^0$  measurements of  $\text{NH}_3$ /air mixtures as a function of equivalence ratio ( $\phi$ ).

Ammonia combustion has garnered attention in recent years as a zero-carbon fuel and as a viable means of energy storage. The merits and drawbacks of  $\text{NH}_3$  combustion are covered extensively in the following review papers: [31-35]. Flame chemistry of  $\text{NH}_3$  is also relevant in the combustion of energetic materials like ammonium perchlorate and ammonium dinitramide, where it is formed as an intermediate species [36, 37]. Accurate measurements of  $\text{NH}_3$ /air flame properties are key to developing accurate chemical kinetic models not only for  $\text{NH}_3$  combustion but also for the combustion of energetic materials.

The experimental challenges associated with studying  $\text{NH}_3$ /air combustion and the challenges of using pure  $\text{NH}_3$  as a fuel due to its low reactivity have led researchers to investigate  $\text{NH}_3/\text{H}_2/\text{air}$  (a list of  $\text{NH}_3/\text{H}_2/\text{air}$  measurements is compiled in [38]) and  $\text{NH}_3/\text{CH}_4/\text{air}$  mixtures [39-44]. Han et al. [43] experimentally investigated the flame speeds of these blends and found that although the models (GRI-Mech 3.0 [45], Okafor et al. [46], San Diego [47]) they studied predicted the  $S_u^0$ s of  $\text{CH}_4/\text{air}$  and  $\text{H}_2/\text{air}$  mixtures well, they performed poorly when predicting the reactivity of  $\text{NH}_3/\text{fuel}/\text{air}$  blends. This is largely a result of the inaccurate rate constants of the reactions involving species with nitrogen. Another study by Zhu et al. [38] showed that  $S_u^0$  shows large sensitivity to abstraction reactions involving nitrogen species as they inhibit reactivity by competing for hydrogen radicals in  $\text{NH}_3/\text{H}_2/\text{air}$  mixtures. This is again shown in the modeling work by Otomo et al. [48] where the improvement of their model in predicting  $S_u^0$ s of  $\text{NH}_3/\text{air}$  and  $\text{NH}_3/\text{H}_2/\text{air}$  flames is largely attributed to the modifications of reactions of nitrogen species. While these blends enhance reactivity and thereby facilitate experimental measurements, they may not isolate the important reactions involving nitrogen species, which will become more prominent for flames fueled only by  $\text{NH}_3$ .

Several measurements of  $\text{NH}_3/\text{air}$  flame speeds have been made in literature [12, 40, 49-60]. The earlier measurements [49-51] do not account for stretch effects, buoyancy, and radiation heat loss aside from Ronney [12] who performed experiments using a drop tower but did not account for stretch effects. As seen in Fig. 1, Ronney's measurements that were obtained during free fall are different from other measurements, obtained for example using the static SEF configuration. All recent  $S_u^0$  measurements, that account for flame stretch, use the SEF method aside from Han et al. who used the heat flux method [40, 52-60]. Aside from accounting for stretch effects no advancements have been made pertaining to the accuracy of measuring  $\text{NH}_3/\text{air}$  flame speeds. Regarding buoyant convection, authors have used a variety of methods to extract an equivalent radius from the buoyant  $\text{NH}_3/\text{air}$  flames. The methods include: half the maximum horizontal flame dimension [50], radius of a circle that equals the projected flame area [53, 58], etc. As described earlier and shown in Sec. 4, these heuristic approaches result in large errors in the magnitude of the measured  $S_u^0$  [9]. To address radiation heat loss effects, which are prominent in  $\text{NH}_3/\text{air}$  flames, several authors have utilized the correlation developed by Yu et al. for hydrocarbon/air flames to account for the error in  $\text{NH}_3/\text{air}$  flame speed measurements [40, 56, 57, 60]. However, this error is incorporated into the uncertainty analysis and does not improve the accuracy of flame speed measurements. Although the measurements by Han et al. [43] are nearly stretch-free, it is not clear how the data are affected by buoyancy-induced flow and radiation heat loss. Their  $S_u^0$  values, as seen in Fig. 1, agree with the data of Hayakawa et al. [53] who used the CONP-SEF approach and did not account for radiation heat loss or buoyancy-induced flow. Another feature evident in Fig. 1 is the large discrepancy between  $S_u^0$  measurements,  $\sim 2$  cm/s for  $S_u^0 \sim 6$  cm/s. This amounts to a difference of 30% and can be attributed to the issues that were discussed earlier, and potentially the different extrapolation techniques utilized. No study to date has compared the direct experimental measurements (e.g.,  $dR_f/dt$ ) from  $\text{NH}_3/\text{air}$  flames to DNS results, and systematically evaluated if large errors can arise during the extrapolation process [61].

### 3. Approach



**Figure 2:** Schematic of the experimental facility.

Mixture	$\phi$	$P$ (atm)	$Ri$ ( $R_f = 3$ cm)	$T_{ad}$ (K)	$R_{f,min}$ (cm)	$R_{f,max}$ (cm)
CH <sub>4</sub> /air	0.6*	2	1.5	1642	2.1 (~ $30\delta_f$ )	3.8
NH <sub>3</sub> /air	0.8*	1	3.5	1864	1.7 (~ $7\delta_f$ )	3.8
	0.9	1	1.8	1981	1.5 (~ $7\delta_f$ )	3.8
	1.0*	1	1.1	2070	1.6 (~ $9\delta_f$ )	3.8
	1.1	1	0.7	2029	1.8 (~ $11\delta_f$ )	3.8
	1.2	1	0.8	1970	1.8 (~ $10\delta_f$ )	3.8

**Table 1:** List of the mixtures studied and their relevant properties.  $R_{f,min}$  and  $R_{f,max}$  denote the upper and lower radius bounds used for interpretation, respectively.  $R_{f,min}$  is also denoted as a multiple of the flame thickness,  $\delta_f$ . (\* indicates conditions for which both static and free-fall measurements were conducted)

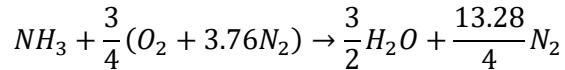
### 3.1. Parameter Space

Static (only at select conditions) and free-fall measurements were performed for a CH<sub>4</sub>/air flame at  $\phi = 0.6$ ,  $P = 1$  atm and  $T_u = 300$  K, and NH<sub>3</sub>/air flames at  $P = 1$  atm and  $T_u = 300$  K over a range of  $\phi$ ,  $0.8 \leq \phi \leq 1.2$ ; see Table 1. Attempts were made to ignite flames at  $\phi = 0.7$  and 1.3 for NH<sub>3</sub>/air in free fall, however, these were unsuccessful. All cases included in this study were repeated twice to ensure consistency (see SM-H). Since this is the first study using this experimental facility, static experiments were also carried out for CH<sub>4</sub>/air flames at  $P = 1$  atm and  $T_u = 300$  K to ensure that the adopted approach is capable of accurately measuring  $S_u^0$ s; details regarding these experiments and the results obtained can be

found in SM-D. The mixtures considered in this study are listed in Table 1. The experimental methods described below are identical for both the static and free-fall experiments, except the use of the drop tower (see Sec. 3.2.1) for the free-fall measurements.

### 3.2. Experimental Approach

All experiments are conducted in a 12.9 L, stainless steel cylindrical chamber with optical access at both ends; see Fig. 2. The internal diameter is 25.4 cm with an aspect ratio of unity. The combustion chamber is fitted with polycarbonate windows that are 1.8 cm thick with an optical diameter of 10.16 cm. The chamber is first vacuumed down to less than 40 Pa, and then filled with a mixture using the method of partial pressures. The equivalence ratio for NH<sub>3</sub>/air cases is determined by the following stoichiometric reaction,



The fuel is filled first followed by the oxidizer, compressed air. The anhydrous NH<sub>3</sub> used has a purity of 99% and the compressed air is desiccated and filtered. Omega PX409-A5V series pressure transducers were used. The transducer with the appropriate full-scale pressure range was used to fill each gas to minimize the uncertainty in the equivalence ratio [62]. Ammonia adsorption, which has been discussed in prior studies, results in the pressure of NH<sub>3</sub> dropping over time which can result in a large deviation in equivalence ratio [43, 52, 59, 63]. This can be circumvented by waiting approximately an hour until the pressure drop is negligible [52, 59], which was verified with repeated tests.

The mixture was allowed to rest for at least 10 minutes before ignition to ensure the gas's quiescence. The chamber is equipped with two stainless steel electrodes (<1 mm thickness, 1.5 mm spark gap), allowing for the central ignition of the mixture. A tunable capacitive discharge circuit allows for the spark energy to be tailored to minimize ignition effects on flame propagation. Due to the low reactivity of NH<sub>3</sub>/air mixtures, substantially larger ignition energy is required in comparison to hydrocarbon/air mixtures. The ignition, drop, and recording are synchronized with a LabView program.

#### 3.2.1. Drop Tower

For the free fall experiments, a lab-scale drop tower was designed and built to minimize buoyancy-induced flow distortions. The drop tower has dimensions of 1.16m x 1.16m x 2.65m and accommodates the chamber, a high-speed camera, and wiring. It consists of a platform on which the combustion chamber and camera are mounted. The platform is hoisted, aligned, and fixed in place by electromagnets that can be disengaged simultaneously for a precise release (see SM-A for images of the drop tower). The platform, which holds both the combustion chamber and camera, has dimensions of 0.4 m x 0.4 m x 0.01 m, weighs ~45 kg, and falls ~1.5 m when released by the electromagnets. A bed of foam cubes is used to decelerate the platform and bring it to rest while preventing any damage to the camera. The drop tower has a free fall time of ~0.5s. An in-house LabVIEW script simultaneously initiates recording, ignition, and the release of the combustion assembly. During free fall, a deviation of less than 2% from the acceleration due to gravity, predicted by theoretical analysis, is confirmed by optical measurements (see SM-A). This is sufficient to establish SEFs for the slowly propagating mixtures listed in Table 1.

### 3.2.2. Direct Imaging/Optical Calibration

The SEFs are directly imaged using a Photron FASTCAM Mini AX50 with a 50 mm focal length lens. Imaging was performed at 2000 fps with a  $1024 \times 1024$  pixel imaging window. The use of direct imaging is necessary as the lab-scale drop tower cannot accommodate a schlieren/shadowgraph system. An optical calibration factor is required to convert the measured pixels to a length scale. The accuracy of this factor is of great importance as the error in  $S_u^0$  is directly proportional to the error in the calibration factor. The advantage of schlieren/shadowgraph imaging is the use of parallel light which greatly facilitates optical calibration. Direct imaging of flame propagation at close distances is challenging due to the three-dimensional nature of the flame in combination with the light rays being not parallel [64]. Specifically, as the distance between the camera and the flame decreases, only a fraction of the hemisphere on the camera side is visible; the poles are not visible. Therefore, an error will result if a calibration factor that is developed using a planar calibration target is utilized to derive the radius of a sphere. To avoid this, an optical calibration technique was developed by imaging high-tolerance aluminum cylinders at various radii (0.635 cm – 3.81 cm) at a distance that was utilized for the experiments as well. Cylinders were chosen as spherical optical targets are prohibitively expensive to procure with dimensional tolerances small enough for calibration purposes. The cylinders provide a similar projection onto the camera sensor as a sphere, in one direction. More details of the procedure are provided in SM-C. The optical calibration results in a correlation that converts the imaged radii in pixels to length in cm. For the current study, the calibration factor is about 7 pixels/mm (does not change with the size of the object in the relevant range of radii), which is sufficient to resolve the flames considered.

The high-speed videos are post-processed using an in-house Python code to extract the radius of the flame. The images are minimally preprocessed using a Gaussian blur to smooth aberrant pixel noise. A numerical gradient of the image yields a set of points; a convex hull of these points yields the outer flame surface. A circle is fit to this set of points using the single-value-decomposition-based Taubin circle fit [65]. The aforementioned correlation is applied to convert the radii in pixels to flame radius,  $R_f$ , in cm. For buoyant, static flames,  $R_f$  is ill-defined as the flame is not spherical. A typical approach utilized in previous studies [12, 50, 55] is to track the maximal horizontal length of the flame and use half of this value as  $R_f$ . This method is also used for the static cases in this study to compare with the flame speeds obtained from free fall experiments at similar conditions denoted in Table 1. The method used to determine flame radius can have a large effect on the post-processed flame behavior. As Berger et al. [9] showed in their DNS study, flame stretch for buoyant flames varies with time along the flame front. This means that the point on the flame tracked by the maximal horizontal length method does not have the same flame stretch as the one obtained in free fall [9], and consequently, does not evolve in the same way; see Sec. 4 for more details. A local second-order fit is applied to the  $R_f$  vs. time data to calculate the derivative,  $dR_f/dt$ . However, as stated earlier, this  $dR_f/dt$  results from a combination of the stretched, burned flame speed,  $S_b$ , and the radiation-induced inward gas velocity,  $u_b$ . To extract  $S_b$ , Eq. 1 [3] is used with  $u_b$  estimated using SRADIF (see Sec. 3.3.2). With the  $S_b$  and  $K$  (Eq. 2 [66]), an extrapolation must be used to compute the unstretched, burned flame speed  $S_b^0$ . Both linear (Eq. 3 [67]) and nonlinear extrapolation models (Eq. 4 [68, 69]) were applied to the inward-flow-corrected  $S_b$  vs.  $K$  results to obtain estimates for the unstretched, burned flame speed  $S_b^0$  at zero  $K$ . The ranges of  $R_f$  for extrapolation are listed in Table 1. The upper bound ( $R_{f,max}$ ) is chosen as 4 cm (30% of the chamber radius) to avoid confinement and pressure rise effects [70, 71]. The lower bound ( $R_{f,min}$ ) is chosen in a way to avoid ignition-affected data. It has been shown in previous studies that ignition effects dissipate as the flame propagates about 5-10 flame thicknesses ( $\delta_f$ ) [72-74]. Based on this and the trends depicted by the acquired data, we chose  $R_{f,min}$  to be at least  $7\delta_f$  (calculated using the respective kinetic models). This is further discussed in Sec. 4.2.

The density ratio  $\rho_u/\rho_b$  of the adiabatic case (i.e.,  $\rho_b$  computed assuming equilibrium conditions) was then used to convert  $S_b^0$  to  $S_u^0$  through mass continuity [28].

$$S_b = \frac{dR_f}{dt} - u_b \quad (1)$$

$$K = \frac{2}{R_f} \frac{dR_f}{dt} \quad (2)$$

$$S_b = S_b^0 - L_b K \quad (3)$$

$$\left(\frac{S_b}{S_b^0}\right)^2 \ln\left(\frac{S_b}{S_b^0}\right)^2 = -\frac{2L_b K}{S_b^0} \quad (4)$$

An uncertainty analysis was performed following a method similar to that developed by Xiouris et al. [62]. Error bars in results depict the combined uncertainty,  $\pm\sigma$ , of the mixture preparation, data acquisition, and data processing steps. For the sake of clarity, the uncertainty bands will only be included in the  $S_b^0$  and not in the  $dR_f/dt$  and  $S_b$  plots; however, the data and  $\sigma$ s are included in SM-B. For more details regarding the uncertainty analysis, the reader is referred to SM-B.

### 3.3. Computational Approach

#### 3.3.1. Planar and spherical flames

Planar, 1-D, steady, freely propagating flame simulations were performed using the free flame module of Cantera [75] including the effects of radiation heat loss. In addition, 1-D SEF DNS at constant pressure were performed using the reacting flow code SLTORC. Details regarding the ability of SLTORC to accurately simulate SEFs can be found in Tavares et al. [28]. SEFs are initialized by a kernel of hot burned gas, and a hyperbolic tangent profile is utilized to transition smoothly between the burned and unburned gas states. The ignition energy is controlled through parameters specifying the initial kernel radius and temperature, which were chosen so that ignition-related effects would be minimized, enabling quasi-steady propagation to be reached at radii relevant to constant-pressure SEF experiments. The time-evolution of  $R_f$  is determined using a user-specified isotherm. Convergence tests were conducted to determine proper values for parameters controlling grid refinement and time step size to allow for grid-independent solutions. For each mixture/case, DNS studies were performed assuming (1) adiabatic conditions, and (2) including radiation heat loss.

In the above planar and spherical flame simulations, radiation heat loss was modeled using the OTL assumption. The OTL model provides an analytical formulation for emission-dominated radiative heat loss flux ( $\dot{q}_{rad}$ ) using Planck mean absorption coefficients ( $\kappa_p$ ) of major radiating species. Radiation reabsorption is ignored in the OTL model, but this effect may need to be considered in future work for slowly propagating flames with relatively large optical thicknesses. Burgess et al. [76] have considered radiation reabsorption in spherical HFC/air flames, but limited their analysis to solely CO<sub>2</sub> reabsorption, as spectrally-resolved radiation properties are not available for HFC refrigerants [76]. Radiation reabsorption effects have been studied in planar NH<sub>3</sub>/air flames considering the emission and reabsorption of NH<sub>3</sub> and H<sub>2</sub>O [25] but have not been formally studied in spherical NH<sub>3</sub>/air flames. However, radiation reabsorption has been shown to become more relevant at higher pressures and may need to be considered in high-pressure NH<sub>3</sub>/air SEFs [25].

The FFCM-1 kinetic model [77] was used for CH<sub>4</sub>/air flame simulations, and the kinetic models developed by Nakamura et al. [78], Stagni et al. [79], and Zhu et al. [38] were used to simulate NH<sub>3</sub>/air flames. Comparisons with the other models, such as [38, 79], can be found in SM-G. For radiative CH<sub>4</sub>/air flames, CO<sub>2</sub>, H<sub>2</sub>O, CO, and CH<sub>4</sub> were considered as major radiative species, while for radiative NH<sub>3</sub>/air flames, H<sub>2</sub>O, NH<sub>3</sub>, NO, and N<sub>2</sub>O were considered as major radiative species. The different values of  $\kappa_p$  for H<sub>2</sub>O, CO<sub>2</sub>, CO, and CH<sub>4</sub> were obtained from Barlow et al. [80], while the values of  $\kappa_p$  for NH<sub>3</sub>, NO, and N<sub>2</sub>O were obtained from Nakamura et al. [78]. The Cantera and SLTORC source codes were modified to include  $\kappa_p$  for radiative species relevant to CH<sub>4</sub>/air and NH<sub>3</sub>/air flames. The DNS results of SLTORC SEFs were subsequently post-processed to determine the evolution of  $dR_f/dt$  with  $K$  for both the adiabatic and radiative cases, as well as the evolution of  $R_f$  with  $t$  for the radiative case to be used in the SRADIF model.

### 3.3.2. Estimating radiation-induced flow

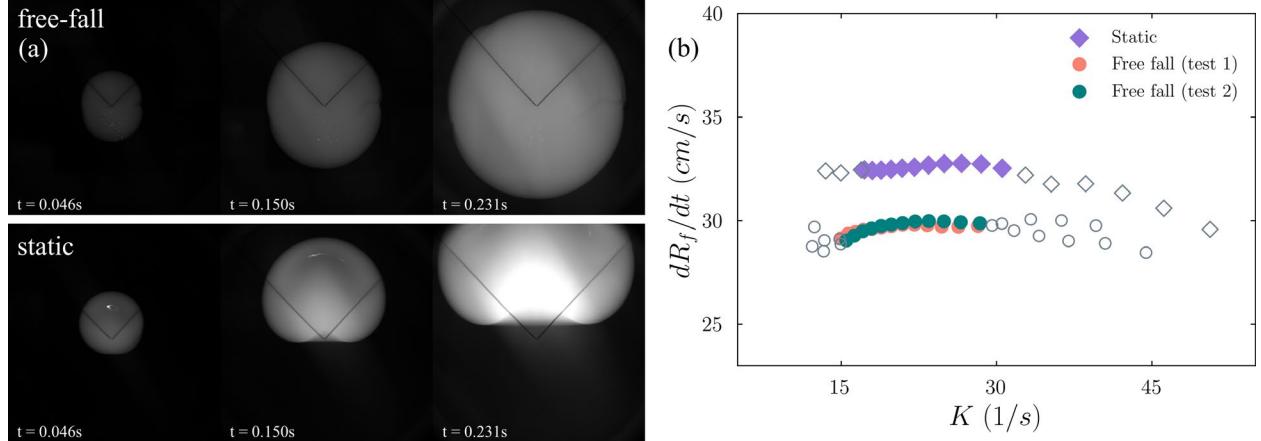
The SRADIF model was used to interpret experimental and DNS-generated  $R_f$  vs.  $t$  data, to correct for radiation-induced inward flow. Details related to the SRADIF model algorithm are briefly described below, and a detailed description can be found in Tavares et al. [28]. The SRADIF model discretizes a sufficiently large spherical gas volume into layers of thin spherical shells of equal width and combines thermodynamic equilibrium and finite rate OTL radiation heat loss calculations to estimate  $u_b$ . Spherical shells are iteratively combusted by performing thermodynamic calculations, using the equilibrium capabilities of Cantera [75], to estimate the gas state at the maximum flame temperature of the radiative flame. During each combusted shell iteration, the SRADIF model accounts for finite-rate radiation heat loss in previously burned gas shells using a radiative cooling time scale derived from  $R_f$  vs.  $t$  measurements. Temperature reductions in each burned gas shell are computed using the OTL radiation model accounting for select radiative species through the different values of  $\kappa_p$ . For each combusted shell iteration, the total shrinkage of burned gas shells due to radiative cooling (i.e., due to reductions in burned gas shell temperature) and the radiative cooling time scale are then used to compute  $u_b$ . Iterating through the combustion of all spherical shells provides the evolution of  $u_b$  with  $K$ , which can be subtracted from  $dR_f/dt$  to obtain  $S_b$ .

In this study, the thermodynamic data of the FFCM-1 [77] and Nakamura et al. [78] chemical models were used to compute gas state properties and equilibrium states for CH<sub>4</sub>/air and NH<sub>3</sub>/air cases, respectively. Additionally, the different values of  $\kappa_p$  are incorporated in the OTL radiation models of Cantera and SLTORC (as described in Sec. 3.3.1) were included in the SRADIF model. The number of spherical shells used by the SRADIF model was varied to ensure shell-independent solution convergence for  $u_b$  and  $S_b$  (~1000 shells).

$S_b$ s derived using the abovementioned procedure are affected by flame zone (radiation heat) losses. Hence the  $S_u^0$  subsequently derived from this  $S_b$  is not *adiabatic*. While Santner et al. [21] proposed a subsequent step to subtract the flame zone losses to obtain the adiabatic  $S_u^0$ , there are several drawbacks to using such a method. First, Santner et al. [21] make multiple assumptions to obtain a tractable analytical form for the flame zone loss correction. Second, the analytical form requires knowledge of the overall or global activation energy (sensitivity of changes in burning flux to changes in  $T_{ad}$ ), often obtained utilizing detailed chemical kinetic models [28]. Since kinetic models for slowly propagating flames (NH<sub>3</sub>/air, HFC/air, etc.) have large uncertainties, the corresponding flame zone loss corrections derived will also be highly uncertain. Therefore, for the purpose of testing kinetic models, it is of more utility to compare the flame-zone-heat-loss-affected  $S_b$  measurements to model predictions that are also affected by flame zone losses. Therefore, corrections for flame zone losses were not performed in this study.

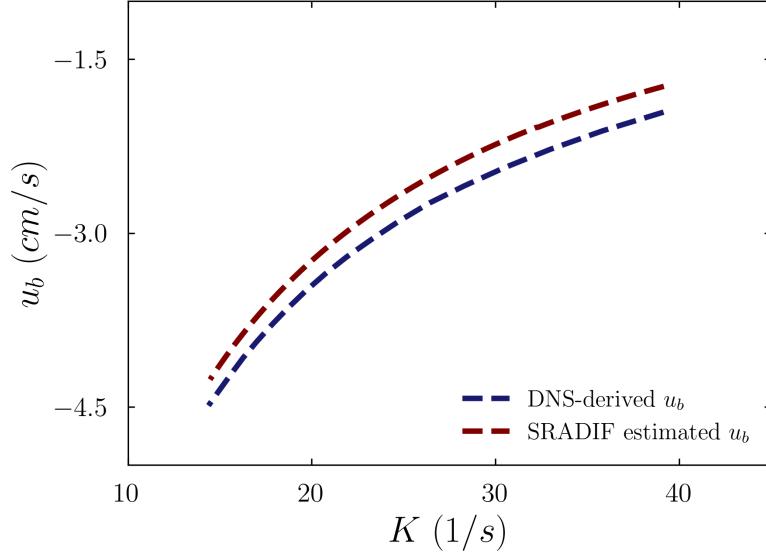
## 4. Results and Discussion

### 4.1. Methane/air



**Figure 3:** a) Static versus free fall temporal evolution for a CH<sub>4</sub>/air flame ( $\phi = 0.6$ ,  $P = 2$  atm,  $T_u = 300$  K) b) Measured, static versus free fall (filled symbols denote data useable for extrapolation),  $dR_f/dt$  as a function of flame stretch for the same CH<sub>4</sub>/air flame with data from two experimental trials shown for the free fall measurements.

As discussed in Sec. 1, we first study a slowly propagating CH<sub>4</sub>/air flame at  $\phi = 0.6$ ,  $P = 2$  atm, and  $T_u = 300$  K. CH<sub>4</sub> is a well-studied hydrocarbon and hence a suitable candidate to first apply the experimental and interpretational approach detailed in Sec. 3. The flame evolution under static and free fall conditions are depicted in Fig. 3a. It is clear that under static conditions the flame undergoes significant distortion as well as upward displacement. However, under free fall conditions, the flame remains more or less spherical, as desired. The deviation from sphericity was also quantified and found to be minimal; more information about this can be found in SM-K. Figure 3b depicts the  $dR_f/dt$  values extracted from these experiments. The free-fall experiments show a high degree of repeatability with the mean, measured flame speeds for the consecutive free-fall runs differing by less than 0.5% in the region used for extrapolation. Note that for the static experiments,  $R_f$  is half the maximum horizontal diameter of the distorted flame, and  $K$  is calculated based on this radius. It is clear that the  $dR_f/dt$  vs.  $K$  behavior is different between the static and free fall measurements. The values extracted from the static case are larger than those from the free fall experiments, similar to the computational results of Berger et al. [9]. If an extrapolation (e.g., linear) is performed using these two sets of data to subtract the effects of stretch, the resulting flame speeds will differ by 14%. However, as discussed in Sec. 3.2.2 (Eqn. 1),  $S_b$  has to be derived from  $dR_f/dt$ , by correcting for the radiation-induced flow, before an extrapolation procedure can be applied.



**Figure 4:** Comparison of DNS-derived and SRADIF-estimated  $u_b$ s for a CH<sub>4</sub>/air flame at  $\phi = 0.6$ ,  $P = 2$  atm,  $T_u = 300$  K

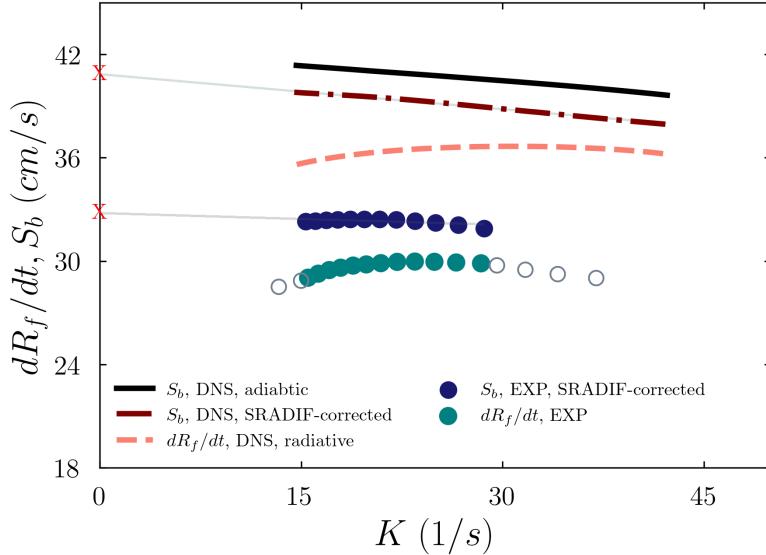
We utilize SRADIF to estimate the radiation-induced flow,  $u_b$ . The accuracy of SRADIF depends on its ability to predict the burned gas state (temperature and species mole fractions) just downstream of the flame. Tavares et al. [28] showed that if the burned gas does not attain equilibrium (i.e., the state of the gas at the maximum flame temperature greatly differs from the equilibrium state), the burned gas temperature and species composition cannot be calculated using equilibrium thermodynamics and leads to large errors in the SRADIF-estimated  $u_b$  values. In a previous study by Tavares et al. [28], it was shown that SRADIF was able to accurately estimate  $u_b$  for R-32 flames. But the  $u_b$  values for R-1234yf/air SEFs had large errors, the reason being that the burned gas did not attain equilibrium as the heat loss resulted in the reacting gas getting frozen at a different metastable state; more details can be found in [28]. Therefore, it is important to test the accuracy of the SRADIF model before utilizing it for slowly propagating CH<sub>4</sub>/air and NH<sub>3</sub>/air flames considered in this study.

DNS was performed for the same spherically expanding CH<sub>4</sub>/air flame at  $\phi = 0.6$ ,  $P = 2$  atm, and  $T_u = 300$  K including radiation heat loss. The full field results were utilized to calculate  $u_b$  using the methodology detailed in Tavares et al. [28]. They derived the inward gas velocity field induced by radiation heat loss  $u_{rad}(r)$  as a function of radial distance  $r$  given by Eq. (5),

$$u_{rad}(r) = -\frac{1}{r^2} \int_0^r \frac{\dot{q}_{rad}}{\rho c_p T} \bar{r}^2 d\bar{r} \quad (5)$$

where  $\dot{q}_{rad}$  is the volumetric radiative heat loss flux (calculated using the OTL radiation model),  $\rho$  is gas density,  $c_p$  is specific heat at constant pressure,  $T$  is temperature, and  $\bar{r}$  is a radial integration variable. Subsequently,  $u_b$  is computed by taking the minimum of  $u_{rad}(r)$ , which occurs in the proximity of the flame zone. Values for  $u_b$  computed directly from DNS results are compared to  $u_b$  values estimated using SRADIF in Fig. 4. Note that, in order to estimate  $u_b$ , SRADIF takes as input, only  $R_f$  vs  $t$  from the DNS result and the unburned mixture condition. It is evident that SRADIF is able to accurately estimate  $u_b$  for the slowly propagating CH<sub>4</sub>/air flame as the differences between the mean DNS-derived and SRADIF-estimated values were less than 10%. As  $S_b$  is obtained by subtracting  $u_b$  from  $dR_f/dt$ , which is numerically much larger (see Figs. 4 and 5), this amounts to less than 1% difference in SRADIF-corrected and DNS-corrected  $S_b$  values. In addition, it is also shown in SM-J that SRADIF performs significantly

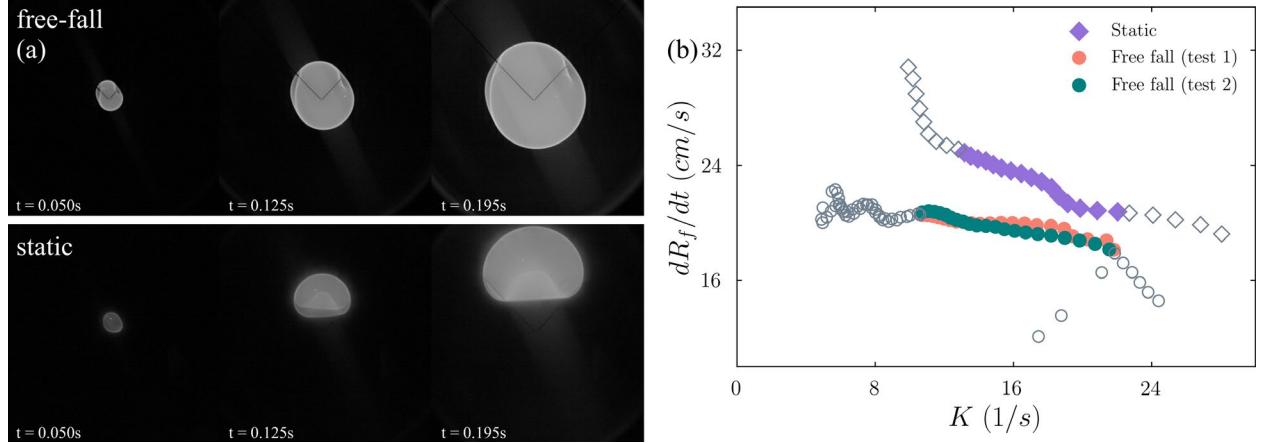
better when compared to the Santner et al. model [21], which utilizes multiple simplifying assumptions as mentioned Sec. 1.



**Figure 5:** Spherical, CH<sub>4</sub>/air flame with  $\phi = 0.6$ ,  $P = 2$  atm,  $T_u = 300$  K: SRADIF corrected experimentally measured data (filled symbols denote data useable for extrapolation) compared to adiabatic DNS computed  $dR_f/dt$ , OTL DNS computed  $dR_f/dt$ , and the SRADIF corrected OTL DNS curve.

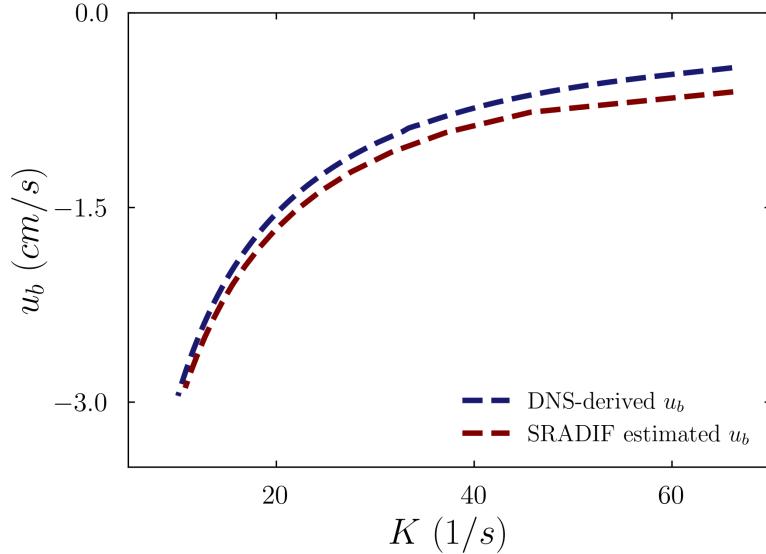
Figure 5 depicts  $dR_f/dt$  and  $S_b$ , obtained from the free fall experiment as a function of  $K$ .  $S_b$  was derived by subtracting SRADIF-estimated  $u_b$  values from  $dR_f/dt$ . Also shown in the plot are  $dR_f/dt$  and  $S_b$  extracted from the DNS simulation result with radiation heat loss, and  $S_b$  ( $= dR_f/dt$ ) from a DNS simulation assuming adiabaticity. Several observations can be made from these results. First, the slope of  $S_b$  vs.  $K$  is substantially different from  $dR_f/dt$  vs.  $K$ ; the magnitudes are also different. Therefore, not correcting for radiation-induced flow can result in errors in  $S_u^0$  of  $\sim 15\%$ . Second, the DNS results indicate that the effect of radiation-induced flow on flame speed is significantly larger than the flame zone loss effect. This is evident through the larger difference between radiative  $S_b$  and radiative  $dR_f/dt$  compared to the difference between adiabatic  $S_b$  and radiative  $S_b$ . Third, although the slopes of experimentally derived  $dR_f/dt$  and  $S_b$  vs.  $K$  are similar to the corresponding DNS values, the linearly extrapolated values (Eqn. 3) differ by  $\sim 22\%$ . This is also reflected in the extrapolated  $S_b^0$ , and density corrected  $S_u^0$ . It is worth examining if any of the assumptions that were utilized in data interpretation or modeling caused this large difference between the experiment and model prediction. The assumption that radiation reabsorption is negligible may not be entirely applicable under this condition. However, this does not explain the difference, as including reabsorption in the DNS calculations will only increase the value of simulated  $dR_f/dt$ , making the difference between data and simulation larger. The derived experimental  $S_u^0$  is also compared to existing measurements at the same condition [81-83] in SM-E; these data were used to optimize and reduce the uncertainty of FFCM-1, the kinetic model used for the simulations. The discrepancies between our derived  $S_u^0$  and existing data can be attributed to previous studies not accounting for the effects of buoyancy-induced flow and radiation heat loss. These results demonstrate the importance of accounting for buoyancy and radiation heat loss effects when interpreting slowly propagating flame data.

## 4.2. Ammonia/air



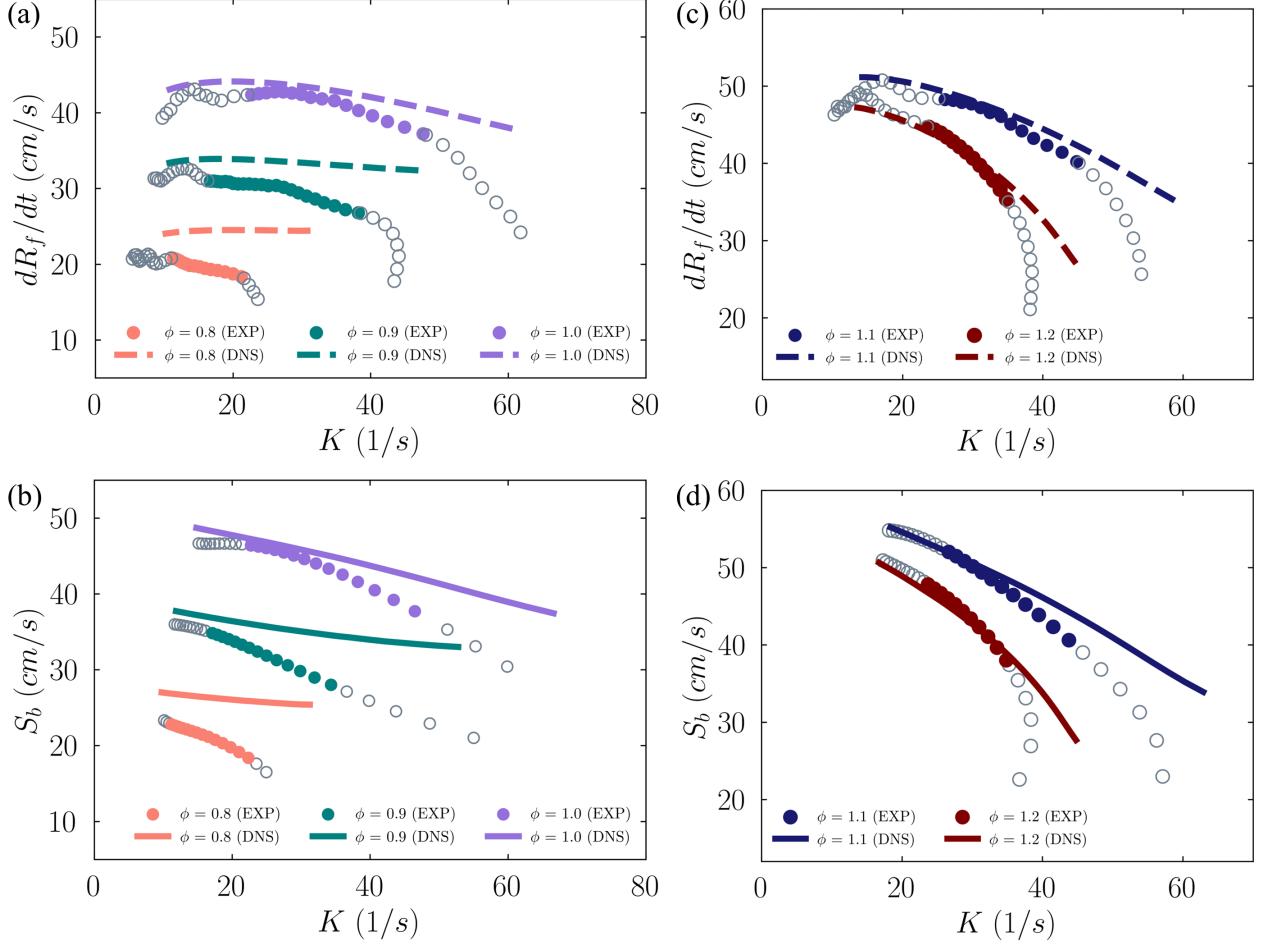
**Figure 6:** a) Static versus free fall temporal evolution for an NH<sub>3</sub>/air flame ( $\phi = 0.8$ ,  $P = 1$  atm,  $T_u = 300$  K) b) Measured, static versus free fall (filled symbols denotes data useable for extrapolation),  $dR_f/dt$  as a function of flame stretch for an NH<sub>3</sub>/air flame ( $\phi = 0.8$ ,  $P = 1$  atm,  $T_u = 300$  K)

NH<sub>3</sub>/air SEFs at  $P = 1$  atm,  $T_u = 300$  K, and  $0.8 \leq \phi \leq 1.2$  are studied in free fall. Static experiments were also performed for  $\phi = 0.8$  and  $\phi = 1.0$  to evaluate the errors that result if  $S_u^0$ 's are derived from buoyancy-distorted flames instead of spherical flames obtained under free fall. Being the slowest flame with the largest  $Ri$  (see Table 1), the  $\phi = 0.8$  case is chosen for an in-depth analysis. Results for the  $\phi = 1.0$  case can be found in SM-I. Figure 6a shows the evolution of the SEF under static and free-fall conditions. Figure 6b depicts the  $dR_f/dt$  values extracted from these experiments. Consecutive free-fall runs for this case are shown in Fig. 6b to highlight the repeatability of the experimental methodology. It is observed in Fig. 6a that the morphology of the flames are significantly different. Under static conditions, the flame develops the distinct shape of a mushroom with the stem removed. The flow field that develops and causes this distinct shape is described in the DNS study by Berger et al. [9]. However, in free fall, the flame remains spherical, demonstrating the capability and precision of the low-cost drop tower to experimentally probe slowly propagating flames. The deviation from sphericity was also quantified and found to be minimal; more information about this can be found in SM-K. Additionally, as seen in Fig. 6b, it is clear that  $dR_f/dt$  vs.  $K$  behavior is markedly different between the static and free fall measurements. The same method described in Sec. 4.1 was used to extract the radius of the buoyant, non-spherical flame. The values extracted from the static case are larger than those from the free-fall experiments and a linear extrapolation of the static case within the usable data range would result in a 44% larger  $S_u^0$  as a result of the large differences in slope! Also, note the substantial increase in  $dR_f/dt$  at large  $R_f$  (or small  $K$ ). This was also observed in other measurements [40, 53] and DNS [9], and is most likely due to the flow field that develops during flame distortion.



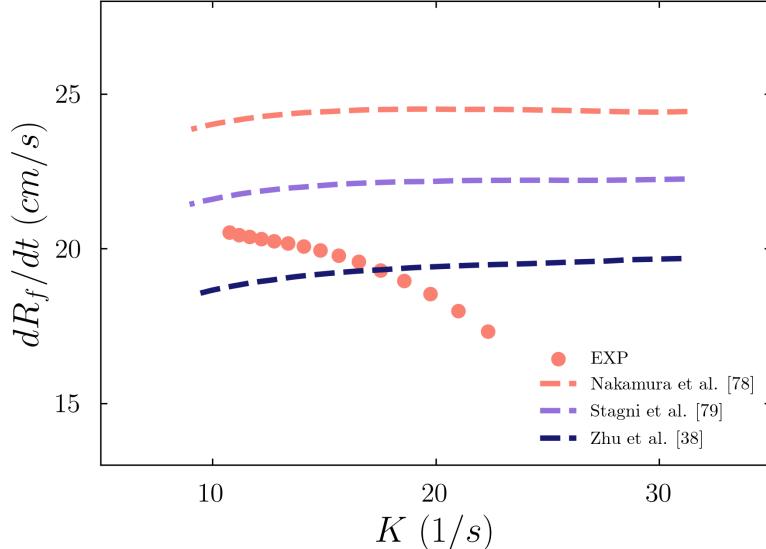
**Figure 7:** Comparison of DNS-derived and SRADIF-estimated  $u_b$ s for an  $\text{NH}_3$ /air flame at  $\phi = 0.8$ ,  $P = 1$  atm,  $T_u = 300$  K

DNS was performed for the same spherically expanding  $\text{NH}_3$ /air flame at  $\phi = 0.8$ ,  $P = 1$  atm,  $T_u = 300$  K including radiation heat loss. The full field results were utilized to calculate  $u_b$  [28]. These values are compared to  $u_b$  values estimated using SRADIF in Fig. 7. Clearly, SRADIF can accurately estimate  $u_b$  for the slowly propagating  $\text{NH}_3$ /air flame as the percent differences between DNS-derived and SRADIF-estimated values is  $\sim 5\%$  which results in a  $0.6\%$  difference in the corresponding  $S_b$ . This was found to be the case for other  $\phi$ s as well.



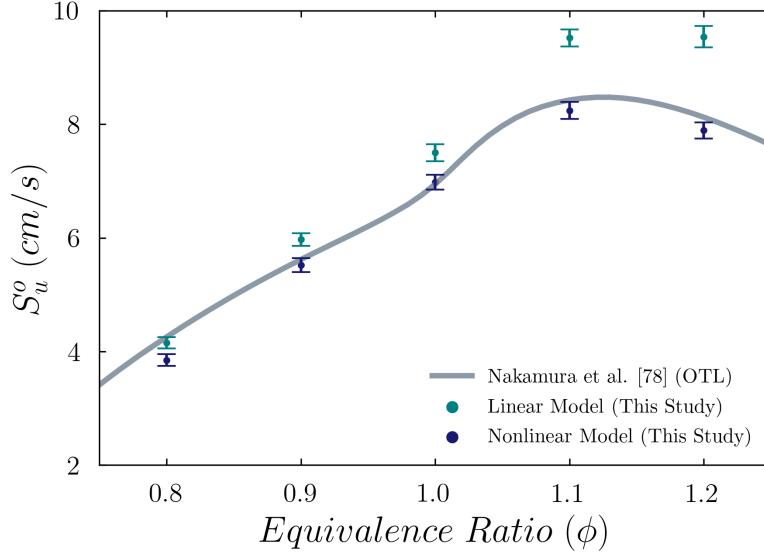
**Figure 8:** a) & b) Evolution of  $dR_f/dt$  from free fall experiments and OTL DNS as a function of flame stretch (solid symbols denotes data useable for extrapolation) for NH<sub>3</sub>/air flames:  $0.8 \leq \phi \leq 1.2$ ,  $P = 1$  atm, and  $T_u = 300$  K. c) & d)  $S_b$  from experiments (SRADIF-corrected) and OTL DNS (DNS-corrected) (solid symbols denotes data useable for extrapolation) for NH<sub>3</sub>/air flames:  $0.8 \leq \phi \leq 1.2$ ,  $P = 1$  atm, and  $T_u = 300$  K

Figure 8a and 8b depicts  $dR_f/dt$  obtained from free fall experiments for  $0.8 \leq \phi \leq 1.2$  as a function of  $K$ . Figure 8c and 8d depicts  $S_b$  that was derived by subtracting SRADIF-estimated  $u_b$  values from these  $dR_f/dt$ . Also shown in the plots are  $dR_f/dt$  with radiation heat loss (Figs. 8a and 8b) and  $S_b$  extracted from the DNS results (Figs. 8c and 8d). The full field results were utilized to calculate  $u_b$  for the radiative DNS [28]. The Nakamura et al. model [78] predictions agree with experimentally measured  $dR_f/dt$  for  $\phi \geq 1$ . For  $\phi < 1$ , the slopes and magnitude of the experimental and simulated curves differ significantly, especially at larger  $K$ . The differences observed between experimental and DNS results are also similar for the  $S_b$  vs.  $K$  curves. This is expected as it was previously shown (Fig. 7) that  $u_b$  values obtained from DNS and SRADIF are consistent. Also noticeable from the data are the prolonged ignition effects. Consequently, care has to be taken in choosing the range of  $R_f$  that will be used for extrapolation. The minimum value of  $R_f$  considered is about 7 flame thicknesses which, as a result of the large  $\delta_f$  of NH<sub>3</sub>/air flames, comes to  $\sim 1.7$  cm (see Table 1). The maximum value of  $R_f$  chosen is  $\sim 3.8$  cm, which is governed by the dimensions of the combustion chamber. In DNS, the flames reach quasi-steady propagation faster than what is observed in experiments, but this does not explain the large difference in magnitude and slope of these curves for the  $\phi < 1$  mixtures. Most notably, the  $\phi = 0.8$  and  $\phi = 0.9$  cases show large differences in flame dynamics between experiments and computations (see Fig. 8a).



**Figure 9:** Comparison of experimentally measured and DNS computed  $dR_f/dt$  as a function of flame stretch using the models of Nakamura et al. [78], Stagni et al. [79], and Zhu et al. [38] for a lean  $\text{NH}_3/\text{air}$  flame ( $\phi = 0.8$ ,  $P = 1$  atm,  $T_u = 300$  K)

To evaluate if this observed discrepancy is due to the particular choice of kinetic model, Figure 9 compares the  $dR_f/dt$  from the  $\phi = 0.8$  case to predictions of three kinetic models. It is evident that all three models fail to reproduce the slope and/or magnitude of the experimental data. Furthermore, there are significant differences between the three models, which is a testament to the large uncertainty in the kinetic models for  $\text{NH}_3$  combustion. Another reason for the observed discrepancy in slopes could be due to the assumption made in the computations that radiation reabsorption is negligible in these flames. Including radiation reabsorption would result in lower radiative heat loss and to a small extent, preheating of  $\text{NH}_3$  in the unburned gas as was seen in the study by Zheng et al. [25] in planar  $\text{NH}_3/\text{H}_2/\text{air}$  flames. Incorporating this into the flame simulations could result in better agreement in the slope between the DNS computed and experimentally measured  $dR_f/dt$  as a function of flame stretch. This is however outside the scope of the current study and will be investigated as part of a future study. Additional comparisons, at the other equivalence ratios, with the three models considered in this study are included in SM-G.



**Figure 10:** Experimentally derived  $S_u^0$  using analytically derived linear and nonlinear extrapolation methods against 1-D OTL Cantera free-flame computations.

Figure 10 depicts  $S_u^0$ 's derived by extrapolating the (SRADIF-corrected)  $S_b$  data using the analytically derived linear (Eqn. 3) and nonlinear models (Eqn. 4). The DNS-assisted extrapolation approach [62], which has been shown to perform well for hydrocarbon-fueled flames, was not utilized due to the significant differences in slopes between the data and model predictions observed in Fig. 8. Also plotted in Fig. 10 are results from freely propagating flame simulations using the Nakamura et al. model [78], including OTL radiation heat loss. Although the differences between the results obtained using the two extrapolation models are small for  $\phi \leq 1.0$ , the differences are larger on the fuel-rich side ( $\phi > 1$ ). Prior studies [53, 54] have used the linear extrapolation model by arguing that the Lewis number ( $Le$ ) is nearly unity across all  $\phi$ 's for  $\text{NH}_3/\text{air}$  flames. They cite a DNS study by Chen [84] who showed good agreement between the linear and nonlinear extrapolation models for mixtures with unity  $Le$ . However, it is clearly seen in Fig. 8b that the shape of  $S_b$  vs.  $K$  curves are nonlinear, and consequently using the linear model results in systematically larger values of  $S_u^0$  (see SM-F).

Another interesting observation from Fig. 10 is the relatively good agreement between the experimental data (derived using non-linear extrapolation) and model predictions. However, in Fig. 8, the model predictions using DNS agree with direct measurements ( $dR_f/dt$ ) only for  $\phi \geq 1$ . For  $\phi < 1$ , the DNS predictions and data display significantly different slopes. Therefore, the agreement seen between the data and the model prediction in Fig. 10 for  $\phi < 1$  does not necessarily mean that the model is able to reproduce the experimental data. Either the assumptions utilized for simulations and/or the extrapolation procedure utilized may not be entirely applicable under these conditions. A detailed study into the effect of radiation reabsorption on these flames could help shed light on this observed inconsistency. In any case, as mentioned in Sec. 3.2.2., comparing direct measurements with the corresponding simulations will avoid potential errors that may arise from extrapolation approaches [61]. However, this is not always feasible for fuels with complex kinetics and hence large kinetic models. Therefore, an accurate methodology is necessary to extract  $S_u^0$  from expansion rate measurements.

The measurements made (non-linear model) are also compared with existing measurements from the literature [12, 43, 52, 53, 57] in SM-G. It is observed that other measurements are consistently lower than our measurements. Even the measurements of Han et al. [43], which uses the heat-flux approach, claim

negligible effect of buoyancy-induced flows are consistently lower than our data ( $> 20\%$ ). Despite the decreased confidence in our data for  $\phi < 1$  (due to the inconsistency observed between Figs. 8 and 10), our measurements have carefully accounted for several aspects that introduce large errors in the derived  $S_u^0$ . Specifically, we have accounted for adsorption of  $\text{NH}_3$  on to the chamber walls, minimized buoyancy-induced flows using a drop tower, corrected for radiation-induced flows using the SRADIF model, and evaluated the correctness of the extrapolation-approaches using DNS. Therefore, these measurements of  $\text{NH}_3/\text{air}$   $S_u^0$ s are the most accurate to date.

## 5. Conclusions

In the present study, a combined experimental and computational methodology to investigate and accurately quantify the propagation rates of slow flames is presented. Slowly propagating flames are subject to gravity-induced convection and radiation heat loss, which if unaccounted for can result in incorrect interpretations of the data, and consequently large errors in measured laminar flame speeds ( $S_u^0$ s). A lab-scale drop tower is developed and utilized to mitigate buoyancy-induced flows, and measure expansion rates ( $dR_f/dt$ ) of slow spherically expanding flames in free fall. A computational model (SRADIF) that combines thermodynamic equilibrium and finite rate optically thin limit radiation heat loss calculations is used to estimate the radiation-induced inward flow. This inward flow velocity is subtracted from the measured  $dR_f/dt$  to obtain the flame speed relative to the burned gas ( $S_b$ ), from which  $S_u^0$  is derived. The methodology was applied first to a slowly propagating fuel-lean  $\text{CH}_4/\text{air}$  flame at 2 atm, and then to  $\text{NH}_3/\text{air}$  flames over a range of  $\phi$  ( $0.8 \leq \phi \leq 1.2$ ). Measurements were obtained both under static and free fall conditions to assess the errors that can arise when deriving flame speeds from natural-convection-distorted flames. The errors that can arise during the various steps of data interpretation (correction of radiation-induced flow, subtraction of stretch effects, etc.) were also analyzed. Listed below are the observations and conclusions made in this study.

1. To achieve intended  $\text{NH}_3/\text{air}$  mixture compositions, it was necessary to wait long durations ( $\sim 1$  hour) during mixture preparation to account for  $\text{NH}_3$  adsorption on stainless steel; similar observations were previously made and discussed by others [52, 59, 63].
2. The low-cost drop tower experiment with deviations of less than 2% from the acceleration due to the earth's gravity was able to successfully establish spherical slowly propagating flames with measured  $dR_f/dt$  as low as  $\sim 20$  cm/s, with a high degree of repeatability.
3. Interpreting data from buoyancy-distorted flames can result in significantly different  $dR_f/dt$  vs. stretch ( $K$ ) behavior. Specifically, if the maximum horizontal dimension of the flame (as used in many previous studies) is used as a surrogate for the diameter of the buoyant, non-spherical flame, the measured  $dR_f/dt$  is consistently higher than what is derived from free fall experiments. Utilizing these incorrect measurements can result in significant errors,  $\sim 40\%$  for the  $\phi = 0.8$   $\text{NH}_3/\text{air}$  case. This demonstrates the necessity of performing free fall experiments to accurately measure slowly propagating flame speeds.
4. Analysis revealed that radiation-induced flow velocities can be significant relative to  $dR_f/dt$  for slowly propagating flames and hence needs to be subtracted from  $dR_f/dt$  to obtain  $S_b$ . The SRADIF model, which utilizes an optically thin limit radiation heat loss model, was used to estimate the inward flow velocities.
5. A systematic approach of comparing direct measurements ( $dR_f/dt$ ) and derived quantities ( $S_b$  and  $S_u^0$ ) to the corresponding model predictions revealed the errors that result from the post-processing steps such as correcting for radiation-induced flow and subtraction of stretch effects using extrapolation approaches. The two errors are coupled; if there radiation-induced flow is not accounted for, there will be large extrapolation errors irrespective of the extrapolation model utilized. For example, linearly extrapolating the  $\phi = 0.8$   $\text{NH}_3/\text{air}$   $dR_f/dt$  values without subtracting

radiation-induced flow velocities result in a value of  $S_b^0$  about 20% lower than the value obtained post-correction (extrapolating  $S_b$  values). And, regarding errors that can arise from stretch correction, for  $\phi = 1.2$ ,  $S_b^0$  values obtained by linear and non-linear extrapolation of  $S_b$  values differ by 19%.

6. For the CH<sub>4</sub>/air case, the  $S_u^0$  measured using the abovementioned methodology showed significant differences (~16% greater) from previous measurements which did not include effects of buoyancy-induced flow and radiation heat loss. Furthermore, the data also differed from state-of-the-art model predictions by ~22%. CH<sub>4</sub> is the most studied fuel in combustion; however, our results indicate that there remain modeling issues, particularly at low flame temperatures where there is strong competition between the chain branching and chain termination reactions.
7. For  $\phi \geq 1.0$  NH<sub>3</sub>/air flames, consistency was observed when comparing direct measurements ( $dR_f/dt$ ) and derived  $S_u^0$  to corresponding model predictions. However, for  $\phi < 1.0$ , the difference between  $dR_f/dt$  and model predictions were greater than the difference between extracted  $S_u^0$  and model predictions. This inconsistency could mean that the extrapolation approach utilized and/or the assumptions utilized (particularly the optically thin limit model for radiation heat loss) are not entirely correct at these conditions. In any case, these results highlight the importance of comparing measurements to direct numerical simulations to assess the performance of a kinetic model.

Nevertheless, we report the most accurate measurements of NH<sub>3</sub>/air flame speeds to date by accounting for the various physics that affect these slowly propagating flames.

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